

# Pipelines Risk Assessment and LUP in HSE

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#### **HSE** involvement in LUP



- Extends back to the early 1970s
- Flixborough (1974) and Seveso (1976)
- Advisory Committee on Major Hazards
- Planning Legislation and HSE as a Statutory Consultee
- Advice given through PADHI





#### **HSE**

Notification of Installations Handling Hazardous Substances Regulations 1982

**COMAH** 

Pipeline Safety Regulations 1996

#### **LPAs**

Planning (Hazardous Substances) Act 1990

Planning (Hazardous Substances)
Regulations 1992

General Development Procedure Order 1995 (GDPO)

# Developments on Land Use Planning



#### **Current system**

- HSE's role is two fold but both advisory -
  - setting consultation distances
  - advising on proposed developments in vicinity of hazardous installations

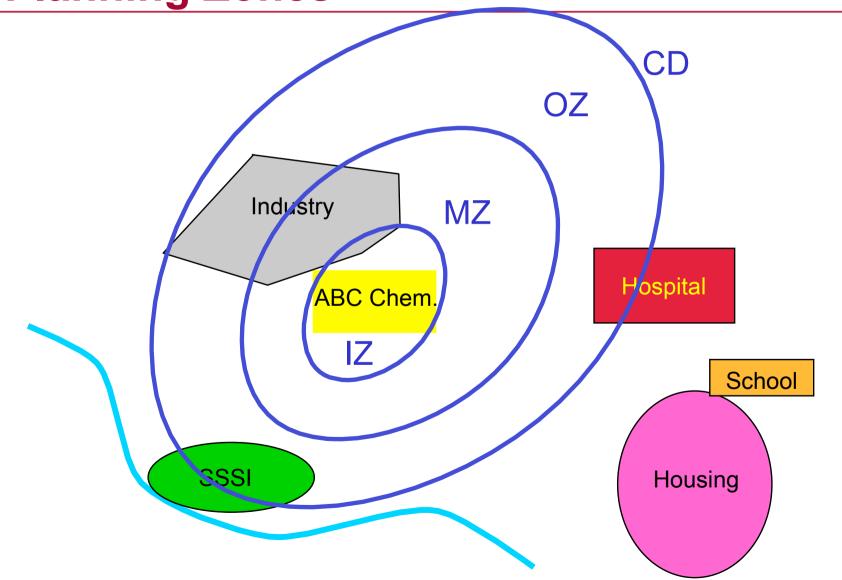




- Zones define areas of particular concern
- Consultation Zone is limit of HSE interest
- Within CD there are:
  - Inner Zone (10 cpm)
  - Middle Zone (1 cpm)
  - Outer Zone (0.3 cpm)
- Chances per million (cpm) per year of receiving a Dangerous Dose
- Consequence based zones (mainly for flammables)

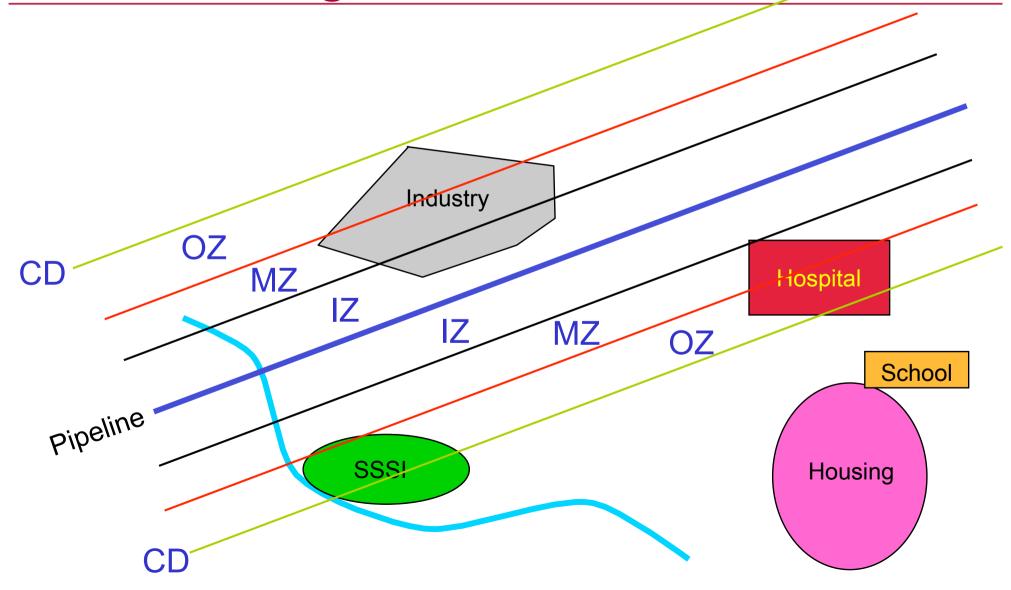


**Planning Zones** 





# **Planning Zones**





#### Societal risk – cross-Gov't work

- HSE LUP advice largely based on individual risk - cumulative affect of developments is not considered
- Population levels/density around sites can increase over time
- Cross-government Task Group
- Not a new concept



#### **Risk Assessment**

- Risk from steady state operation of pipeline
- (Not construction, etc.)



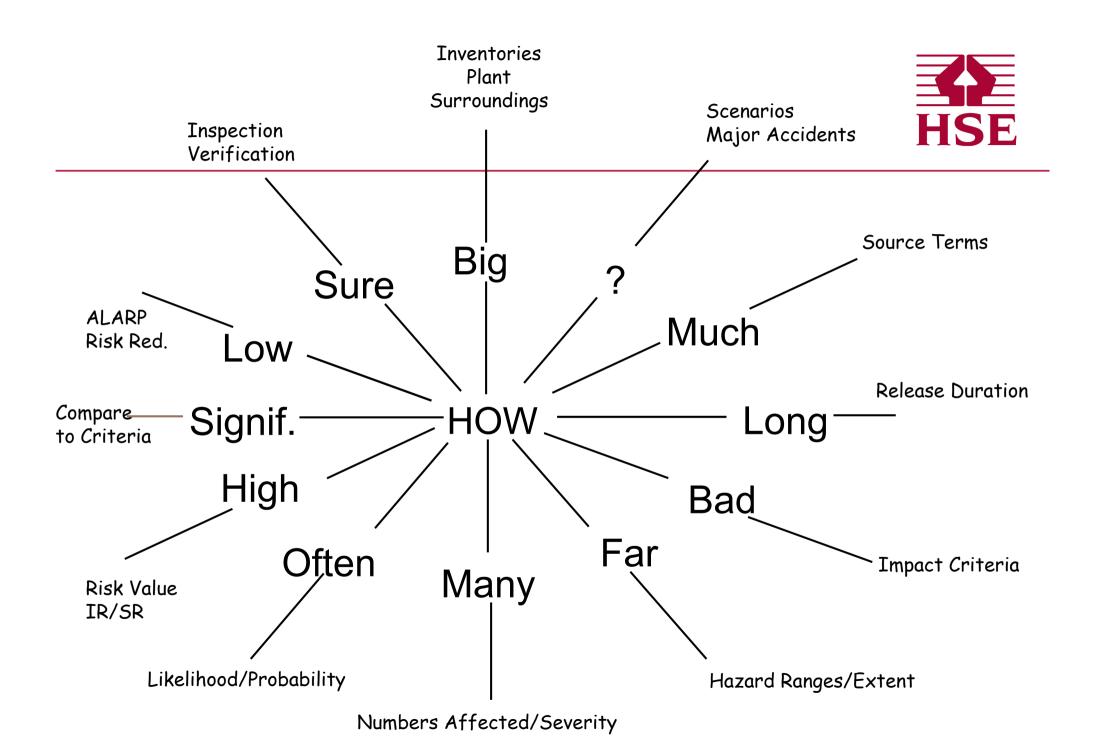
#### **Pipeline Risk Assessment Process**

Inputs to MISHAP

**Event likelihood** 

**Consequence calculations** 

**Risk outputs** 



# General inputs MISHAP01 Version A.8e - General Inputs (untitled)



Assessment description:				
Weather station: no st	ation	<u> </u>	-Substance d	etails
Atmos temperature (*K):	288		State:	
Humidity (%)	60		maile.	hane 💌
	Pipeline D	<u>etails</u>		
Pressure (bar g):	75	Теп	perature (*K):	278
Outer Diameter (mm):	914.4	Len	gth (km):	18
	(standard size)	Orie	ntation (*):	0
Wall thickness (mm);	12.7	Dep	oth (m):	0.9
Release size (mm)				
Release 1:	rupture			<u>0</u> K
Release 2 (Large):	110			<u>C</u> ancel
Release 3 (Small):	75			Help
Release 4 (Pin):	25			Tieth





- Third Party Activity
  - Predictive model
  - Based on structural reliability
  - Uses BG damage data
  - Validated and verified against operational data
  - Similar to model used by Advantica



### **Event likelihood –Failure frequency**

- Other failure modes
  - Mechanical, corrosion, natural causes and other
  - Previously based on EGIG data
  - Now based on UKOPA data
  - Main difference are in "mechanical" and "natural causes"



# Event likelihood –Failure frequency HSE

MISHAP01 - ExtFail Run (Test Run)					
General Inputs (Not Editable Here) Pipeline diameter (mm): 914.4 Pipeline depth (m): 0.9					
Specific Inputs (Not Editable Here)  Base failure frequency (events 2.728E-07 per year per m of pipeline):					
Results - Events per year per m of pipeline					
Release 1 (Rupture): 1.3e-8					
Release 2 (Large): 1.23e-9					
Release 3 (Small): 1.06e-8					
Release 4 (Pin): 1.41e-7 <u>C</u> ancel					
Pipeline Nominal Size  Welp  Help					
Value (mm): 914.4 Print Window					
☐ Pipeline slabbed ☐ Allow for depth of cover (Depth is less than 1m)					



# **Event likelihood –Event probability**

MISHAP01 - Event Tree Edit (Test Run)						
	Win	Specific Inputs dspeed probabi Weather station	lities from:	_		
	Immediate Ignition	Release Unobstructed 0.5	Delayed Local Ignition	Delayed Remote Ignition		
Windspeed 1 (night time)	Yes				FireBall + Jefire	
.2	No	Yes	Yes 0.25		Jetfire	
		No	No		No Ignition	
			Yes 0.25		_	
			No Ye	0.0	JetFire	
					FlashFire + JetFire	
Windspeed 2 (day time)			No	0	No Ignition	
	Yes				FireBall + Jefire	
	No	Yes	Yes 0.25		Jetfire	
<u>0</u> K			No		No Ignition	
		No	Yes 0.25		JetFire	
<u>C</u> ancel			No Ye	es 0.0		
Help			No.		FlashFire + JetFire	
					No Ignition	



# **Consequences – release rates**

MISHAP01 - LOSSP Release 1 Run (untitled)						
Substance Properties for methane						
Mol Wt (kg/kg mole):	16.04	1	Viscosity (Pa.s):	1.08	7e-5	
Critical Press (Pa):	4580000		Sp Heat (J/kg*K):	2197		
Critical Temp (*K):	190.4		Sp Heat Ratio:	1.31		
	LOSSP R	esults	:			
Initial Cor	ditions					
Mass in pipeline (kg)	Mass in pipeline (kg): 702294 Fireball mass (kg): 195091.1					
Release rate (kg/s):	17247.87	Fireba	ll duration (s):		20.7	
Compressibility:	0.839	Relea	se rate (kg/s) at	30 s:	4013.12	
■ Use substance specific A value for fireball calculations						
▼ Use FLAMCALC correlation for fireball duration						
Calculate release i	ate at:	1	<u>V</u> iew Results		<u>G</u> raph	
● 30 s.			OK		U-I-	
Other time			<u>0</u> K		<u>H</u> elp	
			<u>C</u> ancel	<u> </u>	rint Window	



#### Consequences – impact models

- Fireball FLAMCALC
- Jetfire PIPEFIRE
- Flashfire not used for natural gas
- Models have been compared to experimental and incident data (RR036, CRR294/2000)

# **Consequences – impact models**



MISHAP01 - FBALL Fireball 1 Run (Test Run)							
Fireball mass calculated by release model (te):	195.091						
Fireball mass for calculations (te): Fireball duration (s): Fireball radius (m): Distance to 500tdu (m): Distance to 1000 tdu (m): Distance to 1800 tdu (m): Distance to spontaneous ignition (m)	195.091 20.7 176.3 549.0 409.0 307.0 ): 229.0						
Restrict fireball mass to 300 te for calculations							
Restrict fireball duration to 30 s for calculation							
🗷 Use substance specific A valu	e for calculations						
■ Use FLAMCALC correlation for	fireball duration						
<u>View Results</u> <u>Print Window</u> <u>Graph</u>	<u>O</u> K <u>C</u> ancel <u>H</u> elp						

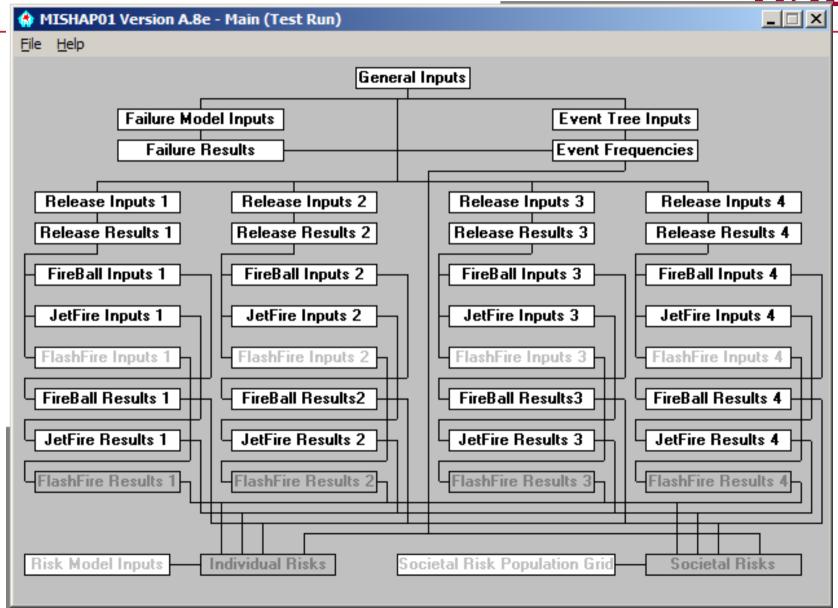




MISHAP01 - PIPEFIRE Je	tfire 1 Run (Test Run)
Surface emissivity (kW/r	m2): <b>256</b>
Flow Rate (kg/sl):	4.013E+3
	Flame Shape
Flame length (m):	710.082
Flame Width (m):	110.207
	PIPEFIRE Results
☐ Include Fireball	
Distance (m) to 500 tdu	461.0
Distance (m) to 1000 td	u: 289.0
Distance (m) to 1800 td	u: 183.0
Distance (m) to 25.6kw/	/m <sup>2</sup> : 189.0
Distance (m) to 14.7kw/	/m <sup>2</sup> : 312.0
<u>V</u> iew Results	<u>G</u> raph
<u>o</u> k	<u>H</u> elp
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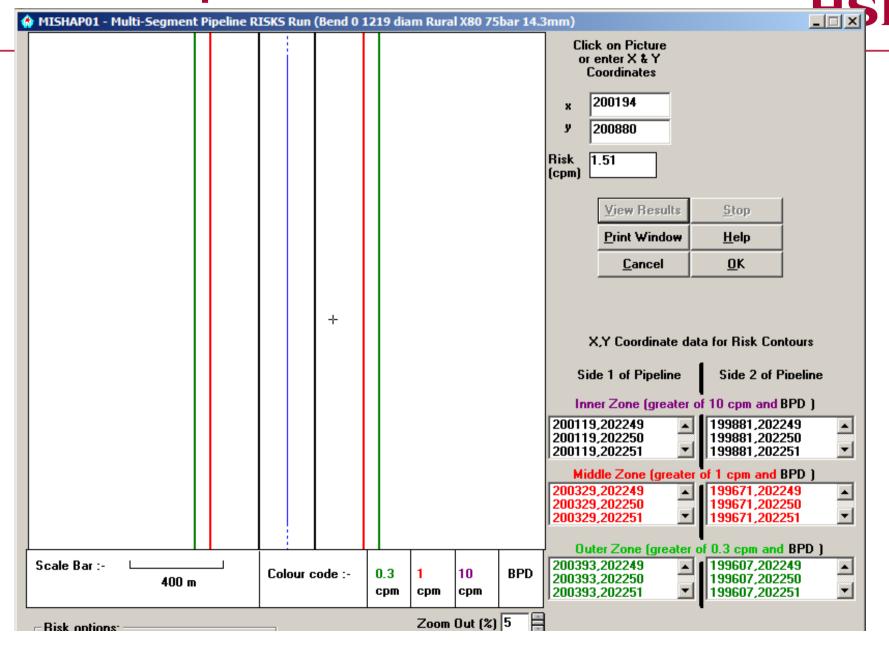




# Risk outputs – Individual Risk

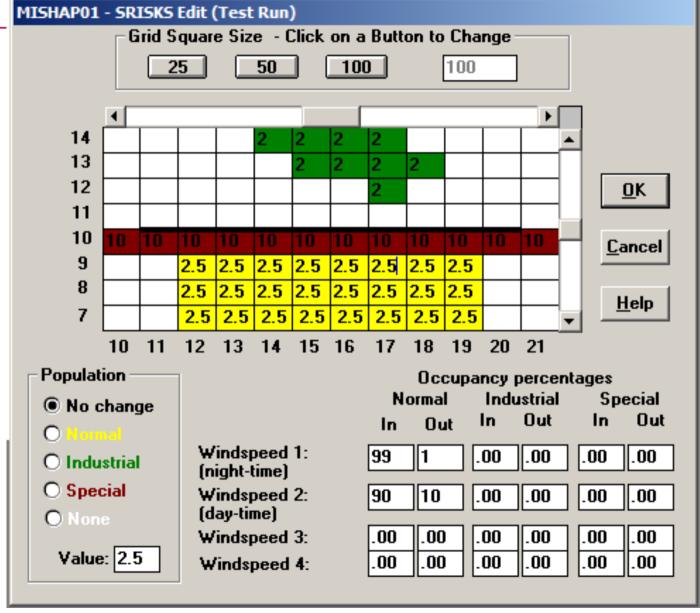
MISHAP01 - RISKS Run (Test Run)							
<u>Fi</u> le							
RISKS Results - Chances Per Million Per Year Windspeeds							
THOROTICS CHARGES	1	2	# iiiuspeet	4	Total		
Fireball followed by jetfire:	0.357	1.537	0.000	0.000	1.894		
Jetfire:	0.265	1.062	0.000	0.000			
Flashfire followed by jetfire:		0.000	0.000	-	1.327		
Total:				0.000	0.000		
rotui.	0.622	2.599	0.000	0.000	3.221		
Distances to Risks: 1e-5		1e-6	281	3e-7	290		
Calculate risks of:  Dangerous dose OP  Risk options:  Uniform Wind Rose O  Wind Always towards to  Target position relative to  East O West	Wind secto	Print \	Results Vindow aph IK	O Release 1	releases O Release 2 O Release 4		
No fireball dose for esca indoor occupants	ping	Н	elp	Add	Delete		

#### Risk outputs – Individual Risk











# Risk outputs – Societal Risk

MISHAP01 - SRISKS Run (Test Run)					
<u>F</u> ile					
Societal F	lisk				
No. of Casualties Frequency (yr-1)	No. of Casualties	Frequer	ncy (yr-1)		
n n or more		n	n or more		
>100000	201 - 501	U UUE +UU	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		
75001 - 100000 IN NNF+NN IN NNF+NN	101 - 201	U UUE +UU	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		
50001 - 75001 IN NNF+NN IN NNF+NN	76 - 101	U UUE +UU			
20001 - 50001 IN NNF+NN IN NNF+NN	51 - 76	U UUE +UU			
10001 - 20001 IN NNF+NN IN NNF+NN	21 - 51	U UUE +UU			
7501 - 10001   n nnF+nn   n nnF+nn	11 - 21 8 - 11	6 50F-07			
2001 - 7501   n nnF+nn   n nnF+nn   2001 - 5001   n nnF+nn   n nnF	8 - 11 5 - 8	2 45F-06			
2001 - 5001   n nnF+nn   n nnF+nn   n nnF+nn	2-5	1 01F-06			
751 - 1001   \( \text{n nnF+nn} \)   \( \text{n nnF+nn} \)	1	0 00E+00			
501 - 751	O	2 19F-07			
		Г			
Set calculation steps: 200 ▼ Nmax 12.16842 <u>View Results</u>					
Risk options:	F(Nmax) 2.0	60E-08	Graph		
○ <u>U</u> niform Wind Rose ● <u>W</u> ind sector	Risk Integral 1.	705.00	<u>u</u> rupii		
O Wind Always towards target	msk mægrar jj.	76E+UZ	<u>0</u> K		
Calculate risks of:		Uala	Canad		
O Dangerous dose  Probit Death <u>Help</u> <u>Cancel</u>					
▼ No fireball dose for escaping indoor occupants Print \					

#### Other substances



- Propane
- Ethylene
- Hydrogen
- Crude Oil
- Ethane
- VCM
- Gasoline (PIPERS)
- Ammonia (Toxic PRAM)

# **PADHI**



**Planning Advice for Developments** near Hazardous nstallations

#### Introduction



PADHI (Planning Advice for Developments near Hazardous Installations) is the name of the procedure used to give a response and advice on consultations involving land use planning proposals.

PADHI+ is the software used by Planning Authorities to generate the advice themselves.

Extranet contains maps of fixed site LUP zones and LUP distances for pipelines.

## Why PADHI?



- Use specialist resource for assessing Seveso reports
- Fundamental review of HSE role in land use planning
  - Recommended advice codified and an IT tool provided to planners to generate HSE advice themselves.



### **PADHI - Basic System**

#### 2 inputs to decision matrix:

- Where the development is
- What it is

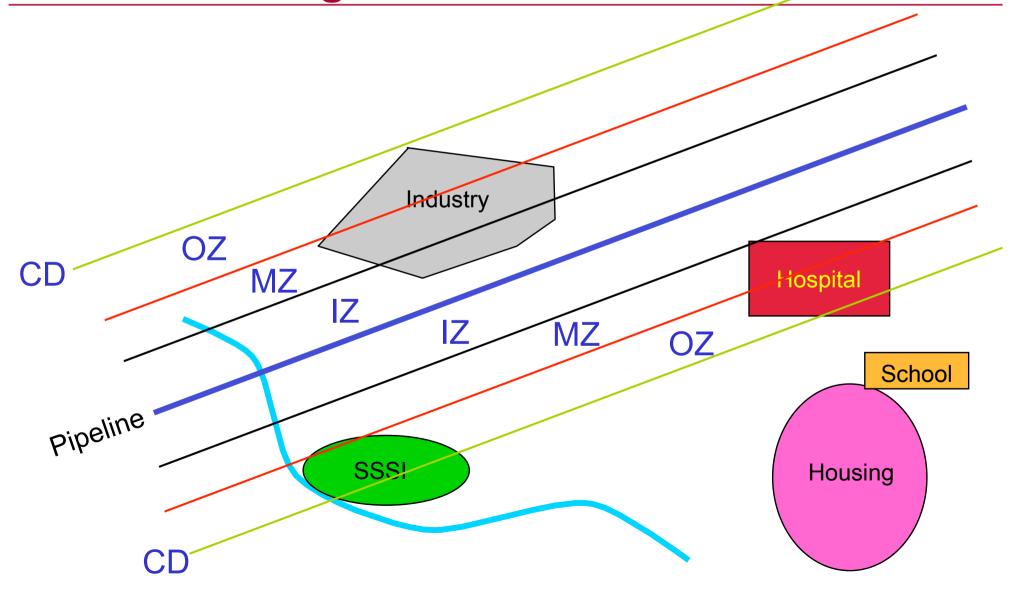
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#### Generate either:

- 'Advise Against' (AA)
- 'Don't Advise Against' (DAA)



# **Planning Zones**





#### **Sensitivity Levels**

- SL 1 people at work, parking
- SL 2 use by the general public
- SL 3 use by vulnerable people
- SL 4 very large and sensitive developments

www.hse.gov.uk/landuseplanning

#### **Decision Matrix**



Sensitivity Level	Development in Inner Zone	Development in <b>M</b> iddle <b>Z</b> one	Development in Outer Zone
1	DAA	DAA	DAA
2	AA	DAA	DAA
3	AA	AA	DAA
4	AA	AA	AA

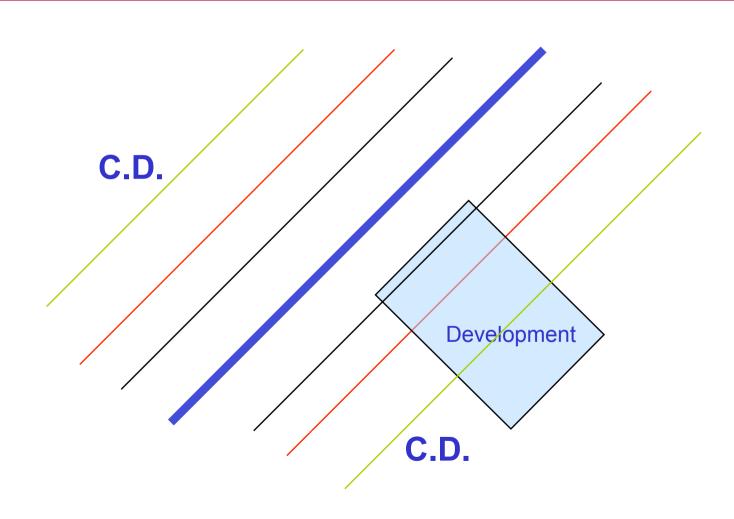
#### Rules



- Rules for:
  - Zone boundaries being straddled
  - More than one hazard
  - -More than one land use
  - Extension to existing development facility



# 'Straddling'





### 'Multiple major hazards'

- More than 1 installation or pipeline
  - Must consider all
  - PADHI decision for each
  - Any AA decision dominates

#### **Second Bite Cases**



