

**Recommendations on Transmission
and Distribution Practice
IGEM/TD/1 Edition 5
Communication XXXX**

**Founded 1863
Royal Charter 1929
Patron
Her Majesty the Queen**

STEEL PIPELINES AND ASSOCIATED INSTALLATIONS FOR HIGH PRESSURE GAS TRANSMISSION

DRAFT FOR COMMENT

1. This draft Standard has been written by the Institution of Gas Engineers and Managers' Panel on IGEM/TD/1, chaired by Jane Haswell and appointed by the Gas Transmission and Distribution Committee.
2. This Draft for Comment is presented to industry for comment in accordance with the standard comment form. Comments should be submitted using the attached Reply Form, by Friday 9th May 2008.
3. This is a draft document which should not be regarded or used as a fully approved and published Standard. It is anticipated that amendments will be made following industry comments and prior to publication.
4. This is a copyright document of the Institution of Gas Engineers and Managers and should not be copied without permission. Enquiries should be addressed in the first instance to Ian Smith:

IGEM
Charnwood Wing
Holywell Park
Ashby Road
Loughborough
Leicestershire LE11 3GH
Tel: 01509 282728
Fax: 01509 283193
Email: ian@igem.org.uk

Organisations to which Draft has been circulated:

- Association of Independent Gas Transporters (AIGT)
- Association of Meter Operators (AMO)
- British Standards Institute (BSI)
- CORGI
- Energy Institute
- Gas Forum
- Gas Industry Registration Scheme (GIRS)
- Gas Industry Safety Group (GISG)
- Health and Safety Executive (HSE)
- National Grid Gas
- National Grid Transmission
- Northern Gas Networks
- Office of Gas and Electricity Markets (Ofgem)
- Phoenix Natural Gas
- Pipeline Industries Guild (PIG)
- Society of British Gas Industries (SBGI)
- Scotia Gas Networks
- United Kingdom Onshore Operators Association (UKOOA)
- Wales and West Utilities.

- IGEM:
 - Council
 - Young Persons Network (YPN)
 - Technical Coordinating Committee (TCC)
 - Gas Measurement Committee (GMC)
 - Gas Transmission and Distribution Committee (GTDC)
 - Gas Safety and Environment Committee (GSEC)
 - Gas Utilization Committee (GUC)
 - Liquefied Natural Gas Committee (LNGC)
 - PTD/1
 - PTD/13
 - PSR/16.

***IGEM/TD/1 Edition 5
Communication XXXX***

***Steel pipelines and associated
installations for high pressure gas
transmission***

Draft for Comment



*Founded 1863
Royal Charter 1929
Patron: Her Majesty the Queen*



***IGEM/TD/1 Edition 5
Communication XXXX***

***Steel pipelines and associated
installations for high pressure gas
transmission***

Draft for Comment

Price Code:
© The Institution of Gas Engineers and Managers
Charnwood Wing
Holywell Park
Ashby Road
Loughborough, Leics, LE11 3GH
Tel: 01509 282728
Fax: 01509 283110
Email: general@igem.org.uk



CONTENTS

SECTION	PAGE	
1	Introduction	1
2	Scope	4
3	Competency, quality assurance and integrity and safety management of pipelines and associated installations.	6
	• 3.1 Competency	6
	• 3.2 Quality assurance and quality control	6
	• 3.3 Safety and integrity of pipelines and associated installations	6
	• 3.4 Pipeline integrity management	9
	• 3.4.1 Process	9
	• 3.4.2 System	10
4	Planning and legal considerations for pipelines and associated installations	11
	• 4.1 Planning	11
	• 4.1.1 General	11
	• 4.1.2 Route selection	11
	• 4.1.3 Land rights/easement details	15
	• 4.1.4 Construction plans	16
	• 4.2 Legal considerations	17
	• 4.2.1 General	17
	• 4.2.2 Legal considerations in the UK	20
5	Materials for pipelines	26
	• 5.1 Standards	26
	• 5.2 Operating and design temperatures	26
	• 5.3 Linepipe	26
	• 5.3.1 Specification	26
	• 5.3.2 Methods of pipe manufacture	27
	• 5.3.3 Strength grades	27
	• 5.3.4 Testing	28
	• 5.3.5 Weldability	28
	• 5.4 Fatigue	29
	• 5.5 Fittings	29
	• 5.5.1 General	29
	• 5.5.2 Bends, tees and headers	29
	• 5.5.3 Impulse piping and fittings	31
	• 5.5.4 Other fittings	31
	• 5.6 Component selection	31
	• 5.6.1 General	31
	• 5.6.2 Insulating joints	31
	• 5.6.3 Pressure vessels	32
	• 5.6.4 Valves and actuators	32
	• 5.7 Factory-applied coatings	33
6	Design of pipelines	34
	• 6.1 Gas pressure and quality	34
	• 6.1.1 Control of gas pressure	34
	• 6.1.2 Gas quality	34
	• 6.2 Design velocity	34
	• 6.3 Sizing of linepipe	34

● 6.4	Wall thickness of linepipe	35
● 6.5	Additional loads	35
● 6.5.1	Classification of loads	35
● 6.5.2	Calculation of stresses	36
● 6.5.3	Acceptance criteria	36
● 6.6	Fatigue	37
● 6.6.1	General	37
● 6.6.2	Definition of fatigue life	37
● 6.6.3	Definition of stress cycles	39
● 6.6.4	Revalidation	39
● 6.7	Area types and design criteria	39
● 6.7.1	Area types	39
● 6.7.2	Estimation of population density	40
● 6.7.3	Boundaries	40
● 6.7.4	Design of pipelines in Type R areas	40
● 6.7.5	Design of pipelines in Type S areas	41
● 6.7.6	Design of pipelines in Type T areas	42
● 6.7.7	Proximity from wind turbines	42
● 6.7.8	Deviation from prescribed proximity criteria	42
● 6.7.9	Sensitive locations	42
● 6.7.10	Seismic activity	42
● 6.8	Risk analysis	45
● 6.9	Impact protection against 3 rd party interference	45
● 6.10	Traffic routes (including roads and railways)	46
● 6.10.1	Pipelines crossing/encroaching within traffic routes	46
● 6.10.2	Pipelines running parallel to other traffic routes	47
● 6.10.3	Water course crossings	47
● 6.11	Pipelines running parallel to other major pipelines	48
● 6.12	Sleeving	49
● 6.12.1	General	49
● 6.12.2	Selection of a sleeving system	49
● 6.12.3	Materials and standards	49
● 6.12.4	Sleeve diameter	49
● 6.12.5	Sleeve length	50
● 6.12.6	Carrier pipe support	50
● 6.12.7	End-seals	50
● 6.12.8	Attachments	50
● 6.12.9	Drain points	51
● 6.12.10	Annular filling	51
● 6.13	Valves	52
● 6.14	Pigging	53
● 6.15	Overhead pipe crossings	55
● 6.16	Design records	56
7	Construction of pipelines	57
● 7.1	General	57
● 7.2	Administration	57
● 7.2.1	Communications	57
● 7.2.2	Supervision	57
● 7.2.3	Construction records	57
● 7.3	Safety	58
● 7.3.1	General	58
● 7.3.2	Safety training	58
● 7.4	Environment	58

	• 7.4.1	General	58
	• 7.4.2	Noise abatement	58
	• 7.4.3	Water	59
	• 7.4.4	Traffic	59
• 7.5		Receiving materials	59
• 7.6		Entry onto land and setting out	59
• 7.7		Working width and fencing	59
• 7.8		Surveying for bends	60
• 7.9		Pipe stringing	60
• 7.10		Field bending	61
• 7.11		Lining-up for welding	61
• 7.12		Welding	61
	• 7.12.1	General	61
	• 7.12.2	Non-destructive testing (NDT)	62
	• 7.12.3	Stress relief	62
• 7.13		Night caps	62
• 7.14		Joint coating	62
• 7.15		Trench excavation	62
• 7.16		Inspection of coating	63
• 7.17		Lowering pipe into a trench	63
• 7.18		Bedding and covering pipe	63
• 7.19		Backfilling	64
• 7.20		Crossings	64
	• 7.20.1	General	64
	• 7.20.2	Road and rail crossings	64
	• 7.20.3	Water crossings, including drainage ditches	65
• 7.21		Sleeved and tunnel crossings	65
	• 7.21.1	Sleeves-general	65
	• 7.21.2	Concrete and alternative materials for sleeves	66
	• 7.21.3	Steel sleeves	66
	• 7.21.4	Pipe spacers for sleeves	66
	• 7.21.5	Annular filling of sleeves	66
• 7.22		Foundations	67
• 7.23		Reinstatement	67
• 7.24		Pigging	68
• 7.25		Marker posts	68
• 7.26		Testing	68
• 7.27		Tie-ins after testing	68
• 7.28		Post-construction coating survey	69
• 7.29		Cathodic protection (CP)	69
• 7.30		Commissioning	69
8		Testing of pipelines and installations	70
• 8.1		Planning/preliminary requirements	70
• 8.2		Hydrostatic testing	71
	• 8.2.1	Preparation for testing	71
	• 8.2.2	Testing of pipelines	71
	• 8.2.3	Testing of installations	72
	• 8.2.4	Test limits	73
• 8.3		Pre-testing	73

• 8.4	Test equipment	73
• 8.4.1	Instrumentation	73
• 8.4.2	Measurement of pressure	73
• 8.4.3	Measurement of volume	74
• 8.4.4	Measurement of temperature	74
• 8.4.5	Test ends	74
• 8.5	Acceptance criteria	74
• 8.5.1	Air content	74
• 8.5.2	Temperature variations	75
• 8.5.3	Test acceptance	75
• 8.6	Safety – general	75
• 8.7	Safety – pipelines and installations	76
• 8.8	Safety – small bore pipework (pneumatic testing)	77
• 8.9	Test sections	78
• 8.9.1	Pipelines and installations	78
• 8.9.2	Pre-testing of pipes, fittings and fabrications	79
• 8.10	Fitting of test ends	79
• 8.11	Water supply	80
• 8.12	Repair of test failures and leaks	80
• 8.13	Recording and documentation	81
• 8.13.1	General	81
• 8.13.2	Test equipment and instruments	81
• 8.13.3	Test record	82
• 8.13.4	Test certificate	82
9	Commissioning of pipelines	85
• 9.1	General	85
• 9.2	Preliminary arrangements	86
• 9.2.1	Planning	86
• 9.2.2	Safety and welfare	86
• 9.2.3	Attachments	87
• 9.2.4	Access to launch and reception sites	87
• 9.2.5	Site security	87
• 9.2.6	Lighting at terminals, etc	88
• 9.2.7	Monitoring of pigs	88
• 9.2.8	Pre-commissioning inspections	88
• 9.3	Preliminary pigging	88
• 9.4	Drying, purging and gassing up	88
• 9.4.1	Super-dry air/nitrogen followed by gas	89
• 9.4.2	Vacuum drying followed by purging and gassing up	90
• 9.5	Pressurising	92
• 9.5.1	Preliminary works	92
• 9.5.2	Pressurisation	93
10	Protection against corrosion	94
• 10.1	General	94
• 10.2	Special situations	94
• 10.2.1	Avoidance of known corrosion hazards	94
• 10.2.2	Pipelines operating of elevated temperatures	94
• 10.2.3	Stress corrosion cracking	94
• 10.3	Coatings	95
• 10.3.1	Internal pipe coatings	95
• 10.3.2	External pipe coatings	95
• 10.3.3	Coating of other below-ground components	96

	• 10.4	Cathodic protection	96
	• 10.4.1	General	96
	• 10.4.2	AC corrosion	97
	• 10.4.3	Mitigation measures	97
	• 10.5	Records	97
11		Operation and maintenance	98
	• 11.1	General	98
	• 11.2	Management	98
	• 11.2.1	Administration	98
	• 11.2.2	Legal and allied considerations	98
	• 11.2.3	Safety management	98
	• 11.2.4	Surveillance, inspection and maintenance frequencies	101
	• 11.3	Pipeline records	102
	• 11.3.1	General	102
	• 11.3.2	Fixed data	102
	• 11.3.3	Surveillance	103
	• 11.3.4	Inspection	103
	• 11.3.5	Maintenance	103
	• 11.3.6	Operation	103
	• 11.4	Operational pressure limits	104
	• 11.4.1	MOP	104
	• 11.4.2	Affirmation of MOP	104
	• 11.4.3	Overpressure	105
	• 11.4.4	Restoration of MOP to a previously declared level, up to the original design pressure	108
	• 11.4.5	Uprating the MOP on a pipeline to a level above the previous design pressure	111
	• 11.5	Reassessment of pipeline design life	114
	• 11.6	Surveillance	114
	• 11.6.1	General	114
	• 11.6.2	Long range ultrasonics	115
	• 11.6.3	Aerial survey	116
	• 11.6.4	Vantage point survey	117
	• 11.6.5	Full walking survey	117
	• 11.6.6	Leakage survey	118
	• 11.6.7	Monitoring of third party activities	118
	• 11.6.8	Ground movement	119
	• 11.7	Inspection	120
	• 11.7.1	Exposed crossings	120
	• 11.7.2	Water course crossings	120
	• 11.7.3	Condition monitoring	123
	• 11.7.4	Inspection and maintenance frequencies	127
	• 11.7.5	Corrosion control	128
	• 11.8	Maintenance	130
	• 11.8.1	Pipelines	131
	• 11.8.2	Installations	131
	• 11.8.3	Valves	132
	• 11.8.4	Valve actuators	133
	• 11.8.5	Remotely operated valves and pipeline protection devices	133
	• 11.8.6	Pig traps	133
	• 11.8.7	Land and buildings	133
	• 11.9	Non-routine activities	134
	• 11.9.1	Pipeline isolation	134

	• 11.9.2	Decommissioning and recommissioning	135
	• 11.9.3	In-line pigging	135
	• 11.9.4	Pipeline damage and repair	136
	• 11.9.5	Under-pressure connections, hot taps and stoppling	137
	• 11.9.6	Permanent decommissioning of pipelines or sections of pipelines	139
12		Installations associated with pipelines	141
	• 12.1	General	141
	• 12.2	Site selection	141
	• 12.2.1	General	141
	• 12.2.2	Installations located on consumers' premises	142
	• 12.3	Layout of site, site security and housing and buildings	142
	• 12.3.1	General	142
	• 12.3.2	Layout of the site	142
	• 12.3.3	Site security	143
	• 12.3.4	Housings and buildings	143
	• 12.4	General design	144
	• 12.5	Pipework design	145
	• 12.6	Stress analysis	146
	• 12.6.1	General	146
	• 12.6.2	Supports	146
	• 12.7	Pipe and fittings	147
	• 12.8	Protection against external corrosion (other than CP)	149
	• 12.9	Valves	149
	• 12.10	Relief valves, slam-shut valves and thermowells	150
	• 12.10.1	Relief valves, vents and drains	150
	• 12.10.2	Thermowells	150
	• 12.10.3	Slam-shut valves (SSVs)	150
	• 12.11	Vibration and acoustic fatigue	151
	• 12.12	Electrical equipment	151
	• 12.12.1	General	151
	• 12.12.2	Hazardous areas	151
	• 12.12.3	Electrical isolation	152
	• 12.13	Lightning, earthing and lighting	152
	• 12.13.1	Lightning	152
	• 12.13.2	Earthing	152
	• 12.13.3	Lighting	153
	• 12.14	Instrumentation and telemetry	153
	• 12.15	Testing	153
	• 12.16	Metering	153
	• 12.17	Maintenance	153

APPENDIX

1	Glossary, acronyms, abbreviations, units and symbols	155
2	References	160
3	Risk assessment techniques	167
4	Structural reliability assessments (SRAs)	178
5	Pressure testing procedures	182
6	Testing – water filling and emptying procedures	212
7	On-line pigging operations	214
8	Water course crossing survey techniques	222

FIGURE

1	Scope of IGEN/TD/1 Edition 5	5
2	Pipeline safety and integrity network	8
3	Relationship between stress range and number of cycles	38
4	Minimum proximity distance from normally-occupied buildings of pipelines designed to operate in Type R areas	43
5	Minimum proximity distance from normally-occupied buildings of pipelines designed to operate in Type S areas	44
6	Commonly used forms of impact protection for pipelines	46
7	Typical pig trap installation	55
8	Measurement of air content	75
9	Example of a pressure testing certificate	83
10	MOP excursions	106
11	Decision algorithm for establishing operating status of a pipeline	109
12	Decision algorithm for uprating MOP of a pipeline	110
13	Overview of uprating procedure	112
14	Reassessment of pipeline design life	114
15	Typical arrangement of a double stopple with by-pass	140
16	Estimation of individual and societal risk	173
17	Societal risk	174
18	Tolerability of risk	175
19	Sample FN criterion (based on extensive application of previous editions of IGEN/TD/1)	176

20	Individual risk transect	177
21	Pneumatic testing of small bore pipework – typical test rig arrangement	189
22	Typical temperature/pressure correlation for pure water in steel pipe	211
23	Typical arrangement of pipework at a pig reception	221

TABLE

1	Types of plan used in planning pipelines /associated installations (typical example of plans used within the UK)	17
2	Methods of pipe manufacture	27
3	Commonly used material grades, SMYS and SMTS	28
4	Least nominal wall thickness of linepipe	35
5	Maximum interaction distance for parallel Natural Gas pipelines. MOP \leq 80 bar	48
6	Least nominal wall thickness of steel sleeves	50
7	Limiting pressure differentials for carrier pipe	51
8	Hydrostatic test conditions for systems designed to operate at a design factor not exceeding 0.3	72
9	Hydrostatic test conditions for systems designed to operate at a design factor exceeding 0.3	72
10	Surveillance, inspection, maintenance and non-routine activities	116
11	Frequency of water course crossing surveys where risk assessment is not carried out in accordance with clause 11.7.2.2	121
12	Frequency of condition monitoring where risk assessment is not carried out in accordance with clause 11.7.3.4	123
13	Selection of maximum design factor (f) for installations	145
14	Limitations on the selection and use of fittings	149
15	Temperature/pressure corrections OD = 60.3 mm	190
16	Temperature/pressure corrections OD = 88.9 mm	191
17	Temperature/pressure corrections OD = 114.3 mm	192
18	Temperature/pressure corrections OD = 168.3 mm	193
19	Temperature/pressure corrections OD = 219.1 mm	194
20	Temperature/pressure corrections OD = 273.0 mm	195
21	Temperature/pressure corrections OD = 323.8 mm	196
22	Temperature/pressure corrections OD = 355.6 mm	198

23	Temperature/pressure corrections OD = 406.4 mm	199
24	Temperature/pressure corrections OD = 457.2 mm	200
25	Temperature/pressure corrections OD = 508.0 mm	202
26	Temperature/pressure corrections OD = 609.6 mm	203
27	Temperature/pressure corrections OD = 762.0 mm	205
28	Temperature/pressure corrections OD = 914.4 mm	206
29	Temperature/pressure corrections OD = 1066.8 mm	207
30	Temperature/pressure corrections OD = 1219.2 mm	208
31	Underwater survey methods	223

SECTION 1 : INTRODUCTION

1.1 Recommendations on the installation of steel pipelines for high pressure gas transmission were first published by the Institution of Gas Engineers in 1965, as Communication 674.

Recommendations, superseding Communication 674, were published progressively between 1970 and 1977 and consolidated in IGE/TD/1 Edition 1, issued as Communication 674 ABCD.

Later in 1977, the then Section 5, Design, was further revised and issued as Edition 2, Communication 1017.

A further revision, IGE/TD/1 Complete Edition 2, was published in 1984 as Communication 1234, extending the maximum permissible design pressure from 70 bar to 100 bar.

A further revision, IGE/TD/1 Edition 3, was published in 1993. This introduced guidance for risk analysis and provided more comprehensive guidance for testing, commissioning and condition monitoring.

Three Supplements to IGE/TD/1 Edition 3 were published in 1999 and 2000 on handling, transport and storage of steel pipe, bends and fittings (Supplement 1), 1219.2 mm (48 inch) pipelines (Supplement 2) and uprating the design factor to 0.8 (Supplement 3).

Supplements 2 and 3 to Edition 3 were included in IGE/TD/1 Edition 4 whereas Supplement 1 became a supplement to Edition 4.

Supplement 1 to IGE/TD/1 Edition 4 is now a Supplement 1 to IGEM/TD/1 Edition 5.

A new supplement to Edition 4 was published in 2008, on land use planning (LUP). This remains current and is now Supplement 2 to IGEM/TD/1 Edition 5.

1.2 IGEM/TD/1 Edition 5 has been drafted by a Panel appointed by the Institution of Gas Engineers and Managers (IGEM's) Gas Transmission and Distribution Committee, subsequently approved by that Committee and published by the authority of the Council of IGEM.

1.3 This Standard applies to the design, construction, inspection, testing, operation and maintenance of pipelines and associated installations designed after the date of publication. Hence, all new pipelines, associated installations and diversions, as well as modifications of existing pipelines and associated installations, should be in accordance with this Edition.

Existing pipelines and associated installations that comply with IGE/TD/1 Editions 1, 2, 3 or 4 may continue to be operated in accordance with the respective Edition, although surveillance, inspection and maintenance may be undertaken in accordance with Edition 5. Operating conditions are not allowed to pass outside the limits of Edition 1, 2, 3 or 4 as appropriate, unless the new conditions are consistent with Edition 5.

Note: In this respect, Section 12 describes what constitutes "installations" and it is important to note that pressure regulating installations (PRIs) are not included. For existing PRIs, reference will need to be made to IGE/TD/9 (obsolete) or IGE/TD/13. In addition, "associated installations" i.e. other than PRIs, were not addressed by IGE/TD/1 Editions 1,2,3 or 4 and reference will be needed to IGE/TD/9 (obsolete) in this respect.

IGEM/TD/1 Edition 5 can be used to provide detailed requirements to support BS EN 1594.

- 1.4 Significant amendments have been made to this edition. These include:
- removal of the upper limit to maximum operating pressure (MOP) (formerly limited to 100 bar)
 - inclusion of advice on the relevant safety evaluation for MOP exceeding 100 bar
 - addition of requirements for associated installations (other than PRIs)
 - removal of requirements for methanol swabbing
 - guidance on alternating current (AC) corrosion and application of new technology associated with corrosion protection
 - inclusion of equations for proximity curves
 - an alternative approach for reaffirmation of MOP, avoiding the requirement for pressure raising in all circumstances
 - the updating of numerous references to legislation and standards.

- 1.5 Engineering requirements are set out for the safe design, construction inspection, testing, operation and maintenance of pipelines and associated installations, in accordance with current knowledge.

This Standard is intended to protect from possible hazards members of the public and those who work with pipelines etc. as well as the environment, so far as is reasonably practicable. It is also intended to ensure that the security of gas supply is maintained.

- 1.6 This Standard is applicable to conditions normally encountered in the transmission of gas. Additional design considerations may be necessary where unusual conditions are encountered, for example unstable ground (including the possibility of mining subsidence), mechanical or sonic vibrations, long self-supported spans, massive special attachments or thermal forces other than seasonal.

Note: Some guidance on dealing with subsidence is provided in Section 6.

- 1.7 This Standard makes use of the terms "should", "shall" and "must" when describing particular procedures. Notwithstanding Sub-Section 1.9:
- the term "must" identifies a requirement by law in Great Britain (GB) at the time of publication
 - the term "shall" prescribes a procedure which, it is intended, will be complied with in full and without deviation
 - the term "should" prescribes a procedure which, it is intended, will be complied with unless, after prior consideration, deviation is considered to be acceptable

Such terms may have different meanings when used in legislation, or Health and Safety Executive (HSE) Approved Codes of Practice (ACoPs) or guidance, and reference needs to be made to such statutory legislation or official guidance for information on legal obligations.

- 1.8 It is now widely accepted that the majority of accidents in industry generally are in some measure attributable to human as well as technical factors in the sense that actions by people initiated or contributed to the accidents, or people might have acted better to avert them.

It is therefore necessary to give proper consideration to the management of these human factors and the control of risk. To assist in this, it is recommended that due cognisance be taken of HS(G)48.

The primary responsibility for compliance with legal duties rests with the employer. The fact that certain employees, for example “responsible engineers”, are allowed to exercise their professional judgement does not allow employers to abrogate their primary responsibilities. Employers must:

- have done everything to ensure, so far as is reasonably practicable, that there are no better protective measures that can be taken other than relying on the exercise of professional judgement by “responsible engineers”
- have done everything to ensure, so far as is reasonably practicable, that “responsible engineers” have the skills, training, experience and personal qualities necessary for the proper exercise of professional judgement
- have systems and procedures in place to ensure that the exercise of professional judgement by “responsible engineers” is subject to appropriate monitoring and review
- not require “responsible engineers” to undertake tasks which would necessitate the exercise of professional judgement that is beyond their competence. There should be written procedures defining the extent to which “responsible engineers” can exercise their judgement. When “responsible engineers” are asked to undertake tasks that deviate from this, they should refer the matter for higher review.

Note: The responsible engineer is a suitably qualified, competent and experienced engineer appointed to be responsible for the execution and for approval of activities associated with the design, construction, operation and maintenance of a pipeline, pipelines and associated installations.

1.9 This Standard does attempt to make the use of any method or specification obligatory against the judgement of the responsible engineer. Where new and better techniques are developed and proved, they should be adopted without waiting for modification to this Standard. Amendments to this Standard will be issued when necessary and their publication will be announced in the Journal of IGEM and other publications as appropriate.

1.10 Requests for interpretation of this Standard in relation to matters within its scope, but not precisely covered by the current text, should be addressed to Technical Services, IGEM, Charnwood Wing, Holywell Park, Ashby Road, Loughborough, Leicestershire, LE11 3GH and will be submitted to the relevant Committee for consideration and advice, but in the context that the final responsibility is that of the engineer concerned. If any advice is given by, or on behalf of, IGEM, this does not relieve the responsible engineer of any of his or her obligations.

1.11 This Standard was published on

SECTION 2 : SCOPE

- 2.1 This Standard covers the design, construction, inspection, testing, operation and maintenance of steel pipelines and associated installations (see Figure 1), for the transmission of dry Natural Gas (predominantly methane), with or without odourisation, at a maximum operating pressure (MOP) exceeding 16 bar. Specific guidance is included for MOP not exceeding 100 bar. For MOP exceeding 100 bar, specific areas will require further justification and documentation, which embrace a safety evaluation.

Note 1: Requirements for steel pipelines for MOP not exceeding 16 bar is contained in IGE/TD/3, and on steel services in IGE/TD/4. These Standards do not address associated installations so reference may also be needed to IGE/TD/13 whose principles may be applied.

Note 2: The term "associated installation" does not include PRIs which are addressed by IGE/TD/13.

While the Standard may be appropriate for use with other gases, the characteristics of the gas and the consequential effect upon design, material, operations and maintenance of the pipeline have to be taken into account. In this context, other gases are those described by 1st family, other 2nd family and 3rd family gases as defined in BS EN 437.

Note: Offshore pipelines are those that are on the seaward side of the low water mark or special boundaries drawn at bays and estuaries.

- 2.2 This Standard covers operating temperatures between -25°C and +60°C inclusive.

- 2.3 This Standard applies to pipelines laid between points on land, including water crossings. For pipelines of which any part is offshore, additional or alternative guidance may be required for the offshore section. However, many of these requirements will remain valid.

The Standard equally applies to pipework design on associated installations including block valves, pig traps, overground crossings, manifolds, multi-junctions, the main connection pipework up to and from the machine trains on compressor stations etc. but does not apply for PRIs (when IGE/TD/13 applies).

Note: This Standard is not intended to cover detailed planning and siting requirements for these installations.

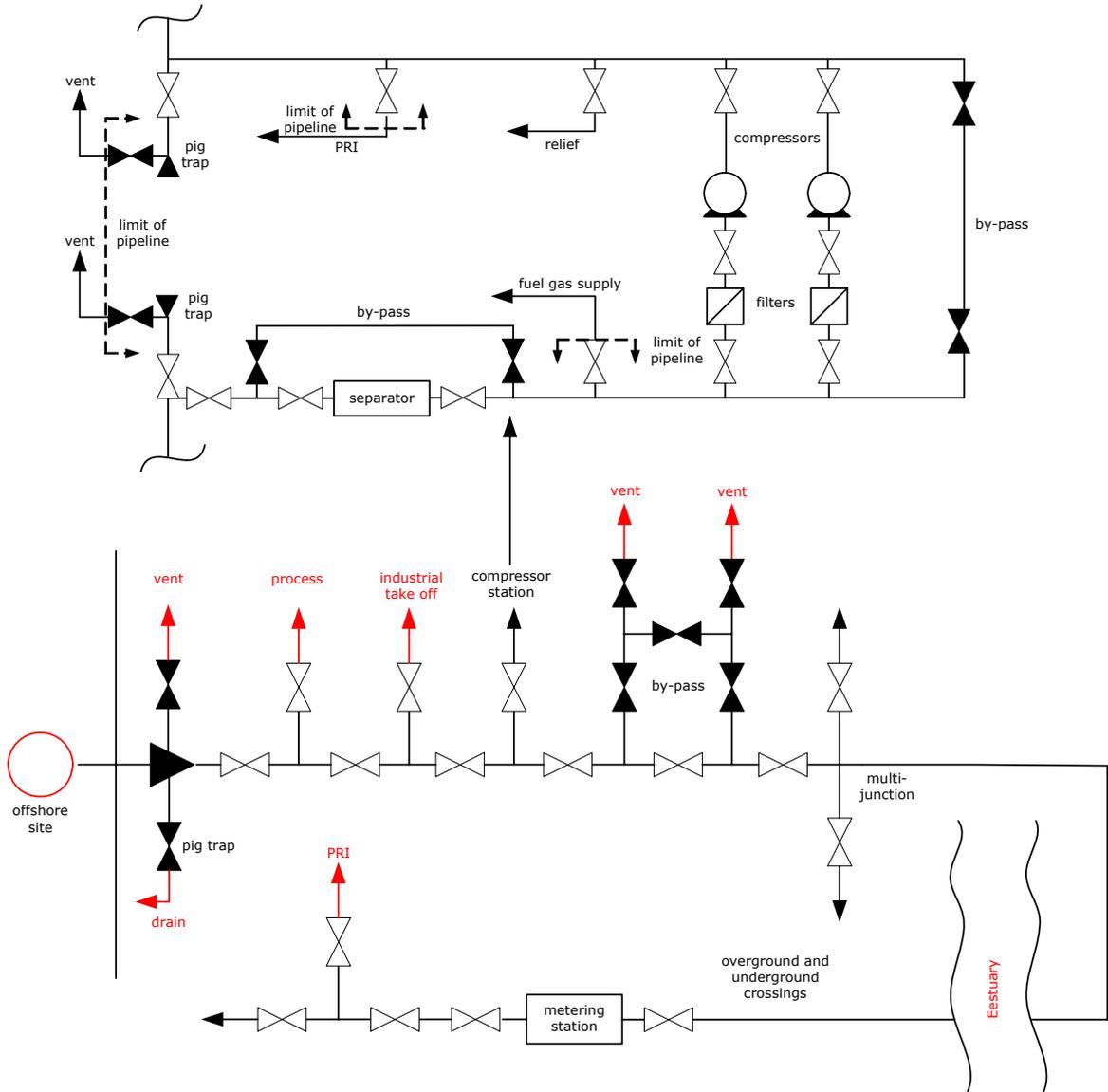
- 2.4 All references to gas pressure are gauge pressure, unless otherwise stated.

- 2.5 Details of all standards and other publications referenced are provided in Appendix 2.

Where standards are quoted, equivalent national and international standards, etc. equally may be appropriate.

- 2.6 Italicised text is informative and does not represent formal requirements.

- 2.7 Appendices are informative and do not represent formal requirements unless specifically referenced in the main sections via the prescriptive terms "should", "shall" or "must".



- covered by IGE/TD/1
- not in scope of IGE/TD/1

Note 1: The diagram is for illustrative purposes only – it does not purport to demonstrate typical pipeline arrangements.

Note 2: Pig traps may be installed at a factory, onshore terminal, refinery, compressor station and otherwise as a component of the pipeline, when the limits of the pipeline end at the outlet of vent valves.

FIGURE 1 - SCOPE OF IGE/TD/1 EDITION 5

SECTION 3 : COMPETENCY, QUALITY ASSURANCE, INTEGRITY AND SAFETY MANAGEMENT OF PIPELINES AND ASSOCIATED INSTALLATIONS

3.1 COMPETENCY

Any person engaged in the design, construction, commissioning, inspection, operation, maintenance or alteration of a pipeline or associated installation shall be competent to carry out such work. This may be achieved by an appropriate combination of education, training, and practical experience.

3.2 QUALITY ASSURANCE AND QUALITY CONTROL

3.2.1 All materials and equipment shall be selected to ensure safety and suitability for the conditions of use, in accordance with relevant legislation, standards, technical specifications and this Standard.

To ensure that products achieve consistently the required levels of quality, it is recommended that all materials and components be obtained from suppliers operating a quality system in accordance with an appropriate standard such as BS EN ISO 9001, or BS EN ISO 9002.

3.2.2 Effective arrangements should be made to ensure that materials and workmanship are in accordance with the construction specification. All material certificates, test certificates, weld records and coat-and-wrap records shall be retained as part of the permanent construction record.

Particular emphasis should be placed on the inspection of materials, welding, pipe coatings, lowering-in, backfill, drainage, reinstatement, testing, and pigging operations. Any workmanship or materials not in accordance with this Standard or construction specifications should be rejected.

3.2.3 The results of inspections shall be retained as an ongoing and permanent record of the pipeline or associated installation.

3.2.4 A quality plan and associated work procedures, to provide control and monitoring of all activities from design through to operation shall be developed. This should include a suitable audit plan to ensure adherence to procedures.

3.3 SAFETY AND INTEGRITY OF PIPELINES AND ASSOCIATED INSTALLATIONS

3.3.1 The initial integrity of a pipeline or associated installation is established through proper design, material selection, sound construction practices and testing procedures. After commissioning and during operation, a programme of condition monitoring and maintenance shall be undertaken to ensure integrity is maintained (see clause 3.3.3).

3.3.2 In order to ensure that an installed pipeline and any associated installation operates at the levels of safety envisaged in Section 6, all of the requirements shall be considered and implemented as necessary. The criteria from any section of this Standard are not intended to be used in isolation. If changes are made to any criteria, the possible impact on other sections should be considered.

Note 1: The integrity of a pipeline or pipeline system is dependent upon many inter-relating activities. Figure 2 shows the main links between the major activities. It does not attempt to show all the items necessary to ensure integrity, nor does it show the complex links within a major activity. However, it does provide a flowchart/checklist to ensure that all aspects of integrity are being addressed.

Note 2: Increasingly, regulatory authorities require pipeline operators to provide positive demonstration that integrity is properly established, monitored and maintained.

3.3.3 After commissioning, the continued integrity shall be ensured by implementing an appropriate safety management system (see also Figure 2).

Note: The safety management system would normally follow the following principles in line with HS(G)65:

- *policy – the operator would have clearly defined policies which set out what is trying to be achieved in terms of safe management of the pipeline/installation*
- *organisation – there would be appropriate organisational structures in place to effectively deliver the policy requirements; these would include clearly defined roles and responsibilities within the organisational structure*
- *planning and implementation - there would be appropriate management controls in place to ensure that pipeline/installation operations are carried out safely and in line with the defined policies. These controls would include ensuring that individuals responsible for carrying out safety related activities have the appropriate training and competencies*
- *measure – the pipeline/installation performance would be measured against agreed standards to reveal when and where improvement is needed*
- *audit – there would be appropriate audit processes in place to ensure that policy requirements are being adequately delivered*
- *review – the overall management process would be under continuous review to ensure that it is delivering the required levels of performance. Normally, this would involve the monitoring of fault, accident and near miss data.*

The safety management system shall be documented in the operator's Major Accident Prevention Document (MAPD) as required by the Pipelines Safety Regulations (PSR) and should be integrated with the operator's Pipeline Integrity Management System (PIMS).

Note: Further guidance on safety management and PIMS can also be found in CEN/TS 15173 and CEN/TS 15174.

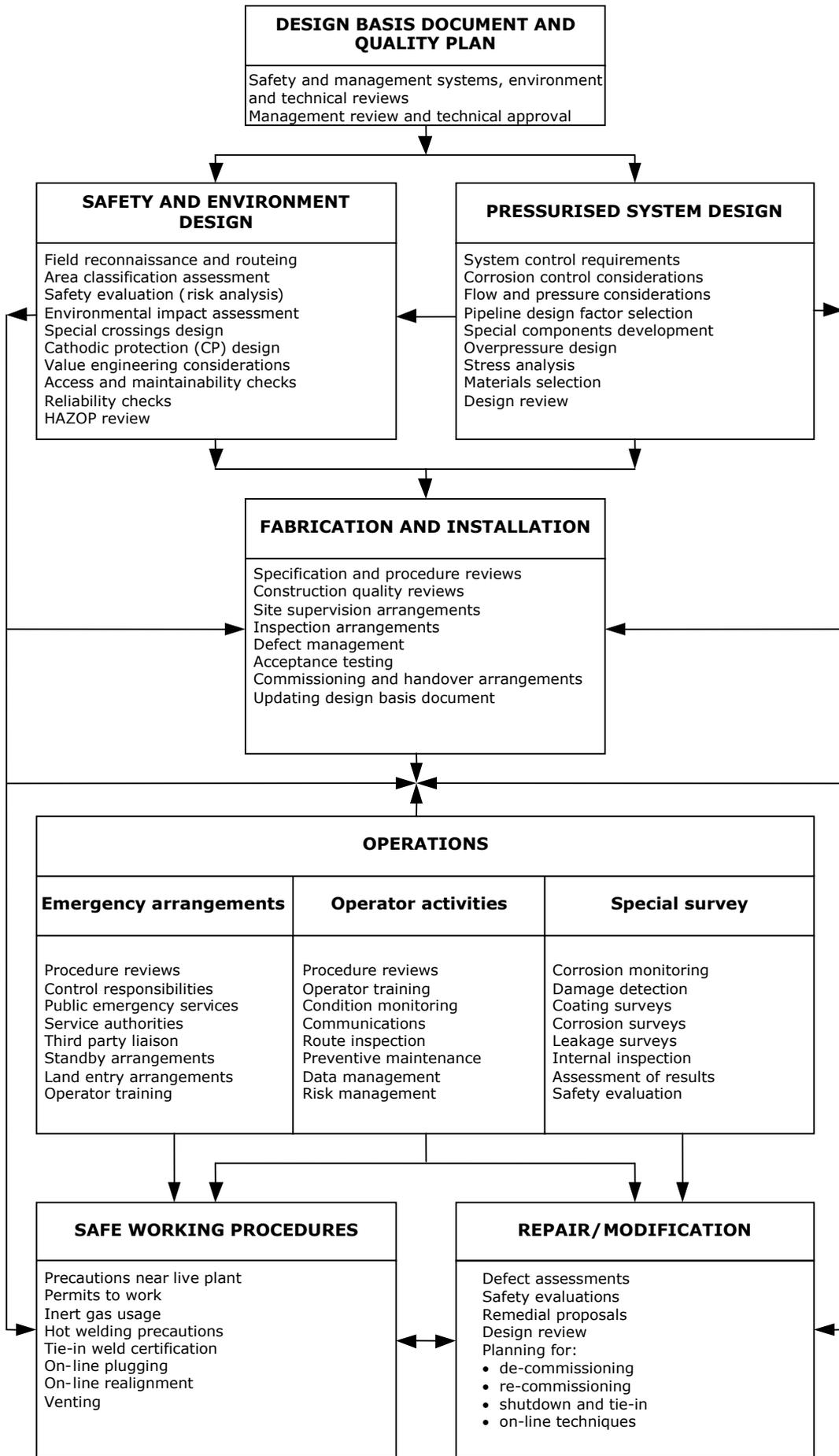


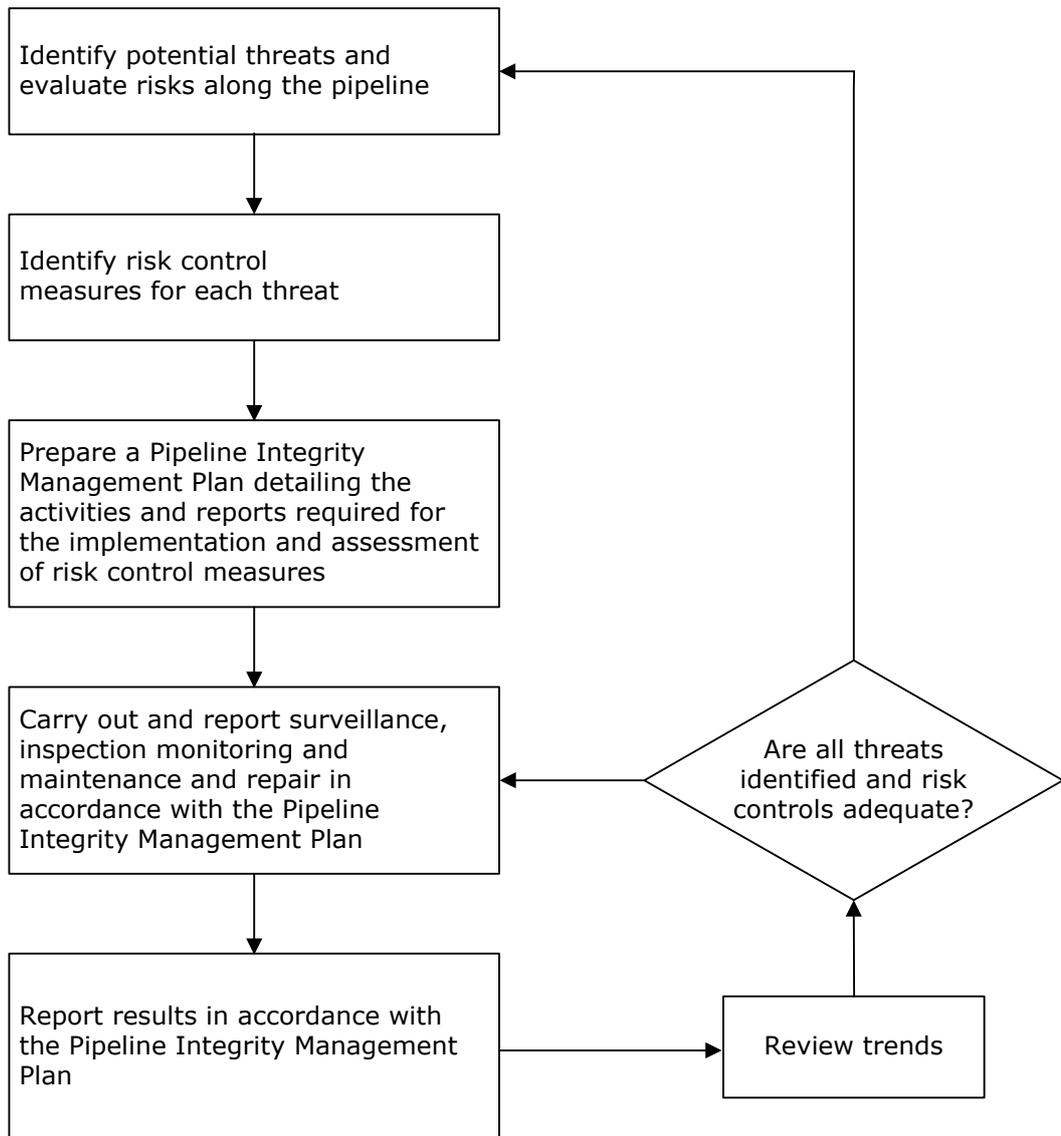
FIGURE 2 - PIPELINE SAFETY AND INTEGRITY NETWORK

3.4 PIPELINE INTEGRITY MANAGEMENT

Pipeline integrity is defined as the strength, quality and condition required to provide the capacity to withstand applied operational and external loads and resistance and tolerance of damage such that product is contained at an adequate level of safety. Comprehensive requirements for integrity are discussed in Sub-Section 3.3.

3.4.1 Process

Pipeline integrity shall be managed and controlled at all stages of the pipeline life cycle. The integrity management process is shown below. The primary requirement of the pipeline integrity management process is the identification of potential threats, evaluation of risks associated with each threat, and the implementation of specific risk control measures.



The threats to pipeline integrity include:

- material and construction defects
- external interference
- corrosion (external, internal, SCC, AC/DC induced etc.)
- fatigue

- overpressure.

These vary along the pipeline route, and this should be taken into account in the evaluation of risks and identification of risk control measures.

The requirements for pipeline integrity management at each stage of the pipeline life cycle required by this code are summarised in the table below.

Stage of Life Cycle	Integrity Management Requirement
Design	Identify route in accordance with Section 4, select materials in accordance with Section 5, design for area type and operational and additional loads and specific locations in accordance with Section 6 and apply corrosion protection in accordance with Section 11 to ensure an adequate level of design strength and resistance to loading and damage.
Construction and testing	Construct pipeline in accordance with Section 8 and test in accordance with Section 9 to ensure adequate quality.
Operation	Management of operational activities in accordance with safe operating procedures in Sub-Section 12.2. Operate within the specified design limits in accordance with Sub-Section 12.4 to ensure an adequate safety margin is maintained.
Surveillance, monitoring, inspection, maintenance and repair	Carry out Surveillance in accordance with Sub-Section 12.5 Carry out monitoring in accordance with Sub-Section 12.6 Carry out maintenance in accordance with Sub-Section 12.7 Carry out damage assessment and repair in accordance with Sub-Section 12.8.

3.4.2 **System**

A pipeline integrity management system which facilitates the integration and relation of integrity data on a section by section basis along the length of the pipeline should be used to ensure that data related to the condition of the pipeline protection, coating and pipewall is accurately related to the pipeline strength and environment on a section by section basis along the length of the pipeline.

The complexity of the system required should be determined by the operator taking into account the length, size and age of the pipeline, the operational arrangements and the competence and experience of personnel responsible for the management of pipeline integrity.

SECTION 4 : PLANNING AND LEGAL CONSIDERATIONS FOR PIPELINES AND ASSOCIATED INSTALLATIONS

4.1 PLANNING

4.1.1 General

The effect a pipeline/installation has on the environment depends largely on the route of the pipeline and shall be taken into account during design and construction.

The environmental impact of the route of a pipeline and the location of any associated installation shall be assessed at an early stage (see clause 4.2.2.14). All areas requiring special consideration for environmental controls shall be identified and allowance made, thus minimising the possibility of changes in design or more expensive remedial measures on completion of the project.

Note: Consultation with outside organisations forms an important aspect of the route selection process, not only to gather information on environmental issues but also to identify those issues perceived to be significant by third parties. These may require the use of "mitigation measures" such as special construction techniques, timing, etc. to achieve agreement on the acceptability of the project.

4.1.2 Route selection

Route selection should be carried out in three levels of detail:

- Level 1 : Route corridor selection
- Level 2 : Reference route selection
- Level 3 : Detail design.

4.1.2.1 Level 1 – Route corridor selection

The following guidance applies for Level 1 to identify the route and possible alternatives and to define route corridors through any area of interest.

Note 1: The evaluation of outline principles from desk study information allows informed decisions to be reached based on engineering and environmental constraints. Normally, this includes indicative costing and an outline programme indicating key dates and notification period to assist in the decision making process.

Note 2: Preliminary consultation with planning authorities and consideration of local plans need to be included as part of the Level 1 work.

Note 3: Requirements for the environmental impact study need to be assessed during the Level 1 work programme and commenced, if required.

- (a) The area of interest should be defined from the initial, intermediate and terminal points of the pipeline route, marked on suitably scaled maps, for example 1:50000, 1:25000, 1:10000. On longer pipelines, smaller mapping scales (1:250000) may be necessary for conceptual routing. Use of satellite imagery and/or aerial photography in the preliminary route selection should be considered.
- (b) Route corridors should, as far as possible, avoid running closely parallel to high density traffic routes, railways, overhead electricity transmission lines, major pipelines or other buried plant.

The length of the route between the various points should be kept to a practical minimum.

Possible route corridors should be identified using the following criteria:

- the pipeline start and finish points

- any intermediate fixed points
 - avoidance, as far as practicable, of any significant environmental, archaeological and future developments and of engineering constraints
 - the shortest distance between the start and finish points, bearing in mind the above criteria and the implication for project costs
 - the requirements in Section 6, including minimum proximity distances between the pipeline and normally-occupied dwellings.
- (c) Records should be kept of factors influencing the final route, particularly those affecting construction, such as contours, crossfall, wet land, made-up ground, corrosion hazards (see Section 10), rock, areas of potential flooding and other special features.

Note should be made of areas which call for early ground investigations, such as geomorphological or bore hole surveys, etc.

Consultation with geological and archaeological institutions should be carried out at this stage.

- (d) The width of the route corridor depends on the complexity of the environment through which it passes but, in general, a width of 1 km should be used. The corridor width should also take into account any anticipated requirements for minor re-routes in congested areas.

Note: The corridor need not be of uniform width throughout its length and may alter in size due to constraints.

- (e) Information required to select the route corridor should be sought from published sources, such as suitably scaled maps, geological surveys, etc. In addition, information on areas covered by major environmental designations should be obtained from published information or through the relevant planning authority(ies) and statutory environmental bodies.
- (f) Sites for associated installations should be selected taking into account design criteria, access and environmental requirements (see Sections 6 and 12).
- (g) The selected route should be examined from vantage points such as public highways, high ground and other areas of unrestricted access.

Note: This may be supplemented by aerial photographic survey, visual survey by helicopter or walking the route (subject to obtaining permission from the land-owner).

4.1.2.2 Level 2 – Reference route selection

The Level 2 process should be used to identify and record more detailed information of environmental and other features, within the route corridor, that will be used to select a preliminary pipeline route. This may be used in negotiations with land-owners/occupiers and as the basis for the next level of the process. Use of satellite imagery and/or aerial photography in Level 2 route selection work should be considered.

This phase of the planning process should be used to examine, develop and refine the proposed solutions/options to determine if they can meet realistically the specified project requirements. Ideas and working principles for the pipeline should be assessed in order to define the essential elements and options available, reducing them to just one for detail design (Level 3).

- (a) Initially, the various constraints, and all potential planning problems likely to have an adverse affect on the pipeline route, should be identified and recorded. Such constraints may be divided into, but are not limited to, the following categories:
- nature conservation
 - archaeology
 - water resources
 - land use
 - landscape features
 - planning policies
 - agriculture
 - socio-economic factors
 - geology
 - heritage features
 - transport infrastructure.

Note: Some of these features may cover considerable areas requiring the boundary of the sites to be established.

- (b) The scope of consultation should be expanded to include, but not be limited to:
- land owners and relevant authorities
 - conservation groups
 - other utilities, etc.
- (c) Negotiations for third party consents for special crossings should, normally, begin with the relevant authorities, for example railways, waterways, highways, etc.
- (d) Any nature conservation site within the boundaries of the route corridor should be identified and recorded.
- (e) Any statutorily-protected site or other known site of archaeological or heritage importance within, or in proximity to, the route corridor, should be identified and recorded.
- (f) Any major water resource feature within the route corridor should be identified and recorded and information obtained on aquifer protection zones and major water abstraction sites.
- (g) Any major geological feature should be recorded and its engineering implications considered.
- (h) Any areas or type of existing land use that could affect the route and/or the design of the pipeline/installation should be recorded.
- (i) Any existing, planned or disused extraction zone should be identified and avoided where possible (see also clauses 4.4.2.1 (f) and (j)).
- (j) Any area within the route corridor that is zoned for future development (domestic, industrial, commercial or mineral) or other developmental controls, should be identified and recorded. Discussions with relevant planning authorities, to establish recent changes in policies or departures from approved plans, should be considered.

- (k) Any major landscape and topographical features within the route corridor should be identified and recorded, to avoid unnecessary difficulties or disturbance.
- (l) Any areas of high-grade agricultural land within the route corridor should be identified and recorded.
- (m) With all relevant information available, both from the above surveys and from the calculations carried out to meet Section 6, a reference route should be selected and suitably scaled plans prepared (typically, 1:2500 or 1:10000).

Note: This requires a population density survey to be carried out in accordance with clause 6.7.1.2.

- (n) At this stage, preliminary material requirements should be established in the form of a preliminary Material Take Off and the locations of the various grades and thicknesses of linepipe marked on the plans to comply with the marked area classification and route crossings etc., including the location and limits of heavy wall or proximity pipe.

4.1.2.3 *Level 3 – Detail design*

The Level 3 process should be used to identify and recorded information to refine the pipeline route.

- (a) Permission should be sought from land-owners to examine the route in detail, paying particular attention to those locations which impose engineering constraints on the proposed route, or of crossings where detailed surveys are required.
- (b) Full consideration for design for safety is required. This should include the use of specific construction techniques for pipeline and installation details, and assessment of information regarding the physical nature of the land to assess whether this is likely to affect the safe constructability of the pipeline.

Note: Compliance with the Construction Design (Management) Regulations (CDM) is required in the UK.

- (c) Due regard should be paid to including suitably specified linepipe and protection at sites of future road/rail construction etc.
- (d) Consideration should be given to the completion of ecological and archaeological field surveys to define accurately the extent of a site or its environmental significance and to take any suitable mitigation measures. Ecological and archaeological surveys will form part of the Environmental Impact Assessment (EIA).
- (e) Records should be kept of any special requirements necessary in respect of contagious/infectious animal and other diseases.
- (f) The final examination of the route should identify whether any minor diversion is required to avoid short lengths of difficult terrain or to meet land-owner/occupier objections or to facilitate trenchless construction/environmentally-compatible construction techniques.
- (g) Consideration should be given to the negotiation of any use of access roads for construction or maintenance purposes and o the agreement of traffic management plans with local authorities (parking, access, egress, etc.).

Note: Planning approval may also be necessary for associated installations and CP.

- (h) Where necessary, planning permission should be obtained for temporary accommodation and material storage areas.
- (i) Other “constraints” that occur along the route of the pipeline (noise, dust, availability of water and its means of disposal, etc.) should be identified.

Note: These are unlikely to affect the alignment of the pipeline but may have an effect on the design or management of construction.

- (j) Fundamental environmental issues, to be addressed during construction, should be defined.

Note: These will contribute to an environmental management plan detailing requirements with regard to environmental matters and include appropriate emergency response procedures for environmental incidents such as spills, etc.

The plan should include details of actions to be taken once construction is completed, for example reinstatement of hedgerows, etc. Monitoring of the plan during construction and, possibly, operation, should be carried out to allow for any unforeseen impacts to be identified and controlled.

Reference should also be made to clause 4.2.2.14.

4.1.3 **Land rights/easement details**

- 4.1.3.1 Appropriate plans should be provided during negotiation of easements to enable establishment of the boundaries of each ownership and tenancy.

The information gained should be marked on suitable scale maps and each ownership given a separate reference number. The reference number should be used on all correspondence and the relevant easement file.

- 4.1.3.2 A “schedule of undertaking”, setting out how to deal with the various aspects of the construction process, should be produced for issue to all land-owners, occupiers, etc

- 4.1.3.3 The working width should be specified.

- 4.1.3.4 The easement file should be readily accessible and contain the following information:

- easement reference number
- name and address of owner(s) and occupier(s) and their land agent(s) and legal adviser(s)
- name of the site where the easement is located
- field reference number or other means of identification
- map reference number and/or strip map number
- length of easement
- width of easement
- working width if different from the width of easement
- rate per unit length payable for easement
- total payment for easement
- date of deed of the easement and entry date
- special conditions applicable to any access routes and terms negotiated

- number of surface boxes or obstructions
- any special features, including marker posts.

4.1.3.5 When the consent of the owner(s) and occupier(s) has been obtained, the formal easement documentation should be prepared.

4.1.4 **Construction plans**

4.1.4.1 Following the detailed examination/environmental assessment of the route, the construction maps (normally strip maps) and drawings should be prepared. Where critical clearances are required from existing features, these should be dimensioned on the strip maps as well as located by co-ordinates, to prevent small survey/co-ordinate inaccuracies resulting in unacceptable clearances.

The information on the strip map should include:

- the proposed position of the pipeline, showing any change of direction, wherever possible using a co-ordinated method based on a land survey
- the position of any associated installation, PRI and CP ground beds
- pipe dump/accommodation access drawings
- easement details and special conditions
- details of additional and restricted working areas
- location of other services and apparatus
- cross reference to special crossings and other drawings
- local government and other relevant boundaries
- reference to any borehole or other geological information obtained
- any access routes negotiated
- changes in nominal wall thickness of the pipeline
- area classification details, i.e R, S, or T (see clause 6.7.1)
- road classification.

Note: Types of plans and drawings normally required, and their subsequent use, are shown in Table 1.

4.1.4.2 North points should be indicated on every drawing and strip map.

4.1.4.3 Strip maps should indicate the length and size of the pipeline. All field numbers, etc. should be shown.

4.1.4.4 Engineering line diagrams, indicating the extent of pressure regimes and the various control systems should be prepared.

SCALE	USE BY PIPELINE PROMOTER	FOR ISSUE TO
1: 50000	Preliminary off-site survey.	Internal circulation.
1: 25000 or 1: 10000	Preliminary field survey. Contract documents. Land procurement.	Land agents.
1: 2500 or 1: 1250 in built up areas	Working drawings. Easement records. Permanent records. EIA.	Land agents. Contractors. Public bodies. Service industries where greater detail is required.
Larger scales	Construction details of special crossings, installations and other areas such as pipe dumps, access, and for record purposes.	Appropriate authorities and contractors.
Not to scale	Engineering line diagrams showing the extent of pressure regimes and control systems.	Internal circulation to appropriate bodies contractors.

Note: The suggested scales may be altered to suit local conditions.

TABLE 1 - TYPES OF PLAN USED IN PLANNING PIPELINES/ASSOCIATED INSTALLATIONS (TYPICAL EXAMPLE OF PLANS USED WITHIN THE UK)

4.2 LEGAL CONSIDERATIONS

The matters dealt with in clause 4.2.1 refer to general national and local legal requirements, particularly legislation and its application to all aspects of design, planning, construction and operation of a pipeline and any associated installation.

The matters dealt with in clause 4.2.2 refer to specific UK legislation in force at the time of publication.

Appendix 2 lists relevant legislation.

4.2.1 General

4.2.1.1 *European Union (EU) Legislation*

In countries within the EU, it shall be ascertained, at the planning stage, whether a pipeline is likely to be subject to EU legislation.

4.2.1.2 *National and local legislation*

Consideration must be given to relevant national and local legislation which may control, regulate or protect, with respect to any pipeline/installation:

- the route
- the specification
- the methods and procedures for construction
- the various authorisations, consents or permissions, whether from owners or occupiers of land through which the pipeline is laid or from private/public organisations having a function or interest in the construction

- the environmental impact.

4.2.1.3 *Land rights and easements*

The rights necessary to lay, operate, inspect, maintain, repair and replace a pipeline/installation and any ancillary equipment must be obtained from land owners and/or occupiers affected by the pipeline/installation.

Note: Usually, this can be done by negotiation and agreement, but it may be appropriate to use compulsory powers of acquisition where appropriate legislation is available for use.

The rights acquired should be such as to permit the satisfactory construction, use, maintenance and replacement of the pipeline and should last for at least the anticipated life of the pipeline or the gas supply agreement.

Note: The precise nature of the rights acquired may vary according to the country of operation.

Excavated and other material should not be removed from the support strip without the land owner's consent.

Care shall be taken to prevent dumping of material over the pipeline, to avoid excessive cover.

The rights shall anticipate the possibility of the whole or parts of the pipeline/installation becoming redundant and/or being put to an alternative use.

Of special concern are the access rights of the pipeline easement, which should anticipate the needs of construction, remedial works to the land following construction and subsequent remedial works to, or replacement of, the pipeline, including consideration of storage and parking facilities on land contiguous to and neighbouring the pipeline.

Note: Where access is along the easement strip only, this is unlikely to be sufficient.

Legal advice should be sought on the content of easement to be acquired and, in particular, on any problem likely to arise on the abandonment of the whole or parts of the pipeline.

The resultant form of agreement with the land owner/occupier should, typically, deal with:

- use of the pipeline/installation
- access
- safe operation of the pipeline/installation (including CP)
- restoration of drainage
- development of the land through which the pipeline runs or on which an installation is located.

4.2.1.4 *Building or engineering work*

Where necessary, permission must be sought for any building or engineering work, from public organisations charged with responsibilities for building and environmental control.

4.2.1.5 *Health and safety law*

Compliance must be achieved with any relevant health and safety law.

Note: This may affect to a considerable degree the route of a pipeline and the location of an installation in terms of the acceptable proximity to significantly inhabited areas, the

specification for the pipeline/installation, the actual method of construction and the general working environment during construction and operation.

4.2.1.6 *Environmental protection*

The route of a proposed pipeline and location of any associated installation must take all relevant environmental considerations into account, including the special protection given by law to flora, fauna and areas of special scientific, geological and historical interest, as well as the restrictions and prohibitions on building and engineering works which may arise. Consideration shall be given to the possible emissions of odour, dust, and noise.

4.2.1.7 *Transmittable diseases*

Consideration shall be given to the possibility of construction being affected by outbreaks of infectious/contagious animal and other diseases along, or in the vicinity of, the proposed route.

Advice should be taken to ensure that, where such outbreaks exist, appropriate procedures and practices are adopted so as to comply with both good farming and veterinary practice and relevant legal restrictions.

4.2.1.8 *Rivers, canals and foreshores*

Where crossings of rivers, canals or foreshores are contemplated, appropriate authorities or owners should be consulted.

Note: Local regulations may be in force which affect proposals to lay pipes over, under or adjacent to rivers or canals.

4.2.1.9 *Railway land*

Consultation with railway undertakings should be carried out at an early stage where it is proposed to cross under or through the land of a railway undertaking.

4.2.1.10 *Deposits of waste*

The disposal of all wastes which are poisonous, noxious or polluting and likely, after disposal on land, to give rise to an environmental hazard, shall be given special attention.

Note: The activity may require authorisation or licensing from an appropriate authority.

Disposals of non-toxic waste water may be subject to licensing with special conditions and the advice of any relevant authority should be sought.

The dumping of waste at sea, whether in territorial waters, tidal waters, rivers or estuaries, may involve the obtaining of a licence, whether from government or a public authority, hence an approach should be made to the appropriate authority before such activities are undertaken.

4.2.1.11 *Control of noise*

Consideration must be given to law or legislation controlling the noise of construction works, and also should be given to the concept of being a good neighbour to those along a pipeline route.

4.2.2 **Legal considerations in the UK**

4.2.2.1 *Gas Act*

The construction of a high pressure gas pipeline is an activity which a gas transporter (GT) is entitled to undertake under the Gas Act as amended.

4.2.2.2 *Pipelines Act as amended*

The Act regulates onshore pipelines in GB, except those of GTs, water companies, the government, and some other (minor) classes of pipeline. The act creates two categories of pipeline:

- "Cross-country" pipelines (those exceeding 16.093 km) require authorisation from the Secretary of State by means of a Pipeline Construction Authorisation (PCA) which carries deemed planning permission
- "Local" pipelines (those 16.093 km or less) including diversions and connections which do not require authorisation from the Secretary of State.

4.2.2.3 *New Roads and Street Works Act*

In laying pipelines in streets, regard must be given to Part III (in Scotland Part IV) of this Act. This requires street authorities to issue works licences and maintain a streetworks register, with the intention of co-ordinating works. Advance notice of certain works will be required, together with notices for starting dates of works.

4.2.2.4 *Town and Country Planning Act*

The lying underground of pipes or other apparatus by a GT is permitted development under the Town and Country Planning (General Permitted Development) Order.

4.2.2.5 *Health and Safety at Work etc. Act*

The Act sets out general duties which employers have towards employees and members of the public, and employees have to themselves and to each other. It is also the "umbrella" under which safety regulations are made, for example:

- Management of Health and Safety at Work Regulations

These regulations apply to all work activities involving pipelines and require, among other things, that employers assess the risks to the health and safety of their employees and of persons not in their employment but who may be affected by their activities and then to make appropriate arrangements for preventative and protective safety measures.

- Pressure Systems Safety Regulations (PSSR)

The only hazard under consideration in these regulations is that due to pressure – not that from any flammable or toxic characteristics of the gas.

An important consideration is the requirement to have a written scheme for the periodic examination by a competent person of the pipeline system and its protective devices.

- Pipeline Safety Regulations (PSR)

These regulations apply to all pipelines constructed in GB, both on and offshore, but exclude pipelines that are:

- wholly within premises
- contained wholly within caravan sites
- used as part of a railway infrastructure
- convey water.

Gas pipelines operating at a pressure of 7 bar or more are “Major Accident Hazard Pipelines” and are subject to additional duties, including notification to HSE, the preparation of emergency plans and procedures, etc. The regulations complement the Gas Safety (Management) Regulations (GS(M)R) and include:

- the definition of a pipeline
- the general duties for all pipelines
- the need for co-operation between pipeline operators
- arrangements to prevent damage to pipelines
- the description of a dangerous fluid
- notification requirements
- the major accident prevention document
- the arrangements for emergency plans and procedures.

4.2.2.6 *Construction (Design and Management) Regulations (CDM)*

These regulations place a duty on clients, designers and contractors to take health and safety matters into account and manage them effectively from the planning stage of a construction project through to commissioning and beyond.

4.2.2.7 *Trees*

Under the Forestry Act, a licence from the forestry commissioners is not required for the felling of trees where the felling is immediately required for the purpose of carrying out permitted development but, where a tree preservation order under the Town and Country Planning Act is in force, the consent of the local authority must be obtained.

Under the Hedgerows Regulations, permission is required from the local planning authority for the removal of most countryside hedgerows.

4.2.2.8 *Transmittable diseases*

The Department of Environment, Food and Rural Affairs (DEFRA) advises that, at least one month before commencing work on agricultural land (or land previously used for agriculture), the DEFRA Divisional Officer and, in England and Wales, the Senior Plant Health and Seeds Inspector, or the Seeds Inspector, or in Scotland the Principal Agricultural Officer for the area concerned, should be contacted with respect to:

- any statutory restrictions which apply to the site or its immediate vicinity and any special precautions which may need to be taken, for example orders made under the Animal Health Act may regulate operations in infected areas
- the presence of any soil-borne diseases, for example rhizomania of beet, wart disease of potatoes etc.
- presence of carcass burial pits on the site or in its immediate vicinity.

Note: If the development involves removing trees, it is advised that the area Forestry Commission Plant Health Inspector be consulted for advice on how to avoid spreading tree diseases.

4.2.2.9 *Rivers, canals and foreshores*

Part 1 of the Environment Act established the Environment Agency (EA) (Scottish Environment Protection Agency in Scotland) (SEPA), and provided for the transfer of functions from the National Rivers Authority (NRA). The EA and SEPA determine and grant consents to discharge wastes into controlled waters and charge for such work – this includes the discharge of water for hydrostatic testing. In England and Wales, the EA also regulates the abstraction of water (which requires an abstraction licence).

The EA and SEPA also undertake pollution control and have the power to prosecute where “poisonous, noxious or polluting matter” is allowed to enter controlled waters. This includes the discharge of silty water from construction sites. Guidance on how to manage sites is obtainable from either agency in the form of Pollution Prevention Guidelines (PPGs), in particular PPG6 “Working at Construction and Demolition Sites”.

British Waterways is a statutory body established by the Transport Act. It owns and manages approximately 2000 miles of canals and river navigations. The British Waterways Code of Practice governs works that might affect its waterways and properties.

Where works are to be constructed in, under or over the seashore below the high water mark of ordinary spring tides, the consent of the Secretary of State is required under Section 34 of the Coastal Protection Act. Where the works are to cross the foreshore, an easement must be obtained from the owners, generally, the Crown Estate Commissioners.

4.2.2.10 *Railway land*

Where apparatus is to be laid through land owned or operated by Railtrack, or other railway infrastructure operator, the appropriate officers should be consulted at an early stage.

4.2.2.11 *Deposits of wastes*

Waste is defined in schedule 22 of the Environment Act as a substance or object which a holder discards, or intends or is required to discard. This definition is based upon an EC Directive 91/156 and is, therefore, known as “directive waste”. “Controlled waste” is defined by the Environmental Protection Act (EPA) and is defined as “household, industrial and commercial waste”. Controls under EPA, for example licensing requirements and the Duty of Care apply only to controlled waste which is also “directive waste”.

Section 34 of EPA introduced a duty of care for waste management. The duty of care applies to anyone who produces, imports, carries, keeps, treats, or disposes of controlled waste. There are a number of objectives, outlined below, which duty holders should achieve, as is reasonable in the circumstances.

Every person who is subject to the duty of care must ensure not only that they do not commit an offence but that any other person does not similarly commit offence. In practice, this means that a waste holder is responsible for taking steps to prevent offences involving waste that they have controlled at some point. They must try to prevent other people from disposing of, treating or storing the waste:

- without a licence
- breaching the conditions of a licence
- in a manner likely to cause pollution or harm to health.

The producer or importer of waste must package it in such a way as to prevent escape of leakage while on site, in transit or in storage. The waste producer or holder must ensure that waste is only transferred to an authorised person. The categories of authorised persons are:

- a waste collection authority
- the holder of a waste management licence or someone who is exempt from holding a licence
- a registered carrier of controlled waste, or someone who is exempt from registration
- a waste disposal authority in Scotland.

In addition, an accurate, written description of the waste must be provided by the producer or importer of the waste and transferred alongside the waste at each stage.

4.2.2.12 *Control of noise*

Noise is a major issue both for designers who should endeavour to “design out” noisy processes wherever possible, and managers of construction/demolition sites where the potential of nuisance should be recognised at the earliest possible stage.

Part III of the Control of Pollution Act (COPA) relates to construction site noise, which is subject to noise abatement zones and licensing enforcement by the local authorities. Under Section 60 of the Act, local authorities have powers to control noise (an vibration) on or from building sites. This control is by the service of a notice placing obligations on the person responsible for the construction operations to observe specified controls to minimise noise. Such a notice can specify types of plant and machinery, permitted hours of operation, boundary noise levels, etc.

When drawing up such requirements, the local authority have regard to any code of practice approved or issued under COPA. They must also have regard to the concept of Best Practicable Means and any alternative plant or machinery which may be used.

BS 5228 has been adopted for this purpose (noise control on construction and open sites (in four parts)). Although these codes have been issued or adopted under COPA, they are not legally binding in themselves. However, the content of each should be taken to represent current good practice.

Noise abatement zones are established essentially for the purpose of rationalising competing sources of noise, particularly where industrial premises and domestic premises are in proximity. Local Authorities are required to keep registers of noise levels of specified premises within noise abatement zones.

Part II of EPA relates to statutory nuisances, which include noise nuisances. Statutory nuisances are defined as including circumstances in which noise is emitting from premises so as to be prejudicial to health or a nuisance. The local authority can serve an abatement notice and enforce it in criminal proceedings before a Magistrates Court in the event of non-compliance without reasonable excuse.

The Noise and Statutory Nuisance Act amends EPA to make noise from vehicles, machinery or equipment in the street a statutory nuisance. If the local authority is satisfied that noise from vehicles, machinery or equipment in the street is causing, or is likely to cause, a nuisance, it must serve an abatement notice on the person responsible.

4.2.2.13 *Pipe laying across country*

There are many bodies and authorities which have an interest in the operations of pipelaying across country. The following list, which is not exhaustive, identifies some of the key consultees:

- Planning officers of Country and District Councils, Local Unitary Authorities and, in Scotland, Regional Councils
- English Nature, Countryside Agency (England), and Countryside Council for Wales and Scottish Natural Heritage
- EA (England and Wales) and SEPA (Scotland)
- DEFRA
- Department for Transport, Local Government and the Regions (DTLR)
- English Heritage and Historic Scotland
- Department for Business, Enterprise and Regulatory Reform (BERR)
- HSE
- Country Landowners Association and the Scottish Landowners Federation
- National Farmers Union and the National Farmers Union of Scotland
- The Coal Authority
- Utilities – electricity, water, telephone and gas companies etc.

4.2.2.14 *Environmental protection*

Consideration should be given to the need for an environmental assessment under Regulations implementing EC Directive 97/11/EC.

For GTs, the relevant legislation is the Public Gas Transporter Pipeline Works (Environmental Impact Assessment) Regulations. These make an Environmental Assessment mandatory for gas pipelines of more than 800 mm diameter and more than 40 km long.

In addition, schedule 3 of these regulations describes pipeline works for which an environmental statement may be required and includes pipelines which pass through sensitive areas (as defined by the regulations) or which operate at pressures greater than 7 bar. Such pipelines require an environmental determination by the Secretary of State at the BERR as to whether an EIA is required, unless a voluntary EIA is undertaken. Early recognition of the need for an EIA, or the need for an environmental determination, is essential if delay is to be avoided during later planning stages.

For non-GTs, the relevant regulations are the Pipeline Works (Environment Impact Assessment) Regulations and the Town and Country Planning (Environmental Impact Assessment) (England and Wales) Regulations.

For projects identified as requiring an environmental determination, it is recommended that as much information as possible is gathered at an early stage, so that the request for a determination can be accompanied by sufficient information to meet the requirements of schedule 3. A supporting statement should also accompany any request for a determination from the relevant planning authority expressing their opinion of the project.

An EI requires consideration for the environment and public participation in the decision making process of project development. An Environmental Statement (ES) is a review document prepared for assessment in the EIA process which should consider both the adverse and the beneficial effects of the project, their significance and the mitigation measures to be applied. Hence, for pipelines

where EIA is required, this process will subsume the need for a Level 3 environmental study (see clause 4.1.2.3).

4.2.2.15 *Protection against risks from fire, explosion and similar events*

The Dangerous Substances and Explosive Atmospheres Regulations (DSEAR) are concerned with protection against risks from fire, explosion and similar events arising from dangerous substances used or present in the workplace. The Regulations require that risks from dangerous substances are assessed, eliminated or reduced. They contain specific requirements to be applied where an explosive atmosphere may be present and require the provision of arrangements to deal with accidents, emergencies etc., and provision of information, training and use of dangerous substances. The Regulations also require the identification of pipelines and containers containing hazardous substances.

SECTION 5 : MATERIALS FOR PIPELINES

This section deals with materials for pipelines. Many of the requirements equally apply for associated installations but reference to Section 12 is required for additional or amended requirements.

5.1 STANDARDS

Linepipe and fittings should be selected from appropriate standards (suitable example references are provided in the text) in accordance with the specification required to meet the design requirements. The material specification should detail the specific testing and inspection requirements to be applied to all materials.

5.2 OPERATING AND DESIGN TEMPERATURES

5.2.1 The majority of a buried transmission system will operate approximately at constant temperature which, in the UK, exceeds 5°C. Therefore, the appropriate design temperature should be 0°C.

Note: In some areas and at some points in a system, the temperatures may be lower or higher than the nominal operating temperature due to local influences. In these circumstances, another design temperature may be appropriate.

The most common examples are:

- *at the exit from a PRI where pipe, normally, will be at a lower temperature for a considerable distance downstream*
- *at the exit from a compressor station where pipe, normally, will be at a higher temperature. However, in this case, consideration needs to be given to the conditions when the compressor is not working*
- *at an exposed overhead crossing or other above ground installation, including a PRI, where the pipe could be at a lower or higher temperature than normal due to ambient temperature or solar heating. Normally, raised temperatures due to these conditions do not influence the material properties of linepipe or fittings, but consideration has to be given to the influence of temperatures both above and below normal on the materials used for coating and lining.*

5.2.2 Pipeline materials should have adequate fracture toughness at or below the minimum design temperature.

Note: It is normal to demonstrate fracture toughness at 5°C below this temperature (see clause 5.3.4.2).

5.2.3 The material properties of linepipe, fittings, coating and lining should be adequate for the conditions that arise both at the minimum and maximum design temperatures, including the effects of contraction and expansion due to climatic temperature variation, as well as the normal design condition.

5.3 LINEPIPE

5.3.1 Specification

The quality of linepipe should be verified with respect to strength, impact energy properties, for example measured using Charpy V Notch Impact Test and the Drop Weight Tear Test (DWTT) and weldability, by testing in accordance with the appropriate linepipe specification.

Steel linepipe is available in a range of strengths, defined by specific minimum yield strength (SMYS), which should be selected in conjunction with other design parameters to provide optimum pipeline design.

Note 1: Historically, the standard most commonly specified for linepipe worldwide has been API 5L. In Europe, increasing use is now being made of BS EN 10208-2 which applies to onshore gas transmission pipelines and is the linepipe standard referenced in BS EN 1594. The equivalent ISO linepipe standard is ISO 3183, which is referenced in ISO 13623. Other industry specifications, such as Advantica L1/E, LX1/E, LX4/E and LX5/E (see Appendix 2.9) may be used to specify additional requirements, for example with respect to toughness, dimensions, fatigue etc. to these national and international standards.

Note 2: Minimum fracture toughness levels ensure that a pipeline can be operated within design limits, without risk of propagating brittle or ductile fractures.

Note 3: The requirements for steel weldability ensure the maximum opportunity for high quality construction under field welding conditions.

5.3.2 **Methods of pipe manufacture**

The methods of manufacture of a pipe should be selected from Table 2.

METHOD OF MANUFACTURE¹	NORMALLY AVAILABLE SIZE
Seamless	559 mm diameter and below
High frequency welded	610 mm diameter and below
Straight seam SAW ²	406 mm diameter and greater
Helical SAW ²	1219 mm diameter and below ³

Note 1: Other methods of manufacture may be considered.

Note 2: Strip end welds are not recommended but, if they are used (where one strip of steel is welded onto the adjoining strip during the manufacturing process), it is recommended that additional inspection and testing is carried out at the strip end welds during the pipe production process.

Note 3: Recommended wall thickness < 20 mm and recommended grade X65 and below (BS EN 10208-2 and ISO 3183 grade L450 and below). See Table 3.

TABLE 2 - METHODS OF PIPE MANUFACTURE

5.3.3 **Strength grades**

SMYS and Specified minimum tensile strength (SMTS) of commonly used grades of pipe to API 5L, BS EN 10208-2 and ISO 3183-2 are given in Table 3 which should be referenced and used when selecting pipe.

API 5L AND ISO 3183 (PSL 2)			BS EN 10208-2		
Grade	SMYS N mm ⁻²	SMTS N mm ⁻²	Grade	SMYS N mm ⁻²	SMTS N mm ⁻²
L245 ¹ or B ¹	245	415	L245 ³ B	245	415
L290 ² or X42 ¹	290	415	L290 ³ B	290	415
L320 ² or X46 ²	320	435			
L360 ² or X52 ²	360	460	L360 ² B	360	460
L390 ² or X56 ²	390	490			
L415 ² or X60 ²	415	520	L415 ² B	415	520
L450 ⁴ or X65 ⁴	450	535	L450 ⁴ B	450	535
L485 ⁴ or X70 ⁴	485	570	L485 ⁴ B	485	570
L555 ⁴ or X80 ⁴	555	625	L555 ⁴ B	555	625
L625 ⁵ or X90 ⁵	625	695			
L690 ⁵ or X100 ⁵	690	760			
1. Grade suffix: R, N, Q, M 2. Grade suffix: N, Q, M 3. Grade suffix: N, M 4. Grade suffix: Q, M 5. Grade suffix: M			Grade suffix: R = as rolled; N = normalized or normalized rolled/formed; Q = quenched and tempered; M = thermomechanically-rolled.		

TABLE 3 - COMMONLY USED MATERIAL GRADES, SMYS AND SMTS**5.3.4 Testing****5.3.4.1 General**

Testing shall be carried out in accordance with BS EN 10208-2, ISO 3183 or API 5L, as appropriate.

5.3.4.2 Impact properties

Linepipe material shall meet the specified impact properties, established by suitable tests at an appropriate temperature (see Sub-Section 5.2).

Note: Fracture toughness measures the resistance of linepipe material to fracture, in either a brittle or ductile manner.

For linepipe of diameter exceeding 323.9 mm, a full wall DWTT shall be considered to assess resistance to brittle fracture.

For linepipe of diameter not exceeding 323.9 mm, extraction of a sample for DWTT is not possible and fracture appearance using the Charpy test should be substituted.

When linepipe is intended to operate at a design factor exceeding 0.3, the possibility of propagating ductile fractures shall be minimised by ensuring that the material possesses an adequate ductile fracture energy absorption.

Note: This can be measured using the Charpy test. Acceptance levels can be determined from published formulae for pipelines of strength grades up to and including X65. For higher grades, the published formulae may be unconservative and specialist advice is needed in these circumstances. In extreme cases, it may be necessary to demonstrate resistance to ductile fracture propagation by full scale testing of representative pipe sections.

The sampling plan for testing shall be designed to ensure that the proportion of pipe reaching the required toughness level is sufficient to restrict the length of a fracture to acceptable levels.

5.3.5 Weldability

The weldability of linepipe material should be demonstrated either by weldability testing or by providing weldability data previously obtained for the type of pipe concerned.

Note: The preferred approach is for the tests to be performed on full pipe lengths. Typical procedures for such full-scale weldability tests are given in Advantica LX1/E, LX4/E and LX5/E and ISO 13847. Alternatively either of the following approaches may be used:

- *weldability tests on pipe pups when the results can be correlated with field behaviour of full pipe lengths or*
- *small-size weldability tests when the results can be correlated with field welding behaviours of full pipe lengths.*

5.4 **FATIGUE**

Provided steels for linepipe are purchased in accordance in clause 5.3.1 and the design complies with Section 6, it is anticipated that all fatigue design requirements will be satisfied.

5.5 **FITTINGS**

5.5.1 **General**

5.5.1.1 Fittings shall be of the appropriate strength for the proposed test pressure. They shall be qualified with respect to strength, fracture toughness and weldability in a similar manner to pipe. Mechanical testing shall be carried out after hot forming and final heat treatment.

Note: Where fittings of sufficient strength to match high strength pipe such as L485 and L555 are not available, a lower strength may be used with suitable thickness compensation.

5.5.1.2 Tensile testing for forged components shall be carried out in accordance with a relevant standard, on specimens taken transverse to the direction of rolling of the original plate.

For fabricated components, specimens shall be taken transverse to the direction of rolling of the original plate.

5.5.1.3 Fittings shall be qualified with regard to fracture toughness by notch ductility testing, for example Charpy testing.

5.5.1.4 The weldability of fittings of a specific type and from a specified source of supply shall be assessed using a full size production sample, and this should be a complete butt weld to a pipe pup. Otherwise, weldability shall be demonstrated by providing weldability data previously obtained for the fitting being used.

Note: A typical full-scale weldability test procedure is given in Advantica WP1/E.

Alternatively, small-scale weldability tests may be performed when the results can be correlated with field welding behaviour of full size components.

Note: The field weldability of large diameter, thick wall fittings can be improved by shop welding pup pieces of linepipe to each end, so that field joining involves only pipe to pipe joints.

Unless otherwise specified, all non-destructive testing (NDT) of fittings shall be carried out after all processing, heat-treatment and final stress relief if applicable.

5.5.1.5 It should be confirmed that purchased fittings are in accordance with specifications.

5.5.2 **Bends, tees and headers**

5.5.2.1 The following standards for wrought bends and tees shall be used as appropriate:

- BS 1640-1,3
- ANSI/ASME B 16.9

- ANSI/ASME B 16.28
- ASTM A105
- ASTM A234
- ASTM A420
- ASTM A860
- MSS SP 48
- MSS SP 59
- MSS SP 63
- MSS SP-75
- ISO 3419
- ISO 15590-2.

Note 1: Bends made from pipe by the induction bending process are covered by ISO 15590-1 and Advantica B11/E.

Note 2: Some material specifications do not contain sufficient requirements to fully qualify fittings in accordance with this section with respect, for example, toughness, dimensions, fatigue etc. In such cases, additional testing may be required.

5.5.2.2 Bends for inclusion within any pipeline shall be manufactured with a minimum radius of three times the nominal outside diameter of the pipe and should allow free passage of pigs (see Sub-Section 6.14).

5.5.2.3 Bends for inclusion in associated pipework not to be subject to pigging shall be to a minimum radius of one and a half times the nominal outside diameter of the pipe.

5.5.2.4 Bends shall be manufactured and tested in accordance with appropriate standards such as those listed in clause 5.5.2.1, supplemented by the requirements needed to qualify fittings in accordance with this Standard.

5.5.2.5 One-piece forged or extruded tees are preferred when available. These should be manufactured in accordance with appropriate standards such as those listed in clause 5.5.2.1, supplemented by the requirements needed to qualify fittings in accordance with this Standard.

Note: These may be supplemented by such as Advantica T1/E, or T2/E for larger tees.

5.5.2.6 Where it is not reasonably practicable to use a forged or extruded tee, the following types of fitting are acceptable but should be subject to specific qualification, including stress analysis where applicable:

- inserted branch fitting (also known as set-in branch tee, or "sweepolet")

This type of fitting is acceptable for all pressure ranges but shall only be used for d/D ratios of the fitting not exceeding 0.6.

- forged butt welded outlet fitting

Although these fittings are, theoretically, acceptable for all pressures and fitting d/D ratios, particular precautions shall be applied for d/D greater than 0.3 when the proposed location in the linepipe shall be carefully examined for defects, including laminations

Note: It is imperative that the welding to the linepipe be carried out by a qualified welder to a qualified procedure.

- set-on branch fitting (also known as weldolet)

- full encirclement branch fitting (split tee)

This type of fitting is acceptable for all pressure ranges and for all ratios of d/D , provided the wrap-round plate completely encircles the main pipe. They shall be designed in accordance with such as ANSI/ASME B31.3.

- 5.5.2.7 Headers shall allow free passage of gauging pigs for which guide bars should be fitted if necessary.

Note: Typical design requirements are given in the standards listed in clauses 5.5.2.1 to 5.5.2.3.

5.5.3 **Impulse piping and fittings**

Fittings and piping for use on pressure-containing instrument and impulse pipework shall be to standards appropriate to the duty required, such as ASTM A 312 and BS EN 10216 with fittings to BS 4368.

5.5.4 **Other fittings**

- 5.5.4.1 Guidelines for production methods and property requirements for other specific classes of fittings shall be obtained by reference to an appropriate standard.

Note 1: Examples are:

- flanges to BS EN 1759-1, BS 3293, ANSI/ASME B16.5, ANSI/ASME B16.47, MSS SP-6, MSS SP-44, Advantica F1/E
- reducers to BS 1640-3, Advantica F3/E
- end caps to BS 1640-3, Advantica F8/E
- screwed and socket welded fittings to BS 3799.

Note 2: Some material specifications do not contain sufficient requirements to fully qualify fittings in accordance with this section with respect to, for example, toughness, dimensions, fatigue etc.

- 5.5.4.2 All bolting and gasket materials for flanged joints shall be in accordance with appropriate standards.

5.6 **COMPONENT SELECTION**

5.6.1 **General**

- 5.6.1.1 For flanged components, the safe maximum working pressure of each component shall be carefully checked to ensure it is not lower than the class rating of its flanges.

- 5.6.1.2 A corrosion-resistant label should be securely fastened to each component, by the manufacturer, to indicate identification number, size, type, class rating and/or maximum working pressure and proof test pressure. The method of attachment of the label shall not adversely affect the strength of the component.

5.6.2 **Insulating joints**

Guidance on the material requirements for insulation joints is provided in Advantica E17/E Parts 1 and 3.

- 5.6.2.1 The insulating joint shall perform its function effectively under all combinations of pressure and externally-applied stresses, as specified to the manufacturer.

- 5.6.2.2 The properties of dielectric materials shall satisfy the insulation requirements specified. They shall also be resistant to methanol and any constituent of gas under normal or abnormal conditions.

5.6.2.3 Where insulating joints are to be welded into a pipeline, the design of the weld preparations shall meet the requirements of an appropriate standard. The fitting shall be designed so as to avoid overheating of the insulation material during site welding.

5.6.2.4 All joints shall be hydrostatically and electrically tested and test certificates should be made available by the manufacturer. Conditions for hydrostatic testing should allow for free expansion of the joint. The duration of the hydrostatic test shall be in accordance with the requirements of Section 9. The hydrostatic test shall precede the electrical test.

5.6.3 **Pressure vessels**

5.6.3.1 Bodies of filters, scrubbers and separators shall meet an acceptable pressure-vessel standard, such as PD 5500 or BS EN 13445, taking account of the level of strength testing in Section 9.

5.6.3.2 The design shall ensure that flanged covers or quick-opening doors cannot be removed or opened while the unit is under any internal pressure.

5.6.3.3 Purge, vent and drain connections should be of adequate size, and suitably located in relation to the body. These connections should be designed to avoid the possibility of freezing-up and to ensure a reasonably short blow-down time.

5.6.4 **Valves and actuators**

5.6.4.1 Valves shall be of cast steel or of forged steel construction, have weld ends or flanges to BS EN 1759-1, and shall be manufactured from fine-grained steel in accordance with BS EN 10028 and BS EN 10029.

Reference should be made to ISO 14313 and to an appropriate standard for detailed design recommendations for high-pressure valves, such as Advantica V6/E, Parts 1 and 2.

5.6.4.2 Performance testing of valves should be carried out in accordance with ISO 14313.

5.6.4.3 All valves should be fitted with a device to indicate accurately the position of the plug, ball, gate or disc. Consideration shall be given to the need to drain the body of the valve.

Where it is necessary to lubricate a valve for continued satisfactory operation, seals shall be provided to minimise the amount of excess lubricant passing into the gas stream.

Note: This is especially important if metering is directly associated with the installation.

5.6.4.4 The dimensions of the flanged ends of valves shall meet the requirements of appropriate standards such as BS 3293, BS EN 1759-3 or BS EN 1514. Requirements for preparation of the ends of valves to be welded in-line should be specified to the manufacturer.

5.6.4.5 Valve bodies shall be hydrostatically tested under the conditions stated in the standard relevant to the type and pressure rating selected, and test certificates provided by the manufacturer.

5.6.4.6 Hydrostatic and pneumatic seat leakage tests shall be applied to all valves under the conditions stated in the relevant standards.

5.6.4.7 Care should be taken to ensure the correct matching of an actuator to a valve, both in terms of required torque and mechanical attachment. The conditions under which the valve is required to operate, including speed of action, should be specified to the manufacturer.

5.6.4.8 Where valves are ordered with actuators, stem extensions, gear-boxes etc, the valve manufacturer should be responsible for matching and fitting them and ensuring that each assembly functions correctly in the intended attitude(s). Removal of the actuator shall not affect the pressure-tightness of the valve.

5.6.4.9 Actuators shall be fully weatherproof. All electrical equipment shall be housed in a flameproof enclosure in accordance with Section 7. A mechanically-independent hand-operated drive should be provided as part of any actuator, and it should be so designed that a maximum effort of 350 N would be sufficient to operate the valve. Interlocks shall be provided to prevent local or remote automatic operation while the hand-operated drive is engaged.

5.7 **FACTORY - APPLIED COATINGS**

5.7.1 Reference should be made to appropriate standards, for example BS EN ISO 12944 for guidance on selection of materials and requirements for their application.

Note: High pH stress corrosion cracking (SCC) may occur under disbonded or porous coatings at elevated temperatures (generally greater than 30°C) where the applied CP creates an alkaline environment in the crevice beneath the coating.

5.7.2 Pipes and fittings should have the required internal and external protection applied at the manufacturer's works.

Materials that are factory-applied shall be compatible with those corrosion protection measures to be applied on site.

In selecting suitable materials, consideration shall be given to the operating regime and the eventual siting of the component, for example buried or above-ground, and the temperature range likely to be experienced.

Note: For example, some coating materials could be affected adversely by solar heating or exposure to ultraviolet radiation.

5.7.3 Coatings shall be tested according BS EN ISO 2813 for physical durability and resistance to chemical attack.

Note: Detailed requirements for corrosion protection are provided in Section 10.

SECTION 6 : DESIGN OF PIPELINES

6.1 GAS PRESSURE AND QUALITY

6.1.1 Control of gas pressure

Pressure shall be controlled to ensure that it is within the appropriate specified limits. IGE/TD/13 should be consulted for design considerations.

6.1.2 Gas quality

The following conditions shall be applied to avoid deposits in a pipeline and to minimise the possibility of any kind of corrosion, including internal stress corrosion:

- the water dew-point, at the operating pressure (OP), to be at all times below the temperature of the pipeline
- the hydrocarbon dew-point, at OP, to be at all times below the temperature of the pipeline

Note: This will also ensure that the calorific value of the gas is not reduced by condensation of hydrocarbons

- gas to be dust-free.

Oil fog should be prevented from passing forward from compressors.

Note: In the UK, GS(M)R contain requirements for gas quality.

6.2 DESIGN VELOCITY

6.2.1 With gas of the quality prescribed in clause 6.1.2, there is no necessity to limit the design velocity. Where dust particles, which could cause abrasion, may be present, arising either from the gas source or from the possibility of the formation of corrosion products within a pipeline, consideration shall be given to limiting the gas velocity in any section of the pipeline where changes of direction take place.

Note: Normally, velocities up to 20 m s⁻¹ are acceptable, even if some dust is present.

6.3 SIZING OF LINEPIPE

Initial sizing should be based on a simple steady-state concept.

Note: The method of determining the required size of pipe, for a given pipeline, will depend on a number of interacting technical and economic criteria.

A number of formulae have been developed for relating pressure drop to gas flow rate, for example Weymouth, Panhandle, Spitzgass, Oliphant and Unwin, which should be used for this purpose.

Note 1: Disc calculators based on these formulae are available, which give sufficiently accurate results for short pipelines. Pipelines over 50 km long require greater accuracy and the use of Panhandle "A", Panhandle "B" or AGA flow formulae is recommended. In particular, this is true where re-compression stations are required.

Note 2: It may be necessary to determine the influence of additional factors to cater for transient flow conditions, which may involve subjecting the system to analysis. By this means, the pipe dimensions necessary to cater for credible fault and planned abnormal operation conditions can be established. Other factors which may need to be considered include any intended use of a pipeline for line pack storage, the location of points of associated high volume storage along a pipeline and the manner of introduction and use of re-compression plant in a pipeline.

6.4 WALL THICKNESS OF LINEPIPE

6.4.1 The minimum wall thickness of linepipe shall be considered to be the nominal wall thickness less the maximum tolerance for under-thickness of the wall.

Note: These factors are given by the relevant linepipe specifications.

6.4.2 The minimum wall thickness of linepipe shall be equal to or greater than the design thickness as determined from:

$$t = PD(20fs)^{-1}$$

- t = design thickness of pipe wall (mm)
- P = design pressure (bar), at the relevant design temperature
- D = outside diameter of the pipe (mm)
- s = SMYS (N mm⁻²)
- f = a factor not to exceed 0.8 but which may have to be reduced considerably by restrictions given below.

Note: For a pipeline operating in the range 0.72 < f ≤ 0.8, clause 6.7.4.3 applies.

In any event, to prevent problems during handling and trenching, the nominal thickness of linepipe shall not be less than indicated in Table 4.

OUTSIDE DIAMETER (mm)		LEAST NOMINAL WALL THICKNESS (mm)
Exceeding	Not exceeding	
	168.3	4.78
168.3	457.2	6.35
457.2	608.6	7.92
609.6	914.4	9.52
914.4	1066.8	11.91
1066.8	1219.2	12.70

TABLE 4 - LEAST NOMINAL WALL THICKNESS OF LINEPIPE

6.5 ADDITIONAL LOADS

6.5.1 Classification of loads

Design and construction of pipelines to this Standard will, inevitably, eliminate many sources of additional loading through careful routing and standard depth of cover. Where particular constraints apply and additional loading has to be accommodated, the design shall anticipate, and the pipeline shall be able to withstand, the following additional loads:

- (a)
 - operating loads, including;
 - thermal expansion and contraction loads. Provision shall be made for the effects of thermal expansion or contraction. Account should be taken of stresses induced as a result of restriction of free thermal movement owing to restraints, for example underground bends and underground swan necks
 - weight of the pipeline
 - the soil dead weight loading due to the depth of cover
 - construction loads arising from;
 - impact protection slabs
 - pipe laying and alignment, for example tie-in connections
 - differential settlement due to variable support arising from trench bottom and bedding conditions

- pressure testing and
- (b) • Environmental loads arising from:
 - subsidence or settlement due to mining activities, de-watering, or the action of additional surface loads, typically embankments
 - subsidence due to the pipe being laid on top of disturbed or built up land, taking into account the effects of differences in support between existing pipe and modified pipe at a tie in interface
 - slope instability
 - frost heave
 - buoyancy
 - live loading from vehicles
 - earthquakes.

Note: Environmental loading may change during the service life of a pipeline.

For in-service pipelines, the effects of any additional load shall be determined and assessed for acceptability.

Any uncertainty in loads and displacements, other than design or operational values, shall be taken into account in order to demonstrate that the resultant analysis is acceptable.

6.5.2 Calculation of stresses

6.5.2.1 Circumferential (hoop and bending), longitudinal (axial and bending), shear and equivalent stresses shall be taken into account to demonstrate that the resultant analysis is acceptable.

Note: For a pipeline affected by external loads, the worst case may occur in the depressurised condition, i.e. zero internal pressure.

6.5.2.2 Stress analysis shall include any restraints on the pipeline including anchors, supports, sleeves and the soil. The flexibility and stress intensification at bends shall be included in the analysis.

6.5.2.3 Any uncertainty range shall be established for restraints and incorporated in the pipeline strength calculation.

6.5.2.4 Structural flexibility and stresses shall be based on nominal dimensions and a modules of elasticity at ambient temperature.

Equivalent stresses shall be calculated as follows:

$$\sigma_{eq} = \sqrt{\sigma_c^2 + \sigma_L^2 - \sigma_c \cdot \sigma_L + 3\tau^2}$$

- σ_{eq} = von Mises (equivalent) stress
- σ_c = circumferential stress
- σ_L = longitudinal stress
- τ = shear stress in plane of pipe cross section.

6.5.3 Acceptance criteria

Note: Alternative criteria to that given below, such as limit state design or allowable strain, may be used where it can be demonstrated that the criteria are relevant and applicable.

6.5.3.1 The maximum allowable through-wall circumferential (hoop) stress should meet the design factor set out in Sub-Section 6.7.

6.5.3.2 The maximum equivalent stress for membrane components should meet:

$$\sigma_{\text{eq}} \leq 0.8 \text{ SMYS where } \sigma_{\text{eq}} = \sqrt{\sigma_h^2 + \sigma_a^2 - \sigma_h \cdot \sigma_a}$$

σ_{eq} = equivalent stress
 σ_h = hoop stress due to internal pressure
 σ_a = through-wall component of the longitudinal stress.

Note: The objective of this condition is to ensure a factor of safety of 1.25 against gross section yield.

6.5.3.3 The maximum equivalent stress for total stresses (membrane and bending) should meet:

$$\sigma_{\text{eq}} \leq 0.9 \text{ SMYS.}$$

Note: See clause 6.5.2.4.

6.5.3.4 For the assessment of ovalisation, the radial deflection shall not exceed 5% of the nominal pipe diameter.

6.6 FATIGUE

6.6.1 General

6.6.1.1 Consideration shall be given to the fatigue life of any pipeline, to ensure that any defect which survives the hydrostatic test, or which is not detected by subsequent internal inspection, does not grow to a critical size under the influence of pressure-cycling.

Special consideration should be given to the adequacy of fittings.

Note: Generally, fittings are designed to a standard which will ensure that they experience lower stress ranges than linepipe when a pipeline is pressure-cycled. Where such circumstances prevail, fittings need not be subjected to a fatigue evaluation.

6.6.1.2 Consideration shall be given to other sources of cyclic stressing, for example thermal loading immediately downstream of a compressor station, which may affect the fatigue life of a pipeline. Specialist advice shall be obtained if these are likely to be significant, as the guidance in clause 6.6.2 is appropriate only for pressure-cycling.

6.6.2 Definition of fatigue life

Fatigue life may be defined by the simplified approach described in clause 6.6.2.1, provided the pipeline has been hydrostatically tested to the requirements of Table 8 and is constructed from linepipe purchased to clause 5.3.1. Alternatively, a detailed fracture mechanics calculation, as described in clause 6.6.2.2 should be used if:

- the pipeline has been hydrostatically tested to a level lower than specified in Table 8, or
- the pipeline will experience maximum stress ranges in excess of 165 N mm^{-2} .

The required fatigue life of the pipeline shall be defined in terms of allowable pressure (stress) ranges and associated numbers of cycles. For the purposes of this Standard, a 40-year life has been assumed but other lives may be appropriate in which case they should be documented.

Note: Where the maximum daily hoop stress range is less than 35 N mm^{-2} , a fatigue assessment is not required.

6.6.2.1 *Simplified approach*

(a) Constant daily pressure-cycling

Where the magnitude of daily pressure-cycling is constant, the fatigue life should be determined from:

$$S^3N = 2.93 \times 10^{10}$$

S = constant amplitude stress range (N mm⁻²)
 N = number of cycles.

Note: For example, if a life of 15,000 stress cycles is required (equivalent to one cycle per day over 40 years), the equation limits the maximum daily variation in hoop stress to 125 N mm⁻².

(b) Variable pressure-cycling

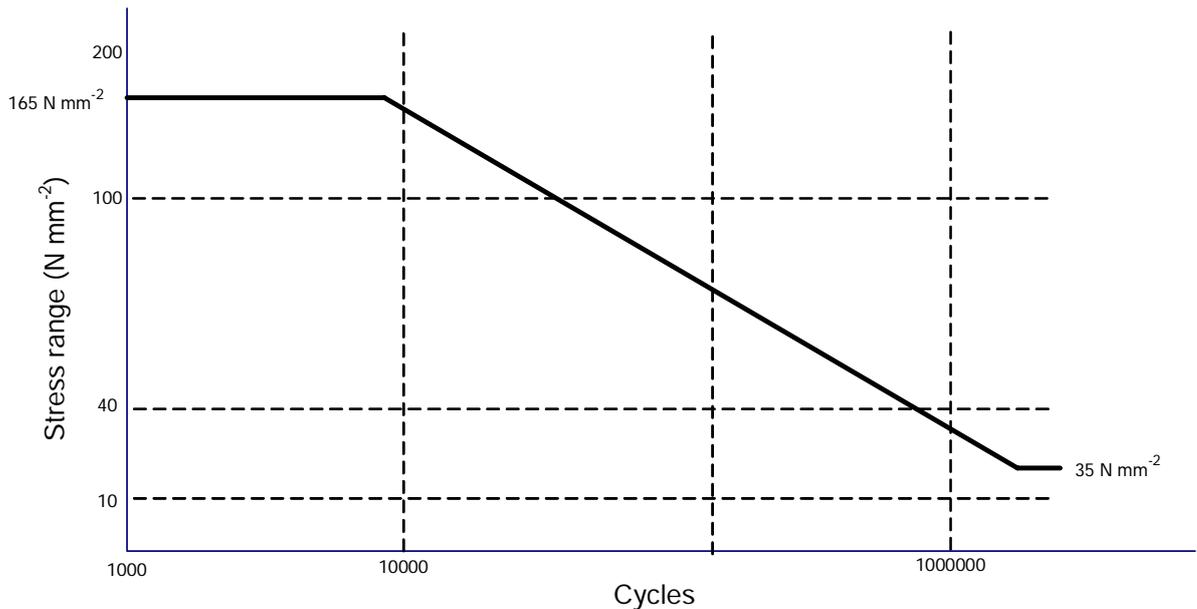
Where the magnitude of daily pressure cycling is not constant, the fatigue life should be evaluated on the basis of (a) above, by totalling the usage of fatigue life from each stress range.

The following condition for the damage fraction should be satisfied to obtain an acceptable fatigue life.

$$D_F = \sum \frac{n_i}{N_i} \leq 1.0$$

n_i = the actual number of cycles accumulated at stress range S_i
 D_F = damage fraction
 S_i = stress range (see N_i and n_i)
 N_i = number of stress cycles allowed at stress range S_i (clause 6.6.2.1(a)).

If the anticipated value of D_F exceeds 0.5, the actual cycles accumulated during operation should be determined in accordance with clause 6.6.3.



Note: This drawing is for illustrative purposes only and is not suitable to derive values.

FIGURE 3 – RELATIONSHIP BETWEEN STRESS RANGE AND NUMBER OF CYCLES

6.6.2.2 *Detailed fracture mechanics approach*

Where the maximum daily stress range exceeds 165 N mm^{-2} , and/or the simplified method in clause 6.6.2.1 is not appropriate or where it is required to assess the fatigue life of defects detected in service, a detailed fracture mechanics calculation should be used to determine the fatigue life.

Note: Recommended methods for such a calculation are given in BS 7910.

Account should be taken of the deleterious effect of pipe ovality and local shape deviations.

The analysis method, material properties and other input data used in the assessment should be documented and fully justified.

The actual cycles accumulated during operation should be determined in accordance with clause 6.6.3.

6.6.3 **Definition of stress cycles**

Any complex (variable amplitude) stress cycles should be recorded and then converted to an equivalent spectrum of constant amplitude stress cycles using a documented algorithm such as the Reservoir or Rainflow method. The appropriate method (see clause 6.6.2) should then be used to define the fatigue life.

Note: Further details of these algorithms are given in ASTM E1049-85.

6.6.4 **Revalidation**

When records or estimates show that the design fatigue life has been reached, the pipeline shall be revalidated by testing in accordance with Section 8, or by internal inspection using a tool capable of the detection of longitudinal crack-like defects, particularly in or near the seam weld. If inspection is used, the detection limits for crack-like defects shall be taken into account when establishing the future fatigue life of the revalidated pipeline (see also Section 11).

6.7 **AREA TYPES AND DESIGN CRITERIA**

6.7.1 **Area types**

6.7.1.1 The location adjacent to a pipeline should be categorized according to population density and/or the nature of the immediate surrounding area. The following designated areas should be used:

- Type R Rural areas with a population density not exceeding 2.5 persons per hectare
- Type S Areas intermediate in character between Types R and T in which the population density exceeds 2.5 persons per hectare and which may be extensively developed with residential properties, schools, shops etc.
- Type T Central areas of town or cities, with a high population density, many multi-storey buildings, dense traffic and numerous underground services.

Note: The area types require different design criteria, with particular reference to operating stress level and proximity.

6.7.1.2 Special consideration should be given to areas where the population may be concentrated or clustered close to the pipeline route, especially in rural areas

where the average population may be 2.5 persons/hectare or less. In such cases, the method of population density assessment may lead to an anomaly in classification of location when consideration shall be given to a more stringent classification than would be indicated by population density alone.

Note: An example of this would be where a reduction in MOP would result in a Type R area pipeline being re-classified as a Type S area pipeline i.e. ribbon developments where the population density distribution is higher close to the pipeline.

6.7.1.3 Where a pipeline route is considered generally to conform to a Type S area classification but displays Type T area characteristics or has other unique features, it shall be subject to detailed assessment by means of risk analysis carried out as part of a safety evaluation.

These assessments shall consider all issues including failure credibility and the distribution of population densities along the pipeline route.

6.7.2 **Estimation of population density**

6.7.2.1 The population density, expressed as the number of persons per unit area, shall be the average within a 1.6 km strip centred on the pipeline of a width 8 times the minimum building proximity distance (BPD) for a Type R area pipeline as defined in Figure 4.

Note: For MOP exceeding 100 bar, Figure 4 may be extended by linear extrapolation using the correlations provided to define the width of the strip used in calculating population density.

6.7.2.2 Measurement of population density shall be based on a survey, for example by aerial photography, of normally occupied buildings and premises where people congregate for significant periods of time, for example schools, public halls, etc.

6.7.2.3 The occupancy of houses should be determined from Census statistics, although the occupancy of typical houses may be assumed to be 3 persons per dwelling.

The occupancy of other buildings shall be assessed.

6.7.3 **Boundaries**

In order to determine the precise boundary between Type R and Type S areas, the population density shall be calculated within circles of diameter 8 times the minimum BPD determined from Figure 4, or the 0.3 cpm individual risk contour (see clause 6.7.2.1). By considering such circles in sequence outwards from the high-density area, the circle within which the population density first falls below 2.5 persons per hectare shall be determined. The centre of the circle shall be taken as the boundary of the Type S area.

6.7.4 **Design of pipelines in Type R areas**

6.7.4.1 *General*

Normally, pipelines should be designed to a maximum design factor of 0.72 (see clause 6.7.4.2).

Note: Under certain conditions and/or circumstances, consideration may be given to a maximum design factor of 0.8 (see clause 6.7.4.3).

6.7.4.2 *For a design factor not exceeding 0.72*

The minimum proximity of pipelines to normally-occupied buildings shall be related to MOP and be as defined in Figure 4, except that Figure 5 may be used if either:

- the pipeline has a design factor not exceeding 0.3, or
- the pipeline has a design factor not exceeding 0.5 (but exceeding 0.3) and a wall thickness of not less than 19.05 mm, or

alternatively, proximity shall be justified by a risk analysis as part of a safety evaluation (see Sub-Section 6.10).

Note: Safety evaluation in this context is defined as a full risk assessment of the section of pipeline being considered, taking account of all factors affecting safety. Normally, it is not intended to mean a safety evaluation of the whole pipeline.

A safety evaluation of the whole pipeline should be carried out for design pressures greater than 100 bar (see Appendix 3)

In any event, the proximity distance shall not be less than 3 m.

6.7.4.3 *For a design factor exceeding 0.72, but not exceeding 0.8*

In addition to the recommendations in clause 6.7.4.2, structural reliability analysis (SRA) should be undertaken, in accordance with Appendix 4.

Note: The SRA may be subject to regulatory review.

6.7.5 **Design of pipelines in Type S areas**

6.7.5.1 Normally, pipelines should be designed to a maximum design factor of:

- 0.3 or
- 0.5 for pipelines having a wall thickness of not less than 19.05 mm.

Note 1: A higher design factor (but not exceeding 0.72) may be justified by a risk analysis as part of a safety evaluation (see Sub-Section 6.8 and Appendix 3).

Note 2: Safety evaluation in this context is defined as a full risk assessment of the section of pipeline being considered, taking account of all factors affecting safety. Normally, it is not intended to mean a safety evaluation of the whole pipeline.

6.7.5.2 When uprating a pipeline, design factors exceeding 0.72 but not exceeding 0.8 may be used if justified by a structural reliability analysis and risk analysis (see Appendices 3 and 4). However, design factors in this range should not be used unless the pipeline is located predominantly within Type R areas with only minor excursions in Type S areas.

Note: "Minor excursions" in Type S areas are where a pipeline route is considered, in general, to conform to a Type R area classification but displays Type S characteristics. Examples of features associated with such minor excursions are:

- a short length of affected pipeline
- affected length of pipeline in predominantly agricultural land
- low population density, albeit in excess of 2.5 persons per hectare
- population concentration beyond the Type R proximity distance defined in Figure 4 (see also clause 6.7.1).

6.7.5.3 The minimum proximity of pipelines to normally-occupied buildings shall be related to MOP, and be as defined in Figure 5.

In any event, the proximity distance shall not be less than 3 m.

6.7.5.4 A pipeline designed to operate in Type S areas should be capable of internal inspection. If this is not practicable, provision shall be made such that the pipeline can be subjected to above-ground inspection (see clause 11.6.3.6).

6.7.6 **Design of pipelines in Type T areas**

A pipeline in a Type T area shall be designed, constructed, operated and maintained in accordance with IGE/TD/3.

6.7.7 **Proximity from wind turbines**

The minimum proximity distance between any pipeline and a wind turbine should be 1.5 times the mast height of the wind turbine.

6.7.8 **Deviation from prescribed proximity criteria**

If the prescribed criteria (see clauses 6.7.4 to 6.7.6) is to be relaxed, following a risk analysis during the initial design of a new pipeline, consideration shall be given to any required remedial work that may be necessary at an earlier stage during the life of the pipeline, as some of the margins will have been reduced.

Note 1: Refer to Sub-Section 6.8.

Note 2: This will tend to increase the whole life cost of the pipeline.

6.7.8 **Sensitive locations**

Careful consideration shall be given to pipelines in the vicinity of sensitive locations which may result in a change of pipeline design; for example location, wall thickness, proximity, protection, etc.

Note: Development of such locations during service could have a serious impact on pipeline operation.

6.7.10 **Seismic activity**

6.7.10.1 Consideration shall be given to the effects of seismic loading on pipelines located in areas where earthquakes may occur. Seismic loading can result from ground shaking during the earthquake event, followed by permanent ground movements resulting from the earthquake, which may include displacement of geological faults, soil liquefaction and landsliding associated with soil and slope instability.

6.7.10.2 In areas considered susceptible to earthquakes, full geological and seismological investigations should be carried out to identify pre-existing faults and their potential for movement, soil type and strata and the existence of any areas susceptible to landsliding in the vicinity of the fault. Analysis of historical seismic data should be carried out to assess the likelihood of occurrence within a return period of 1000 years of an earthquake of magnitude which may damage the pipeline and, hence, if necessary identify the earthquake design case.

6.7.10.3 Where the likelihood of a damaging earthquake is considered significant, the static and dynamic effects of ground shaking should be considered on above ground pipework and plant, and the static effects of potential permanent ground movement should be considered on the above ground and buried pipeline sections which may be affected. The analysis of buried pipeline sections should include pipe-soil interaction effects. The analysis should assess whether the pipeline section has sufficient flexibility to accommodate design case displacements, and whether the magnitude of stresses and strains which may be induced are acceptable.

Certain types of structure, by reason of their function, location or form, may warrant explicit consideration of seismic activity. For further information on these circumstances and assessment methods, reference should be made to EN 1998-4 and BS EN 1594.

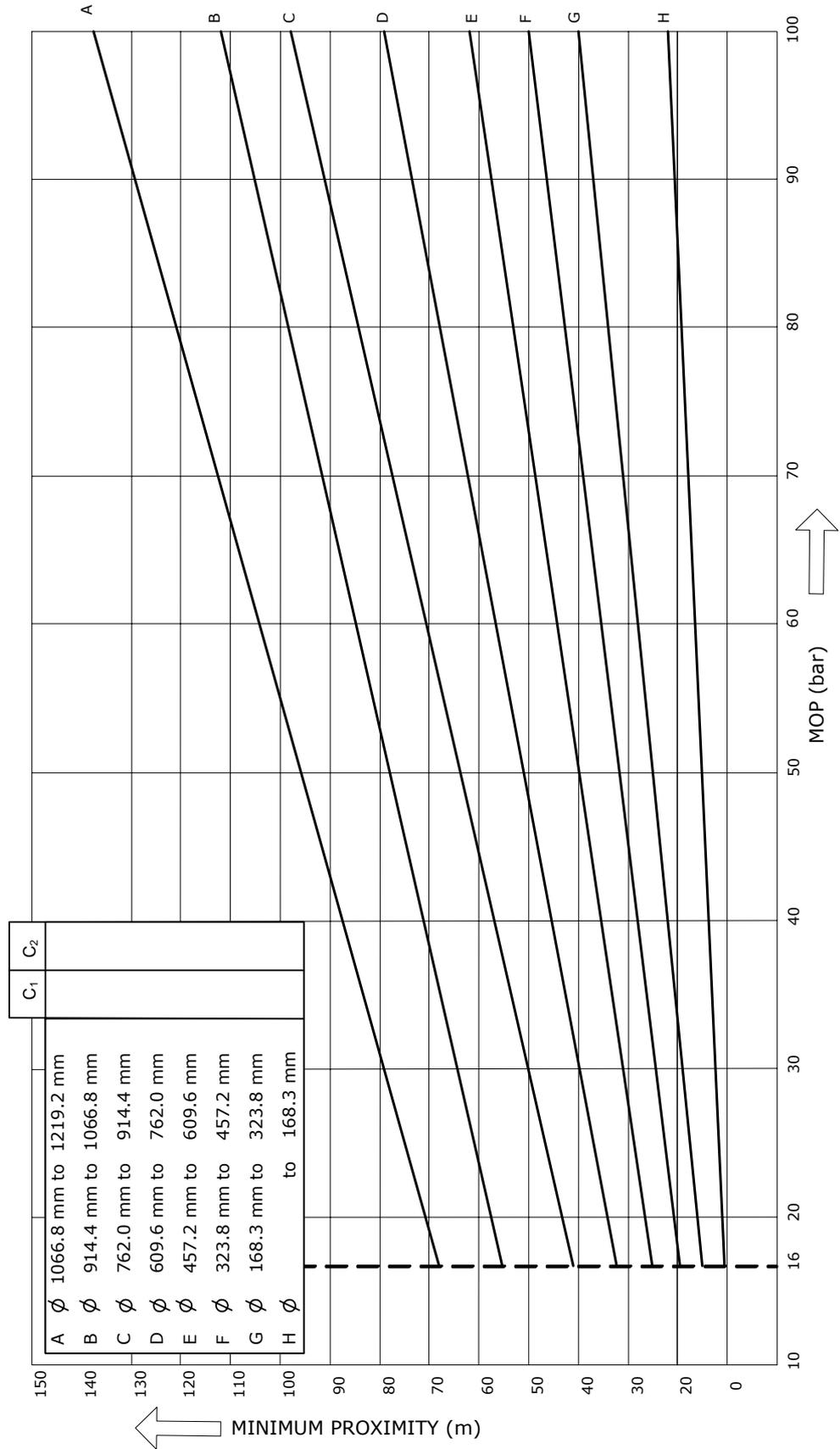
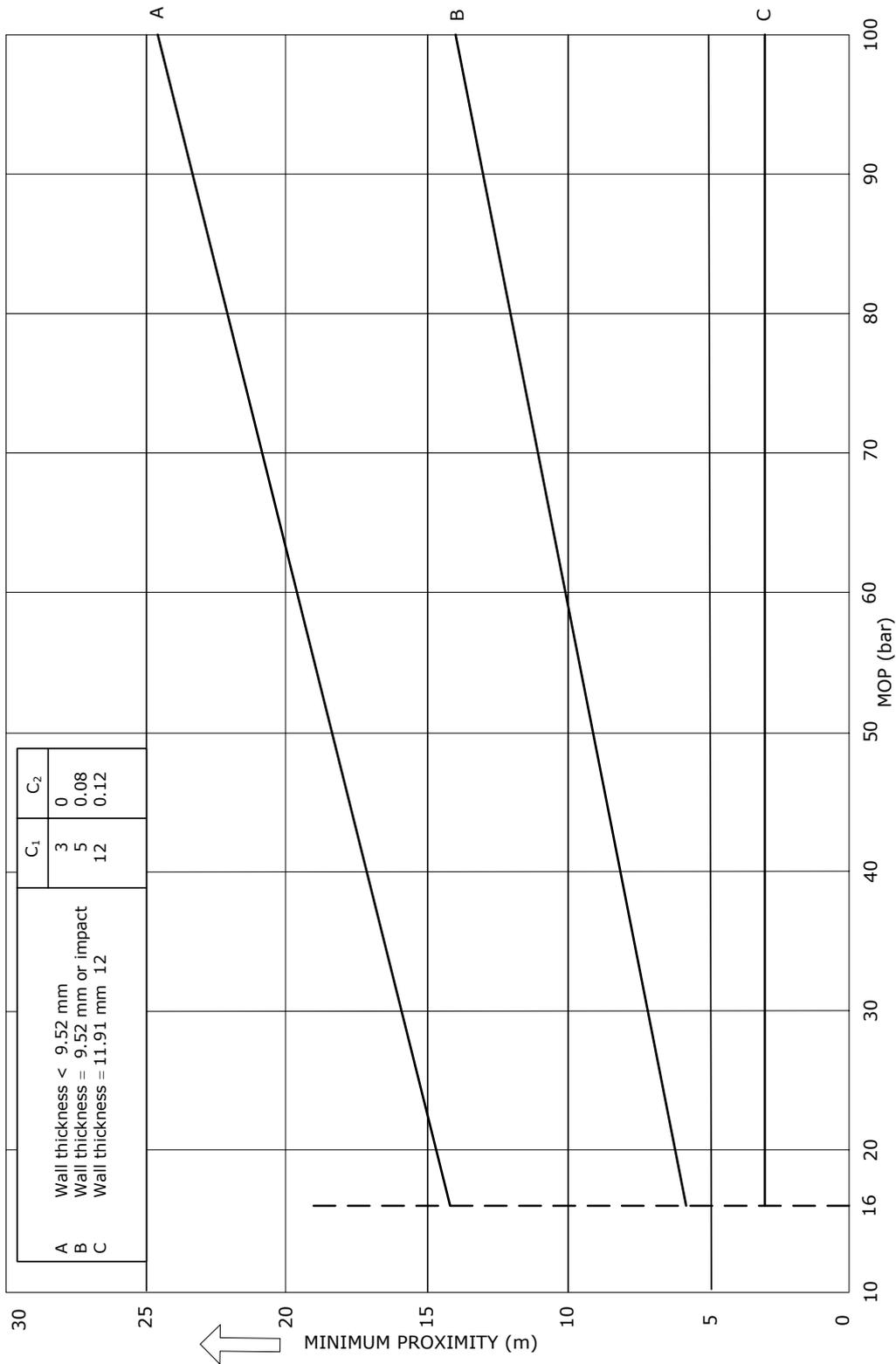


FIGURE 4 - MINIMUM PROXIMITY DISTANCE FROM NORMALLY-OCCUPIED BUILDINGS OF PIPELINES DESIGNED TO OPERATE IN TYPE R AREAS



Note 1: For design factor not exceeding 0.3 and nominal wall thickness < 9.52 mm, a pipeline can be operated with proximities derived from curve B, provided that additional protection is installed in accordance with Sub-Section 6.8.

Note 2: A pipeline with a wall thickness < 11.91 mm may be operated with proximities less than those derived from lines A or B (but not less than that of line C) if this can be justified by a risk analysis carried out as part of a safety evaluation (see Sub-Section 6.8).

MINIMUM BUILDING PROXIMITY DISTANCE = C1 x C2 x MOP

FIGURE 5 - MINIMUM PROXIMITY DISTANCE FROM NORMALLY-OCCUPIED BUILDINGS OF PIPELINES DESIGNED TO OPERATE IN TYPE S AREAS

6.8 RISK ANALYSIS

Any risk analysis performed as part of a safety evaluation shall take into account the frequency and consequences of all significant pipeline failure modes. Care should be taken to ensure that the methodology adopted is consistent with the criteria used to assess the results.

It is not intended that risk analysis is used to justify deviations from the design criteria included in this Standard. Where the design requirements cannot be achieved, risk analysis may be used to investigate and justify alternatives. In such cases, the justification for any deviation from the design requirements shall be fully documented and include an "as low as reasonably practicable" (ALARP) assessment.

Note 1: Guidance on risk assessment techniques and criteria is given in Appendix 3 together with examples. Further information can be found in IGE/SR/24.

Note 2: The results of such a risk analysis may need to be considered by the relevant statutory

6.9 IMPACT PROTECTION AGAINST 3RD PARTY INTERFERENCE

6.9.1 Protection against 3rd party interference can be an effective means of reducing the likelihood of third party damage at, for example, road crossings, sensitive locations, etc.

When protection is to be provided, commonly used methods are:

- protection slabs including concrete slabs and slabs without side supports
- marker tape
- heavy wall pipe
- increased cover
- concrete surround.

Note: Additional protection can affect the efficiency of above-ground surveys, such as Pearson Surveys and close interval potential surveys (CIPS).

The form of protection shall be selected to suit the circumstances, by undertaking a site-specific risk analysis.

6.9.2 In Figure 6, which shows typical protection slab design, "h" should, be not less than 500 mm which is considered to be the length of the drill bit of a hand-held pneumatic jackhammer. The dimension "h" should be taken from the highest layer of reinforcement within the slab to the pipe.

6.9.3 The overall width of the protection should be adequate to guard against lateral encroachment from excavating machinery.

6.9.4 The reinforcing shown in Figure 6 is indicative only and should be designed for each situation. If pre-cast concrete slabs are used, consideration should be given to stresses due to handling and any additional reinforcement should be provided as required.

6.9.5 When using the "slab with side supports" protection (Figure 6), the reinforcement should be designed and positioned to suit the method of construction.

6.9.6 The use of any protection measure may alter the distribution and intensity of external loads around the pipe. The design should consider such effects and demonstrate that they do not result in unacceptable stresses within the pipe.

Note: In particular, this is important where construction or other traffic loading may arise.

6.9.7 Care should be taken during design and installation to ensure that the satisfactory operation of any CP system will not be affected.

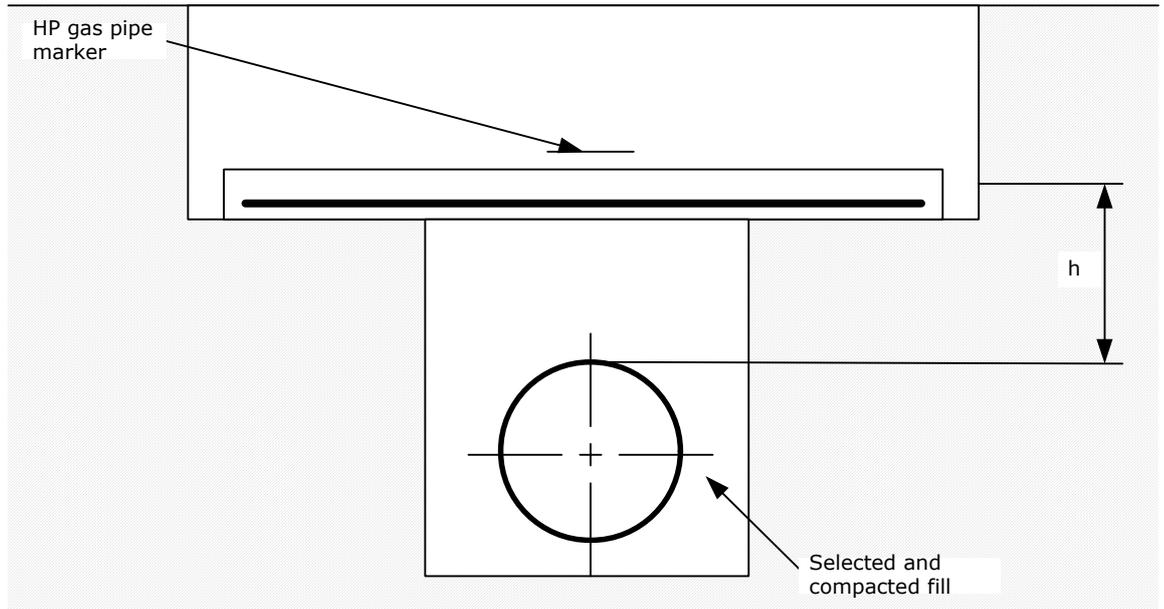


FIGURE 6(a) - Concrete

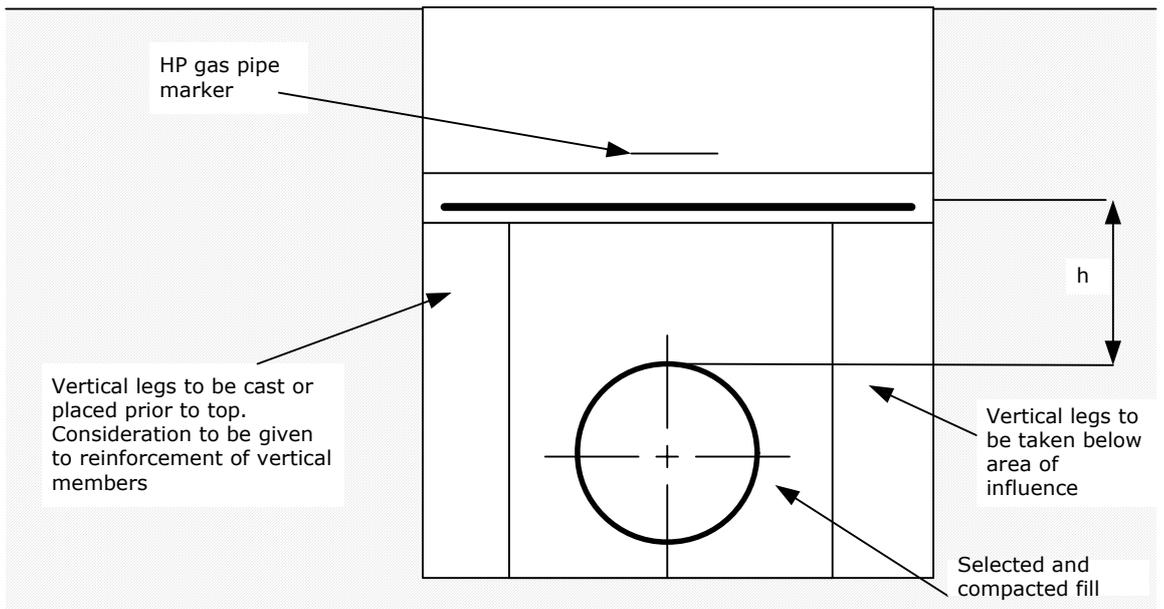


FIGURE 6(b) - Slab with support

FIGURE 6 - COMMONLY USED FORMS OF IMPACT PROTECTION FOR PIPELINES

6.10 **TRAFFIC ROUTES (including roads and railways)**

6.10.1 **Pipelines crossing/encroaching within traffic routes**

6.10.1.1 Two categories of traffic route have been designated according to the traffic density. The decision as to which category a particular route belongs should be

made taking account of the risk of interference and diurnal or seasonal variations in traffic density.

6.10.1.2 A pipeline which either crosses, or encroaches within, the appropriate minimum proximity distance of a high density traffic route, shall have a nominal wall thickness of not less than 11.91 mm.

A pipeline which either crosses or runs within the boundary of other traffic routes shall either have a nominal wall thickness of not less than 9.52 mm or shall be provided with impact protection in accordance with Sub-Section 6.9. Normally, the design factor shall not exceed:

- 0.3 or
- 0.5 for pipelines with a nominal wall thickness of not less than 19.05 mm.

Alternatively, a higher design factor (but not exceeding 0.8) may be justified by a risk analysis as part of a safety evaluation (see Sub-Section 6.8 and Appendix 3).

Note: Safety evaluation in this context is defined as a full risk assessment of the section of pipeline being considered, taking account of all factors affecting safety. Normally, it is not intended to mean a safety evaluation of the whole pipeline.

6.10.1.3 In assessing any change to a traffic route, the risk level must be equivalent to (or less than) the minimum of that for a pipeline complying with IGEM/TD/1 with:

- a design factor of 0.3 or
- a design factor of 0.5 and a minimum nominal wall thickness of 19.05 mm.

Note 1: The assessment should demonstrate that the risk levels are within the equivalent levels for a pipeline complying with IGEM/TD/1, or that the risk levels are ALARP (see A3.2).

Note 2: The safety evaluation of the pipeline has to be agreed by the pipeline operator, who holds the statutory duty under PSR for the safe management of the pipeline.

Any additional thickness shall be extended beyond the edge of the carriageway or railway track. This extension shall ensure that no part of the unmodified pipeline is closer than the minimum proximity distance derived from Figures 4 or 5, as appropriate to the design conditions of the unmodified pipeline. The distance should be measured from the edge of the carriageway or the outer rail of railway track. Where the hard shoulder is used by traffic as part of motorway widening or increased utilization schemes, the distance should be measured from the edge of the hard shoulder.

6.10.2 **Pipelines running parallel to other traffic routes**

Normally, special precautions are not required for a pipeline running parallel to another traffic route, but consideration shall be given to such precautions if the pipeline route is at any point inside the boundary of the traffic route.

6.10.3 **Water course crossings**

6.10.3.1 Pipeline crossings of rivers and canals that convey waterborne commercial or recreational traffic shall be classified as a traffic route and assessed using clause 6.10.1 as general guidance with regard to density of traffic, design factor and pipe wall thickness.

6.10.3.2 The design of water crossings shall identify all foreseeable events, the likelihood and consequence of such events taking place and mitigation of identified risks.

6.10.3.3 The design of water crossings shall not be less onerous than that required for the land pipeline and should take into account the following additional features within the selected pipeline crossing route corridor:

- type and intensity of shipping, fishing and other commercial or recreational activities
- geology, environmental, currents, stability and erosion of banks and beds
- ship anchoring, dredging and dumping
- presence of other services
- installation methods, loads and stresses, buoyancy effects, stability analysis
- coating, corrosion protection requirements
- operational requirements, including consideration of isolating line valves at each side of a crossing.

6.11 PIPELINES RUNNING PARALLEL TO OTHER MAJOR PIPELINES

Where practical, new pipelines should be routed to avoid running closely parallel with existing major pipelines (see clause 4.1.2). Where this is impractical, construction of a new pipeline in parallel with an existing one is acceptable where a sufficient separation distance between the two pipelines can be maintained to limit the possibility of escalation in the event of a failure.

The minimum separation distance required to prevent escalation is a complex function of the pipeline parameters and ground conditions. Reference to Table 5 should be made for guidance on the maximum interaction distance expected for a range of pipeline diameters and ground conditions for buried Natural Gas pipelines of MOP up to 80 bar.

Provided that the separation distance between the centreline of the larger diameter pipeline and the nearest point on the circumference of the other pipeline is greater than the maximum interaction distance estimated for the larger diameter pipeline, escalation as a result of a failure on one pipeline interacting with the other can be considered extremely unlikely. Where these minimum distances cannot be achieved due to practical constraints, specialist advice should be sought.

PIPELINE DIAMETER (mm)	MAXIMUM INTERACTION DISTANCE (m)		
	SOIL TYPE		
	Sandy	Mixed	Clay
273	7	5	3
324	7	5	3
406	8	5	3
457	8	5	3
610	8	5	4
762	9	6	5
914	10	6	6
1067	11	7	7
1219	12	8	8

Note 1: The table is applicable to parallel Natural Gas pipelines only. Situations where a Natural Gas pipeline is parallel to a pipeline transporting another gas or liquid (or where MOP for a Natural Gas pipeline exceeds 80 bar) are outside the scope of this simple guidance and have to be assessed on a case-by-case basis.

Note 2: The calculated separation distances assume that both pipelines are at the same depth and that this depth is approximately as given in IGEM/TD/1

TABLE 5 - MAXIMUM INTERACTION DISTANCE (m) FOR PARALLEL NATURAL GAS PIPELINES. MOP ≤ 80 bar

6.12 SLEEVING

6.12.1 General

- 6.12.1.1 Where a pipeline is to cross a major obstacle such as a road, railway, river, etc., pipe of increased wall thickness should be used in preference to sleeving. A sleeve should be used only when required to facilitate construction of a carrier pipe.

Note: Existing sleeves which meet the Class 1 or Class 2 design requirements of IGEM/TD/1 Edition 2 may continue to be used to allow the pipeline to operate up to its original design factor.

- 6.12.1.2 Where uprating of a pipeline above the original design factor would cause an existing sleeve to exceed its design limit, risk assessment shall be used to determine acceptability at the increased design factor.

- 6.12.1.3 If a sleeve is to exceed 150 m in length or the incorporation of a bend is required, specialist advice should be sought.

- 6.12.1.4 The sleeving of valves, tees and isolating joints is not considered practicable and such items should not be included in construction sleeves.

6.12.2 Selection of a sleeving system

- 6.12.2.1 Where it is considered necessary to install a sleeve to facilitate construction, preference should be given to the use of grouted concrete pipe to reduce the CP problems inherent with steel sleeving.

- 6.12.2.2 Where a concrete sleeve cannot be used, the steel sleeve and carrier pipes shall be designed and constructed to maintain electrical isolation between them.

The carrier pipe should be coated using approved materials and procedures, installed so as to avoid damage to the coating, and the annulus grouted with cementitious material.

Test cable attachments should be made to the sleeve and carrier pipes to enable suitable monitoring to be carried out.

- 6.12.2.3 Where a grouted steel sleeve cannot be installed, steel sleeves may be designed for nitrogen filling, in which case forged end-seals shall be fitted. Both the factory and field-applied coatings for the sleeve shall be chosen to avoid damage during construction, as the sleeve will form part of the CP system for the pipeline.

Note: Corrosion protection of the carrier pipe within the sleeve will be provided by the inert nitrogen-filled environment.

6.12.3 Materials and standards

- 6.12.3.1 Plastic pipes shall not be used for sleeving as this will prevent CP of the carrier pipe within.

- 6.12.3.2 Concrete sleeve sections should be made to BS 5911 and be designed for the fill and surcharge loads and for the type of bedding.

6.12.4 Sleeve diameter

The internal diameter of a sleeve shall exceed that of the external diameter of the carrier pipe by at least 150 mm. Consideration shall be given to a diametral

difference of 300 mm where constructional difficulties may arise, for example in a long sleeve.

6.12.5 Sleeve length

6.12.5.1 The length of a sleeve shall be the minimum necessary for construction of the carrier pipe.

6.12.5.2 The nominal wall thickness of a steel sleeve shall not be less than that indicated in Table 6, in order to protect against damage by mechanical plant and/or provide adequate strength for handling.

OUTSIDE DIAMETER OF SLEEVE (mm)		LEAST NOMINAL WALL THICKNESS (mm)
Exceeding	Not exceeding	
	457.2	6.35
457.2	609.6	7.92
609.6	914.4	9.52
914.4	1066.8	11.91
1066.8	1219.2	12.70
1219.2	1422.4	15.87

TABLE 6 - LEAST NOMINAL WALL THICKNESS OF STEEL SLEEVES

6.12.6 Carrier pipe support

6.12.6.1 A suitable support system shall be designed to enable the carrier pipe to be installed, and to remain supported adequately and positioned within the sleeve.

6.12.6.2 Support shall be capable of withstanding the mechanical loads that arise due to the weight of the carrier pipe when filled with water (for hydrostatic testing) and the forces caused by the relative movement of the carrier pipe normal to, or along, the pipe axis during construction, without causing damage to the protective coating of the carrier pipe.

6.12.6.3 The support system shall be designed such that the carrier pipe is supported adequately around the circumference, is positioned concentrically within the sleeve, and the flow of grout through the annulus during grouting is unimpeded as far as practicable.

6.12.6.4 Where a steel sleeve is used, the spacer support system shall provide and maintain electrical isolation between the sleeve and carrier pipes.

6.12.7 End-seals

6.12.7.1 Any end-seal shall be designed to contain twice the maximum pressure exerted by the fill in the annulus between the carrier pipe and the sleeve, during installation and in service.

Note: Cementitious or proprietary end-seals may be used for concrete sleeves, dependent upon the requirements to install fill and drain pipes through the seals.

6.12.7.2 Proprietary rubber seals or other options that provide electrical insulation shall be used for grouted steel sleeves.

6.12.8 Attachments

Any attachment such as vent and fill pipes and cable connections should be designed to standards appropriate to their intended use.

6.12.9 **Drain points**

6.12.9.1 While any sleeve should be designed to prevent the ingress of water, drain-points should be fitted to remove water following construction.

Note: These may be of a temporary nature and may be removed following commissioning.

6.12.9.2 Any sleeve should be laid to a fall with the drainpoint(s) at the lowest point(s) of the sleeve.

6.12.10 **Annular filling**

6.12.10.1 In selecting fill material, consideration shall be given to the requirements of any relevant authority and of maintenance requirements.

6.12.10.2 The annulus shall be filled completely.

Note: Cementitious grout is recommended for filling sleeves.

6.12.10.3 The differential of the annular pressure over the internal pressure in the carrier pipe should not exceed the values given in Table 7 at any time during the annular filling. This is to avoid the possibility of collapsing the carrier pipe during annular filling

D/t_{min}	MAXIMUM EXCESS OF ANNULUS PRESSURE OVER INTERNAL PRESSURE OF CARRIER PIPE (bar)
50	9.7
60	5.2
70	3.4
80	2.2
90	1.6
100	1.2

t_{min} minimum wall thickness of the carrier pipe (mm) as defined in Sub-Section 6.4 and D is the outside diameter of the carrier pipe.

TABLE 7 - LIMITING PRESSURE DIFFERENTIALS FOR CARRIER PIPE

6.12.10.4 Selection of a suitable material for filling the annulus shall be made dependent on the need for corrosion protection of the carrier pipe.

Note 1: Normally, control of corrosion will be achieved by a combination of pipe coating, annular fill and CP.

Note 2: The intent of cementitious fill is to provide a non-corrosive environment, to allow CP current to flow to the carrier pipe, to withstand external loads imposed on the sleeve and carrier pipe and to resist the ingress of free water.

6.12.10.5 Cementitious fill should be free from any additive, for example nitrates or calcium chloride, likely to cause deterioration of the sleeve or carrier pipe when it sets.

Note: It is recommended that proprietary grout that shows no significant change in volume when placed be used.

Care should be taken to ensure complete filling of the annulus.

6.12.10.6 Steel sleeves designed for nitrogen filling should use forged end-seals and coated steel pipework for the fill connections to minimise leakage potential.

6.12.10.7 Drain and fill/vent connections should be fitted on all nitrogen-filled steel sleeves and be designed to allow periodic maintenance, testing and refilling.

Any permanent drain-point should have a diameter of not less than 50 mm.

A three-way valve should be permanently fitted above ground in a secure housing to facilitate pressure testing, gas sampling and refilling operations.

6.12.10.8 An annular design pressure of 1.5 bar shall be used for all nitrogen-filled sleeves.

6.13 VALVES

6.13.1 In a cross-country pipeline, valves shall be provided at suitable intervals to limit inventory loss and facilitate maintenance, repair, modification, testing and commissioning.

6.13.2 Section isolation valves (also referred to as "block valves") shall be installed at suitable intervals. In industrial and commercial areas, and residential areas of high population density, the spacing of valves should be reduced.

Note 1: These may be hand-operated, automatic or remotely-controlled.

Note 2: Valves may reduce the total duration of a release. In terms of risk reduction, it would be necessary to install valves, with a rapid response to any failure, at short intervals along the pipeline to significantly reduce the risk level.

6.13.3 Any main isolation valve shall be of the full bore ball type.

6.13.4 In determining the spacing of valves, consideration shall be given to the following factors:

- MOP of the pipeline
- diameter of the pipeline
- time taken to arrive at the valve site
- probability of leakage
- proximity to normally-occupied buildings
- areas of high population density, such as residential areas
- industrial and commercial areas
- need for valves for operational purposes
- position of the nearest offtakes and other existing valves
- topography and terrain covered by the pipeline
- ease of continuous access for operation and maintenance
- protection from vandalism
- continuity of service/supply
- expected development along or adjacent to the pipeline section between valves
- significant natural conditions that may affect the operation and security of the pipeline, for example ground movement, etc.
- time to blow down/vent the isolated section of pipeline in case of emergency or maintenance
- sections required for hydrostatic pressure testing of the pipeline.

6.13.5 Section isolation valves shall be installed at either side of any major river or estuary crossing where the pipeline could be damaged by a ship's anchor or scouring of the river bed.

6.13.6 Any block valve should be installed below ground with the valve-operating device readily accessible from above ground.

Note: Stem extensions can be used to elevate the valve operator above ground.

Consideration shall be given to extending the sealant/lubrication and valve vent pipework for ease of access.

Any valve shall be supported to prevent settlement which may affect the integrity of the pipeline system.

- 6.13.7 Where necessary, suitable pressurising bridle/by pass and vent connections shall be provided either side of any main line isolation valve in the pipeline to facilitate valve operation while minimising the risk of seat damage and to allow any section of pipeline to be vented within a reasonable time.

Any vent connection provided shall be located so as to allow venting operations without causing undue hazard.

Where vents and/or by-passes are required, their sizing shall be such as to allow a section of pipeline to be depressurised as rapidly as practicable during an emergency situation. They should be designed in accordance with Sub-Section 6.12.

6.14 **PIGGING**

- 6.14.1 Any pipeline should be designed to allow initial and periodic internal inspection using pigs. Consideration shall be given to equipment for loading and unloading pigs and to the selection of bends, valves, tees and other components, so as to permit effective and safe pigging.

- 6.14.2 Pigging stations should be provided at intervals as required for the techniques being used for internal inspection.

Consideration shall be given to whether a permanent or portable facility is required, and what type of pig trap configuration is needed, i.e. launch, receive or universal (which has launch and receive capability) in conjunction with the relevant user/operator function.

- 6.14.3 The design, construction and testing of pig-traps shall meet an acceptable pressure vessel standard, such as PD 5500, appropriate to MOP of the pipeline, with dimensions to accommodate the pigs to be used.

- 6.14.4 When designing a pig trap for a pipeline, the following should be incorporated:

- an oversize diameter of at least 100 mm greater than the nominal diameter of the pipeline.

Note: Typically, an eccentric reducer is incorporated in the pig trap so that when the pig enters the receive facility, the "cups" which ensure there is a gas-tight seal between the pig and the inside of the pipeline to allow the vehicle to be propelled along it, are disengaged and, thus, allows gas to flow around the pig. (which helps to stop the pig).

- suitable tappings of at least 25 mm nominal size, so that the trap may be purged in front of, and behind, the pig, with interconnecting pipework to enable the pressure to be equalised across the pig during pressurisation and depressurisation.

Note: An equalising bridle arrangement is required to balance the gas pressure around the pig trap to prevent sudden and uncontrolled pig movement. The bridle arrangement also enables parts of the facility to be vented and purged.

- adequate access to, and working space in front of, the trap for the delivery of pigs/inspection vehicles, craneage etc. Consideration shall be given to equipment access and clearances for loading and unloading all types of "pigs" and internal inspection equipment, i.e. pig trap height-above-ground level

- bonding of the pig trap and closure to earth.

- 6.14.5 Consideration shall be given to the selection of bends, valves, tees and other components, to ensure effective and safe pigging of any pipeline. In particular:
- where a branch connection diameter exceeds 25% of the pipeline diameter, guide bars should be incorporated in the branch connection.

The design of guide bars should be to a suitable standard such as Advantica T1/E or T2/E

- care shall be taken to ensure thermowells or other insertion devices are not installed on the pipeline that is to be pigged
- the number of bends on the final approach to, or initial despatch from, a pig trap should be kept to a minimum
- bends for inclusion in the pipeline should have minimum bend radius of 3 times the pipe outside diameter
- pipework configurations with multiple branch connections, such as tees and sweepolets, in close proximity, should be avoided to ensure that the pig will not come to rest with one "cup" being by-passed in one connection and the second "cup" in the second connection.

- 6.14.6 On pig launch facilities, the length of the pig trap between the closure and the small end of the reducer should be sufficient to accommodate the longest pig to be used. The length of pipework between the pig trap reducer and the isolation valve should take account of the designs of pigs to be used and should allow for satisfactory engagement of pig cups.

- 6.14.7 On pig receive facilities, the length of pipework between the isolation valve and the small end of the pig trap reducer should exceed the longest length of pig to be used.

- 6.14.8 A safety latch should be fitted on any pig trap door, the design of which should include the provision of suitable devices:

- to securely fasten the door while it is subject to internal pressure and
- to prevent the door being blown open violently by any residual pressure in the vessels.

The devices should ensure that the vessel cannot be pressurised until the door is closed securely, that the door cannot be opened unless any pressure has been vented suitably and the door is restrained for the first part of its travel until the seal is broken.

- 6.14.9 Sufficient pressure monitoring points should be included to allow temporary pig tracking equipment to be installed for pigging operations.

- 6.14.10 Indication devices, for example "pig alerts" should be positioned strategically on the pigging facility to give warning of despatch or receipt of pigs.

The pig alerts incorporated on the pipeline should be provided with a suitable valve arrangement to facilitate removal in the event of damage.

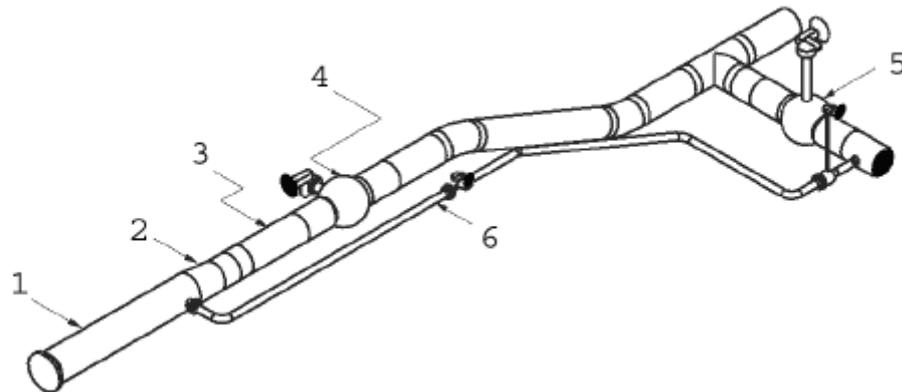
- 6.14.11 If the pigging facilities are to be used for internal inspection, additional provisions and clearances should be provided, if required (see clause 11.8.3).

Note: An example of a typical layout for pig traps for use with internal inspection equipment is shown in Figure 7.

- 6.14.12 A pig trap installation should provide, as a minimum, the following:

- insulation joints for CP purposes
- drains, vents, pressure points and control connections (see Figure 7)
- a facility for removing or replacing the trap, where it is not part of the permanent installation.

6.14.13 Consideration shall be given to the design, location and operation of any liquid collection or despatch system, to ensure the safety of operators and to prevent spillage.



- 1 Pig trap barrel
- 2 Eccentric reducer
- 3 Pig trap throat
- 4 Pig trap isolation valve
- 5 Branch/offtake valve
- 6 Forcing/receive gas line.

FIGURE 7 - TYPICAL PIG TRAP INSTALLATION

6.15 **OVERHEAD PIPE CROSSINGS**

6.15.1 Overhead pipe crossings, for example of rivers, canals, railways and roads, should be avoided, wherever possible.

6.15.2 Where an overhead crossing is unavoidable, it shall be designed, located and maintained to:

- accept the stresses imposed on the pipe, carrier system and foundations and supports, within acceptable limits. Reference should be made to IGE/TD/12
- be acceptable in environmental aspects
- have sufficient headroom to ensure the piping system is secure from possible damage due to the movement of vehicles, railstock or shipping beneath them
- have suitable barriers to restrict access, except to those concerned with maintenance
- have suitable accessibility to all components for the purpose of painting and lubrication
- avoid interference between the CP system for the pipeline and any supporting structure

- have suitable barriers or protection to prevent damage to the carrier pipe by vehicles
- have supports whose bases are on firm ground and incapable of being weakened by scouring.

6.16

DESIGN RECORDS

Comprehensive records shall be compiled during the design phase and, upon completion, should form part of the package of "as-built" documentation that is handed over to the operator.

Such records should include maps showing, where appropriate, that thick wall pipe was required, together with the reasoning, any calculations, drawings of any installations, materials and coating properties.

SECTION 7 : CONSTRUCTION OF PIPELINES

7.1 GENERAL

The following requirements should not be considered as exhaustive and are intended to cover only points of particular significance.

7.2 ADMINISTRATION

7.2.1 Communications

Good communication between construction centres and field crews, at all levels, should be maintained. Maximum use should be made of modern communication techniques in the control of all activities on pipeline systems. Operatives should be trained in the effective and disciplined use of such equipment.

7.2.2 Supervision

7.2.2.1 In selecting the level of supervision required, consideration shall be given to:

- the nature and complexity of operations being undertaken
- the potential risks that operations impose.

7.2.2.2 Supervisory activities shall only be undertaken by people who are competent and have the appropriate level of authority.

7.2.2.3 Every endeavour should be made to plan the operations so that the period of occupation of land is kept to a minimum.

Note: Depending on the size of the project, it may be necessary to divide it into sections (either by location or by activity or by a combination of both) each supervised by personnel experienced in the activities taking place in the section.

7.2.3 Construction records

Comprehensive "as laid" records of the pipeline shall be prepared during the construction period. These should include details such as:

- grade and wall thickness of linepipe used for the carrier pipe
- information on, and the location of, butt welds
- protective materials used
- precise pipeline route and depth at frequent intervals
- details of land ownership
- land drain reinstatement
- particulars of the CP system, sleeves (including materials and components), bends, valves, tees, etc.
- test records
- location of tie-in welds between test sections
- differences between "design" and "as laid" information, with reasons
- presence of other nearby below-ground plant and connections to other pipelines
- any other relevant information that is not readily obtainable by surface inspection, including archaeological details
- modification to the original design.

Where explosives have been used, the relevant sections should be indicated on the "as laid" records.

Following completion of construction work, the construction records should be deposited with the pipeline owner/operator under a formal handover system.

7.3 **SAFETY**

7.3.1 **General**

7.3.1.1 A high standard of safety shall be maintained at all times.

7.3.1.2 A safety management plan shall be prepared, which clearly defines:

- how health and safety law is to be managed
- the safety procedures, codes of practice and standards to be implemented
- the roles and responsibilities of individuals on the pipeline project.

7.3.1.3 Where a pipeline forms part of a larger installation, the health and safety plans shall encompass the interfaces of the different elements of the project.

7.3.1.4 Adequate supervision shall be provided to project employees, the public, property and plant.

7.3.1.5 Work supervisors shall be capable of ensuring that all necessary safety precautions are taken for the protection of personnel, members of the public and property that might be affected by the works.

7.3.2 **Safety training**

Employers must provide such instruction, training and equipment as is necessary to ensure, as far as is reasonably practicable, the health and safety of all personnel.

7.4 **ENVIRONMENT**

7.4.1 **General**

7.4.1.1 Work shall be conducted within the framework of the project environmental management plan, adopting the same principles as for the safety management plan which should identify existing legislation, and shall be in accordance with appropriate guidance and codes of practice.

7.4.1.2 Consideration shall be given to the identification and minimisation of emissions to air, surface and ground water courses and also the disturbance of all land involved in the works.

7.4.1.3 Efforts shall be made to minimise disturbance to natural resources, ecologically sensitive habitats and archaeological sites.

7.4.2 **Noise abatement**

7.4.2.1 A certain amount of noise is inherent in all construction operations. The best practicable methods shall be employed to minimise noise emissions to levels acceptable to site personnel and third parties and must be employed sufficiently so as to comply with regulations.

7.4.2.2 Special consideration shall be given to:

- designing out noise-generating operations before construction starts
- siting and possible screening of plant and equipment
- use of acoustically-attenuated powered tools, compressors and generators
- avoiding operations outside normal working hours

- controlling noise related to venting operations associated with pigging and/or following testing.

7.4.3 **Water**

Any fuel, lubricant and chemical shall be stored, used and disposed of in such a way as to minimise the possibility of adverse environmental impact.

7.4.4 **Traffic**

Consideration shall be given to implementation of a Traffic Management Plan, agreed with the appropriate statutory authority, in order to minimise the nuisance and damage caused to public roads and footpaths.

7.5 **RECEIVING MATERIALS**

7.5.1 A formal control system shall be adopted for the recording of materials throughout receipt, storage, transport and issue.

7.5.2 All materials shall be inspected upon receipt on site. Any damaged materials shall be rejected or, in cases of minor damage, conditionally accepted. The storage and handling of pipes shall be such as to prevent damage to the pipe (see IGEM/TD/1 Supplement 1). Certain types of surface damage to the pipe may be repaired by an approved method. Otherwise, the section of pipe containing the damaged section shall be cut out.

7.5.3 Great care shall be taken to prevent damage to, or disbondment of, any protective coating. Slings or other equipment used for handling pipes shall be designed so as to avoid damage to the pipes or coating. If the coating is disturbed or damaged, the portion affected shall be repaired by an approved method. Where the damage is extensive, the affected area shall be recoated completely.

7.5.4 Pipework materials shall be handled, transported and stored in accordance with IGEM/TD/1 Edition 5 Supplement 1.

7.5.5 Materials shall not be stored below overhead power lines.

7.6 **ENTRY ONTO LAND AND SETTING OUT**

7.6.1 A pre-entry survey of the route should be carried out to establish and record initial conditions of the site and to agree with the land-owners and occupiers the requirements for such as route fencing, points of access, location of temporary water troughs, temporary crossings of the working width, etc.

7.6.2 The setting out of the route of the pipeline in accordance with maps and drawings should be checked and agreed before construction begins. Such setting out should include locating and marking existing services.

7.7 **WORKING WIDTH AND FENCING**

7.7.1 In all circumstances, the limits of the working width shall be marked clearly. Temporary fencing should be provided throughout the period of construction, along each side of the working width, to protect trees with preservation orders and also to close off the working width at all points of access from public roads. This should be stock-proof where stock is kept on adjoining land.

7.7.2 Where appropriate, consideration shall be given to the installation of cut-off or header drains along and outside the working width.

Note: This can assist in maintaining a dry working width during construction and prevent silting or blockage of any existing drainage system.

7.7.3 Before pipes are strung, the working width should be cleared of all standing crops, scrub, hedges and similar obstruction, stripped of topsoil and graded where necessary. This work should be planned to cause the least possible disturbance to the owners and occupiers.

7.7.4 Trees and hedgerows shall not be removed without the prior consent of the landowner.

Note: There might also be a requirement to seek formal consent from the appropriate statutory authority before this activity can be actioned.

7.7.5 Any topsoil and surface material stripped shall be kept separate from the subsoil, preferably on the opposite side of the working width.

Note: The width and depth of topsoil to be stripped will vary according to local circumstances.

7.7.6 Consideration shall be given to the protection of the environment, including measures required when crossing areas of moorland where topsoil stripping may need to be limited to the width of the trench and special protection provided to heathers and grasses.

7.8 **SURVEYING FOR BENDS**

A survey should be made to schedule bend requirements, taking into account changes in direction in both the horizontal and vertical planes and making allowance for any grading which will be carried out.

Note: It is advisable to indicate the position of bends and the deflection required, by suitable means, at the side of the working width.

7.9 **PIPE STRINGING**

7.9.1 Linepipe shall be strung in such a manner that the least interference is caused with the land crossed. Gaps shall be left at intervals as agreed with the occupier of the land to permit the passage of farm stock and equipment across the working width.

7.9.2 Care shall be taken to avoid damage to pipe and fittings, during stringing, by handling in accordance with IGEM/TD/1 Supplement 1.

7.9.3 If pipes are strung out on ground of a nature that could cause damage to the coating, they shall be laid on padded timber bearers of appropriate size, with two timbers per pipe. Wooden wedges should be used to hold the pipes in position.

7.9.4 When using cranes on pipe spreads, a survey of overhead power supply lines shall be made and suitable safeguards introduced to protect personnel and plant. Reference should be made to HS(GS)6. Ideally, the risk from this hazard should be eliminated or reduced at the design stage by either adjusting the pipeline route or diverting power lines.

When it is necessary to work in the vicinity of overhead electric cables, reference shall be made to the electricity supply authority before site work commences. Its advice should be sought, for example on possible temporary isolation; minimum clearances; alternative access points; barriers and goal posts.

The same methodology as for overhead power supply lines shall be applied when working in the vicinity of buried services (see HS(G)47 and IGE/SR/18).

7.10 **FIELD BENDING**

7.10.1 Pipes may be bent cold in the field. Bending shall be performed, without wrinkling, on a suitable machine.

Note: An internal mandrel will be required, particularly for larger diameters.

7.10.2 In the finished bend, the angular deflection measured along any axial length equal to the diameter of the pipe shall not exceed 1.5° (this corresponds to the minimum ratio of radius, measured from the inside of the bend to diameter of the pipe) being in the order of 40 to 1.

7.10.3 Each pipe that is bent shall incorporate a minimum length of 1.25 m of straight pipe before and after the bent portion.

7.10.4 A bend shall not be made within two pipe diameters of a girth weld, which has already been made.

7.10.5 When longitudinally welded pipes are used, the weld shall be at about 45° to the plane of the bend and longitudinal welds of consecutive cold bends shall not coincide.

7.10.6 Before any bend is incorporated in the pipeline, it shall be tested for ovality with a gauging plate of diameter not less than 95% of the nominal bore, subject to a minimum clearance of 25 mm. Coating and wrapping applied before bending shall be examined and any damage made good.

7.11 **LINING-UP FOR WELDING**

Pipes shall be supported adequately to avoid damage to coating and to enable both safe access and sufficient clearance for the welding and subsequent weld inspection and coating activities.

7.12 **WELDING**

7.12.1 **General**

Prior to any welding operation, whether on a pipeline or an associated installation, welding processes and systems shall be assessed and approved. This should include the testing, qualification, approval of welding procedures and welders as well as arrangements for inspection, acceptance criteria and rectification of welds.

Pipe and fittings shall be prepared, welded and inspected in accordance with a suitable specification. Cut pipes should have details of pipe reference numbers transferred to the inside of the pipe on each cut end.

Where pipe is welded above ground prior to lowering into the trench, the pipe shall be supported on suitably placed padded timbers. The support should be designed so as to prevent movement of sections of pipe.

Where tie-ins are being undertaken, for example at special crossing locations, particular care shall be taken to ensure that the support is designed to suit the specific requirements at the location. Support shall remain in place until all welding operations have been completed.

7.12.2 **Non-destructive testing (NDT)**

7.12.2.1 All welded joints shall be inspected using NDT procedures in accordance with a suitable specification.

7.12.2.2 Where radiographic inspection is required, it should be planned in relating to other work to ensure safety and avoid delay.

7.12.3 **Stress relief**

In certain circumstances, for example where the pipe wall thickness is greater than 30 mm, heat treatment of site fabrications may be necessary. Consideration shall be given to the need for stress relief using post-weld heat treatment on thick sections, or alternatively the need to carry out an Engineering Critical Assessment to confirm (specify) the toughness requirements, determine the critical crack size and define relevant inspection requirements. Reference should be made to such as PD 5500, BS 7910 and BS 2633.

7.13 **NIGHT CAPS**

The open ends of welded sections of pipeline shall be closed by the use of suitable nightcaps, to prevent the ingress of foreign bodies and water.

7.14 **JOINT COATING**

The uncoated external portion of pipeline joints shall be protected to a standard at least equivalent to, and compatible with, the linepipe coating.

7.15 **TRENCH EXCAVATION**

7.15.1 Normally, pipelines shall be laid to contour with adequate cover (typically not less than 1.1 m from the true ground level) to minimise damage by third party interference.

7.15.2 The trench width shall exceed the pipe diameter by a margin which will permit proper back filling and compaction. Consideration shall be given to increasing this margin for larger diameter pipes.

7.15.3 The bottom of the trench shall be prepared to permit even bedding of the pipeline and shall be free from all objects or material that might cause damage to, or deterioration of, the pipe and pipe coating (see also Sub-Section 7.20).

7.15.4 Care shall be taken during excavation, by the adoption of appropriate safe excavation techniques, to ensure the stability of excavations, that other buried plant is not damaged and that the minimum amount of damage or disturbance is caused to land drains.

The position of all services and land drains, affected by pipeline construction, shall be marked carefully at the edges of the working width.

7.15.5 Where any part of a pipeline is laid on top of disturbed or made-up ground, for example embankments, the ground shall first be consolidated as far as possible. Any likely further compaction or settlement shall be treated as an additional environmental load.

7.15.6 Where it is necessary to use explosives, statutory regulations regarding their storage must be strictly observed. Agreement shall be obtained from land-owners and authorities affected concerning the use of explosives and the timing of blasting operations.

The presence of adjoining underground structures or services and their proximity to the line of the trench shall be taken into account when deciding on the size of the explosive charge to be used. The same considerations shall be applied where the line of the trench is near to buildings which may be affected by blasting.

A condition survey shall be undertaken, in advance of blasting, for any structures that might be affected. Blasting shall not be undertaken beneath overhead power lines that are in service.

7.16 **INSPECTION OF COATING**

7.16.1 Immediately before pipe is lowered, the whole of the pipe coating shall be examined carefully by means of a suitable holiday detector set at an appropriate voltage to provide a sufficient arc length for the thickness and nature of the coating material. All flaws indicated by the holiday detector shall be marked and repaired before the pipe is lowered. A record should be kept of such damage (unless very minor) and should be included in construction records.

If disbondment of the coating is suspected at any point, the coating shall be removed, replaced and retested.

In addition to the holiday detection of the coating, pipe shall be inspected for damage such as dents, gouges, grooves, notches, arc burns, etc. Such damage shall be rectified by grinding or by cutting out the section of pipe containing the damage.

7.17 **LOWERING PIPE INTO A TRENCH**

7.17.1 All equipment in contact with the pipe coating when pipe is lowered into a trench shall be appropriate to prevent damage to the coating.

7.17.2 Care shall be taken to ensure that over-stressing of the pipeline does not occur during the lifting and lowering operation and that, after lowering, the pipe is not over-stressed or damaged.

7.18 **BEDDING AND COVERING PIPE**

7.18.1 Pipe shall be evenly bedded on the bottom of the trench throughout its length. All material used for bedding and surrounding the pipe shall be suitable for the purpose and free from sharp edged stones.

7.18.2 Special measures shall be considered at branch connections to avoid undue stresses occurring.

Note: Uneven vertical movements/settlements can be reduced/avoided by using more substantial foundations/bedding techniques to support the branch connection and main pipeline in the area of the connection.

For larger diameter pipes, consideration shall be given to bedding and haunching the pipe to provide support to the underside of the pipe to prevent pipe ovality resulting from the surcharging of backfill material over the pipe.

7.18.3 Where conditions are such that flotation may occur after backfilling, consideration should be given to the installation of depth markers to indicate the position of the pipe relative to the land surface.

7.18.4 Where weighted pipe is installed through peat bog, marshland, etc., consideration should be given to the installation of depth markers to indicate the position of the pipe relative to the land surface.

7.18.5 Where the excavation is in rock, there shall be a bed of earth, sand or other suitable material to a minimum depth of 150 mm beneath the pipe.

7.19 **BACKFILLING**

7.19.1 Backfilling should follow soon after the lowering-in of the pipe.

Fine-grade material free from sharp-edged stones shall be filled and compacted carefully round the side of the pipe and to a minimum consolidated height of 150 mm above the pipe.

7.19.2 The trench should be backfilled in layers, each layer being compacted adequately.

Note: The Highways Agency "Specification for Highway Works Clause 0600 series "Earthworks" provides further guidance on materials and composition.

7.19.3 Care shall be taken to prevent any solid or liquid material that could be injurious to the coating of the pipe from coming into contact with the pipeline.

7.19.4 Wherever reasonably practicable, excavated materials shall be replaced such that the original solid sequence is preserved.

7.19.5 Where, on sloping ground, pipe bedding and surround material has been installed, care shall be taken to prevent loss due to slippage or washout.

Note: This could, in extreme cases such as in rocky ground, lead to physical damage to the pipeline if preventative measures are not put in place. There are a number of additional precautions that may be taken to deal with this problem, which include physical barriers and specialist fill materials. The pipeline is particularly vulnerable to this form of damage during hydrostatic testing due to its increased weight.

7.19.6 Backfilling, drainage and replacement of the topsoil should be completed prior to hydrostatic testing but if, under exceptional circumstances, it is necessary to undertake the topsoiling or further work within the working width after hydrostatic testing, the position of the pipeline shall be marked clearly and precautions taken to ensure that heavy plant and vehicles do not pass over it except at properly constructed and clearly defined cross points.

Note: Close supervision is required for all work over the pipeline and a permit to work system is advisable.

7.20 **CROSSINGS**

7.20.1 **General**

Crossings shall be constructed by a procedure acceptable to, and approved by, the appropriate statutory authority.

Note: These may include open cut, boring, directional drilling or tunnelling methods.

7.20.2 **Road and rail crossings**

Crossings shall be carried out in a manner that minimises the disruption to normal traffic flow. Particular attention must be given to the statutory requirements for warning signs and lights during the construction of road crossings.

7.20.3 **Water crossings, including drainage ditches**

7.20.3.1 At water crossings, the pipeline shall be laid at a cover allowing for future bed movement, invert lowering, dredging operations, etc. Where water crossings are installed by the open cut method, temporary flume pipes or other methods should be considered to ensure that there is no disruption to water flow during construction. Consideration shall be given to the application of a weight coating to maintain negative buoyancy of the pipe during construction and in service. Attention should be given to maintaining the integrity of flood or tidal barriers during construction. Care shall be taken to prevent pollution of watercourses by oil, silt, etc.

7.20.3.2 Consideration shall be given to the possibility of future cleaning and deepening operations on drainage ditches. Where such operations are likely, and where the pipeline is installed by open cut methods, heavy wall pipe i.e. design factor ≤ 0.3 should be installed. Where such activities are considered for drainage ditches on existing crossings, the installation of a concrete protection slab of adequate strength and dimensions should be placed between the pipe and the cleaned bottom of the ditch to prevent impact damage. The top of the slab should be not less than 300 mm below the true cleaned bed of the crossing/ditch.

7.21 **SLEEVED AND TUNNEL CROSSINGS**

7.21.1 **General**

7.21.1.1 A sleeve is a close fitting casing through which a carrier pipe is inserted. Normally, the carrier pipe is concentrically located and the annular space between the pipe and sleeve is relatively small; typically the internal sleeve diameter will be 150 mm to 300 mm greater than the external diameter of the carrier pipe. Usually, the ends of the sleeve are sealed and filled with either grout or nitrogen.

Note: Accepted construction techniques include micro-tunnelling and pipe jacking.

7.21.1.2 A tunnel is an underground or underwater passage, the dimensions of which are significantly greater than the pipeline diameter. The minimum diameter of a tunnel is often determined by the access requirements of the miners and the specialist equipment used for construction. In such cases, the design and construction shall be in accordance with relevant codes.

Consideration shall be given to the requirements of pipeline installation, pipeline support, restraint of pipeline movement, venting of enclosed spaces, access for maintenance, corrosion protection, testing and validation, de-commissioning and dismantling at the end of the asset life.

Where there are difficulties of access and/or venting or there is the potential of flooding, consideration shall be given to installing the pipeline in a sleeve filled with grout or nitrogen.

7.21.1.3 Where, due to ground conditions, it is considered necessary to install a construction sleeve for bored crossings, preference should be given to the use of concrete pipe sleeves to reduce CP problems inherent with steel sleeving. Appropriate standards should be selected for each material.

Note: The choice of other materials will depend on their ability to meet the relevant design requirements of Sub-Section 6.11.

7.21.2 **Concrete and alternative materials for sleeves**

Concrete pipes used for sleeves shall comply with an appropriate standard and be installed, one length at a time, to a true line with suitable gradient. The jointing requirements specified by the manufacturer shall be followed.

Provision for the annular fill which, normally, will be cementitious, should be made by fixing risers of 50 mm diameter at each end. Where the length of continuous sleeving exceeds 120 m, the maximum annular space should be provided and consideration given to using intermediate filling points.

7.21.3 **Steel sleeves**

7.21.3.1 For grouted steel sleeves, a high quality external coating is not required as the sleeve will not be protected against corrosion by the application of CP. However, checks shall be carried out before and after carrier pipe tie-in operations to ensure that there is no electrical contact between the carrier pipe and the sleeve.

Note: Such a contact would make it impossible to cathodically protect the carrier pipe within the sleeve.

Such checks shall be carried out and any electrical short circuit remedied before the annulus is grouted. A further check shall be carried out after grouting operations to ensure that electrical isolation is maintained.

Welding and inspection procedures shall be in accordance with the appropriate standards.

For steel sleeves that are to be nitrogen filled after the carrier pipe has been installed, the forged end-seals shall be welded into position and pressure tested with air to 3 bar. Fittings welded to sleeves shall be of compatible material specifications and welded to approved procedures. As the steel sleeve and its attachments will be part of the CP system on the pipeline, all joints, pipework and fittings shall be coated using approved materials and procedures.

7.21.3.2 Whenever welding is carried out on a sleeve in position, precautions should be taken to prevent damage to the spacers or the external coating of the carrier pipe. Any protective material used for this purpose should either be fixed securely or be removed after construction.

7.21.4 **Pipe spacers for sleeves**

7.21.4.1 The carrier pipe support system shall be designed so as to avoid any damage to the carrier pipe coating during installation. Care shall be taken to avoid:

- blocking drain points or annular fill inlets
- displacement of the carrier pipe.

The carrier pipe should be adequately supported at the sleeve ends.

7.21.4.2 Particular attention shall be given to the consolidation of the backfill under the sleeve ends and the adjacent carrier pipe.

7.21.5 **Annular filling of sleeves**

7.21.5.1 *General*

Filling of the sleeve annulus shall be carried out after hydrostatic testing of the pipeline.

7.21.5.2 *Grout filled sleeves*

Checks shall be carried out immediately before and after grouting, to confirm continuing electrical isolation between the sleeve and carrier pipe.

The annular fill shall be tested to ensure compliance with the specification. Water for mixing should be clean.

The total volume should be calculated prior to the start of filling and a careful check made to ensure that the actual volume placed correlates closely with that calculated.

The annulus between the carrier pipe and the sleeve should be clean and drained of water before any filling operations commence. Care should be taken to ensure the recommended water/solids ratio is not exceeded and that grouting pressures do not exceed specified levels.

Suitable means of sealing should be used to prevent undue loss of material from sleeve ends.

7.21.5.3 *Nitrogen-filled sleeves*

The annulus shall be purged with nitrogen to reduce the oxygen content to below 2% and nitrogen used to raise the annulus pressure to 1.5 bar.

All fittings shall be leak-tested and the recorded pressure used to initiate the nitrogen fill maintenance records.

7.22 **FOUNDATIONS**

Foundations shall be constructed to accommodate the nature of the grounds and the requirements of the structure to be supported. Construction shall conform to BS 8110-1/2 or BS 8004.

Note: HSE Research Report 319 "Safer foundations by design" provides guidance on the management of risks arising from various ground engineering processes.

7.23 **REINSTATEMENT**

7.23.1 In order to protect the pipeline from construction damage, every effort shall be made to complete all reinstatement activities prior to hydrostatic testing.

7.23.2 Any operation that cannot be completed prior to the hydrostatic test shall be carried out under a formalised written procedure such as a permit system.

7.23.3 Work shall not be undertaken while the hydrostatic test is in progress.

7.23.4 As soon as practical after backfilling, and prior to topsoiling, the work width should be cleared of all construction debris and any surplus materials. The ground profile should be reinstated so that the pipeline working width matches as closely as reasonably practical its original contour.

7.23.5 Consideration shall be given to the ripping of subsoil to break up the compaction that will have occurred with the passage of heavy construction plant.

Note: This activity can help prevent future drainage problems due to an effect known as "panning".

7.23.6 Consideration shall be given to either reinstating existing land drainage or installing new header drains.

Note 1: Any new header drains may be additional to any cut off drains that were installed prior to the commencement of pipeline construction.

Note 2: The previously excavated trench line could suffer from settlement that could lead to future drainage problems if special measures are not undertaken.

Note 3: Drainage issues can result in high operating costs during the life of the pipeline if not undertaken to an appropriate design and to a high standard of workmanship.

Note 4: Areas subject to erosion, such as the banks of watercourses, may require specialist reinstatement techniques. In some cases, these will be under the control of an Authority and any technique will have to be agreed with it in advance. Similarly, public roads and accesses will require prior agreement with the relevant authority for any reinstatement technique that is used.

7.23.7 Once the topsoil has been replaced and fences reinstated, a joint inspection should be undertaken with the landowner or occupier prior to formally returning the land back to their use.

7.24 **PIGGING**

7.24.1 Steps shall be taken to ensure that the pipeline is free from internal obstruction following construction operations.

Note: It is recommended that a cleaning/swabbing procedure be carried out prior to gauging.

7.24.2 Pigging shall also be carried out if associated pig traps and test ends are designed specifically for the purpose.

7.24.3 At the stage before testing and again at the stage before commissioning, a suitable gauge plate or geometric pig shall be passed through the pipeline to prove the bore to the specified acceptance procedure.

If a geometric pig is used, all local reductions in diameter equal or greater than 2.5% diameter shall be investigated, assessed and, where necessary, remedial action shall be taken.

If a gauge plate is used, its diameter shall be 95% of the minimum bore of the pipeline/fittings, subject to a minimum clearance of 25 mm on diameter.

Note: The recommended acceptance level of 5% for diameter reduction is specified to identify ovality or out-of-roundness of the pipe as a result of construction activities.

7.25 **MARKER POSTS**

7.25.1 The position of the pipeline shall be indicated at suitable intervals by means of markers. These should be at field boundaries, at all crossings and, where practicable, at changes in direction. They shall indicate the location of the pipeline after reinstatement of the ground.

7.25.2 Consideration shall be given to the provision of suitably located markers specially designed for observation from the air.

7.26 **TESTING**

Testing should be undertaken in accordance with Section 8.

7.27 **TIE-INS AFTER TESTING**

7.27.1 Consecutive sections of pipework should be made so as to overlap such that the tie-ins can be made with a single weld. Where the tie-in is required between two previously tested sections, and cannot be achieved in a single weld, it shall be

made using pipe previously hydrostatically tested to a pressure not less than the test pressure of the adjacent sections.

7.27.2 Tie-ins shall be aligned properly without the use of jacks to prevent joints being left under stress. Changes to ambient temperatures should be given due consideration when tie-ins involve long lengths of exposed pipe. They should not be made when the temperature is above 30°C or below 5°C.

7.27.3 All tie-in welds shall be subjected to full NDT to the standard applied to the rest of the pipeline.

7.28 **POST-CONSTRUCTION COATING SURVEY**

On completion of pipeline installation, a Pearson-type survey shall be carried out to locate any areas of coating damage on the buried pipeline. Any damage found shall be repaired.

7.29 **CATHODIC PROTECTION (CP)**

CP should be installed in accordance with Sub-Section 10.4.

7.30 **COMMISSIONING**

Commissioning should be undertaken in accordance with Section 9.

SECTION 8 : TESTING OF PIPELINES AND INSTALLATIONS

This section covers pressure testing of pipelines and associated installations. Testing, filling and emptying procedures shall be in accordance with Appendices 5 and 6.

Prior to the use of any high pressure pipeline or its associated installation(s), a strength test should be carried out.

Note 1: For pipework, this is achieved by pressurising the pipework to a level above MOP.

Note 2: The philosophy used to determine the test pressure for pipelines is different to that used to determine the test pressure for associated installations.

With the current standards of construction, supervision and inspection, it is no longer considered appropriate to carry out pneumatic leak testing of pipelines either prior to, or after, the hydrostatic test.

Note 1: Pneumatic testing may be employed as a leak test for installations which are assembled from pre-tested sections or where items, such as regulators, are omitted from the hydrostatic test.

Note 2: Pneumatic testing, as an alternative strength test to the hydrostatic test, is appropriate only in instances where the removal of test water is extremely difficult, such as with small bore pipework not exceeding 25 mm diameter.

8.1 PLANNING/PRELIMINARY REQUIREMENTS

8.1.1 The following shall be specified:

- the required maximum test pressure and the test duration
- acceptance criteria
- the testing specification to be followed
- whether a pressure/volume plot is required
- any items to be excluded from the test.

8.1.2 Responsibilities shall be defined clearly and should include, but may not be limited to:

- the management of the test
- obtaining appropriate approval for the test procedure
- ensuring that adequate safety precautions are implemented and followed
- ensuring that the test procedure is followed correctly
- compilation of the final test record.

8.1.3 At least two people, with experience in pressure testing, shall be present during testing.

8.1.4 A schedule shall be prepared for all operations for the test, stating clearly responsibilities during all phases of the work. The schedule should include:

- safety precautions
- details of the design and supply of any test fittings
- proposed location of the test cabin, pumps and other test equipment
- means of filling and pressurising, including water sources, test connections and vent points
- a test procedure, including details of the test sections
- means of de-pressurising and emptying, including details of drainage connections and method of disposal of water
- a detailed test program, giving proposed dates

- an emergency procedure to be carried out in the event of a test failure through rupture
- requirements for permits and notifications to regulatory bodies.

8.2 HYDROSTATIC TESTING

8.2.1 Preparation for testing

Prior to the commencement of testing, a pro-forma shall be prepared, detailing the following:

- an accurate description of the pipework to be tested and the limits of the test section
- where necessary, the test limits specified by weld, pipework section and local or national co-ordinates
- for complex pipework configurations or installations, an engineering drawing. Such drawings should, ultimately, form part of the final test documentation
- the maximum specified test pressure required in the test section (see clause 8.1.1)
- the differences in elevation between the lowest and highest points in the test section and the test pressure control point
- the maximum test pressure to be reached at the test pressure control point, taking into account the effects of the hydraulic head due to differences in elevation
- the total volume of the test section, expressed in litres of water
- the maximum permitted air content of the test section, expressed as a percentage of its total volume
- the required rate of pressure rise in the test section and, where applicable, the calibration of the pressurising pump, expressed in litres per stroke of the pump
- the specification, its current edition and section to which the test procedure is to comply.

8.2.2 Testing of pipelines

8.2.2.1 A pipeline designed for operation at a design factor exceeding 0.3 shall be tested to the requirements of Table 8, thus ensuring freedom from defects which might reach a critical size in service.

Note 1: Upper limits are set according to the manufacturing process and the pipe coating.

Note 2: This test requirement may be relaxed to a pressure of 1.5 x MOP if either:

- *the pipeline is not significantly line packed i.e the daily variation in hoop stress does not exceed 35 N mm⁻² or*
- *a fatigue assessment of the expected pressure cycling shows that the required design life is achieved.*

Note 3: The fatigue life data, provided in Sub-Section 6.6, are based on the benefits of high-level testing in limiting the size of defects entering service, as well as the introduction of beneficial residual compressive stresses on the remaining defects.

8.2.2.2 A pipeline designed for operation at a design factor not exceeding 0.3 shall be tested to a pressure of at least 1.5 x MOP (see Table 8) except when subject to daily stress cycles exceeding 35 N mm⁻², the pipeline shall be tested to the criteria of Table 9.

Note: This requirement may be relaxed if a fatigue assessment shows that the required design life due to pressure-cycling is achieved with a lower test level.

Reduction of the test pressure to 1.5 x MOP may restrict the possibilities regarding future uprating of the pipeline, hence the test pressure values provided in Table 9 shall be used wherever possible.

8.2.2.3 Tests to Table 8 shall be measured at the lowest point of the test section whereas tests to Table 9 shall be measured at the highest point of the test section.

8.2.2.4 When considering a diversion or new pipe section which will form part of an existing pipeline and have a design factor of less than 0.72 (typically for impact protection or proximity infringement measures), the test pressure should be the greater of:

- in accordance with Table 8, based on a wall thickness and material grade equivalent to a design factor of 0.72 or
- equivalent to the existing pipeline test pressure.

MINIMUM TEST PRESSURE FOR SEAM WELDED AND SEAMLESS PIPE	
Pre-installation test	Main test
1.5 MOP + 10%	1.5 MOP

Note: Higher values may be applied at the discretion of the responsible engineer, in which case the upper limit would be that indicated in Table 9.

TABLE 8 - HYDROSTATIC TEST CONDITIONS FOR SYSTEMS DESIGNED TO OPERATE AT A DESIGN FACTOR NOT EXCEEDING 0.3

SEAM WELDED PIPE (SAW)		SEAMLESS PIPE		SEAM WELDED PIPE (ERW/HFW)	
Pre-installation test	Main test	Pre-installation test	Main test	Pre-installation test	Main test
FIRST occurring of: (a) f = 1.1 (b) Half-slope P/V Plot	FIRST occurring of: (a) f = 1.05 (b) Half-slope P/V Plot (c) Max pressure in pre-installation test	FIRST occurring of: (a) f = 1.0* (b) Half-slope P/V Plot	FIRST occurring of: (a) f = 0.9** (b) Half-slope P/V Plot (c) Max pressure in pre-installation test	FIRST occurring of: (a) f = 1.05 (b) Half-slope P/V Plot	FIRST occurring of: (a) f = 1.0 (b) Half-slope P/V Plot (c) Max pressure in pre-installation test.
Note 1 & 7	Note 2 & 7	Note 3 & 7	Note 4 & 7	Note 5 & 7	Note 6 & 7
<p>Notes</p> <ol style="list-style-type: none"> 1. Attempts should be made to ensure test reaches not less than f = 1.05. 2. Special investigations are required if test does not reach f = 1.0. 3. Attempts should be made to ensure test reaches not less than f = 0.95. 4. Special investigations are required if test does not reach f = 0.85. 5. Attempts should be made to ensure test reaches not less than f = 1.0. 6. Special investigations are required if test does not reach f = 0.95. 7. See A5.2.9 for definition of half slope. <p>* For seamless pipe with coal tar coating, the test pressure should be limited to that equivalent to a design factor of 0.9 and the test followed by an inspection for coating damage.</p> <p>** For seamless pipe with coal tar coating, the test pressure should be limited to that equivalent to a design factor of 0.85.</p>					

TABLE 9 - HYDROSTATIC TEST CONDITIONS FOR SYSTEMS DESIGNED TO OPERATE AT A DESIGN FACTOR EXCEEDING 0.3

8.2.3 **Testing of installations**

Installations shall be tested at 1.5 x MIP. However, having regard to the complex nature of the pipework and fittings, in an installation with stress

concentrating features, a test limit of design factor 0.9 shall be used to ensure that there are no local areas of excessive strain.

Where a test section includes pipework of different diameters, wall thickness or grade, the test level should be determined by the combination giving the lowest test pressure (see also Table 9).

8.2.4 **Test limits**

Where reference is made to a test limit being a fraction of the design factor, the required test pressure shall be calculated:

$$P_t = 20t_n fsD^{-1}$$

P_t	=	test pressure (bar)
t_n	=	nominal wall thickness (mm)
s	=	specified minimum yield strength (N mm ⁻²)
f	=	design factor (as defined in Table 9 or clause 8.2.2)
D	=	outside diameter of the pipe (mm).

8.3 **PRE-TESTING**

Pipe and fittings shall be pre-tested if any of the following circumstances apply:

- the pipe or fittings cannot be hydrostatically tested after installation, for example for tie-in sections/pups or sub-assemblies which are to be incorporated into an existing operational installation
- the pipe or fittings are to be installed in close proximity to operating plant and where it is not possible to protect the plant against a hydrostatic test failure or where the use of a sub-assembly as above is impractical
- it is considered that the consequences of a post-construction test failure are such as to justify pre-testing.

Note: Otherwise, pre-testing is not necessary.

8.4 **TEST EQUIPMENT**

8.4.1 **Instrumentation**

Pressure gauges, dead weight testers, pressure recorders and test equipment for the measurement of volume, pressure and temperature, shall have current test certificates as verification that they are in accordance with the accuracy and sensitivity requirements of this section.

8.4.2 **Measurement of pressure**

For hydrostatic testing of small fabrications and pneumatic testing of small bore pipework (see Appendix 5), a certified Standard Test Gauge to BS EN 837-2, having an accuracy of + 0.25% at any point on the scale, may be used.

The gauge selected should have a full-scale deflection such that the test pressure falls between 60% and 90% of that full-scale deflection.

In all other cases, the hydrostatic test pressure should be measured by a dead weight tester, having resolution of 0.02 bar between 30 and 300 bar and an accuracy of 0.07 bar at the pressure being read.

8.4.3 **Measurement of volume**

The accuracy of the equipment used to measure the water which is added or removed during the test is of paramount importance, as this equipment will be the basis of the accuracy of the air content plot and the slope.

The equipment used for adding or subtracting water shall have a resolution of at least 0.0002% of the fill volume for a pipeline which is subject to a yield test, and a resolution of at least 0.0005% of the fill volume for a non-yield test pipeline and smaller installations.

8.4.4 **Measurement of temperature**

8.4.4.1 The water temperature within the test section shall be monitored, either by direct measurement or by measuring the pipe wall temperature. The ground temperature adjacent to buried pipework shall be monitored and compared with the water temperature readings. Consideration shall be given to the effects of exposed pipework relative to buried pipework in any particular test section.

8.4.4.2 Measurement of temperature shall be made using thermocouples to BS 1041-4 Type K or equivalent.

Note: These will enable remote readings to be taken from a safe distance (at least 100 m).

8.4.4.3 Any meter should have a resolution of 0.1°C.

Note: Although the repeatability is very good, the accuracy between zero and 400°C can be $\pm 3^\circ\text{C}$, so it is recommended that, before use, meters or recorders, extension leads and thermocouples are checked by a liquid in glass, Laboratory Series 'A' thermometer, to BS 593, having an accuracy of $+ 0.02^\circ\text{C}$ between -20°C and $+ 100^\circ\text{C}$.

8.4.4.4 If a liquid in glass thermometer is used, for example in air temperature measurement, it should have a resolution of 0.1°C.

8.4.5 **Test ends**

8.4.5.1 Test ends shall be suitable for a design pressure of not less than the expected maximum test pressure.

8.4.5.2 Any test end shall be subject to a strength test at not less than 1.25 times the expected maximum test pressure.

8.4.5.3 The design of a test end shall state the maximum number of operating cycles prior to revalidation or disposal.

8.4.5.4 Test ends shall be identified uniquely.

8.4.5.5 A system shall be established to record the usage of test ends.

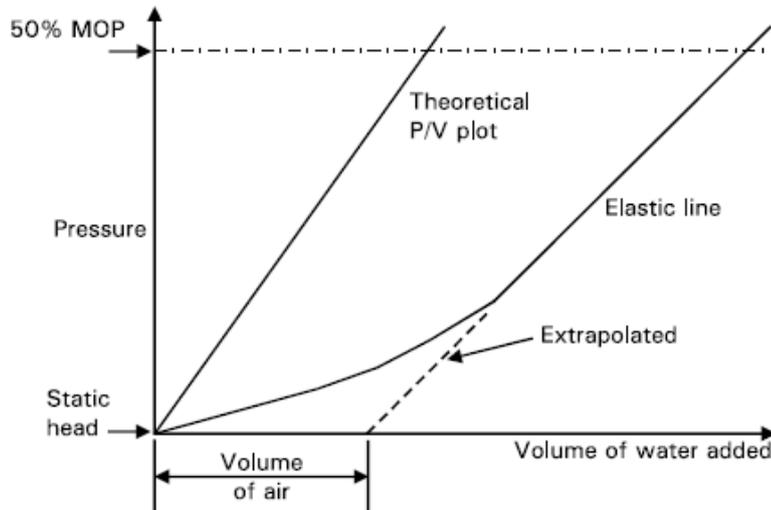
8.5 **ACCEPTANCE CRITERIA**

8.5.1 **Air content (see Figure 8)**

The air content shall not exceed 0.2% of the fill volume of a pipeline under test or 0.5% of the volume of an installation or short length pipeline diversion (typically up to 1 km).

Note: It is essential that all air is dissolved in solution to obtain a true hydrostatic test to which hydraulic parameters and criteria will apply.

Reference should be made to the relevant part of Appendix 5 for the procedure to calculate of air content.



Note: The air content is determined by constructing a P/V plot from static head pressure into the linear section of the P/V plot curve and extrapolating back to the axis. The volume of air is then read directly from the horizontal axis and compared with the total volume of the test section.

FIGURE 8 - MEASUREMENT OF AIR CONTENT

8.5.2 Temperature variations

Variations in temperature during the test shall be taken into account.

Note 1: Changes in temperature above or below ground, during a test, will affect the test pressure and make assessment of the soundness of the test impossible unless the changes are taken into account.

Note 2: The various temperature/pressure corrections provided in A5.1.1 indicate the change in pressure versus change in temperature for most sizes of pipe used in the gas industry.

8.5.3 Test acceptance

The relevant procedure for test acceptance criteria shall be as given in Appendix 5.

8.6 SAFETY – GENERAL

8.6.1 The safety of personnel and the general public is of paramount importance and measures to ensure safety shall be specified/included in the test procedure.

Safety precautions must comply with statutory and other relevant regulations. The precautions should be approved.

8.6.2 Prior to testing, all personnel engaged on testing or associated work shall be aware of the possible consequences of failure of a test or test fitting under pressure conditions and the hazards associated with the energy stored within a test section, particularly when it contains water and/or a gas.

8.6.3 All personnel engaged in pigging operations shall be instructed on the precautions necessary to ensure the safe operation and reception of pigs.

8.6.4 The test area shall be specified, approved and defined clearly to all personnel (see clause 9.8.4).

- 8.6.5 During testing and subsequent pressure-reducing operations, all construction or operational work in the test area or on the pressurised sections shall cease and all persons not involved directly should be evacuated from the test area.
- 8.6.6 Test equipment shall be situated in a safe location, away from public highways, other inhabited areas, depots and sites.
- 8.6.7 A certain amount of noise is inherent in all testing operations. Best practice should be employed to minimise noise emissions to levels acceptable to site personnel and the general public.

Special consideration shall be given to:

- siting and possible screening of plant and equipment
- use of acoustically-treated power tools, compressors and generators
- avoidance of operations outside normal working hours
- the use of a silencer to decrease noise levels during venting operations.

- 8.6.8 Suitable precautions shall be taken to protect any adjacent pipework or equipment from the potential effects of failure of the pipework under test.
- 8.6.9 During testing using media other than air or water, precautions shall be taken to prevent personnel from entering areas, for example pump pits, where dangerous concentrations of nitrogen or other test fluids may be present.

8.7 **SAFETY - PIPELINES AND INSTALLATIONS**

- 8.7.1 Testing shall not commence until confirmation has been received from the appropriate authority, in writing, that the following precautions have been taken:

- prior notification of testing has been given, in writing, to persons in the vicinity of the pipeline or installation.

An individual assessment should have been made for persons who will be resident near the pipeline or installation, during the period of the test

- prior notification of testing has been given to the local Police and other authorities who may be affected
- protective walls, constructed of sand bags, earth bunds or other methods, have been placed in agreed locations.

Particular attention shall be paid to blanked or capped ends of pipes and any adjacent operational pipework.

- 8.7.2 If testing is extended, additional notification to those specified in clause 8.7.1 shall be given.

- 8.7.3 Warning notices, stating "WARNING – PIPEWORK UNDER TEST", "NO PARKING", "NO ACCESS", "RESTRICTED ACCESS" AND "ACCESS BY PERMIT ONLY" shall be placed at appropriate locations, for the duration of the test.

The boundaries of the test area shall be defined using marker tapes, or a fence and at night, lighting shall be provided at appropriate locations.

- 8.7.4 It shall be ensured that, from the start of pressurisation, during the test period and until de-pressurisation, no person approaches within the following safety distances from the test section:

- for a test pressure equivalent to a design factor no exceeding 0.45, a distance of 30 m

- for a test pressure equivalent to a design factor exceeding 0.45, a distance of 100 m.

If it is necessary, because of site restrictions, for personnel to approach nearer than these distances, a suitable protective wall shall be constructed (see clause 7.8.1).

Note 1: For a test pressure not exceeding a design factor of 0.45, the 30 m safety distance may be reduced, after taking into account the proposed test pressure and the design pressure of the test section.

Note 2: It may be impractical to apply these safety distances to points of access to the general public, for example roads. In these instances, all reasonable measures need to be taken to ensure that the public do not dwell at these locations, by way of "NO PARKING" signs and regular patrols (see also clauses 8.8.3 and 8.8.5).

- 8.7.5 Patrols shall be provided to watch special points of hazard during the test, in particular road, rail and water crossings and other points of public access.
- 8.7.6 Standby emergency crews shall be available to deal with washouts or other damage.
- 8.7.7 The test pressure shall be reduced to a safe level before any work is permitted within the safety distance. The safe pressure level shall be not greater than static head plus 1 bar, unless specified otherwise in Appendix 5.
- 8.7.8 Hoses shall be anchored securely using an approved method to reduce the risk of injury to personnel in the event of failure.
- 8.7.9 High-pressure test hoses shall be:
- visually checked for damage prior to use
 - certified within a 6 month period preceding the test.

8.8 **SAFETY - SMALL BORE PIPEWORK (PNEUMATIC TESTING)**

- 8.8.1 Potentially, pneumatic testing is a more hazardous operation than hydrostatic testing at the same pressure, in that any failure is likely to result in more serious consequences.

There shall be appropriate consultation, at the pipework design stage, on the adequacy of the safety precautions proposed.

- 8.8.2 Safety precautions shall be subject to written approval before any testing work takes place, with particular reference to the following:
- adequacy of protection of any adjacent pipework or equipment
 - extent of the area cleared for test purposes (see clause 8.6.6)
 - adequacy of any applicable NDT carried out before the test, including testing previously carried out by others
 - procedures to prevent local chilling during filling and emptying
 - extent of remote monitoring provided during the test.

- 8.8.3 All personnel engaged in the test shall be instructed fully regarding the possible hazards involved in pneumatic testing.

- 8.8.4 Attention shall be paid to preventing whip in small bore pipes following failure.

Hoses shall be anchored securely using an approved method to reduce the risk of injury to personnel in the event of failure.

- 8.8.5 High-pressure test hoses shall be:
- visually checked for damage prior to use
 - certified within a 6 month period preceding the test.
- 8.8.6 The test area shall be clearly defined. It shall include all enclosed areas through which the pipework runs and local access ways.
- The boundaries of the test area shall be defined by marker tapes and purpose-made warning notices stating "WARNING – PIPEWORK UNDER TEST", which shall be displayed at all points where access may be gained to the test area.
- 8.8.7 As the pressure of the test medium is reduced from high pressure storage, its temperature will fall. The test arrangements shall be such that the temperature of the medium entering the pipework under test is not lower than the agreed test temperature.

In order to prevent condensation within pipework, the temperature of the test medium shall not be allowed to fall below the dew point at the corresponding test pressure.

8.9 TEST SECTIONS

8.9.1 Pipelines and installations

- 8.9.1.1 The pipework test sections may be made as long as is practical, provided the maximum variation in altitude in each section does not exceed 60 m.

The test sections shall be determined in advance of construction or re-testing giving due regard to the following:

- availability and disposal of water for testing
- topography

Note: In mountainous terrain, where strict compliance with the 60 m altitude limitation would unduly restrict test lengths, consideration may be given to a relaxation of this limit, providing that over or under-stressing of the pipework test section does not occur at the elevation extremes.

- impact of test failures where washout may give rise to a hazardous situation
- access to test points for tie-in and reinstatement works
- for re-testing existing pipelines or installations, the time scale that the pipeline or installation can remain out of commission, given the impact of a rupture
- potential damage to orifice plates, metering equipment, unidirectional valves and the like, that have been tested independently in accordance with IGE/TD/13 or IGE/GM/8 and where removal of part of all of the item may be necessary.

Spool pieces or blind flanges may be inserted where items have been removed or omitted, provided these are designed and constructed to a standard of at least that of the permanent pipework

- all small bore pipework, such as impulse and instrumentation lines, need to be disconnected and approved plugs or blind flanges installed
- testing against closed valves is not appropriate
- all below-ground pipework needs to be backfilled so far as is practical
- all underground connections prone to leakage, such as flanged joints and drain points, valve spindles and the like, need to be left exposed fully for inspection during the test

- consecutive sections of pipework need to be constructed so as to overlap such that the tie-in can be made with a single weld (see Sub-Section 7.26)
- all pipework is supported adequately to take the additional load imposed by the weight of the test water
- at installations, the pipework test sections may be combined and tested together
- all connections to lower design pressure systems are capable of being positively isolated
- annuli of ball valves are pressurised, where necessary by means of temporary connections from the annulus vent to the test section pipework, or by closing the valve by approximately 50%. The manufacturer's instructions for testing shall be observed.

8.9.2 **Pre-testing of pipes, fittings and fabrications**

8.9.2.1 Pipes to be pre-tested shall be assembled into strings, with a maximum of 4 strings per test and a maximum of 12 pipes in each string.

Note: Where a string fails or half strokes occurs before reaching the required test pressure (see Tables 8 and 9), this string may be isolated and the remaining strings tested with minimum delay.

Pipe which has not been affected by nor identified as attributing to the string failure, may be suitable for use in the main pipeline but shall not be used at locations in the higher risk areas.

8.9.2.2 Pipe strings shall be at a minimum spacing of 5 m and supported by an approved method which is designed specifically to provide a sufficient regular gradient to ensure that air can be vented readily.

8.9.2.3 Due regard shall be paid to ground conditions when designing pipe supports, in particular when an increase in support height is required to accommodate pipework gradients.

8.9.2.4 Where ground conditions make a regular gradient impractical or potentially dangerous, pigs or other means shall be employed to achieve a satisfactory fill.

8.9.2.5 Each pipe or fitting that has been pre-tested shall be identified clearly as such, together with the relevant test pressure.

8.9.2.6 Details of the pipes or fittings shall be retained as a permanent record with the test documentation.

8.9.2.7 Fittings for pre-testing shall not be welded directly together.

8.9.2.8 Fabrications which are to be concrete-coated, for negative buoyancy, shall be tested prior to the application of the concrete, in order to prevent fracture or spalling of the concrete.

Note: This test may be additional to any subsequent testing that is carried out once the fabrication is concrete-coated and installed.

8.10 **FITTING OF TEST ENDS**

8.10.1 Valves shall not be used for isolating test sections.

8.10.2 All test sections shall be sealed by suitable end enclosures, such as blind flanges, specifically-designed spades or purpose-built test ends.

Note: The use of pig traps is not a preferred method of sealing prior to hydrostatic testing.

8.10.3 Welded test ends shall only be fitted by means of an approved welding procedure.

All such fitting welds shall be subjected to full NDT examination, equivalent to that employed on the pipework section to be tested.

8.10.4 Where appropriate, test ends shall incorporate a device to establish that pigs or spheres have been launched successfully or received.

8.10.5 Each test end shall be identified uniquely.

8.10.6 Consideration shall be given to the frequency of use of test ends. Such information shall be recorded carefully, in order that periodic independent re-testing may be carried out.

8.11 **WATER SUPPLY**

8.11.1 For the purposes of hydrostatic testing, only approved clean water shall be used.

8.11.2 During the selection of test sections, account shall be taken of the need for consents or licences for the extraction/disposal of water (see Section 4).

8.11.3 Where the water source contains a high degree of solids in suspension, consideration shall be given to the use of filters, settlement tanks or lagoons.

8.11.4 Where there is a possibility of contamination or de-oxygenation of the water during testing, the problem shall be addressed and resolved prior to the commencement of testing operations.

8.11.5 Filling and emptying shall be carried out in accordance with Appendix 6.

8.12 **REPAIR OF TEST FAILURES AND LEAKS**

8.12.1 Prior to the commencement of any testing works, a comprehensive repair and NDT procedure shall be established.

8.12.2 Materials used for repairs shall be compatible with the existing pipework.

8.12.3 Where a leak is suspected, the test section pressure shall be reduced to the design pressure prior to carrying out a visual examination.

8.12.4 Work to repair any leak or failure shall not be carried out until the pressure has been reduced to a safe level (see clause 8.7.7).

8.12.5 In the event of a test failure, the test section shall be repaired and re-tested as follows:

- where failure occurs prior to the pre-determined test limit, the repair shall be made with pipe which may not have been pre-tested.

After completion of the repair and refilling of the test section, the test shall be recommenced from the beginning, including a new air content check.

The records for the test failure shall be retained as part of the permanent record of the pipeline or installation or

- where failure occurs after the pre-determined test limit, the time under test shall be noted and the repair made using pre-tested pipe.

After completion of the repair and refilling, the test section shall be subjected to a further air content check.

The test section shall then be re-pressurised to the test limit attained in the original stage of the test.

The test shall then proceed for a further period, such that the aggregate time will be at least equal to the required test period.

Where pre-tested pipe is not available, the test shall be recommenced from the beginning, as in Sub-Section 8.1.

8.13 RECORDING AND DOCUMENTATION

8.13.1 General

8.13.1.1 A documentary record of all tests shall be compiled and retained for the life of the pipeline or installation.

8.13.1.2 Care shall be exercised in the identification of test documentation to ensure that it can be identified accurately in the future.

8.13.1.3 The documentary record shall include:

- test or calibration certificates for all instruments and equipment used in the measurement of the test (see clause 8.13.2)
- the records produced during the test (see clause 8.13.3)
- a test certificate (see clauses 8.13.4 and Figure 9).

8.13.2 Test equipment and instruments

8.13.2.1 All instruments and test equipment used for the measurement of pressure, volume and temperature shall be certified for accuracy (see Sub-Section 8.5).

8.13.2.2 The following instruments should, as a minimum, be provided at the test control centre:

- where a P/V plot is specified in the procedure;
 - dead weight tester
 - pressure gauge
 - temperature indicators
 - pressure and temperature recorders
 - duplicate water volume measurement equipment
 - calibrated tanks for volume measurement.
 - pump stroke indicator or rev counter.
- where a P/V plot is not specified in the procedure;
 - standard test gauge
 - temperature indicators.
- for small bore pipework subject to a pneumatic test;
 - standard test gauge
 - temperature indicators.

8.13.2.3 Gauges and recorders shall be calibrated and certified immediately prior to testing operations.

Note: Where subsequent movement of the testing equipment over rough terrain is required, it is recommended that this be carried out immediately prior to each test.

8.13.2.4 Dead weight testers shall be certified within the 12 month period preceding the test.

- 8.13.2.5 Pressurising pump delivery shall be checked by a calibrated tank and verified in writing.
- 8.13.2.6 A means of measuring accurately any water drained off during the test shall be provided.
- 8.13.2.7 High-pressure test hoses shall be certified within a 6 month period preceding the test.

8.13.3 **Test record**

The test record shall, where referred to in the relevant test procedure, contain the following documentation:

- an air inclusion plot, together with all tabulated measurements and calculations
- tabulated measurements and graphical plots of pressure against volume during the pressurisation period, which represents the stress/strain graph for the pipework steel
- tabulated results of pressure against time during the initial decay and test hold period
- volume of water added or drained from the test section once the pressurisation limit is reached
- visual records of pressure and temperature
- tabulated measurements of temperature. Care shall be taken, when measuring water temperature in the test section, to ensure the temperature transducer is correctly located
- identification of any joints or materials that cannot be tested
- details of all pipework tested, including any unique material or fitting identifiers where pre-testing is carried out
- a test certificate (see clause 8.13.4).

8.13.4 **Test certificate**

On completion of each test, a test certificate shall be compiled which should include, but is not limited to, the following information:

- an accurate description of the pipeline project or installation to which the test relates
- a detailed description of test start and finish points
- details of all pipework tested including diameter, wall thickness, grade, manufacturer and external coating
- the required maximum test pressure in the test section, together with details of its derivation or source
- the test pressure achieved at the maximum, minimum and test control point locations, together with their relative locations
- the procedure, Edition and Section with which the test complies
- date and time of test start and finish.

Note: Figure 9 provides an example of a test certificate.

SECTION 9 : COMMISSIONING OF PIPELINES

9.1 GENERAL

9.1.1 When a pipeline is to be brought into service following construction, it shall be purged of air using an approved direct or indirect process prior to gas being transmitted.

Measures shall be taken to prevent the formation of methane hydrates in methane-rich transmitted gases caused by water which remains after hydrostatic testing.

Note: Other hydrocarbon gases can also form hydrates.

Tests shall be carried out to monitor any odorant level when the pipeline is put into service.

Note: A possibility exists, particularly if there has been a significant lapse of time between gassing up the pipeline and putting it into service, that the odorant level of the gas may be affected adversely.

9.1.2 Prior to gassing up, a new pipeline shall undergo hydrostatic testing (see Section 8). Although preliminary pigging runs may appear to be effective in removing water from the pipeline, a certain volume inevitably remains on the inner surface. In order to effectively dry the pipeline, the maximum possible amount of free water shall be removed by multiple pigging runs. Water also gathers at low points and in the body cavities of ball valves.

Note 1: The presence of water in a gas transmission pipeline can result in corrosion, the formation of solid hydrate of contamination of the product. Water may also cause very serious operational difficulties.

Note 2: It is considered that, at dewpoints at or below -20°C , corrosion will not occur. This degree of dryness is attainable with more or less standard desiccant dryers, which will output air at -40°C dewpoint at atmospheric pressure.

Note 3: Where vacuum drying is used, the value of -20°C is equivalent to a saturation vapour pressure of 1.032 mbar, which is attainable by the use of vacuum pumps of a reasonable capacity, on a normal pipeline system.

The dewpoint required should be decided at the design stage and stated in the specification for commissioning.

9.1.3 The choice of method for the removal of water, to be followed by gassing up of a pipeline, should be made following consideration of the proposed timing of the operations, the nature and characteristics of the gas to be transmitted and the design, operation and maintenance criteria for the particular pipeline system.

Note 1: The principal circumstances which may occur are:

- a dry pipeline, which can be commissioned straight to gas. Refer to IGE/SR/22
- a wet pipeline which is dried prior to gassing up
- a wet pipeline which is dried and gassed up simultaneously.

Note 2: The methods available for drying are:

- using super-dry air or dry inert gas, where an air-drying plant and compressor produce dry oil-free air to push a series of pigs through a pipeline, collecting water until the required dryness is achieved
- vacuum drying, where evacuation of a pipeline causes water to boil off at the ambient temperature of a pipeline, the vapour formed being drawn off until the required dryness is achieved.
- operational drying, where a pipeline may be purged using an inert gas and then gassed up and operated at a pressure where hydrate formation will not occur at ambient temperatures. When checks prove an acceptable dewpoint is achieved, the pipeline may be elevated to its full operating pressure. In this case, care is needed to ensure

water does not collect in pipework on installations and subsequently freeze due to the Joule Thompson effect.

Combinations of the above methods, except operational drying, can be used for particular circumstances or conditions.

Note 3: Gassing up may be carried out immediately after any of the above drying operations.

Guidance on commissioning is given in IGE/SR/22.

For vacuum drying, consideration may be given to the direct injection of gas into the vacuum created in the pipeline.

9.2 **PRELIMINARY ARRANGEMENTS**

9.2.1 **Planning**

9.2.1.1 A detailed programme of operations and procedures shall be prepared, circulated and approved in advance of the operation. The programme should nominate a person to be in sole charge of operations. The programme and procedure(s) shall define clearly all stages of the commissioning operations, together with the duties and responsibilities of the personnel involved, incorporating and appropriate permit to work system. The authorised procedure should also detail initial and final valve positions and movements.

9.2.1.2 Advance consultations, to agree the timing of the operations, shall take place with the appropriate control centre operators. These should also agree the daily volume and rate of flow of gas to be used. Similarly, advance consultation shall take place with the nominated person responsible for safety concerning the precautions, which shall be observed and drawn to the attention of all personnel.

9.2.1.3 Before commissioning, a certificate of compliance shall be handed to the pipeline operator. Commissioning shall not take place until all operating, maintenance and emergency procedures are established and in place.

9.2.1.4 Upon completion of commissioning, a formal handover shall ensure that all records of design, construction, and testing are given to the pipeline operator.

9.2.2 **Safety and welfare**

9.2.2.1 *Statutory regulations*

In the UK, all aspects of the commissioning and pressurisation of a pipeline are subject to The Health and Safety at Work etc. Act (HSWA) and other appropriate legislation as listed in Appendix 2.

Arising from HSWA, an employer must ensure that all personnel are made fully aware of the relevant safety aspects, including the dangers of toxic materials.

Necessary safety precautions must be taken for the protection of personnel, members of the public and property that might be affected by the works.

9.2.2.2 *Safety and welfare equipment*

Safety and welfare equipment shall be available on site.

Personnel must wear appropriate personal protective equipment (PPE) during all operations.

9.2.2.3 *Notification to relevant authorities*

The police, fire and civil aviation authorities, as well as other interested parties, should be given advance notice of the date on which commissioning is to be carried out.

9.2.2.4 *Safety training*

Employers must provide such instruction, training and equipment as is necessary to ensure, as far as it is reasonably practicable, the health and safety at work of all personnel.

Note: A high concentration of nitrogen can cause asphyxiation.

9.2.3 **Attachments**

Attachments, for example pig signallers, vents, pressure gauges and recorders, should be fitted at both launch and reception points on the line, together with valved attachments to facilitate the injection and reception of nitrogen. In addition, suitable gas sampling points shall be considered.

The methanol injection point or vacuum connection shall be downstream of the launcher trap isolation valve and should be not less than 50 mm diameter.

Pig launchers, pig launcher cradles, pig receivers and pig receiver cradles shall be bonded to unloading equipment.

9.2.4 **Access to launch and reception sites**

9.2.4.1 *Road access*

A suitable hard surface access road and hard standing should be provided. The road surface should be at least reasonably level.

Adequate clearance beneath overhead obstructions should be available to allow free access and operation for plant vehicles.

9.2.4.2 *Access to valves*

Facilities shall be provided to enable site personnel to gain access to all valves and equipment in a safe and proper manner.

9.2.5 **Site security**

Site security shall be ensured with adequate security fencing. If this is not possible, the site should be manned continuously.

Suitable notices must be displayed prohibiting access by unauthorised persons and "NO SMOKING" and "NO NAKED LIGHTS" notices must be displayed prominently. Where other operations are proceeding on the site, an area for each operation shall be defined clearly by physical barriers with additional appropriate warning notices displayed around the perimeter.

Sources of ignition shall not be sited within 15 m of any point of possible leakage of gas or flammable liquid.

9.2.6 **Lighting at terminals, etc.**

Floodlighting, suitable for Zone 1 in accordance with an appropriate standard, shall be considered at both launch and reception sites and any other locations as necessary, for example at block valves.

9.2.7 **Monitoring of pigs**

Listening points should be provided at suitable intervals along the pipeline so that the progress of pigs can be reported.

Note: Block valve installations can be used for this purpose as, normally, facilities exist at these points for fixing pressure gauges which will give a positive indication of the passage of pigs.

Arrangements shall be made for listening observers to be in communication with both launch and reception terminals and any other manned locations.

Alternative methods of detection, using proprietary tracking/listening devices, should be considered.

9.2.8 **Pre-commissioning inspections**

Before operations commence, all installations shall be inspected to conform that:

- all valve attachments, actuators, pig signallers and pig trap doors are operational
- all valves are operational and maintained
- all necessary vents, drains, test gauges etc. are in position and functional
- all valves, pig signallers, etc. are identified and referenced correctly and are in their correct position in accordance with the approved procedure
- all other preliminary requirements are satisfied
- warning notices, fire fighting equipment and barriers are sited as appropriate
- reception and storage tanks, vehicles or other equipment are not placed in direct line with, and sited at least 15 m away from, the pig trap door
- communication systems are operational.

A certain amount of noise is inherent in all commissioning operations. The precautions outlined in clause 8.4.2 shall be applied during commissioning.

9.3 **PRELIMINARY PIGGING**

The entire pipeline should be swabbed thoroughly and satisfactorily gauged in a preliminary pigging operation.

Note: This may have been carried out during the testing procedure (see Section 8).

Several pigging runs will be necessary to remove as much water as possible from the line. Consideration should also be given to the use of magnetic pigs/geometric pigs/gauging pigs and cleaning pigs. After pigging, precautions shall be taken to prevent the ingress of water and foreign matter into the pipeline.

Particular attention shall be given to clearing water from ball valve bodies.

9.4 **DRYING, PURGING AND GASSING UP**

A pipeline should be commissioned by one of the following procedures:

- super dry air/nitrogen followed by gas

- vacuum drying followed by purging and gassing up

9.4.1 **Super-dry air/nitrogen followed by gas**

The optimum length for drying by this method is approximately 30 km. Normally, lengths greater than this are avoided to prevent abrasion of the pig material.

This method utilizes an air drying unit and compressors to produce dry, oil-free air or a dry inert gas which is used to propel foam pigs through the pipeline. These pigs absorb water, remove pools of water at low points and distribute any residual water as a thin film on the internal pipe wall to facilitate faster evaporation. On completion of the drying/purging operation, the pipeline can be gassed up immediately or sealed off for gassing up at a later date.

Alternatively, a pipeline can be simply dried by passing super dry air or gas through the pipeline after the free water has been removed by multiple pigging runs.

In order to minimise the time required for an air drying operation, it has to be recognised that a given mass of air can take up only a limited amount of water vapour, the precise amount being calculable from the initial dryness and the temperature with reference to saturation tables. Thereafter, the larger the throughput, the shorter will be the drying time. However, the rate at which water molecules are transferred from the pipe wall to the free stream is, in part, dependent on a coefficient which is proportional to pressure and temperature. The pressure in the drying medium needs to be kept low.

In order to determine the dryness of the pipeline, the moisture content of the air at the discharge end of the section is measured by recording the dewpoint temperature. The moisture content of the discharged air can be obtained by reference to the dewpoint temperature in standard saturation vapour pressure tables.

9.4.1.1 *Operational equipment*

(a) Super-dry air

The air drying/super-dry air equipment should be located at the launching end of the pipeline and connected to allow the repeated dispatch of foam pigs during the operation. The air-drying unit should have sufficient capacity to suit the pipeline size and be able to achieve a dewpoint temperature below that specified. The unit should have two absorption vessels with fully automatic change over facilities for regeneration to allow for continuous working. Dewpoint temperature measuring instrumentation should be installed at both the pig launching and receiving stations to allow continuous monitoring to take place. This should be calibrated and checked in accordance with an agreed procedure and check list.

(b) Inert gas

The equipment and instrumentation for inert gas should be located and operated as for the super dry air method. Sufficient capacity should be available to suit the pipeline size and dewpoint temperature required.

Note: The gas may be supplied in a gaseous form from bottles or be a direct supply pipeline or be in liquid form in tankers, in which case a vaporiser will be required of sufficient capacity to suit the speed of supply.

9.4.1.2 *The drying operation*

As soon as the first pig has been despatched, the instrumentation at the launching end should be checked to ensure the air drying unit is attaining the required dewpoint temperature.

Pigs should be discharged at regular agreed intervals, established from calculations based on the length and internal condition of the pipeline, as well as the ambient temperature of the ground and dewpoint temperature to be achieved.

Instrument readings at the receiving end should commence when there are no further signs of moisture being expelled or when the pipe begins to discharge dust.

Note 1: An approximation of the number of foam pigs required following the dewatering operation is as follows:

<i>Internally coated pipe</i>	<i>0.5 pigs/km</i>
<i>Uncoated pipe</i>	<i>1 to 1.3 pigs/km</i>

Note 2: The mechanism of air drying is such that the exhausted air will be saturated until very close to the end of the operation. If the dewpoint sensors come into contact with free water, they will take a considerable time to recover and, if contaminated by particle matter, will need to be replaced.

9.4.1.3 *Completion of the drying cycle*

Shortly before drying is concluded, the block valve cavities should be purged with dry air/nitrogen by closing partially the mainline valve and venting to atmosphere. The pipeline can be considered to be dry along its whole length when the required dewpoint has been reached at the receiving end. The line should then be closed off and the air drying equipment removed.

9.4.1.4 *Gassing up*

The pipeline should be commissioned in accordance with IGE/SR/22. If gassing up is to take place some time in the future, the pipeline should be secured in dry air or an inert gas. When gassing up is due to take place, the dewpoint should be re-checked prior to introduction of the gas behind pigs and an inert gas slug.

9.4.2 **Vacuum drying followed by purging and gassing up**

The temperature at which water will undergo a change of state from liquid to vapour is dependent on its pressure. At normal atmospheric pressure, this change of state occurs at 100°C. This is known as the "saturation vapour temperature". If the pressure is reduced, the change of state will occur at a lower temperature. Thus, at a pressure of 10 mbar, water will evaporate at 7°C, and it is this vapour which is extracted by the vacuum drying process.

Note: Typically, a dewpoint of -20°C is equivalent to a saturated vapour pressure of 1.032 mbar.

The method may take longer than drying with air or nitrogen but, when fuel costs are taken into account, vacuum drying may prove cost effective.

9.4.2.1 *Operational equipment*

The vacuum plant should be installed at the agreed location and run for a specified period against closed connections to ensure that leaks associated with the temporary connection have been minimised and that the agreed minimum pressure can be achieved.

The pumping equipment should have sufficient capacity to suit the pipeline volume and be able to achieve a dewpoint temperature below that specified, but care should be taken to regulate the flow during evaporation to avoid over-rapid cooling of the free water during evaporation. Certified vacuum gauges and temperature measurement instrumentation should be installed at both ends of the pipeline to allow continuous monitoring to take place.

Dewpoint temperature measuring Instruments should will be accurate to $\pm 2^{\circ}\text{C}$ and the instrumentation should be calibrated and checked.

9.4.2.2 *Personnel*

Personnel should be available for each location of equipment and/or instrumentation, in sufficient numbers to allow for continuous working over a number of days.

9.4.2.3 *Evacuation*

The pressure of the system is reduced to the point where the water in the pipeline is able to boil at the temperature of the pipeline surroundings. At a pressure of between 200 and 300 mbar, an evaluation of the system in-leakage should be made by temporarily ceasing drawdown and isolating the system for a set period, usually 12 hours, quantifying the air in-leakage. If the air in-leakage is large, remedial measures should be taken to locate and reduce the leakage. After a successful leak check, the vacuum plant should be brought back on line and pressure reduction continued until the specified pressure is reached.

9.4.2.4 *Evaporation*

Evaporation of free water will commence nearest the vacuum pump(s) and will move away from the pump(s) as the process progresses.

Given a constant temperature and a frictionless system, the pressure will be constant throughout and evaporation will take place simultaneously along the length of the pipeline.

However, a dynamic pressure gradient will exist within the pipeline due to the frictional effects on the flow of vapour. While evaporation will take place at a relatively constant pressure, the pressure seen at the pump suction will be lower than that seen where evaporation is taking place. Therefore, the distance from the vacuum pump(s) of the area being dried will increase with time, and will be characterised by pressure at the pump suction falling, with consequent reductions in the quantity of vapour pumped.

Evaporation will continue until all free water is evaporated. The pipeline will now contain water vapour at low pressure.

9.4.2.5 *Final drying*

The water vapour in the pipeline should removed and the system pressure reduced to a level where the pipeline is at or below the saturated vapour pressure.

Having established that all the water vapour has been removed, a "soak test" should be conducted following system isolation, and the pressure monitored over an agreed period, usually 24 hours. The dryness of the pipeline can then be proved since, at these low pressures, any water remaining will evaporate, producing a system pressure increase greater than that evaluated by in-leakage (previously assessed during the leak check isolation during the evacuation process).

If the valves obtained indicate the presence of water in the system, the vacuum plant should be brought back on line until the agreed dew point level has been reached.

Following a successful soak test, the line should be re-evacuated to the ultimate level achievable and the system made ready to commission.

Where dewpoints drier than -20°C are specified, it may be necessary to investigate a dry air or nitrogen purge. This requires dry air (typically at -40°C or better) or nitrogen to be introduced at one end of the pipeline section while drawing through the section using vacuum plant at the remote end, thus preventing water "dropping out" of the vapour on to the pipe wall through the effects of over compression.

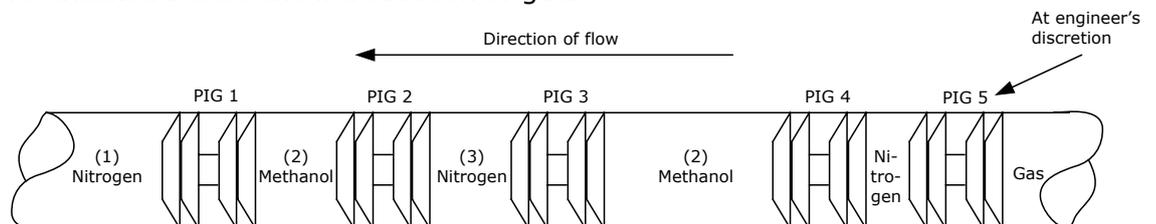
The air purge should be maintained at a constant level until the required dewpoint is reached. Subsequently, the line should be re-evacuated to the ultimate level achievable and the system made ready to commission.

9.4.2.6 *Gassing up*

The pipeline should either be gassed up immediately into vacuum or packed with dry air or nitrogen for gassing up at a later date.

If gassing up is to take place immediately on completion of vacuum drying, this can be undertaken directly into vacuum with vacuum pumps at the remote end drawing off vapour to prevent water drop out due to the effects of over compression. The discharge from the pumps should be monitored to detect the presence of gas. When gas is detected at the remote end, the pumps should be shut down and the gas taken to vent until the dewpoint specified for the gas is achieved. Gas injection should continue until the agreed commissioning pressure is attained.

When gassing up into dry air or nitrogen, the dewpoint temperature should be re-checked before the introduction of gas.



9.5 **PRESSURISING**

9.5.1 **Preliminary works**

All valves shall be positioned to allow the pressurisation of flanges and fittings. Any leakage shall be reported.

Consideration shall be given to the use of a flow meter in the gas admission line. All valves shall be checked for their positions, in accordance with the authorised procedure.

9.5.2 **Pressurisation**

9.5.2.1 *Pipelines*

Gas should be admitted via the control valve, ensuring that the maximum permitted flow rate agreed with the control centre is not exceeded. All flanges and fittings shall be checked for leak tightness at 7 bar intervals. Any leakage shall be reported immediately.

The means of rectification shall be authorised.

During pressurisation, the pressure gradient along the pipeline shall be monitored and recorded, using gauges connected direct to the pipeline at bridles, valves, pressure reduction station inlets and the terminal ends.

On reaching the full pressure, all valves on the system shall be checked to ensure they are in their correct positions in accordance with the authorised procedure.

The pipeline may now be considered operational and maintenance procedures instituted.

9.5.2.3 *PRIs*

All PRIs fed from the pipeline shall be brought into operation and monitored regularly for gas dewpoint and performance.

If the PRI inlet dewpoints are not satisfactory, consideration shall be given to the following:

- use of low outlet flow rates
- gas pre-heating
- regulator small bore pipework heating.

If the gas is odourised, the odourant level shall be checked at the PRI outlets. If necessary, the odourant level shall be corrected by odourant injection at the new systems source.

On completion, all sample points, temporary pressure connections etc., shall be removed and the fittings plugged.

SECTION 10 : PROTECTION AGAINST CORROSION

10.1 GENERAL

10.1.1 Provided the quality of the gas as described in Section 6 is maintained, it is not expected that a pipeline carrying dry Natural Gas will suffer internal corrosion.

External corrosion of a buried pipeline may arise from the nature of the surrounding ground, from contact with other buried metallic structures or from the pick up and discharge of stray DC electric earth currents, for example such as may occur with an electric traction system.

Prevention of external corrosion shall be achieved by a combined system of coating and CP. An external coating alone should not be considered adequate corrosion protection.

10.1.2 Reference should be made to appropriate standards for guidance on the selection of materials and requirements for their application, for example BS 5493 and BS EN 23270.

10.1.3 All internal and external painting and coatings systems shall be in accordance with an approved specification. The coatings should be tested for physical durability and the resistance to chemical attack.

10.1.4 Consideration shall be given to the temporary protection of weld preparation areas during transport, handling and storage, guidance on which is provided in IGEM/TD/1 Supplement 1.

10.2 SPECIAL SITUATIONS

10.2.1 Avoidance of known corrosion hazards

At the route planning stage, consideration shall be given to the avoidance of the more obvious corrosion hazards, for example by routing to avoid:

- stray DC earth current areas
- paralleling of high voltage overhead power lines
- pylons
- contaminated ground
- naturally aggressive ground, for example peat.

10.2.2 Pipelines operating at elevated temperatures

Where a pipeline or section of pipeline operates at an elevated temperature, for example immediately downstream of compressors, the coating material shall be suitable for service in such conditions.

Note: Such suitable materials include thermosetting powders and liquids and three layer systems with a polypropylene outer sheath.

10.2.3 Stress corrosion cracking (SCC)

If coatings susceptible to disbondment are used, the maximum operating temperature should be limited accordingly.

Note: SCC may occur under disbonded coatings at elevated temperatures (generally than 30°C), where effective CP at adjacent coating damage provides the causative chemical environment. It may also occur at normal temperatures, where mildly acidic ground water is present under the disbonded coating, in the absence of effective cathodic protection, due to the shielding effect of the coating.

10.3 COATINGS

Wherever possible, coatings for pipes and fittings should be factory-applied. Materials used for coating on site shall be compatible with any factory applied coatings.

In selecting suitable materials, consideration shall be given to the operating regime and the eventual siting of the component, for example buried or above ground, and the temperature range likely to be experienced.

Note: Some coating materials could, for example, be affected adversely by solar heating or exposure to ultra violet radiation.

10.3.1 Internal pipe coatings

10.3.1.1 Notwithstanding the non-corrosive nature of dry Natural Gas, pipes should be internally coated to prevent rusting during transit and storage.

Note 1: The presence of rust could give rise to problems of internal dust and blockage of filters, etc. during operation.

Note 2: In certain circumstances, it may be advisable not to use an internal coating, for example when the pipeline is carrying gas laden with hydrocarbon condensate.

10.3.1.2 A further advantage of internal coating is the reduction of friction losses within the pipeline.

Note: Normally, the internal coating system would be epoxy based, and be applied to a surface blast cleaned to an approved standard and profile or to a surface which has been chemically cleaned, phosphated and thoroughly washed in accordance with an approved specification.

10.3.1.3 The thickness of the coating material shall be selected to match the duties required, for example expected duration of storage, ability to withstand methanol swabbing, ability to withstand pigging, etc.

10.3.2 External pipe coatings

10.3.2.1 Factory-applied coatings

Factory-applied external coating systems shall be such as to provide long term electrical and mechanical characteristics, which are suited to the diameter and operating conditions of the pipe and the nature of the environment. The coatings shall adhere strongly to the pipe and resist satisfactorily cathodic disbonding at holidays.

The coating shall be applied to a clean, dry surface.

Note: Blast cleaning is the preferred method of cleaning.

The coating system should proceed with minimum delay after surface preparation and in accordance with a recognised specification.

Note: The coating material may be fusion bonded powder, coal tar incorporating a glass fibre reinforcement, extruded high density

Where a reflective layer is applied to the protective coating, it should be omitted for a distance of 300 mm at each end of the coating.

If pipes are to be installed by thrust or auger boring, appropriate coatings shall be used.

Where pipework extends above ground, coatings specified for below ground applications shall not be used. The first 500 mm of pipework emerging from the

ground shall be given additional protection, for example with a multi-component liquid, to provide a satisfactory transition between the pipeline coating and the paint system.

For pipework that will be lagged for thermal or acoustic purposes, approved coatings such as multi-component liquids or grease based tapes should be used.

10.3.2.2 *Field-applied coatings*

Field-applied coating systems shall be selected and applied in accordance with an appropriate procedure to reproduce, as far as possible, the factory-applied coating.

Note: In some situations, for example where the factory-applied coating is extruded polyethylene, the use of compatible, spirally applied wrapping tape or compatible shrink materials may be acceptable.

In all cases, the pipe should be blast cleaned and the selected coating system should be applied in accordance with a recognised specification.

Note: There may be occasions when it is desirable to apply a second protective coating to factory-coated pipe, for example to improve mechanical features of the coating in rocky ground, or as a further safeguard at particularly hazardous points.

Additional protection may be required to prevent migration of objects within the ground. This may involve containment of selected fill around the pipe or use of membranes or barriers where these are used, effective operation of the CP systems shall be ensured.

Following welding and weld inspection, the pipe coating shall be completed at joint areas. While the requirements of clause 10.3.2.2 apply, particular care shall be taken to ensure that the materials chosen are compatible with, and adhere strongly to the pipe coating. An adequate overlap by the field-applied material shall be provided on to the original cleaned pipe coating.

Note: Since this work will, normally, be carried out in the field, it is particularly important to consider the suitability of the coating material for the site and climatic conditions and its ease of application.

10.3.3 **Coating of other below-ground components**

All below-ground components, forming part of a cathodically protected pipeline, shall be coated to a common standard. Valves, etc., sited below ground level, shall be so coated even when housed in chambers.

The complex shape of some components may require consideration of coating materials other than those used for pipes. All coating employed shall be resistant to mechanical damage, particularly where there is a likelihood of personnel accessing pits, etc.

10.4 **CATHODIC PROTECTION (CP)**

10.4.1 **General**

As soon as possible during construction, CP shall be applied to the pipeline in accordance with standards such as BS 7361-1. CP may be applied either by means of sacrificial anodes or by the impressed current method.

Attention shall be, particularly, paid to the following aspects of BS 7361-1:

- the need for electrical insulation joints at offtakes and other installations
- other forms of electrical isolation

- the provision of permanent monitoring facilities
- possible secondary effects such as coating disbondment or electrical interference with adjacent buried structures
- the protection of sleeves (see Sub-Section 6.11)
- the need to avoid inadvertent earthing of the CP system through such items as pipe supports, instrument connections, electrically operated valve actuators, reinforced concrete piles remaining after construction, etc.

A CIPS of the entire pipeline shall be undertaken as soon as possible after complete commissioning of the CP system, in order to fully validate and provide a "fingerprint" of the CP system.

10.4.2 **AC corrosion**

When pipelines are routed parallel to overhead high voltage power lines, voltages can be induced into the buried pipeline. The mechanism of AC corrosion is not fully understood but European case studies indicate that, where the AC current density is between 30 and 100 Am⁻² measured on a 10 cm² coupon, the corrosion risk is uncertain but at values exceeding 100 Am⁻² there is a risk of AC corrosion.

When routing pipelines, long parallelisms with overhead power lines of 132 kV or greater should be avoided or at least minimized:

- separation distance > 500 m should be maintained for parallelisms > 3 km
- separation distance > 200 m should be maintained for parallelisms < 3 km.

10.4.3 **Mitigation measures**

Following measurement of the induced voltage and current, AC voltage >15 V or current density greater than 100 Am⁻² will require mitigation measures to be undertaken. This may require specialist design using modelling software packages. Earth gradient wires, installed as part of an AC mitigation scheme, should be connected via solid state DC decoupling devices irrespective of the gradient wire material. 10 cm² coupons should be installed at fixed test posts along the parallelism in addition to the usual corrosion coupons to facilitate subsequent monitoring of the AC current density.

10.5 **RECORDS**

Permanent records should be maintained of all corrosion control measures. These should include:

- type of internal coating
- types of external factory/field applied coating
- disposition and type of CP components and bonds
- CP monitoring results
- state of interference bonds and shared schemes
- paint system performance
- results of inspection surveys, for example Pearson, CIPS, nitrogen sleeves etc.
- remedial work carried out
- sleeve protection details, including any auxiliary anodes.

Note: An integrated computer/pipeline management system may require additional specific information.

SECTION 11 : OPERATION AND MAINTENANCE

Certain parts of this section apply to the operation of pipelines constructed before the publication of this edition of IGE/TD/1. Details of the application of specific editions of IGE/TD/1 to the operation of pipelines are shown in the decision algorithms, Figures 11 and 12.

11.1 GENERAL

All diversions, modifications and repairs of existing pipelines shall be in accordance with all sections of this, the latest edition of IGE/TD/1. In addition, reference shall be made to IGE/GL/5.

11.2 MANAGEMENT

11.2.1 Administration

11.2.1.1 A system of surveillance, inspection and maintenance shall be established for all high pressure pipelines and their ancillary equipment. A pipeline integrity management system shall specify the operational surveillance, inspection and maintenance required. It should set out schedules, procedures and instructions under which these activities should be carried out.

Such schedules, procedures and instructions shall embrace all aspects, including liaison with other departments, third parties and those responsible for gas movement or control. Such arrangements should be reviewed and updated as appropriate.

11.2.1.2 A separate Emergency Procedures Manual (EPM) shall be provided to deal with situations which necessitate emergency actions (see clause 11.2.3.8). The EPM should include details of the organisational response to emergencies, the safety precautions to be observed in preventing loss of life, injury and damage to property and the means of resourcing specialist services and equipment. The preparation of the EPM shall take account of local authority emergency plans.

11.2.2 Legal and allied considerations

The requirements of Section 4 shall be observed. All work must be in accordance with the relevant legal requirements, and shall be in accordance with safety codes and recommendations of appropriate bodies.

11.2.3 Safety management

If it is decided to use discretion in the application of this Standard, the risks associated with any variation shall first be considered (see also IGE/SR/24).

11.2.3.1 Emergency contacts

Arrangements shall be made for the receipt of reports of gas escapes by correspondence and in person, at company premises occupied during normal working hours. Adequate publicity should be given to the methods of reporting gas escapes.

Contact telephone numbers for use by the general public shall be publicised widely, and adequate telephone answering facilities shall be manned at all times in order to receive calls reporting gas escapes. Reference should be made to IGE/SR/20 for further guidance.

11.2.3.2 *Training*

Personnel engaged in activities on high pressure pipelines shall be adequately and regularly trained. The training shall cover all aspects of safety and emergency procedures and equipment, as well as technical matters concerning the operation and maintenance of high pressure pipelines and associated equipment.

11.2.3.3 *Equipment*

Personnel engaged in activities on high pressure pipelines shall be issued with suitable protective clothing and equipment and, where necessary, emergency rations. Vehicles used shall be equipped with all necessary communication and safety equipment. Measures shall be taken to ensure that safety equipment is used whenever necessary.

11.2.3.4 *Permit to work system*

A documented permit to work system shall be in place to supplement other job instructions when the work is non-routine, may be potentially hazardous and a risk to personnel and others, or could damage plant or equipment.

An authorised person shall determine which activities require a permit to work by taking into consideration the potential hazards associated with the work activity. Attention shall also be given to factors which may change, requiring the issue of a new permit to work.

A permit to work system shall have the following features:

- clear identification of who may authorise particular work activities and who is responsible for specifying the necessary precautions.
- training and instruction in the use of permits
- monitoring and auditing to ensure that the permit to work system operates as intended.

11.2.3.5 *Non-odorised gas*

Particular attention shall be given to enclosures, confined spaces and public – reported gas escapes where systems transport non-odorised gas.

11.2.3.6 *Inspection and routine work*

The following requirements provide a general guide when carrying out routine pipeline maintenance, including the physical inspection of exposed pipelines (which does not involve mechanical damage assessment).

- (a) Appropriate communication routes shall be established between the site and the operational control centre.
- (b) Before starting work, the site shall be examined for gas leakage. If a significant gas presence is found, the remaining procedures of this clause, and those of clauses 11.2.3.7 and 11.2.3.8 shall be put in hand. In these circumstances, a working area, based on gas concentration measurements, shall be established and monitored to ensure a safe working environment.
- (c) Smoking, naked lights and other sources of ignition shall not be allowed in the vicinity of the work and prohibition notices to this effect should be displayed. Fire fighting equipment should be available on site. The

positioning of powered plant shall be considered carefully, as such equipment can be a source of ignition.

- (d) Entry shall not be made to any building, trench or other confined space where gas may be trapped or which may be oxygen – deficient, until the space has been ventilated and the atmosphere checked, particular regard being paid to the danger of asphyxiation and explosion. Monitoring shall be carried out during the operation to ensure a continuing safe environment.
- (e) A final leakage check shall be carried out on completion.
- (f) The necessary equipment shall be available to ensure safe access to, and egress from, the work area and the necessary precautions shall be taken to exclude non-essential personnel and the general public.

11.2.3.7 *Non-routine works*

Before carrying out non-routine works, written procedures shall be prepared and clause 11.2.3.4, concerning permits to work, followed.

When carrying out non-routine major works, additional precautions to those provided in clause 11.2.3.6 apply:

- (a) At least two operatives shall be present.
Note: Under certain circumstances, extra operatives may be required, for example when entering and working within deep pits.
- (b) Sufficient sets of breathing apparatus shall be available on site.
- (c) Where deep pits and confined spaces are involved, safe means of access shall be provided, harness and life lines shall be available and at least one operative shall be detailed to observe others working in such spaces.
- (d) At least one member of the team shall be experienced in first aid and rescue operations.
- (e) Where it is necessary to cut into a commissioned or decommissioned pipeline, cold cutting equipment shall be used until it has been confirmed that there are no hazardous substances present.

11.2.3.8 *Emergency procedures*

The following requirements are provided as a general guide with respect to emergency procedures and reference should be made to IGE/SR/20:

- both operative and supervisory staff level shall be adequate at all times to handle reported escapes. Procedures shall be established in order to ensure that there is a system in place which can identify the likely source of escapes and will enable mobilisation of the appropriate resources as soon as is reasonably practical
- emergency procedures shall be established and all operational personnel shall be made aware of them including any requirement of themselves under such procedures
- emergency procedures shall be reviewed periodically and updated as changes in circumstances occur.

11.2.3.9 *Venting gas*

The venting of gas shall be minimised in order to reduce environmental impact. Reference should be made to IGE/SR/23.

11.2.3.10 *Electrical continuity*

When making a break in a pipeline or dismantling associated equipment, a temporary continuity bond shall be fitted across the intended break. Any impressed current CP system shall be isolated but restored as soon as the work is complete.

Note: Attention is drawn to the possibility of induced currents being present which are independent of CP systems. Also, CP currents can take time to dissipate after isolation.

11.2.3.11 *Noise abatement*

A certain amount of noise is inherent in operation and maintenance activities. The best practicable methods should be employed to minimise noise emission, to protect site personnel and the general public. Any relevant legal requirements must be applied. Reference should be made to IGE/TD/13.

Consideration shall be given to:

- provision of suitable ear protection to site personnel
- siting and screening of plant
- use of acoustically-treated power tools compressors and generators
- the timing of all operations and maintenance activities, which shall take into account the impact on the environment.

11.2.4 **Surveillance, inspection and maintenance frequencies**

11.2.4.1 Provided that appropriate data is available, then, as a first preference, frequencies shall be determined by a risk-based approach and the use of software tools where appropriate.

Frequencies that have been determined using a risk-based approach should be reviewed periodically. Such a review should take account of the results of previous surveillance, inspection and maintenance.

11.2.4.2 A risk-based approach shall take into account a complete inventory of existing equipment and a comprehensive history of all occurrences and work undertaken on the equipment in question.

Note: It may be necessary to justify a risk-based approach to a regulatory body.

11.2.4.3 A risk-based approach shall take into account those factors which influence the probability and consequences of failures occurring in pipelines. Expert advice shall be sought as appropriate to determine a suitable risk-based approach. However, the following shall be taken into consideration:

- age and standard of construction of the pipeline
- design assumptions for pipelines having a design factor exceeding 0.72
- previous surveillance, inspection and maintenance
- the results obtained from CP monitoring
- any evidenced of ground movement
- ground conditions
- operating temperature history of the pipeline
- implications of loss of gas supply

- density of population surrounding the pipeline.

11.2.4.4 If there is not sufficient data to support a risk-based approach, a prescribed frequency shall be used as identified in the appropriate clause (see Table 10).

11.3 PIPELINE RECORDS

11.3.1 General

11.3.1.1 Pipeline records shall be readily available and continually updated, categorised under the following headings:

- fixed data
- surveillance
- inspection
- maintenance
- operation.

Note: Records may be held in hard copy, for example paper, microfilm, etc., or electronically, for example digital computer records.

11.3.1.2 An administrative procedure, preferably with a document flow diagram to suit the needs of the particular organisation, shall be defined to initiate and control the modification of records. The procedure should indicate the method of re-issuing plans, drawings or documents and include details of interested parties who have a specific requirement for detailed records, for example local Police and Fire authorities.

11.3.1.3 The number of persons holding pipeline records shall be strictly limited and indicated clearly on a distribution list for documents. Previous records should be destroyed, unless required for archival purposes in which case they should be marked as superseded.

11.3.1.4 A review of the accuracy of pipeline records shall be made at intervals not exceeding four years as part of the audit required for affirmation of MOP (see clause 11.4.2.1).

11.3.2 Fixed data

11.3.2.1 The following fixed data shall be retained:

- design records as identified in Sub-Section 6.16
- construction records as identified in clause 7.2.5
- any other relevant documents.

11.3.2.2 The route of a pipeline should be recorded on maps to a scale of 1:10,000, along with detailed maps to a scale of not less than 1:2500.

11.3.2.3 In addition to other information deemed necessary, the 1:10,000 maps should show the boundaries of all environmentally-sensitive areas, in order that appropriate advice may be sought prior to working within, or adjacent to, such an area.

11.3.2.4 The 1:2500 maps should show relevant construction data for the pipeline as identified in clause 4.1.4, including location of the pipe, reference to owners and occupiers, and any modifications to the pipeline.

- 11.3.2.5 Detailed drawings shall include:
- all installations forming part of, or attached to, the pipeline
 - special crossings
 - the location of other services
 - pipeline profile.

The drawings should include unique identifiers for all valves and other equipment shown on the drawings.

- 11.3.2.6 Full details of any addition, diversion, modification or permanent decommissioning of any section of the pipeline shall be recorded at the time and subsequently included in the fixed data.
- 11.3.2.7 Records shall be maintained of all attachments to the pipeline, including under-pressure connection, hot taps and stopples and these should be integrated into the fixed data of the pipeline.
- 11.3.2.8 Records shall be maintained of all repairs carried out and these should be integrated into the fixed data of the pipeline.

11.3.3 **Surveillance**

- 11.3.3.1 All information arising as a result of surveillance activities shall be used to confirm or update existing records. Updating should take place as soon as practical after the event.
- 11.3.3.2 Records shall be kept of the surveillance carried out on the pipeline. These should be in such a form that encroachments can be readily recorded and monitored.

11.3.4 **Inspection**

- 11.3.4.1 Detailed records of inspections carried out shall be recorded against an item of plant or location or section of pipeline, so that defect trends can be readily identified.
- 11.3.4.2 Results shall be stored for the life of the pipeline.

11.3.5 **Maintenance**

- 11.3.5.1 All information arising as a result of maintenance activities shall be used to confirm or update existing records. Updating should take place as soon as practical after the event
- 11.3.5.2 Records shall be kept of the maintenance carried out on the pipeline. These should be in such a form that the recurrence of faults can be readily detected. Damage and interference by third parties, together with the remedial action taken, should also be recorded.

11.3.6 **Operation**

- 11.3.6.1 A record shall be kept of pressures to which the pipeline is subject to facilitate the calculation of stress cycles and the affirmation of MOP.
- 11.3.6.2 Records of pipeline temperature shall be maintained as appropriate to determine that it remains within design limits.

11.4 OPERATIONAL PRESSURE LIMITS

11.4.1 MOP

11.4.1.1 In considering operational limits, it is necessary to decide to which Edition of IGEM/TD/1 the pipeline is operating. The operating edition shall be determined using Figure 11 and should be declared. Figure 12 shall be used when considering upgrading a pipeline.

11.4.1.2 If a pipeline does not comply with any edition of IGEM/TD/1, and if it cannot be upgraded to meet this edition, consideration shall be given to operating the pipeline in accordance with IGE/TD/3 latest edition.

11.4.1.3 The pipeline MOP shall be in accordance with this edition or previous editions if the pipeline is to be operated in accordance with those editions. MOP may become limited by the following:

- the design section of the particular edition of IGEM/TD/1 to which the pipeline is being operated
- infrastructure or other development adjacent to the pipeline
- the materials used for the construction of the pipeline and the most recent in-service performance of these materials
- the pressure rating and acceptability of any equipment added to the line since construction
- the most recent pressure test data, inspection results or risk analysis
- the recommendations of clause 11.4.2
- any significant changes to the parameters used in risk assessments carried out as part of a safety assessment of the pipeline.

Other factors which may limit the MOP are:

- temporary operational constraints
- previous operating conditions
- operating temperature
- ground movement
- fatigue
- interference
- pipeline defects
- internal and external stress corrosion cracking
- legislation.

11.4.1.4 MOP shall be determined and declared annually.

11.4.1.5 The annual declaration of MOP shall be based on the most recent pipeline audit (see clause 11.4.2.1), the pipeline pressure history (see clause 11.4.2.5), and all relevant information arising from surveillance, inspection, maintenance and operation.

11.4.2 Affirmation of MOP

11.4.2.1 An audit of the pipeline shall be carried out at intervals of not more than 4 years to confirm MOP. Nothing in this section should preclude more frequent audits if the terms referred to under clause 11.4.1 give cause for concern.

Where a SRA (see clause 6.7.4.3 and Appendix 4) has been adopted for a pipeline having a design factor exceeding 0.72, the first pipeline audit should include an audit of the SRA. The actual service performance should be compared

with the assumptions used in the SRA. Subsequent pipeline audits should identify any changes in performance which might affect the validity of the assessments performed.

11.4.2.2 Proximity and population density infringements identified during pipeline surveillance should be considered as soon as possible, but the opportunity should be taken to verify compliance as part of the four yearly audit.

11.4.2.3 Infringements resulting from changes in proximity, population density, or traffic density shall be evaluated with reference to Sub-Section 6.7 or to Sub-Section 6.10 as appropriate.

When used to assess infringements, risk analyses should provide:

- quantification of associated individual and societal risks
- data to assist the quantification of potential benefits associated with upgrading and/or risk mitigation measures.

11.4.2.4 Where necessary, MOP shall be reviewed and revised.

11.4.2.5 Where the maximum pressure experienced by a pipeline during any period of five consecutive years has been 7 bar or more below the declared MOP, a formal confirmation of the declared MOP supported by the results of the pipeline reaffirmation report and stating that the pipeline is fit to operate at the declared MOP, shall be prepared and certified by the responsible engineer. Where an integrity statement cannot be prepared and certified, either pressure raising to confirm integrity at the current declared MOP shall be carried out, or the MOP shall be re-declared at the highest level of pressure actually experienced during that period.

Where MOP is re-declared, notification must be given under PSR.

Where a SRA (see clause 6.7.4.3 and Appendix 4) has been adopted for a pipeline having a design factor exceeding 0.72, the 4 year period may have to be shortened as a result of the SRA and pipeline audit.

11.4.2.6 Where monitoring of the fatigue usage of the pipeline is required by Sub-Section 6.6, the life consumed since the last revalidation shall be checked at intervals which should not exceed 10% of the most recent estimate of the total pipeline fatigue life.

Where a SRA (see clause 6.7.4.3 and Appendix 4) has been adopted for a pipeline having a design factor exceeding 0.72, and where the estimated future pressure-cycling (see Sub-Section 6.6) results in a significant probability of failure within twice the identified design life of the pipeline, the pipeline shall be monitored to establish the actual cyclic loading experienced by the pipeline.

11.4.3 **Overpressure**

11.4.3.1 The sustained operating pressure of a pipeline system shall not exceed MOP.

Note 1: This sustained operating pressure is the maximum set pressure for the pressure regulating devices. However, when operating at or near MOP, this pressure may be exceeded by no more than 2.5% of its value due to the variations of pressure regulating devices (see Figure 13 and IGE/TD/13).

Note 2: Variations of pressure regulating devices are caused by the characteristics of automatic control systems (see BS 1523-1). The relevant characteristics are:

- steady oscillation which occurs when a pipeline system is in a steady state and the pressure deviation oscillates equally about the set pressure

- *pressure overshoot witch occurs when a pipeline system is not in a steady state and the pressure regulating system is caused to take correcting action which results in a maximum pressure deviation.*

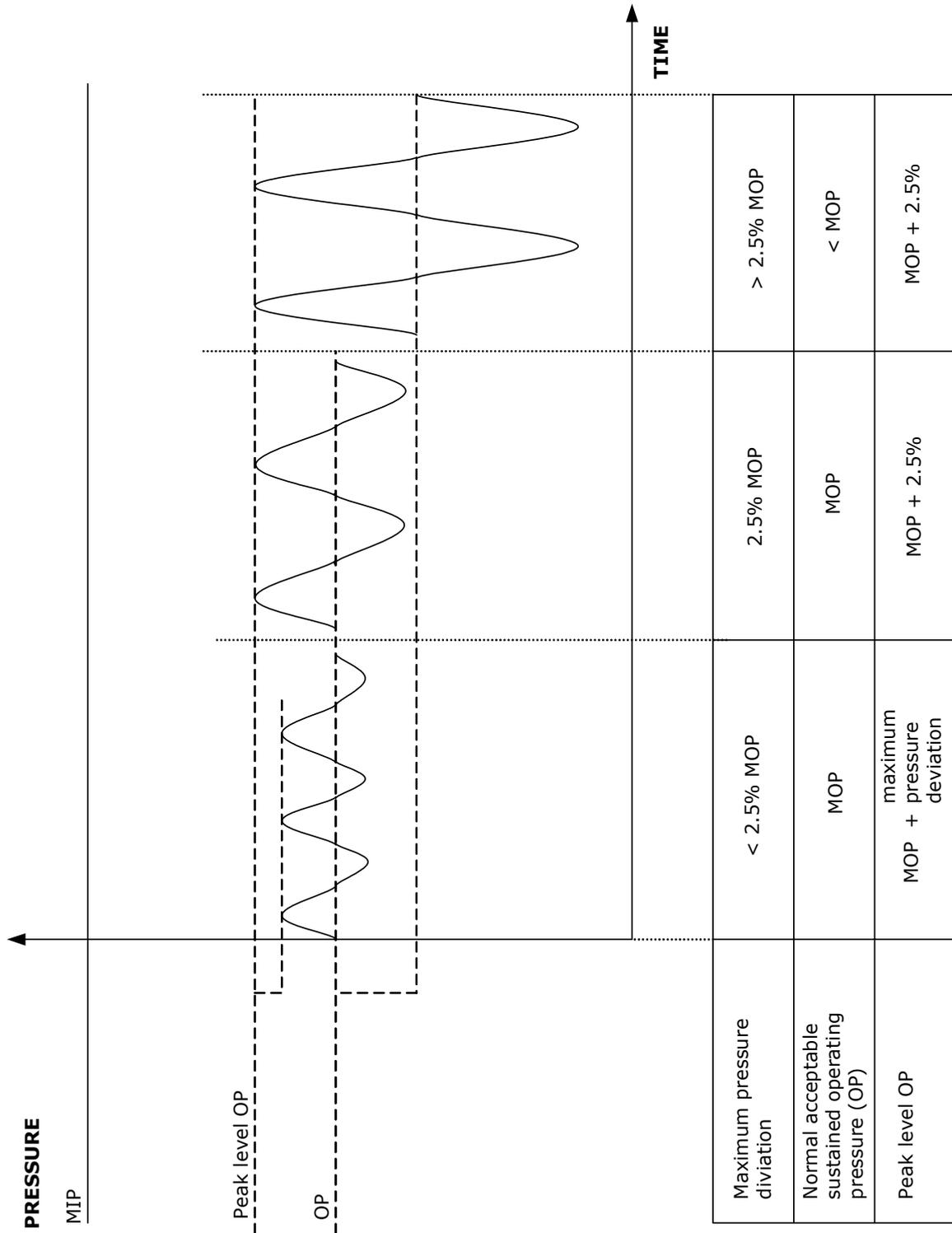
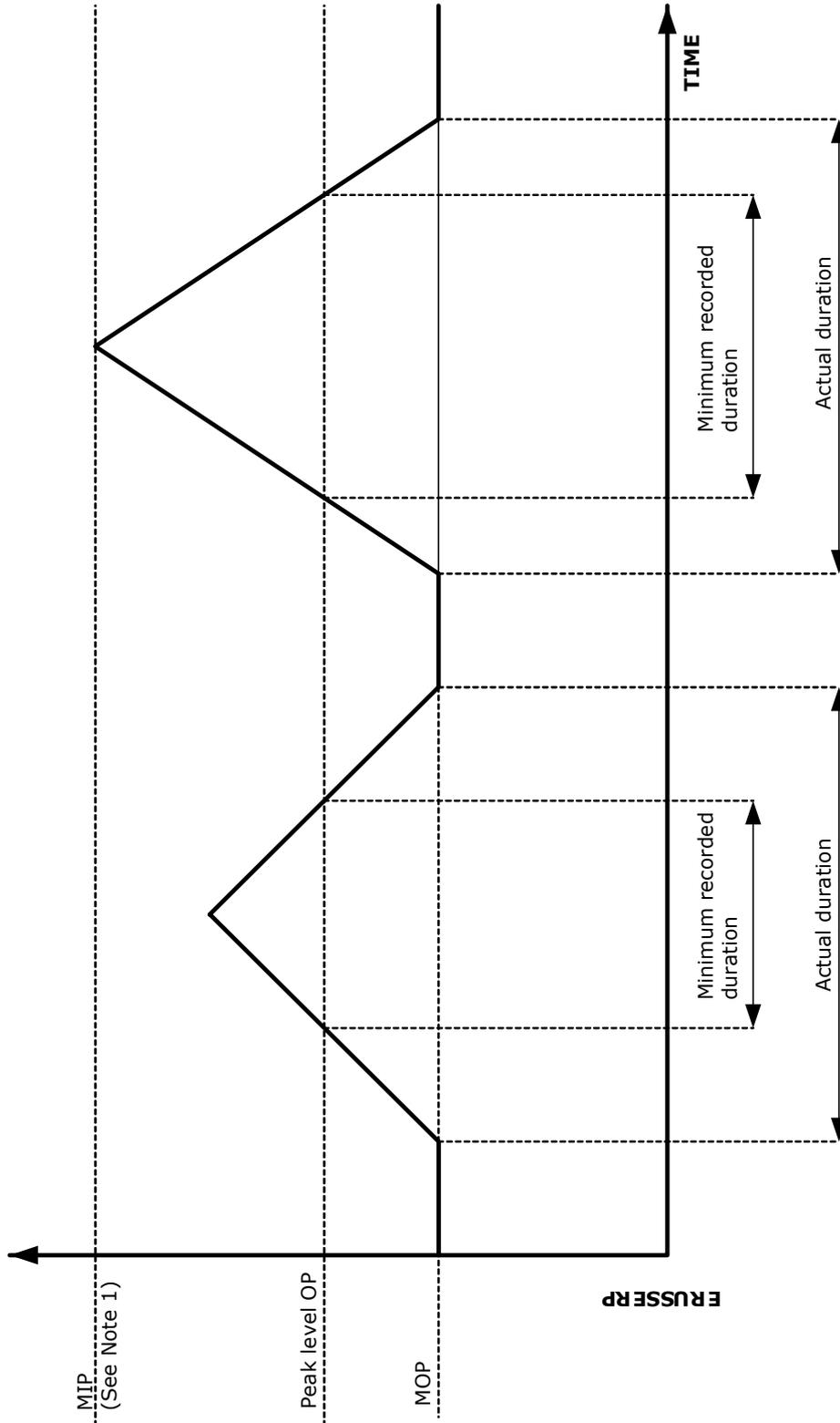


Figure 10(a) - Sustained operating pressure

FIGURE 10 - MOP EXCURSIONS (cont'd overleaf)



Note 1: $MIP = MOP + 10\%$ (can be less for pipelines of design factor > 0.72)

Note 2: Duration not to exceed 5 hrs for any single pressure excursion and not to exceed 20 hrs cumulative per annum

Figure 10(b) - Incidental pressure rises

FIGURE 10 (cont'd) - MOP EXCURSIONS

- 11.4.3.2 An incidental pressure rise is admissible, but facilities shall exist to limit automatically, by relieving or shutting off, MIP to 10% above MOP and provided, when it occurs, it does not endure for more than 5 hours in excess of MOP and provided, when it occurs, it does not endure for more than 5 hours in excess of MOP at any one time or for more than 20 hours per year.

Note: Determination of the duration of an incidental pressure rise may exclude the duration of acceptable pressure deviations (see clause 12.4.3.1).

Where a SRA (see clause 6.7.4.3 and Appendix 4) has been adopted for a pipeline having a design factor exceeding 0.72, MIP shall have been determined as part of the design.

Note: This value may need to be less than 10% above MOP.

11.4.4 **Restoration of MOP to a previously declared level, up to the original design pressure**

- 11.4.4.1 The revised MOP shall be specified clearly. Irrespective of the construction date of the pipeline, care shall be taken to ensure that all the requirements of clause 11.4.1 are satisfied before the existing MOP is increased to a higher level. The revised MOP shall not exceed the design criteria set out in Section 6 and the previous hydrostatic test shall meet the criteria set out in Section 7.

Where a SRA (see clause 6.7.4.3) and Appendix 4) has been adopted for a pipeline having a design factor exceeding 0.72, but subsequently MOP has been reduced, then, prior to restoring the MOP to a level giving design factor exceeding 0.72 consideration shall be given to the continuing validity of the data, models and assumptions used in the SRA assessments.

- 11.4.4.2 Reference shall be made to the records of design, construction, testing, modifications subsequent operation, maintenance and any other works carried out. This review should include a detailed survey of PRIs and any other attachment to the pipeline.

- 11.4.4.3 The pipeline shall be examined for structural faults using either internal inspection (see clause 11.6.3.5) or hydrostatic testing (see Section 8) to a level suitable for the revised MOP.

Where such an examination has taken place within the previous 5 years, consideration shall be given to the subsequent operating environment and to the extent of the proposed increase in MOP. Where considered necessary, a further internal inspection of hydrostatic test should be undertaken.

- 11.4.4.4 Where physical or gas supply constraints prevent structural examination using either internal inspection or hydrostatic testing, consideration may be given to the use of external inspection techniques (see clause 11.6.3.6). These shall be used only where it can be demonstrated that the associated risk is acceptable. If adopted, the highest standard of external inspection should be carried out within 12 months of the proposed pressure increase.

The time interval between any such external inspection and the restoration of the MOP shall be minimised.

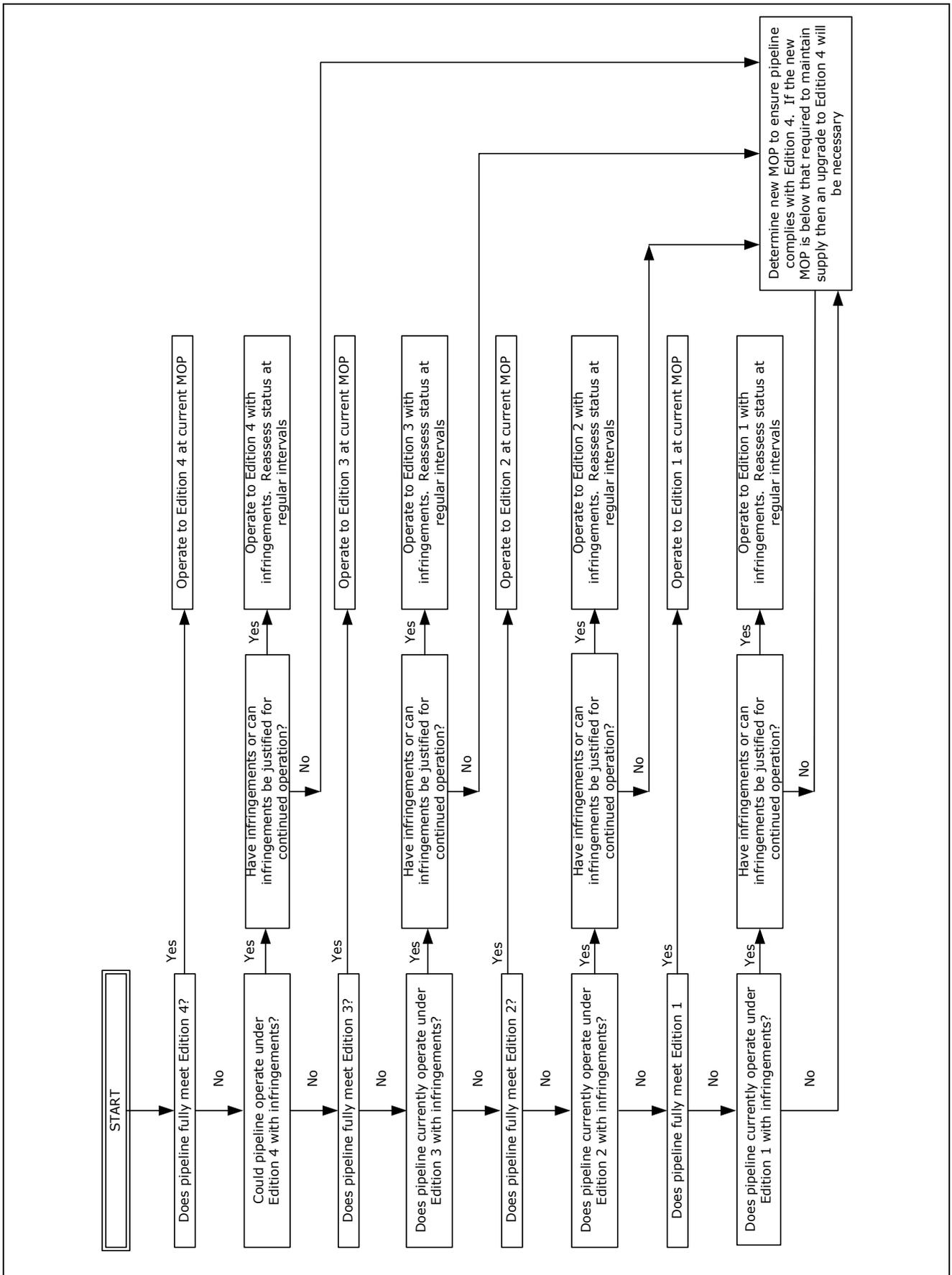


FIGURE 11 - DECISION ALGORITHM FOR ESTABLISHING OPERATING STATUS OF A PIPELINE

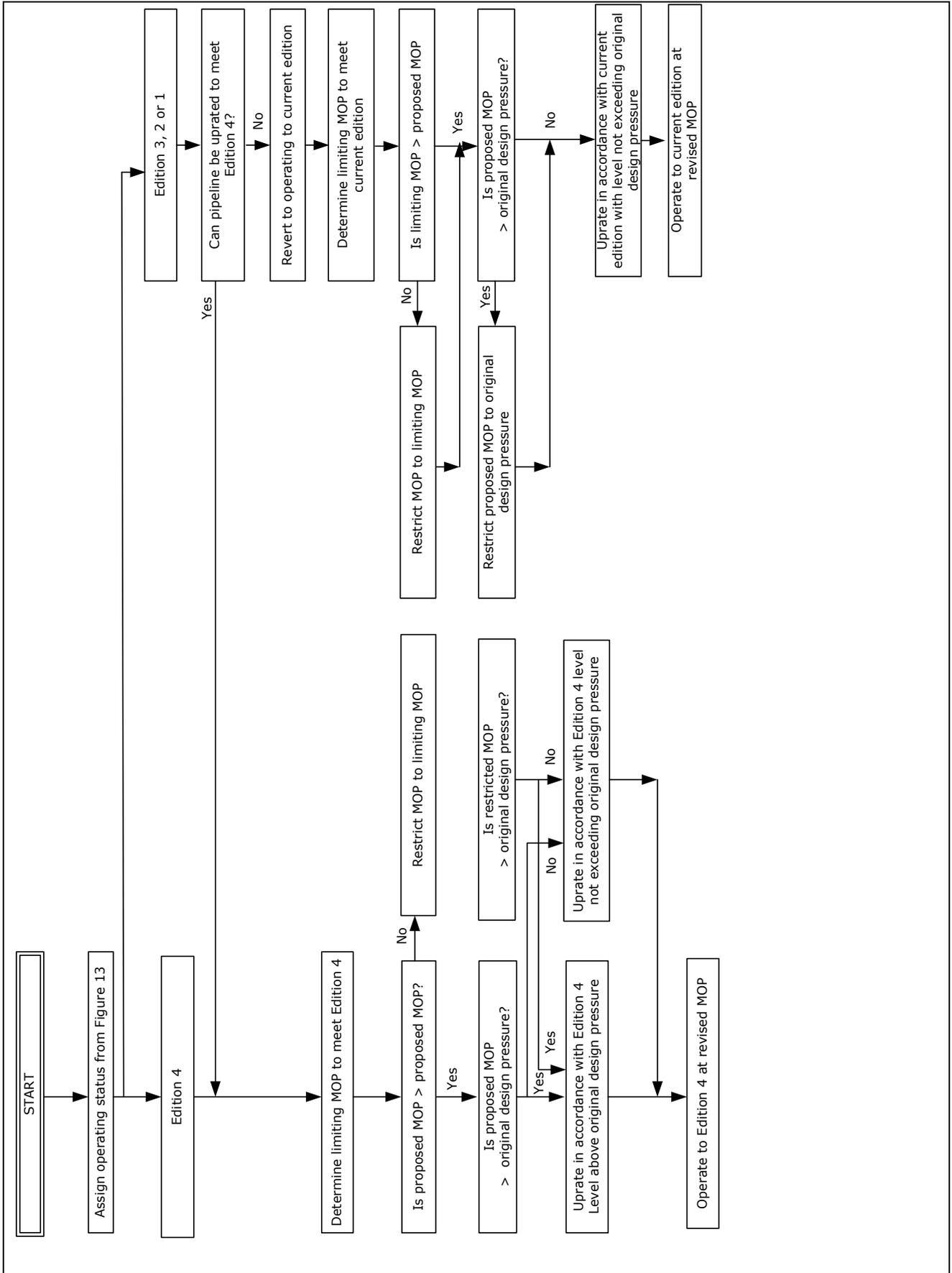


FIGURE 12 - DECISION ALGORITHM FOR UPRATING MOP OF A PIPELINE

- 11.4.4.5 If acceptable after consideration of clauses 11.4.4.3 or 11.4.4.4, the pressure shall be raised in accordance with the following:
- immediately prior to raising MOP, the pipeline is surveyed to ensure that no operations are being carried out adjacent to the pipeline
 - the pressure is raised in incremental steps not exceeding 10% of the original design pressure
 - the pressure is held after each incremental step to allow sufficient time for the pipeline to be surveyed for any sign of leakage. This shall incorporate the whole length of the pipeline, with particular regard being given to those lengths which are subjected to routine leakage survey (see clause 11.5.10). It shall also incorporate installations and any attachments to the line
 - consideration is given to carrying out a leakage survey at the locations of all mechanical joints after 1 month of operating at the higher pressure.

11.4.5 **Upgrading the MOP of a pipeline to a level above the previous design pressure**

11.4.5.1 *General*

The upgrading of a pipeline to a pressure level above the previous design pressure shall be controlled in accordance with formal procedures. The following control stages shall be adopted:

- viability – identification of any fundamental characteristic which may prevent upgrading
- assessment – completion of design review and identification of all modifications necessary
- revalidation – confirmation that the pipeline condition is acceptable for the proposed MOP
- modification – completion of all necessary modifications
- pressure raising – increasing the pressure and confirmation of gas tightness.

Note: Figure 13 shows an overview of the upgrading procedure.

11.4.5.2 *Viability*

To determine whether a proposed pipeline upgrading is viable, exhaustive examinations of the records, physical characteristics and original design features shall be made.

The following shall be considered in assessing the viability of upgrading a pipeline:

- original design criteria
- construction standards and procurement details
- previous test results
- metallurgical details of all pipeline materials and those of the attachments to it
- operational records, including:
 - modifications since construction
 - repairs
 - condition monitoring results and actions
 - pressure cycling/fatigue history
 - service history
 - CP history
 - proximity and population density infringements and area classification.

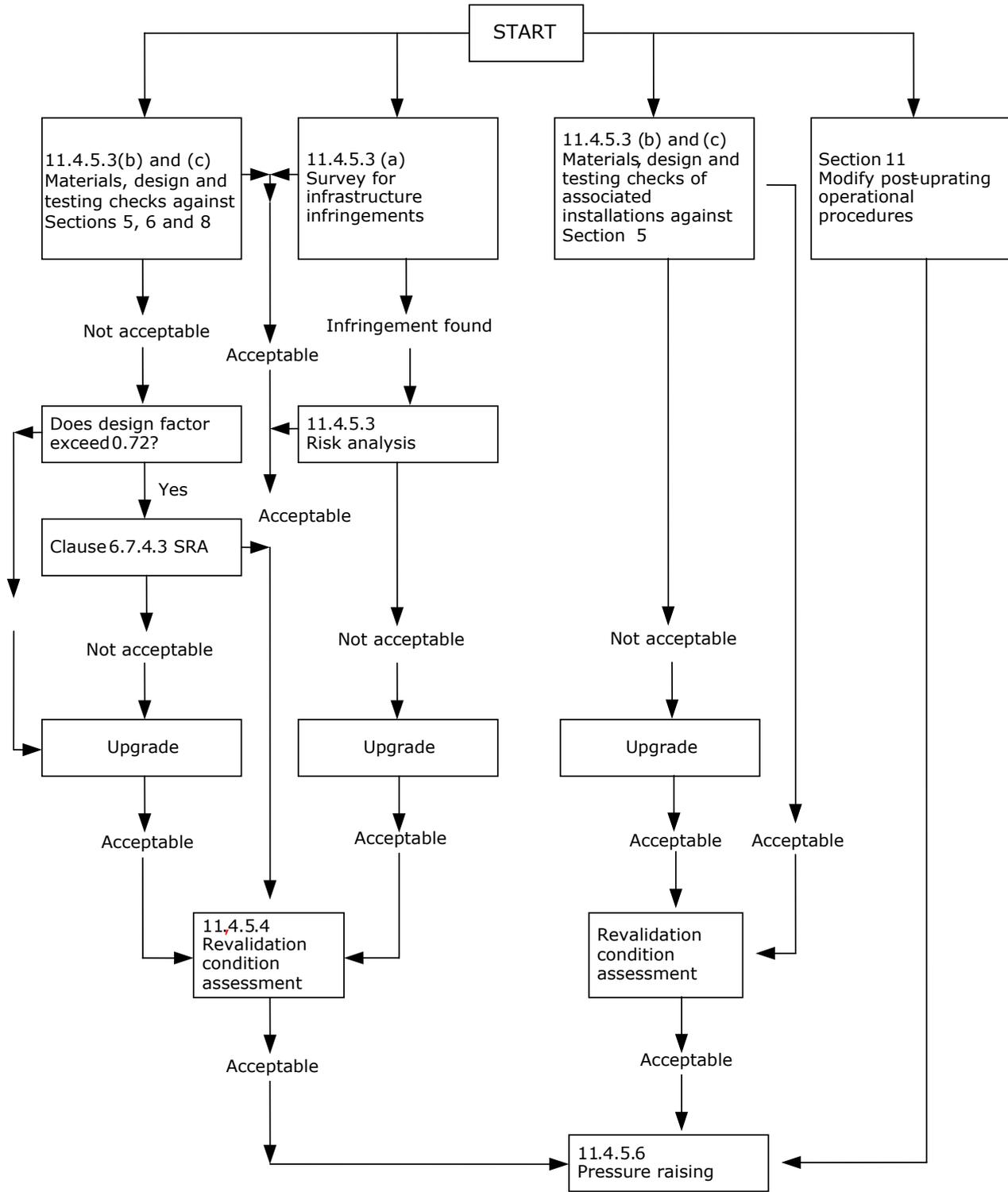


FIGURE 13 - OVERVIEW OF UPRATING PROCEDURE

- operating temperature history
- products carried previously in the pipeline
- susceptibility to stress corrosion cracking
- residual construction and operating stresses, including those due to ground movement particularly associated with deep mining, quarrying and landslips
- stress analysis on components included in, or attached to, the pipeline
- proximity of third party equipment
- special crossings and the requirements of rail, river or road authorities.

11.4.5.3 *Assessments*

Once a proposed uprating has been determined viable, the following assessments should be applied:

- a complete survey of the pipeline for any infringements of this Edition at the proposed revised MOP
- the information gathered under clauses 11.4.5.2 and 11.4.5.3(a) against Sections 5, 6 and 7, for the proposed revised MOP
- a stress analysis, if necessary, of components included in, or attached to, the pipeline for the proposed revised operating pressure. Any changes to operating temperature which are likely to result from the proposed uprating shall be taken into account.

Any infringement of this Edition may be identified at this stage. A risk analysis of the infringements shall be carried out, for the proposed revised MOP, in accordance with Sub-Section 6.8. If required by legislation, the level of risk must be agreed between the pipeline operator and the regulatory authority, taking into account the requirements of Section 6.

The results of all assessments shall be considered and all modifications necessary for the proposed revised MOP should be determined.

11.4.5.4 *Revalidation-condition assessment for uprating*

Revalidation of the pipeline shall be carried out either by:

- an internal inspection using an appropriate standard of internal inspection (see clause 11.6.3.5), taking into account the proposed revised MOP of the pipeline. Any features should be further analysed for growth potential using appropriate fitness-for-purpose techniques or
- hydrostatic test when any features previously identified should be reassessed for the proposed hydrostatic test pressure, using appropriate fitness for purpose techniques.

When the pipeline is suitable for uprating with modifications, the modifications should be carried out before the hydrostatic test is undertaken.

Note: The modifications which may be necessary are described in clause 11.4.5.5.

The pipeline should then be subjected to a hydrostatic test, consistent with the revised MOP, as described in Section 8.

11.4.5.5 *Modifications*

When all the requirements of clauses 11.4.5.2, 11.4.5.3 and 11.4.5.4 have been taken into account and the pipeline is suitable for uprating with modifications, such modifications shall be carried out before any pressure increase is allowed.

It may be necessary to carry out repairs, replace components, relay or divert sections or carry out protection measures.

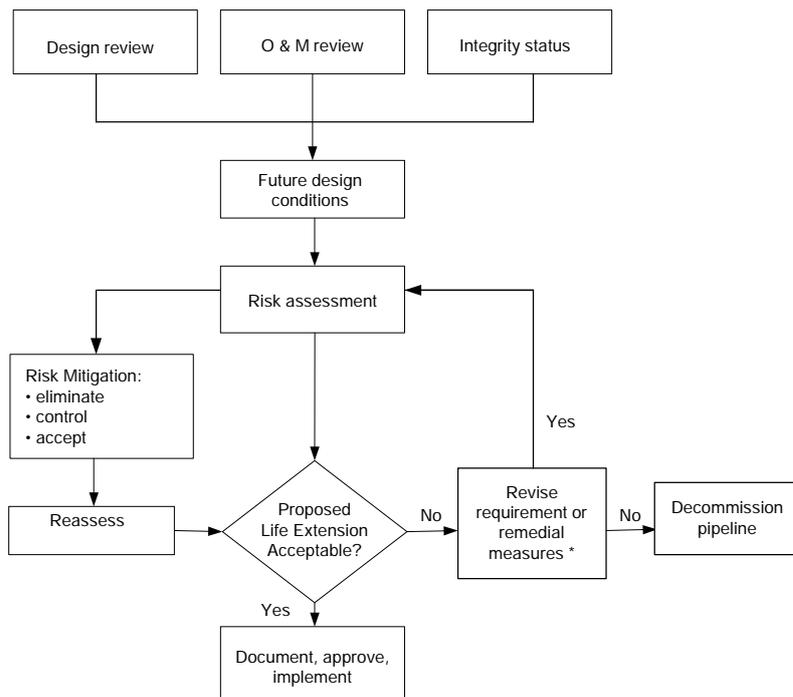
11.4.5.6 *Raising the pressure to the revised MOP*

If it is determined that the pipeline is suitable for uprating, having carried out the appropriate requirements of this section, the raising of the pressure should be in accordance with clause 11.4.4.5.

If required, any changes to MOP shall be notified to the appropriate regulatory authority.

11.5 **REASSESSMENT OF PIPELINE DESIGN LIFE**

The process applied to the reassessment of the pipeline design life shall include all activities detailed under clauses 11.4.4 and 11.4.5. In addition, formal reviews shall be undertaken of the condition and remaining life expectancy of pipeline CP systems; the condition of ancillary systems and equipment obsolescence. Specific consideration shall be given to the assessment of the remaining fatigue life of the pipeline, and the identification of any locations of active corrosion and the assessment of the rate of corrosion growth at such locations. Where necessary, plans for remedial/rehabilitation/replacement actions shall be developed and progressed. An overview of the process is given in Figure 14.



* For example, reduce MOP; reduce pressure cycling; repair pipeline

FIGURE 14 - REASSESSMENT OF PIPELINE DESIGN LIFE

11.6 **SURVEILLANCE**

11.6.1 **General**

11.6.1.1 Reasonable precautions should be taken to reduce the risk of damage to the pipeline. Surveillance activities should be completed in accordance with this edition to minimise the likelihood of damage by external factors and third

parties, and also to determine where the environment in which the pipeline is situated has altered.

11.6.1.2 The frequency of surveillance activities should be set by a risk-based approach (see clause 11.2.4). If this is not practicable, the frequency should be prescribed as identified in the relevant clause (see Table 10).

11.6.1.3 The type and frequency of surveillance activity should be determined for each pipeline section taking into consideration a range of factors, including:

- location
- depth of cover
- design of pipeline (wall thickness, operating pressure/stress, attachments etc.)
- historical records
- extent of third party activity
- environmental conditions, including the weather.

11.6.1.4 Where a section of pipeline is operated in accordance with a risk-based design, the level of surveillance shall be appropriate to the location concerned.

Frequencies and levels shall be reviewed at regular intervals to determine that they are still appropriate.

11.6.1.5 An effective management structure and arrangements shall be in place to ensure that:

- any encroachment onto the pipeline is reported immediately according to an agreed procedure
- the necessary action is taken to protect the pipeline and that the pipeline is monitored from the first notification to final completion.

11.6.1.6 Route plans must be deposited with the relevant authorities in accordance with legislation or where considered appropriate.

11.6.2 **Long range ultrasonics**

Long range ultrasonics is based on guided ultrasonic waves which are transmitted along a section of pipe. It is typically used where it is difficult to gain access over the pipeline, for example where the pipeline passes under a road.

Note: When carrying out an inspection of below ground pipework which has a coal tar coating, the wave strength may diminish rapidly. Similarly, some soils may have the same effect.

In addition, the image may be affected by wave background noise for areas of inspection within 1 metre of the transmitter contacts.

ACTIVITY	REFER TO CLAUSE
Surveillance	
Aerial	11.6.8
Vantage point	11.6.9
Walking	11.6.10
Leakage	11.6.11
Third party liaison	11.6.12
Ground movement	11.6.13
Inspection	
Exposed crossings	11.7.1
Water course crossings	11.7.2
Condition monitoring	11.7.3
Corrosion control	11.7.4
Maintenance	
Pipeline	11.8.1
Valves	11.8.2
Actuators	11.8.3
Remotely operated valves	11.8.4
Pig traps	11.8.5
Land and buildings	11.8.6
Non routine	
Isolation	11.9.1
Decommissioning/recommissioning	11.9.2
Internal inspection	11.9.3
Repair	11.9.4
Under pressure working	11.9.5
Permanent decommissioning	11.9.6

Note: The recommended frequencies in the referred clauses should be increased in areas of intense third party activity, areas of ground movement, or other circumstances when the integrity of the pipeline could be compromised such as flood conditions for water courses, or where large public gatherings occur adjacent to the pipeline, for example festivals, agricultural shows, etc.

TABLE 10 - SURVEILLANCE, INSPECTION, MAINTENANCE AND NON-ROUTINE ACTIVITIES

11.6.3 Aerial survey

11.6.3.1 An aerial survey of all pipelines should be undertaken every two weeks unless the frequency is set by a risk-based approach in accordance with clause 11.2.4.

Note: The purpose of this survey is to report on ground activities which, if allowed to develop, might affect the pipeline.

11.6.3.2 Pipeline markers or some other effective navigational aid, for example Global Positioning Systems (GPS), should be used to enable accurate surveys to be carried out.

11.6.3.3 Observers should be notified of known encroachments. They should record all encroachments or likely encroachments and report them according to an agreed procedure.

Note: Normally, this activity is completed by an observer from a helicopter but can also be achieved by fixed wing aircraft or by the use of satellites. Still or video photography can aid the process. The primary advantage of helicopters is the ability to land immediately at any perceived high risk situation affecting the pipeline.

11.6.3.4 The chosen method for aerial survey should be capable of reporting on any of the following occurrences which may be taking place in the vicinity of the pipeline:

- work on drainage, ditching, fencing or any other farm activity, with the exception of normal top soil cultivation
- fires of any description, including straw burning
- civil engineering or building work of any kind
- tree felling and timber transportation
- discoloration of vegetation or other evidence of leakage
- blasting and mineral extraction
- ground movement and changing water courses
- the removal of surface soil and conversely tipping and/or stacking of materials over the pipeline
- the condition/presence of aerial and other marker posts
- any temporary sites of public gathering, for example camp sites, festivals, agricultural shows, etc.
- any other unusual feature which may affect the pipeline.

Where a serious infringement is observed, immediate action should be taken, for example by landing to investigate, reporting by radio or returning immediately to base to report.

11.6.4 **Vantage point survey**

11.6.4.1 As an alternative, or as a supplement, to aerial surveys, a vantage point survey should be carried out. This survey should be undertaken every 2 weeks unless the frequency is set by a risk based approach in accordance with clause 11.2.4. The survey should be undertaken by an observer from pre-determined fixed points along the route, the points being selected to ensure that all relevant parts of the route are visible.

11.6.4.2 The actions taken as a result of the survey should be as those following an aerial survey listed in clause 11.5.7.4.

11.6.5 **Full walking survey**

11.6.5.1 All parts should be walked at least once every 4 years, unless the frequency is set by a risk-based approach in accordance with clause 11.2.4. If it can be demonstrated that sufficient surveillance takes place during aerial/vantage/overhead crossing/water course crossing/overline and on line condition monitoring surveys and liaison activities, then separate walking surveys of all or part of a pipeline may not be required.

11.6.5.2 Where appropriate, notice should be given to the owner/occupier/tenant before a ground patrol enters the land.

11.6.5.3 Suitable precautions, including the use of disinfectant sprays, should be taken where necessary to counter the risk of spreading animal and plant disease.

The walking patrol should observe and report on similar features to those outlined in clause 11.6.8.4 in addition to which the following should be checked and duly reported:

- exposed crossings and installations inspected for security
- the condition of surface boxes, markers posts, etc.

11.6.6 **Leakage survey**

11.6.6.1 If a leakage survey programme is deemed appropriate, the frequency should be set by a risk-based approach in accordance with clause 11.2.4. If this is not possible:

- for pipelines conforming to and operating to IGE/TD/1 Edition 4, a leakage survey should be carried out annually at:
 - sleeve ends not fitted with rigid end seals
 - points where impact protection has been provided
 - those sections of pipelines which cannot be inspected by on-line pigging or a suitable overline survey technique.
- for pipelines not conforming to but operating in accordance with earlier editions of IGE/TD/1, the above survey frequency should be carried out quarterly at the stated locations
- where sections of the pipeline have infringements resulting from changes in proximity, population density or traffic density, the survey frequency should be carried out quarterly at the infringement locations.

Note: Leakage surveys have been shown to be of limited benefit except in circumstances at a specific location where a survey is deemed appropriate.

11.6.6.2 Where a leakage survey is to be carried out at points of proximity or other infringements or where impact protection has been installed, the length of pipeline to be surveyed should include the section of the infringement or the protection concerned plus the proximity distance for the pipeline at either end of the section concerned.

11.6.7 **Monitoring of third party activities**

11.6.7.1 *General*

A system should be established to collect information on third party activities and assess the impact of such activities on pipelines. This may include "one call systems", information exchange agreements between parties, "dial before you dig" arrangements, etc. Monitoring procedures should be established in accordance with IGE/SR/18.

11.6.7.2 *Liaison with owners/occupiers, tenants and other authorities*

Regular contact should be maintained with owner/occupiers and tenants of land through which a pipeline passes.

Note: This can best be achieved by depositing, with the occupier, a plan showing the pipeline location and the easement width and by personal visits to the occupier and, if practical, the owner, on at least an annual basis.

This contact should be carried out by personnel who have knowledge of the issues involved in reminding the owner/occupier of their obligations when working in the vicinity of the pipeline and its associated equipment.

In conjunction with the above, a reminder letter should be sent annually, detailing the obligations under the Deed of Grant and the requirement to give notice of any work likely to affect the pipeline.

Note: It is recommended that this is done approximately 6 months after the personal visit.

Where appropriate, similar visits may be made to highway and river authorities and other utilities and contractors. A regular visit should be made to local planning authorities and emergency planners to ensure they are aware of the existence of the high pressure pipeline.

11.6.7.3 *Objectives of visits*

The objectives of these visits should be to determine:

- the accuracy of existing records, for example change of ownership or tenancy
- that the existence of the pipeline is known to the occupier and owner
- whether any work adjacent to the pipeline is planned in the future and whether any work has been done since the previous visit, without the knowledge of the pipeline operator.

11.6.8 **Ground movement**

11.6.8.1 *Mining*

- (a) If mining activities are carried out in the vicinity of pipelines, an assessment should be made of the likely effect on the pipeline of any resultant ground movement, so that any necessary protective measures can be implemented.
- (b) Liaison should be maintained with mining companies, which should be furnished with details of pipeline routes. If mining activities are to be carried out in the vicinity of a pipeline, details, including the programme, should be obtained from the mining company of the type of mining, panel dimensions and location, geological features and any adjacent or previous mining in the area.
- (c) Data on predicted subsidence, including horizontal and vertical displacements, along the pipeline route should be obtained together with information on ground topography and other geotechnical features.

11.6.8.2 *Other causes of ground movement*

There may be other causes of ground movement, for example ground-slip, salt extraction, quarrying, open cast mining, landfill, etc. whose effect on the pipeline should be considered.

11.6.8.3 *Prediction/control of pipeline stress*

- (a) Predictions of pipeline stresses (Sub-Section 6.5) should be made using an appropriate stress analysis procedure, taking account of the above information, soil properties and pipeline geometry. The predicted stresses should be assessed according to limiting criteria, to prevent tensile, compressive or bending failure.

If the predicted stresses approach or exceed acceptable levels, the ground displacements should be monitored by accurate survey methods and the pipeline should be monitored by appropriate means, such as strain gauges. Consideration should be given to residual stresses existing in the pipeline and these may have to be measured.

- (b) Where a SRA (see clause 6.7.4.3 and Appendix 4) has been adopted for a pipeline having a design factor exceeding 0.72 and ground movement occurs or is predicted to occur, the assessment of the continuing fitness for purpose of the pipeline in the vicinity of the ground movement should take cognisance of the SRA assessments performed. The acceptability of any increase in failure probability in the vicinity of the ground movement should be considered when deciding upon remedial actions.

- (c) Appropriate remedial measures should be carried out where unacceptable stresses occur. If the pipeline is to be exposed, due consideration should be given to any adverse effect on security and the environment.

Before exposing a pipeline, consideration should be given to the dangers of movement caused by the release of stresses which may occur during exposure.

Note: Remedial measures include the controlled exposure of the pipeline, realignment vertically or horizontally, cutting the pipeline, replacement of the backfill by low friction material or insertion into the pipeline of bellows or sliding joints.

- (d) Specialist advice should be sought before action is taken.

Note: With certain configurations of bends in the pipeline, a reduction in operating pressure does not necessarily reduce the stress in the pipeline, and may increase it.

11.7 **INSPECTION**

Inspection of the pipeline shall be carried out to ensure that the pipeline is not deteriorating.

11.7.1 **Exposed crossings**

- 11.7.1.1 Exposed crossing points shall be inspected for security, mechanical defects, condition of supports and associated structures/foundations, paintwork, protective wrap and guards. Concrete parts of pipe supports shall also be inspected for any degradation, for example cracking or powdering of the concrete caused by an alkali-silica reaction. Refurbishment shall take place as necessary.

- 11.7.1.2 The frequency of inspections should be set by a risk-based approach in accordance with clause 11.2.4. If this is not practicable, the inspections should be at least annually.

Note: Where the crossing is the subject of vandalism or other adverse conditions, more frequent inspections may be justified.

- 11.7.1.3 For corrosion control of exposed crossings, reference should be made to clause 11.6.4.2.

11.7.2 **Water course crossings**

11.7.2.1 *General*

The profile of the pipeline beneath any water course shall be determined.

Surveys shall be carried out to allow the identification of changes from the original state of both the pipeline and its immediate surroundings, for example, river beds, river banks and landfalls, and to provide sufficient information to be able to demonstrate the continued integrity of the pipeline and its fitness for purpose.

11.7.2.2 *Frequency of surveys*

The frequency of surveys should be set by a risk-based approach in accordance with clause 11.2.4. If this is not practicable, the frequency should be in accordance with Table 11. In addition to the items identified in clause 11.2.4, a risk-based approach shall take into account:

- regulatory requirements
- the nature of the water course, seasonable variations and severe weather patterns
- the stability of the riverbed
- the activities of other parties, for example, dredging
- previous inspection history
- the results of studies to evaluate the risks to the pipeline integrity.

	Depth of cover (m)			
	≤ 0.5	> 0.5 ≤ 1.1	> 1.1 ≤ 4	> 4
	Survey interval (years)			
Major water course tidal	1	1	1	1
Major water course (navigable)	2	3	5	15
Minor water course	5	5	5	Not required
Other water course (generally wadeable)	During external condition monitoring or close interval potential survey of the pipeline. Additional inspections where the local situation requires.			

Note: Tidal water course crossings can be subject to extensive and rapid erosion. This may result in loss of cover making the pipeline vulnerable to impact or vortex-induced vibration.

TABLE 11 - FREQUENCY OF WATER COURSE CROSSING SURVEYS WHERE RISK ASSESSMENT IS NOT CARRIED OUT IN ACCORDANCE WITH CLAUSE 11.7.2.2

11.7.2.3 *Minor water courses*

Surveys shall be carried out of river crossing points and other locations affected by adverse water and associated ground conditions.

Surveys shall be tied into a recognised geographical grid and shall determine the position of the pipeline, in both plan and elevation, in relation to the riverbed.

Liaison with the controlling water authority shall form an essential part of the survey.

11.7.2.4 *Major water courses*

Pipelines which cross busy navigable water courses, estuaries or large expanses of water such as lakes or lochs, shall be surveyed to ensure that any condition or event likely to be detrimental to the integrity of the pipeline or the safety of others is discovered as soon as possible.

Note: These types of pipeline crossings are susceptible to third party interference from shipping as a result of collision or grounding and to damage caused by anchors and trawl boards. Additionally, high water currents may cause erosion of the landfall section or disturbance of the material placed over or around the pipeline.

Any scouring of material from beneath the pipeline will result in free spanning, which induces stresses in the pipeline. In extreme cases, the spanning can grow in length and, unless checked by remedial action, may result in damage to or failure of the pipeline length.

Spanning may also subject the pipeline length to fatigue damage if vortex induced vibration of the span occurs. Such fatigue damage is likely to affect girth welds and requires specialist assessment; the requirements of Sub-Section 6.6 are not appropriate for this case.

11.7.2.5 *Scope of surveys*

When determining the scope of the survey, the following shall be considered:

- size and nature of the water course
- pipeline crossing design specification and method of construction
- local environmental constraints
- information required
- type of features to be identified
- mechanical damage to the pipeline and its corrosion protection coatings
- CP
- changes in position of the pipeline or signs of movement in any direction
- location of sand and mud banks including details of drift
- extent of any loss of cover along buried or protected sections
- condition of weight coating and the extent of any loss of coating
- debris in close proximity to the pipeline which may become a danger to its integrity
- condition of river banks or landfall sites.

Note: Based on the initial and any subsequent surveys of major water courses and trends in seabed movement, exposure and burial can be determined and any areas of concern highlighted for further monitoring.

- results of studies to evaluate the risks to the pipeline integrity.

11.7.2.6 *Selection of survey techniques*

Information necessary to ascertain the applicability of a specific survey method shall include:

- width and depth of crossing
- water flow rate (tidal or constant)
- pipeline exposure or burial
- strategic importance of the pipeline
- navigability, volume and type of shipping
- necessity to monitor known damage and/or remedial works.

Note: Further information on the selection of suitable techniques, depending on different water depths their application, is provided in Appendix 8.

11.7.2.7 *Survey operations*

A detailed programme of operations shall be prepared and agreed with affected parties. The programme shall define individual and functional responsibilities as well as safety procedures.

Reference should be made to Appendix 8 for further information on survey procedures.

11.7.2.8 *Survey results*

The results of surveys shall be reported in a suitable format to enable both the location and significance of features to be readily determined, and to provide a comparison with previous survey results. Reference should be made to Appendix 8 further information on the content of survey reports.

The results from each survey shall be examined as soon as possible and appropriate integrity analysis and remedial work initiated as required to ensure the continued fitness for purpose of the pipeline and the safety of others, for example those involved in fishing activities in the vicinity of pipe spans.

11.7.3 Condition monitoring

11.7.3.1 Appropriate inspection shall be carried out for new pipelines, immediately following commissioning, to provide a database for future inspection of that pipeline (finger printing).

Note: The engineering standards and specifications used in the design and construction of pipelines, combined with the various non-destructive inspections and hydrostatic tests immediately following construction, ensure the eradication of critical defects at that time.

11.7.3.2 The condition of a pipeline shall be established periodically. The condition monitoring regime for a pipeline shall be determined following consideration of factors such as relevant legislation, performance of corrosion prevention measures, operation of the pipeline under pressure cycling or at elevated temperatures, and trend analysis of pipeline deterioration. Specialist advice should be sought for each of the potential damage mechanisms.

11.7.3.3 The condition of a pipeline shall be established by:

- the use of internal inspection devices on those pipelines which can be monitored using such devices
- the use of approved external inspection techniques on those pipelines or sections of pipelines which cannot be monitored using internal inspection devices. On pipelines which can be monitored using internal inspection devices, these external inspection techniques can be used to provide additional intermediate inspections as necessary
- the use of hydrostatic testing on those pipelines or sections of pipelines not suitable for either of the options above.

11.7.3.4 *Frequency*

The frequency of condition monitoring activities should be set by a risk-based approach in accordance with clause 11.2.4. If this is not practicable, the frequency should be in accordance with that prescribed in Table 12.

TYPE OF MONITORING	MAXIMUM INTERVAL BETWEEN MONITORING
Internal	Not to exceed 10 years
Above-ground	
a. For pipelines subject to internal inspection	Not to exceed 10 years to be carried out mid-way between internal inspections.
b. For pipelines not subject to internal inspection	Not to exceed 5 years
Hydrostatic test	Not to exceed 20 years

TABLE 12 - FREQUENCY OF CONDITION MONITORING WHERE RISK ASSESSMENT IS NOT CARRIED OUT IN ACCORDANCE WITH CLAUSE 11.7.3.4

11.7.3.5 *Internal inspection*

Methods of internal inspection are subject to continuing development and may be modified as new, different or improved information on the significance of defects is obtained. This Edition indicates a proven method for monitoring the condition of the pipeline, using internal equipment under on-line conditions, but does not preclude other steps as may be considered necessary in particular circumstances.

- (a) Reference should be made to clause 11.9.3 for details of how to carry out internal inspection by means of on line pigging.
- (b) In selecting internal inspection equipment, consideration shall be given to the following equipment characteristics:
 - feature detection and sizing capability, which is appropriate for the quantitative assessment of the structural integrity of the pipeline and associated repair policy
 - feature location accuracy to minimise subsequent excavation
 - its purpose. The following list may not be exhaustive as internal inspection is the subject of continuing development:
 - inspection for pipe deformation for example dents, wrinkles and ovality
 - inspection for metal loss, resulting from, for example, corrosion and mechanical damage
 - inspection for SCC
 - inspection for exposure, loss of weight coating and/or free spanning, in major water course crossings.
- (c) The results of an inspection shall be reported in a suitable format to enable both the location and significance of defects to be readily determined, and to provide a comparison with previous inspection results. The pipeline operating conditions, at the time of inspection, shall also be reported.
- (d) The results of an inspection shall be examined as soon as possible and appropriate remedial work initiated to ensure the continued fitness for purpose of the pipeline. Where external corrosion is found, an investigation of the CP system shall be undertaken.

11.7.3.6 *External inspection*

- (a) These techniques shall be used on those pipelines or sections of pipelines which cannot be monitored using internal inspection devices and to provide additional intermediate inspections where necessary on pipelines normally monitored using internal inspection devices.

For the types of inspection techniques, reference shall be made to BS 7361-1.

Note: Additional impact protection can affect the efficiency of above ground coating surveys, such as Pearson and CIPS.

- (b) For pipelines with a design factor not exceeding 0.3, survey procedures shall be adopted to assess the effectiveness of CP. For other pipelines, survey procedures shall be adopted which are designed to detect areas of mechanical damage.

- (c) For pipelines with a design factor not exceeding 0.3 or pipelines of wall thickness 19.05 mm or greater with a design factor not exceeding 0.5, the following monitoring methods shall be used:
- a CIPS carried out over the entire length of pipeline being monitored. Where the polarised potential does not meet the criteria for effective CP, as specified in BS 7361-1, a Pearson type survey for coating defects should be carried out
 - where electrical interference on the pipeline makes CIPS inaccurate, a separate, simultaneously recorded, pipe-to-soil potential at an appropriate point on the pipeline to calculate a compensation for the amount of interference
 - where a pipeline is protected by sacrificial anode groups, a CIPS measuring "on" potentials, and supported by polarised potentials measured from buried coupons at test points.

Note: This will enable a polarised potential profile to be estimated for the pipeline.

Consideration shall be given to excavating all locations of coating defects where the CP is not effective and to carry out external pipe wall inspections. Following any repair work and after consolidation of the backfill, necessary remedial action should be taken to ensure that the pipeline meets the criteria for effective CP.

- (d) For pipelines with a design factor exceeding 0.3, or pipelines of wall thickness 19.05 mm or greater operating at a design factor exceeding 0.5, the following monitoring methods shall be used:
- a Pearson type survey for coating defects carried out over the entire length of pipeline being monitored
 - a CIPS carried out over the entire length of pipeline being monitored
 - where electrical interference on the pipeline makes the polarized potential survey inaccurate, a separate simultaneously recorded pipe-to-soil potential at an appropriate point on the pipeline should be used to calculate a compensation for the amount of interference
 - where a pipeline is protected by sacrificial anode groups, a CIPS measuring "on" potentials, and supported by polarised potentials measured from buried coupons at test points.

Note: This will enable a polarised potential profile to be estimated for the pipeline.

Consideration shall be given to excavating all locations of coating defects identified by the Pearson type survey and to carry out external pipe wall inspections.

Where the potential survey does not meet the criteria for effective CP specified in BS 7361-1 or an equivalent standard, remedial action shall be taken.

- (e) Other survey methods shall be considered where particularly difficult faults are unable to be resolved by normal survey procedures.
- Current attenuation survey
Similar to the Pearson survey this detects loss of an injected ac signal through measurements of the magnetic field with pairs of coils. The method will also identify the current strength and direction of flow and is a useful technique in locating uninsulated contacts as well as coating defects.

- Direct current voltage gradient (DCVG)

The voltage gradient that exists at coating defects is measured between two reference electrodes using a voltmeter with an accuracy of ± 10 mV as the pipeline is traversed. This method will provide information on the relative sizes of coating defects and other sources of current loss but will not determine whether the applied CP is effective.

The DCVG technique can be used in areas where measurements may be susceptible to AC interference. The DCVG survey technique can also, in some circumstances, determine the shape of a coating defect (from which a cause may be inferred e.g. backfill or mechanical damage), the location of the defect on the pipeline (top, bottom or side) and whether the defect is actively corroding.

The following alternative survey techniques may be considered for application in place or in addition to CIPS.

- Current drain test (CDT)

Coating defects can often be introduced during the construction process. At some locations, such as trenchless crossings, these defects will not be able to be detected by Pearson or DCVG surveys. A current drain test at these locations can give a qualitative assessment of coating quality and indication on whether additional cathodic protection will be required at the location. In the context of managing CP systems, CDT is also employed to provide an indication of coating quality, for the identification of shorted insulating joints/flanges, pipeline to sleeve shorts, and to confirm cathode faults.

The principle of a CDT is to use an external power source to drain current from coating defects on the pipeline to a temporary earth bed and to measure the effects along the pipeline. Although the current required to achieve CP can be calculated for new systems, this can be unreliable for existing systems, where the level of coating breakdown is unknown or other current drain sources exist. In such cases, the current requirement can be accurately determined by the application of a current drain test.

- Electromagnetic current attenuation surveys

The electromagnetic current attenuation survey technique can be used to indicate where buried steel pipework is free from significant coating defects in a situation where a complete CIPS is not possible. CIPS can be especially difficult where pipes are laid below concrete, tarmac etc., making it impossible to obtain reliable pipe to soil potential readings due to either poor ground contact of the reference electrodes or at locations such as railways, busy road crossings and in towns and cities where the safety of the public and CIPS operatives due to the use of trailing cables can be compromised.

The technique can also locate cathode faults on cathodically protected pipelines. A cathode fault is present when the current demand to achieve CP is excessive due to an inadvertent contact with another metallic structure such as a cast iron water main, concrete reinforcing bar contact or an insulation joint failure.

The technique requires an AC signal to be applied between the coated pipe and remote earth by means of a battery-powered transmitter connected between the pipe and one or more earth spikes. The strength of the AC signal is measured along the pipe with an antenna (not connected to the pipe). A coating defect or metal to metal contact with a foreign structure can be identified through an observable drop in the signal gradient.

- Long range ultra sonics

Long range ultra sonics is based on guided ultrasonic waves which are transmitted along a section of pipe. It is typically used where it is difficult to gain access over the pipeline, for example where the pipeline passes under a road.

11.7.3.7 *Frequency*

The frequency of condition monitoring activities should be set by a risk-based approach in accordance with clause 12.2.4. If this is not practicable, the frequency should be in accordance with that prescribed in Table 10.

11.7.4 **Inspection and maintenance frequencies**

11.7.4.1 Provided that appropriate data is available, then, as a first preference, frequencies should be determined by a risk-based approach and the use of software tools where appropriate. Frequencies that have been determined using a risk-based approach should be reviewed periodically.

Such a review should take account of the results of previous inspection results.

11.7.4.2 A risk-based approach requires a complete inventory of existing equipment and a comprehensive history of all occurrences and work undertaken on the equipment in question.

During the planning phase of the on-line inspection, consideration shall be given to the implications of the loss of gas supply should the device get stuck and appropriate contingency plans put in place to mitigate this.

Note: It may be necessary to justify a risk-based approach to a regulatory body.

11.7.4.3 A risk-based approach shall take into account those factors which influence the probability and consequences of failures occurring in pipelines. Expert advice should be sought as appropriate to determine a suitable risk-based approach. However, the following shall be taken into consideration:

- age and standard of construction of the pipeline
- design assumptions for pipelines having a design factor exceeding 0.72
- previous inspection results
- the results obtained from CP monitoring
- any evidence of ground movement
- ground conditions
- operating temperature history of the pipeline
- density of population surrounding the pipeline.

11.7.4.4 If there is not sufficient data to support a risk-based approach, a prescribed frequency should be used as identified in the appropriate clause (see Table 10).

11.7.4.5 *Inspection feature investigation and remedial works*

Inspection features, reported as a result of condition monitoring operations, shall be inspected and repaired in accordance with clause 11.8.4.

11.7.5 **Corrosion control**

11.7.5.1 *CP monitoring and maintenance work*

- (a) The continued effective operation of a CP system is totally dependent upon a satisfactory level of monitoring and maintenance, and shall form part of the pipeline management system.
- (b) Due regard shall be taken of the possible ageing effects on the pipeline coating systems and on locations where the integrity of the CP system may become increasingly vulnerable.
- (c) The periods of monitoring and the continuing suitability of the representative test locations shall be periodically reviewed and changed as required.
- (d) Suitable procedures can be found in BS 7361-1. The following minimum routines shall be considered:
 - (i) for sacrificial anode systems, pipe/soil potentials at representative points and points of low protection should be checked at 6 monthly intervals. For impressed current systems, a status check should be made monthly to establish that the CP system power source(s) are functioning within limits that have previously been shown to give the required levels of protection throughout the system. Checks should also be made on the integrity and accessibility of the means of electrical isolation.
 - (ii) pipe/soil potentials should be measured and surface components examined to a schedule such that, in general, all points considered to be critical to the effectiveness of the system are checked annually.
 - (iii) after the commissioning period, and where practicable, a CIPS should be carried out over the total length of the pipeline and thereafter at intervals not exceeding 10 years.
 - (iv) crossing points with other cathodically protected structures (whether bonded or not) and any other interference bonds, should be tested annually to ensure that no adverse changes have occurred.

11.7.5.2 *Corrosion monitoring of exposed pipe*

- (a) Exposed pipe shall be inspected for areas where undue corrosion might occur, for example any fabrication where there are crevices open to the atmosphere, or areas of metal where painting is made difficult due to the design of the structure. Particular attention shall be paid to pipe corrosion hidden by supports.
- (b) The paint system exposed pipe shall be examined on a planned and regular basis and rectified as necessary in an approved manner.

- (c) Special attention shall be given to the areas of the structure which are covered with lagging and which may, therefore, be subject to an additionally corrosive environment.
- (d) Special consideration shall also be given to the condition of any electrical insulation where deterioration could adversely affect the CP system.

11.7.5.3 *Corrosion protection of sleeves*

- (a) Schedules for pipeline inspection shall include appropriate checks on sleeves and attachments, for example resistive bonds.

Note: Information on sleeve/carrier pipe eccentricity can be gained from suitable carrier pipe internal inspection vehicles.

- (b) Pipelines designed, constructed and maintained to either Edition 1 or Edition 2 of IGE/TD/1 may have sleeves that were constructed to give additional protection either to the public, or to the pipeline, from third party activities. These sleeves were built to either Class 1, 2 or 3 standards and shall be maintained depending upon their type.

Note: Audits are carried out periodically to reaffirm the MOP and the Edition of IGEM/TD/1 to which a pipeline operates (clause 11.4.2.1). Sleeve classifications may be re-designated as part of these surveys.

- (c) Pipelines designed, constructed and maintained to Edition 3 or Edition 4 may have sleeves built to facilitate construction. Where these sleeves are steel, they shall be maintained depending upon their type.

- (d) The carrier pipe shall always be protected, even if, as a result, the sleeve potential fails below the protection criteria.

Note: Lack of sleeve protection is an acceptable risk when corrosion of the carrier pipe would be the unacceptable alternative.

- (e) All Class 1 sleeves shall be cathodically protected. Nitrogen-filled Class 2 and Class 3 sleeves shall also be cathodically protected, to prevent loss of nitrogen through corrosion damage and the consequent loss of protection to the carrier pipe within the sleeve.

- (f) Unprotected Class 2 and Class 3 sleeves shall be maintained in a condition that does not affect adversely the CP system of the carrier pipe.

- (g) All metallic sleeves shall be fitted with test facilities.

- (h) For nitrogen-filled sleeves, CP shall be effected from the main carrier pipe protection system, either by virtue of welded/forged end seals or via a direct cable bond surface facility where epoxy grouted end seals are installed.

Note: For either of these situations, the CP system of the pipe and sleeve may be augmented locally where damage to the sleeve coating causes reduction of CP.

- (i) Protection of the section of carrier pipe within grouted sleeves will only be effective if the annual space is filled completely with a conductive material, if there is no metallic contact between the sleeve and the carrier pipe and if the carrier pipe is free from significant coating damage.

- Grouted Class 1 sleeves
 - where the annular space between the sleeve and carrier pipe is filled with a conductive material, including normal cementitious grouting materials, the external surface of the sleeve may be protected by the main carrier pipe CP system. The use of separate CP on the sleeve should be avoided since accelerated corrosion of the carrier pipe can result
 - CP of the external surface of the sleeve may occur, due to the interception of current from the carrier pipe CP system. Where measurements of sleeve to soil potential indicate that protection does not occur by interception, a resistive device should be fitted between the carrier pipe and sleeve
 - the resistive device should ensure that the current drained provides a sleeve to soil polarised potential in the range -0.85 V to -0.95 V. However, the carrier pipe to soil polarised potential should be at least 0.1 V more negative than the sleeve to soil polarised potential
 - consideration should be given to protecting the resistive device from electrical surges. When the CP system has stabilised, both the pipe to soil and sleeve to soil "on", potentials should be recorded, for use as a basis for comparison in future monitoring routines.
- Grouted Class 2 and Class 3 sleeves

Although there is no requirement to cathodically protect grouted sleeves in these categories, they shall be constructed and maintained in a condition that does not adversely affect CP of the carrier pipe.

11.7.5.4 *Coatings*

A comparison of the predicted and actual performance of the pipeline coating shall form part of pipeline audits (see clause 11.4.2.1).

Consideration shall be given to the actual performance of the coating under stress corrosion cracking conditions.

In assessing the susceptibility to SCC, account shall be taken of the types of coating used on the body of the pipe and at field welds and their influence on SCC of the pipeline.

11.8 **MAINTENANCE**

An effective system of preventative maintenance shall be instituted on pipelines and associated equipment. In preparing maintenance schedules, due account shall be taken of the latest information on equipment faults and other defects and their frequencies. Maintenance schedules shall be updated in the light of the latest information on equipment performance. Equipment defects shall be rectified as soon as possible.

Note: The following outlines the maintenance of pipelines and associated equipment, including valves, bridles and other primary attachments, up to and including the launch and reception pig traps.

11.8.1 Pipelines

11.8.1.1 *Aerial markers and pipeline marker posts*

Aerial markers and pipeline marker posts shall be maintained to ensure that they are visible. The information contained thereon shall be verified, updated and checked for legibility.

11.8.1.2 *CP systems*

Maintenance of CP systems shall be carried out in accordance with clause 11.6.4.

11.8.1.3 *Nitrogen-filled steel sleeves*

- (a) The frequency of pressure checks on nitrogen-filled sleeves shall be set by a risk-based approach in accordance with clause 11.2.4. If this is not practicable, the pressure shall be recorded at three monthly intervals.
- (b) If a serious loss of fill pressure is sustained, investigation shall be made as to its cause. In the event of the leakage being from the sleeve pipe or attachments, necessary repairs shall be carried out. If the leak is from a flexible end-seal and satisfactory sealing is not practicable, consideration shall be given to replacing the end-seal with a rigid end-seal or fully grouting the sleeve.
- (c) In the event of a marked increase in fill pressure, it shall be assumed that a leakage exists in the carrier pipe and action taken accordingly. Chemical analysis of the fill gas shall be carried out at the first step in determining the cause of the pressure increase.
- (d) Where vents have been fitted, the frequency of checks of the pressure relieving device should be set by a risk-based approach in accordance with clause 11.2.4. If this is not practicable, checks should be carried out at three monthly intervals.

11.8.1.4 *Grouted steel sleeves*

- (a) For cementitious and other fills, a visual inspection of the end-seals and annular fill shall be made, if the opportunity arises.
- (b) In the event of an electrical short being confirmed, it shall be considered that the carrier pipe is not protected. In such cases, the electrical short should be removed. If this is impractical, the sleeve may be fitted with end-seals, so that annular voids can be nitrogen-filled. However, where such nitrogen-filling is considered not to provide corrosion protection throughout the sleeve length due to the nature of the annular fill, replacement of the sleeved section may be required.

11.8.2 Installations

11.8.2.1 The aims of operation and maintenance shall be to ensure that any installation associated with a pipeline:

- operates in a safe and environmentally sound manner
- offers sufficient reliability for the operating conditions within which it is used and will continue to operate until its next maintenance
- is in sound mechanical condition
- operates at the appropriate set points

- is installed correctly.

11.8.2.2 Operation and maintenance shall be designed to maximise the availability of the associated gas supply. Contractual arrangements for gas supply, with 3rd parties, shall be taken into account.

11.8.2.3 The risks and consequences of failure associated with operating and maintaining an installation shall be considered from design, through installation, commissioning and operation.

The modes of failure will be governed largely by the plant design and the operating method used. Using this knowledge, in addition to a good maintenance history, an effective maintenance strategy can be devised to reduce the risk of failure to an acceptable level.

Consequences to be considered shall include failure to supply gas and impact on the downstream system.

Note: For new plant, or in the absence of any operational or maintenance history, it may be desirable to use manufacturers' recommendations as the initial basis of all maintenance activities. Normally, plant history will be gained, over time, from operational/ maintenance data or may be gained from experience of similar equipment/installations.

11.8.2.4 A maintenance regime, which includes the requisite skills, experience and resources, shall be established or contracted to ensure maintenance is undertaken safely and effectively.

11.8.2.5 Arrangements shall be made to deal with emergencies both inside and outside normal working hours.

11.8.3 **Valves**

11.8.3.1 The frequency of valve maintenance and operation should be set by a risk-based approach in accordance with clause 11.3.4. If this is not practicable, valves should be maintained, operated fully and their seals proved at least annually.

In maintenance operations involving the movement of a valve, due regard shall be given to the monitoring of pressures on both sides of the valve.

11.8.3.2 In the exceptional circumstance where the system does not allow for complete valve closure, the valve shall be moved off the seat and closed partially. Due account shall be taken of the permissible pressure drop across the valve.

11.8.3.3 Where possible, valve body vents should be installed with the vent valve located immediately off the valve.

Note: For buried valves, an extension may be fitted at ground level and a further valve fitted where it may be operated safely.

11.8.3.4 Special consideration shall be given to the maintenance of valves which are normally-closed for operational purposes.

11.8.3.5 Unless adequate precautions have been taken against corrosion, maintenance schedules shall include a visual inspection of the valve body, accessible moving parts and adjacent pipework.

11.8.3.6 Where valves are located in unfavourable conditions, such as in valve chambers subject to flooding or general dampness, consideration shall be given to increasing the maintenance frequencies to take account of these conditions.

11.8.3.7 Covers on valve chambers shall be maintained, to ensure that they can quickly be removed.

Checks shall be made to ensure that there is no gas build up in valve chambers

11.8.4 **Valve actuators**

11.8.4.1 The frequency of maintaining and proving all actuators should be set by a risk-based approach in accordance with clause 11.2.4. If this is not practicable, actuators should be maintained and proved at least annually. For remotely operated valves, reference should be made to clause 11.8.5.

11.8.4.2 Inspection and maintenance of electrically-operated actuators shall ensure that the installation is electrically sound. Electrical inspection and maintenance shall be carried out in accordance with BS 7671.

11.8.4.3 For gas storage cylinders not connected to the pipeline, the bottle pressures shall be recorded and topped up, as necessary, at intervals of not more than monthly.

11.8.4.4 The maintenance schedule shall include for any statutory requirements for testing/revalidation of pressure vessels associated with valve actuators.

11.8.5 **Remotely operated valves and pipeline protection devices**

11.8.5.1 Remotely operated valves shall be maintained in accordance with clause 11.8.3. In considering a schedule of maintenance operations, account shall be taken of the need to test the equipment by remote operation or by simulating line-break conditions. For remotely operated block valves, an inspection and testing schedule should be carried out at a frequency set by a risk-based approach in accordance with clause 11.2.4. If this is not practicable, they should be inspected and tested annually.

11.8.5.2 Operations involving the closure of block valves by remote operations and by simulation techniques shall be a co-ordinated exercise with all relevant parties, for example control room, operators of other parts of the system, etc.

11.8.6 **Pig traps**

11.8.6.1 Maintenance of all components of pig traps, including end closure seals, bleed locks, electrical bonds, locking rings, pig signallers and fasteners, shall be undertaken just prior to use, after painting and at a frequency set by a risk-based approach in accordance with clause 11.2.4.

If it is not practicable to use a risk-based approach, maintenance shall be carried out at least every 10 years.

11.8.6.2 In addition to clause 11.8.6.1, temporary or removable pig traps shall be inspected before use for any mechanical damage due to handling.

11.8.6.3 A record shall be kept of the pressure cycles sustained by pig traps, including portable pig traps.

11.8.7 **Land and buildings**

11.8.7.1 The maintenance of sites associated with valve and pig trap locations shall include any buildings, access roads, drains and cable ducts. Attention shall be paid to the provision, location and maintenance of fire fighting equipment, in accordance with statutory requirements.

11.8.7.2 Attention shall be paid to the condition of fences, gates and locks, hedgerows and ditches, weed control, grass cutting and general control of vegetation.

11.9 **NON-ROUTINE ACTIVITIES**

11.9.1 **Pipeline isolation**

11.9.1.1 The isolation of a pipeline, or part of a pipeline, shall be carried out to ensure that the appropriate level of safe isolation from all sources of danger is achieved. The risks of any uncontrolled release of gas shall be reduced to a minimum.

11.9.1.2 Attention shall be paid to the disconnection and isolation of associated electrical and gas power sources, instrumentation and control equipment, CP systems, etc. Power gas storage systems shall be depressurised. Attention shall also be given to drains, valve body cavities, instrumentation piping and "dead legs" in pipework systems.

11.9.1.3 Procedures shall be established for pipeline isolation using techniques outlined in HS(G)253.

11.9.1.4 When deciding on the isolation method, the following constraints shall be taken into account:

- the requirement to keep the rest of the pipeline system operating while working on an isolated section
- the requirement to remove safely flammable gas, vapours and other fluids
- the duration of the work activity
- the need for "redundancy" in the isolation system
- the effect on pipeline materials.

11.9.1.5 Pipeline isolation procedures shall:

- consider all reasonably foreseeable risks
- take into account the nature of the work to be undertaken, for example hot tapping, dismantling, etc.
- ensure that the level of isolation is satisfactory and secure, for example, physical disconnection, double-block-and-bleed, locking of valves (especially those which are remotely operable), etc. The aim should be to achieve as a minimum a double block and bleed isolation. Main line block valves may have bypass schemes around them to allow pressure equalisation, maintain pipeline flow during main valve isolation, etc. When a main line valve is used for isolation, the by-pass shall be shut down and a comparable standard of isolation (i.e. double block and bleed isolation) applied.
- specify the requirements for testing and proving the adequacy of the isolation
- specify monitoring arrangements
- require that valves and other plant be identified properly and labelled
- specify suitable means of communication, especially between work sites and control centres
- reference the permit to work system and other procedures, for example hot work certificates.

11.9.1.6 Procedures shall be used to return the pipeline to its original safe condition on completion of works. Special attention shall be given to ensuring that the work activity has been carried out and completed satisfactorily.

11.9.2 **Decommissioning and recommissioning**

11.9.2.1 *General*

A detailed programme of works and procedures shall be prepared and followed for all pipeline decommissioning and recommissioning operations. Purging shall be carried out in accordance with IGE/SR/22.

11.9.2.2 *Decommissioning*

Pipelines, or pipeline sections, that are to be taken out of service for modification works, maintenance or repair shall be decommissioned to remove gas and other hazardous substances.

The pipes shall be cleared and purged of flammable gases, vapours and residues. Reference should be made to IGE/SR/23 when gas is to be vented.

Pipeline surveillance shall continue to be applied after a pipeline is taken temporarily out of service. The CP system shall be maintained.

Consideration shall be given to decommissioning pipelines or pipeline sections that may not be used to flow gas for an extended period of time.

11.9.2.3 *Recommissioning*

Prior to recommissioning any pipeline, particularly those that have been decommissioned for extended periods of time, measures shall be taken to establish the integrity of the pipeline to be assured that it continues to be fit for its intended purpose.

For pipelines that have been decommissioned for modifications or other work activities, all work shall be verified as having been completed and correctly executed prior to recommissioning. Special attention shall be paid to NDT results and integrity of the pipeline prior to any pressure testing or the introduction of gas.

During recommissioning, the rate of fill shall be controlled and the pressure not allowed to exceed permitted limits.

Leakage checks shall be carried out periodically during the filling and pressurisation process. Pipeline external coating integrity and CP effectiveness shall be established according to the requirements of clause 11.6.4.

11.9.3 **In-line pigging**

11.9.3.1 An assessment of the pipeline shall be undertaken by the examination of records and as-laid information, plus site visits and site inspections, to confirm that the pipeline is piggable. Items that should be checked include the radius of bends, the length of the pig trap oversize pipework, the offtake tee sizes and configurations and whether offtake tees greater than 50% of the mainline diameter are fitted with guide bars of adequate design and construction.

Note: Guide bar requirements can vary, for example depending on pig design, branch orientation and gas flows. Requirements for new construction are given in clause 6.14.5 and for new underpressure connections in clause 11.8.5.2.

11.9.3.2 Launch and receive facilities shall be built or modified to ensure that they will accept the pigs which it is proposed to run. All other pipeline equipment shall be modified as necessary, to ensure the free passage of the pigs.

Note: Launch and receive arrangements suitable for on line pigging are identified in Sub-Section 6.14.

11.9.3.3 The design and manufacture of the pigs shall be to an appropriate standard for the anticipated pipeline operational conditions and the pipe configurations, to avoid damage to the pipeline or the pig. Where considered necessary, the pig shall be designed such that it will allow the passage of gas in the event of it becoming jammed.

11.9.3.4 The design of metal-bodied pigs shall include a means of dissipating any build up of static charge.

11.9.3.5 Where practical, pigs should be designed to be equipped with a location device.

11.9.3.6 A detailed programme of works and procedures shall be prepared and followed for all on line pigging operations. Reference should be made to Appendix 7 for further information.

11.9.4 **Pipeline damage and repair**

Whenever a pipeline is found to be defective or damaged, precautions shall be taken to afford protection to employees, contracted personnel and members of the public as outlined in clause 11.2.3.

11.9.4.1 *Damage types*

When a pipeline defect is found, the type of damage shall be identified.

Note: In general, pipeline damage is of one of the following types:

- *damage caused mechanically by interference which may involve a combination of loss of wall thickness, cracking, spalling, gouging, and denting*
- *cracking caused by stress corrosion or fatigue*
- *general loss of wall thickness by corrosion*
- *damage caused by ground movement which may involve a combination of buckling, denting and cracking*
- *damage caused to protective coating only which should be repaired in accordance with the procedures set out in clause 10.3.2.2.*

11.9.4.2 *Pipeline damage inspection and repair procedures*

Suitable procedures shall be prepared for the safe inspection, categorisation and repair of damaged or defective pipelines. Specialist advice should be sought when drawing up the procedures.

The procedures shall identify an appropriate number of damaged categories. The definition of each category shall give a clear indication of the level of severity.

For each type of damage considered by the procedures, guidance shall be given on how to allocate a damage category based on actual damage size and required pipeline design and operating conditions.

Based on the damage category, the procedures shall identify safe working practices and appropriate repair methods. The procedures shall identify any subsequent operational restriction which may be caused by a particular repair method.

11.9.4.3 *Safety in incidents where a gas escape is not involved*

Whenever the pipeline is suspected of having been damaged or has become defective, the pressure shall not be allowed to rise above the level at the time the defect was found or first suspected.

Before excavation on the suspected damage or defect, the operating pressure shall be reduced to 85% of the level above.

Note: Depending on the severity of the damage, and by reference to the procedures defined under clause 11.8.4.2, it may be necessary to reduce the pressure further.

11.9.4.4 *Safety in incidents where a gas escape is involved*

Careful consideration of the risks associated with pipeline gas escapes shall be undertaken before working on any such escape.

Where a defect or damage is combined with loss of gas, the safety precautions in clause 11.8.4.3 shall be implemented, as a minimum. Further actions shall be regulated by the particular circumstances of the incident. The requirements in clause 11.2.4.7 shall be applied.

Note: Where the gas pressure, volume of leaking gas, geometry and location of the pipeline allow, a temporary repair may be made by the application of a suitable leak clamp.

11.9.4.5 *Repair method*

A temporary repair shall maintain the pipeline in a safe condition until a permanent repair can be effected.

Note: It may be also be necessary to reduce the operating pressure of the pipeline until it can be repaired.

A permanent repair shall ensure the restoration of the damaged section of pipeline to the standard of the original undamaged pipe.

Note: This may be by replacing the damaged section with a new piece of pipe or installing a shell or other suitable proprietary repair system. Expert assessment may allow minor damage to be repaired by dressing out.

The method of repair shall be selected with reference to the procedures outlined in clause 11.8.4.2, the type and category of damage, the operating conditions of the pipeline and any requirements to maintain gas supply.

11.9.5 **Under-pressure connections, hot taps and stoppling**

11.9.5.1 *General*

A detailed programme of works and procedures shall be prepared and followed for all hot tap and stopple operations, in addition to those required under clause 11.2.3.7.

11.9.5.2 *Materials and equipment*

The materials, design and construction of hot tap and stopple connections shall be in accordance with appropriate standards, taking into account the design criteria of the pipeline. Care shall be taken to ensure that the equipment is suitable for the operating conditions, i.e. pressure and temperature, the product in the pipeline, the pipe diameter, wall thickness and material

Where a branch connection diameter exceeds 25% of the pipeline diameter, and is to be included in a pipeline to remain piggable, the connection shall include

provision for the setting of a suitable plug incorporating either guide bars or the original pipe coupon.

Design and construction requirements for any guide bar assembly shall be suitable for the required duty.

Critical dimensions shall be maintained during the alignment and mating of underpressure tees with associated tapping equipment and stoppling equipment. Required tolerances between load bearing members shall be achieved in order to obtain a safe and securely set stopple plugging head.

Note: The alignment and mating of underpressure tees with associated tapping equipment and stoppling equipment is essential to ensure successful operations, particularly at high pressures.

11.9.5.3 *Preparations and considerations*

Depending on the reason for the stopple operation, the number of positions requiring provision for stopple plugs should be determined. Vertical positioning of stopples and hot taps is preferred, but consideration should be given to the reduction in ground cover the remaining fittings will incur.

Consideration shall be given to the examination of pipeline welds exposed prior to the stopple operation, to ensure they are adequately sound to meet the stresses resulting from the stopple operation. If defective welds are located by examinations, consideration shall be given to reinforcing the welds by use of appropriate repair methods before any other attachments are made to the pipe.

Pipe wall quality and thickness check shall be carried out at the point of attachment of fitting to the pipeline.

Note: Figure 15 shows a typical arrangement for a double stopple operation.

Spacings between fittings shall be selected to suit the actual pipeline diameter.

11.9.5.4 Excavations for stopple and hot taps shall be substantial, and consideration shall be given to:

- adequate clearance to operate equipment
- easy escape routes
- firm base with provision of a sump for draining
- access to operate equipment.

11.9.5.5 The carrier pipe shall be supported adequately, considering the operation involved.

Note: Attention is drawn to the weight of the drilling and stoppling equipment which can be considerable on large diameters.

11.9.5.6 Welding and weld inspection shall be carried out in accordance with appropriate standards. The selection and preparation of the location on the pipeline to accept welded-on fittings shall also be in accordance with appropriate standards.

11.9.5.7 Where works involve the assembly of a series of fittings onto the pipeline for stoppling with bypass, the initial fitting locations shall be selected so that alternative locations are available between them.

Note: This will allow a new stopple tee to be installed, should the initial stopple fail to seal or any other operational problem occur.

11.9.5.8 Before penetration of the pipeline, the fitting and equipment shall be pneumatically leak tested at a pressure equivalent to the pipeline operating pressure at the time.

11.9.5.9 Where sections of pipeline are to be removed, installed or permanently decommissioned, the requirements of clauses 11.8.2 and 11.8.6 shall be observed.

11.9.6 **Permanent decommissioning of pipelines or sections of pipelines**

11.9.6.1 *General*

A pipeline that is no longer to be used for the conveyance of gas shall be taken out of service, with all hazardous fluids removed and the following options considered:

- use the pipeline for another purpose or
- remove the pipeline or sections of the pipeline or
- leave the pipeline or sections of the pipeline in-situ, but rendered permanently safe.

Note: This may involve removing components, for example valves, and capping open ends so as to leave all sections gas tight.

The following factors shall be taken into account when deciding on the most appropriate option:

- public safety
- environmental protection
- future land use
- legal duties and residual liabilities
- practical difficulties and financial considerations
- maintenance requirements, for example to prevent corrosion of the pipeline leading to pipe wall collapse or becoming a channel for the conveyance of water or gases.

11.9.6.2 For pipelines left in-situ, consideration shall be given to residual liabilities with the owner or operator of the pipeline, which may remain in perpetuity.

Note: There may be a continuing duty to monitor the condition of the pipeline and a requirement for maintenance or remedial action, for example to ensure that the pipeline route remains safe and without danger as a result of decommissioning.

11.9.6.3 *Taking a pipeline out of service*

The following steps shall be taken when taking a pipeline out of service:

- consider dismantling and removal – recommended for all above ground sections but economic considerations may limit this option to short sections of buried pipeline
- clear and purge the pipeline of any flammable gases, vapours or residues
- physically separate from other parts of the system and isolate from all possible sources of gas
- if appropriate, fill remaining pipeline sections with non hazardous material, for example by grouting, especially large diameter pipelines at road and rail crossings or at other locations sensitive to subsidence.

Note: Practical and economic considerations may limit this to short sections of buried pipeline.

- where it is not practicable to fill a large diameter pipeline section with grout, charge with an inert gas and seal permanently the vent and fill points. Leakage tests should be carried out and pressures checked periodically and re-charged as necessary.

11.9.6.4 *Identification of permanently decommissioned pipelines left in-situ*

The pipeline or pipeline sections shall be identified by suitable markers.

11.9.6.5 *Records of permanently decommissioned pipelines left in-situ*

Records of permanently decommissioned pipelines left in-situ shall be maintained.

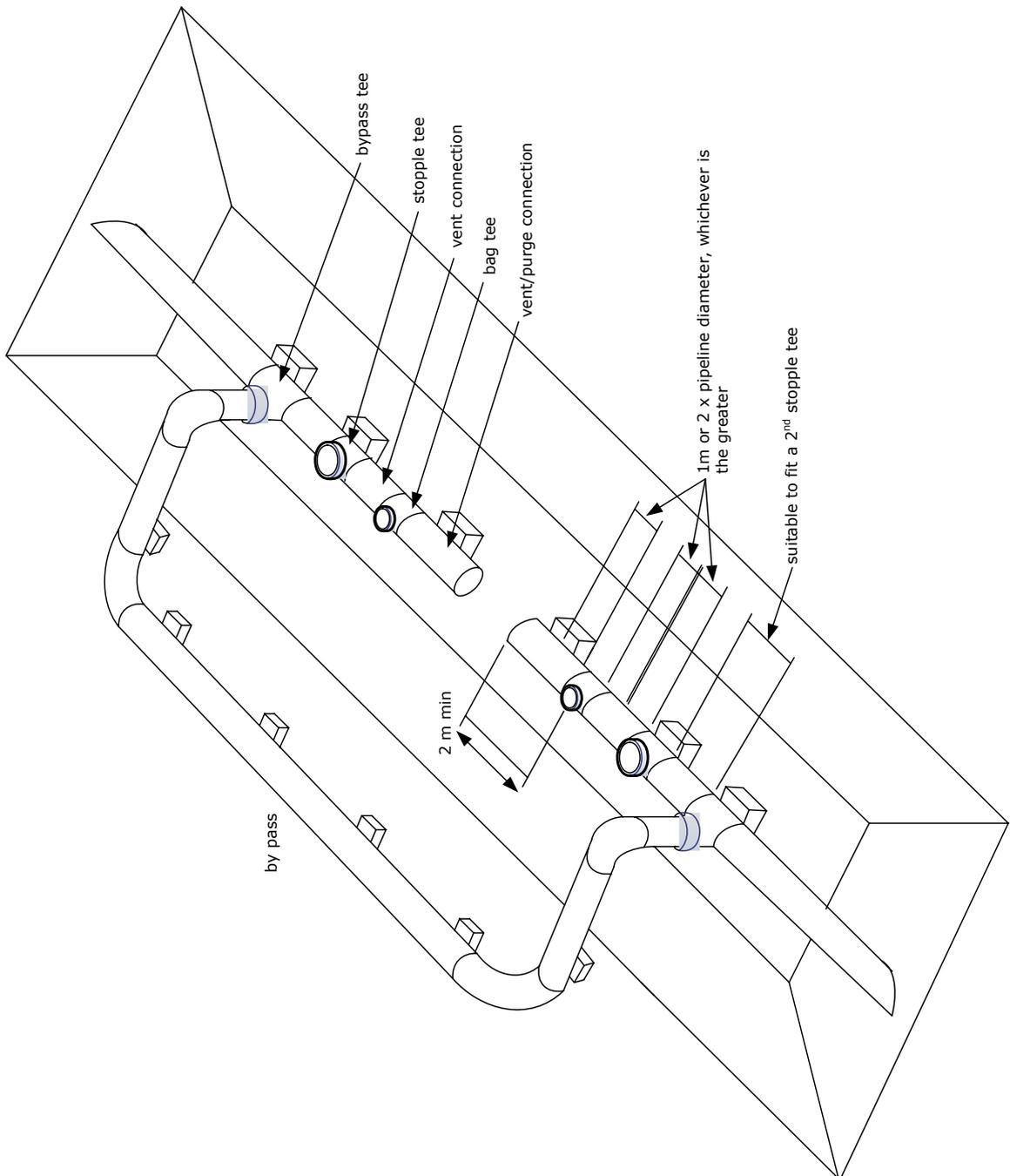


FIGURE 15 - TYPICAL ARRANGEMENT OF A DOUBLE STOPPLE WITH BY-PASS

SECTION 12 : INSTALLATIONS ASSOCIATED WITH PIPELINES

An installation (excluding PRIs) on a pipeline generally comprises one or more of the following:

- line valve or branch connection
- pig/trap installations
- overhead pipe crossing
- meter installation when the design should also be in accordance with IGE/GM/8 or IGE/GM/4
- multi-junction station with or without in-line metering and which can include pig trap(s) and/or line valve(s)
- compressor stations
- other offtakes.

12.1 GENERAL

12.1.1 This section covers installations that are associated with a pipeline (hereafter referred to as "installations") with inlet pressures greater than 16 bar that are not a PRI (which are covered by IGE/TD/13).

Due to geometry, physical configuration and functional requirements, installation pipework may be subject to greater external forces due to pressure, temperature, vibration and restraint forces than the transmission pipeline, so additional design requirements are required. Requirements relating to these additional requirements are covered in this section.

12.1.2 Installations may be below ground or above ground. Below ground installations are classed as part of the pipeline, and are subject to the same design requirements as the pipeline, whereas the design requirements for above-ground installations and elements of below-ground installations that are above ground may differ and are covered by this section.

The point of demarcation between the pipeline and an above ground installation shall be immediately downstream of the first inlet isolation valve and immediately upstream of the last outlet isolation valve. Where pig traps are fitted, the demarcation shall be the first isolation valve downstream of the receiving pig trap and immediately upstream of the launching pig trap. However, in cases where pipework between these boundaries is buried, this section may be applied.

12.1.3 For any pipe or pipework of MOP not exceeding 16 bar, this section does not apply and reference should be made to IGE/TD/3.

Any pipework stress analysis of installations should be carried out in accordance with IGE/TD/12.

12.2 SITE SELECTION

12.2.1 General

12.2.1.1 The primary consideration when selecting a site shall be a safe and economic location consistent with the preservation of natural amenities, including the avoidance of nuisance by noise. Other considerations that shall be applied include:

- avoidance of proximity to residential properties or areas that may be subject to residential development (see Sub-Section 6.7)
- positioning the installation away from overhead power lines

- ability to procure land and planning permission taking account of the potential for possible future development
- accessibility of the site
- the required preparation of the site including levelling of the site, diversion of cables and pipelines, removal of trees etc.
- impact that the local environment could have on the installation, including damage due to traffic accidents, adjacent ignition sources, flooding, subsidence, noise etc.
- availability of utilities including telecommunication, electricity, water and drainage
- proximity to tall buildings where any currents around the building may cause problems with gas dispersion (see IGE/SR/23)
- attainment of all proximity requirements quoted in other sections of these Recommendations.

12.2.1.2 Where large volumes of gas may have to be vented, the site shall be chosen so that safe dispersal can be assured.

Note: IGE/SR/23 provides appropriate guidance.

12.2.1.3 In selecting the site, regard shall be paid to any statutory or local legislation which may apply (see Appendix 2).

12.2.2 **Installations located on consumers' premises**

If situated on a consumer's premises, an installation shall be located as near as practicable to the point where the incoming pipeline enters the premises at the property boundary and should have independent access.

Note: The requirement to use the volume of the downstream pipework to dampen the impact of pressure fluctuations may also be a consideration when selecting the location of the installation on consumers' premises.

12.3 **LAYOUT OF SITE, SITE SECURITY, AND HOUSINGS AND BUILDINGS**

12.3.1 **General**

The layout of the site and security provisions shall take account of security against unauthorised interference and operation and any constraints imposed by the planning authority.

12.3.2 **Layout of the site**

12.3.2.1 The layout of the site shall take account of the following:

- access to plant and equipment for construction, maintenance and in an emergency, including access for emergency vehicles and their ability to turn. Access to plant for maintenance should include consideration of access to pig traps to enable pigging operations to be carried out safely
- site drainage and water table
- the potential extent of any hazardous area, including consideration of the location of gas heaters and other burner equipment. Under normal circumstances, any hazardous area should not extend beyond the site boundary. However, where the hazardous area is well above ground level and away from any sources of ignition, an exemption may be justified
- ensuring that equipment is located sufficiently far away from the security fence to protect it from external interference, for example through vandalism.

- 12.3.2.2 Any installation should be located away from public highways and railways and at least at the minimum distances defined in this Standard. Installed plant shall be sufficiently clear of roads so as to avoid damage from moving vehicles and loads.
- 12.3.2.3 Consideration shall be given to the lighting of the site, having regard to the size of site, location and other relevant factors.
- 12.3.2.4 Roadways inside the site shall be kerbed to prevent vehicles trespassing off the hard access. Vulnerable pipework or equipment shall be protected by safety barriers.
- 12.3.2.5 The location and layout of the installation shall be selected to preserve the natural amenities of the area, due regard being given to screening, by trees or artificial means, architectural features and decorative colour schemes to meet the requirements of the local authority.

12.3.3 **Site security**

- 12.3.3.1 Site fencing or other enclosures shall be provided to secure the site against entry by unauthorised persons.

Note: It may be appropriate at some locations to supplement the security fence with an additional perimeter fence.

- 12.3.3.2 Consideration shall be given to the provision of locking devices on valves, including auxiliary valves located externally on the site.
- 12.3.3.3 Consideration shall be given to installing intruder detection devices.
- 12.3.3.4 Where the presence of vehicular traffic could cause a hazard, the use of safety barriers shall be considered.
- 12.3.3.5 Prominent signs shall be displayed, prohibiting smoking and other ignition sources.
- 12.3.3.6 A permanent notice shall be displayed clearly, showing the emergency telephone number which may be used by the public or others.

12.3.4 **Housings and buildings**

- 12.3.4.1 Enclosure of all or part of an installation may be provided by adopting one of the following methods which may be acceptable to the planning authority:
- complete or partial enclosure in a building
 - enclosure by removable covers or by bund walls fitted with removable covers
 - housing wholly or partly in an underground pit or pits, fitted with removable covers.
- 12.3.4.2 Where equipment is installed in any type of housing, consideration must be given to providing adequate access to the equipment and a safe means of escape in an emergency.
- 12.3.4.3 Consideration shall be given to providing explosion relief if an explosion in the housing could present a hazard to the general public or employees (except where a working procedure is in place to limit the potential for the ignition of any explosive atmosphere).

Note: Further guidance on requirements for explosion relief is given in IGE/TD/13.

12.3.4.4 All buildings, rooms, chambers, pits or other forms of housing for installations or ancillary equipment shall be adequately ventilated in order to maintain a safe atmosphere under the conditions which may be reasonably anticipated.

Note: Guidance on the ventilation of above and below ground housings is given in IGE/SR/25.

12.4 **GENERAL DESIGN**

12.4.1 The design of any installation shall include consideration of:

- its complete life-cycle through concept design, detail design, material and equipment procurement, fabrication, installation, testing, commissioning, operation, maintenance, modification and final decommissioning
- fabrication and methods of construction, together with any heat treatment, NDT and inspection, the methods and procedures being in accordance with appropriate standards
- risk to any person and effect on the environment. Any hazard associated with the installation should be identified, risks evaluated and measures taken to reduce risk to ALARP (see IGE/SR/24)
- facilitating the safe isolation, inspection and maintenance of plant and equipment
- the provision of sufficient safety systems to protect the installation against overpressurisation
- the provision of sufficient isolation valves and valved purge and vent points to enable de-pressurisation and subsequent testing
- ensuring that all plant and equipment is capable of withstanding the most severe conditions of coincident pressure, temperature, chemical action and mechanical loading that may occur during normal operation and reasonably-foreseeable adverse conditions, for example the elevated temperature immediately downstream of a compressor station
- the required level of reliability, taking into account the requirements for the safe operation of the system continuity of supply, plant and equipment failure characteristics and redundancy, for example by the inclusion of multiple streams, etc.
- minimising the effect on the environment of gas venting through the operation of control devices, etc.
- the duty of the installation, including flow, pressures and temperatures
- any requirements for telemetry and/or metering.

12.4.2 Where electrical equipment is installed on site, appropriate explosion-protected electrical apparatus shall be provided in areas where gas may be present.

12.4.3 Consideration shall be given to the need for providing anchorages for the pipework system. These shall be designed to be effective under all operational conditions.

12.4.4 All joints between the pipeline and the first valve of the installation, including the inlet to the first valve, shall be welded in order to restrict possible future leakage which cannot be isolated by closure of the valve.

The number of small diameter connections to the main pipeline shall be restricted to a minimum, be of robust design and, where practicable, be of not less than 50 mm diameter.

12.4.5 Any foundation shall be designed and constructed to accommodate the proven nature of the ground and requirements of the structure to be supported. Design and construction shall conform to appropriate standards such as BS 8110 (for structural concrete) and BS 8004 (for foundations).

12.4.6 Pipework shall be sized such that the gas velocity will not exceed 20 m s⁻¹ for unfiltered gas and 40 m s⁻¹ for filtered gas at the outlet of any installation under conditions of maximum flow and lowest operational pressure.

Note 1: Diameter changes may influence the performance of the system in respect of noise, turbulence and vibration. A change in diameter can be achieved by the use of forged fittings or taper pieces to provide a smooth transition.

Note 2: Where it is essential to the design requirements, gas velocities within the streams may exceed the recommended filtered gas velocity subject to the system design capability, noise levels and good engineering practice.

12.4.7 The design pressure of components and pipework shall be compatible with their location in relation to pressure boundaries.

12.5 PIPEWORK DESIGN

12.5.1 The design of pipework on installations shall comply with Section 6 except for above ground installations when clauses 12.5.2 or 12.5.3 should be applied.

12.5.2 The minimum wall thickness shall be selected by using the largest of the values determined in the formula given in clause 12.5.3 and those in Table 13.

Note 1: Table 13 values will be found to apply at relatively low pressures and the formula will be found to apply at higher pressures.

Note 2: Greater wall thickness may need to be specified following any specialist stress calculation made in accordance with additional recommendations such as in IGE/TD/12.

12.5.3 The minimum wall thickness of pipe shall be not less than the nominal wall thickness less the maximum tolerance for under-thickness of the wall and shall be at least PD (20fs).

- t = design wall thickness of pipe (mm)
- P = design pressure (bar)
- D = actual outside diameter of pipe (mm)
- f = maximum design factor determined from Table 13
- s = specified minimum yield strength (N mm⁻²)

SITE DESCRIPTION	AREA*	MAXIMUM f
Location manned	All	0.67
Location protected against External interference and unmanned	R S T	0.67 0.5 0.3
Location unprotected against interference and unmanned	All	0.3

Note: See Sub-Section 6.7.

TABLE 13 - SELECTION OF MAXIMUM DESIGN FACTOR (f) FOR INSTALLATIONS

12.5.4 Pipework shall be capable of sustaining, without overstress or unacceptable displacement, the following loads under design and conditions:

- self weight
- weight of fluid
- internal pressure – maximum design and test
- thermal expansion and contraction due to temperature gradients
- additional loads as listed in Sub-Section 6.5.

12.6 **STRESS ANALYSIS**

12.6.1 **General**

12.6.1.1 Any stress analysis considered necessary should be carried out in accordance with IGE/TD/12.

Note: The need for formal stress analysis of buried installations depends upon the function and complexity of the installation. Where the installation duplicates or replaces an existing system, or can be reliably assessed through comparison with previously analysed pipework arrangements and, with the agreement of the owner/operator, formal stress analysis may not be required. Similarly, where there are a number of similar installations on the pipeline, for example block valves or branched connections, a single generic analysis may be justified.

12.6.1.2 Formal stress analysis shall be carried out for above ground installations. The purpose of the analysis is to demonstrate that the pipework arrangement has sufficient flexibility to prevent thermal expansion/contraction and pressure loads or movements of supports from causing:

- failure of piping or supports from overstress or fatigue
- joint failure (leakage)
- high stress or distortion in pipework and fittings
- excessive loads on connected equipment.

12.6.1.3 The stress analysis model of an above ground installation shall include pipework supports. The results of the analysis shall be used in the detailed design of the supports, and the as-built support arrangements shall be checked to confirm these agree with the assumptions of the analysis.

12.6.1.4 Where formal stress analysis is required, relevant soil properties are required to ensure pipework restraint is adequately modelled. Where site-specific properties are not available, the stress analysis shall take into consideration appropriate upper and lower bound values for soil stiffness and friction.

12.6.1.5 An installation will be subject to internal and external forces such as ground movement and changes in temperature and pressure. Special attention shall be given to the design in the following circumstances:

- where movement of an underground pipeline may impose stresses on an above-ground connection
- where large changes in temperature are possible
- where adequate flexibility is difficult to obtain, for example in a long meter run or similar straight run of above ground piping
- where fatigue stressing caused by regular pressure and/or temperature changes or vibration may occur.

Reference should be made to IGE/TD/12, which gives detailed guidance and a method for comprehensive analysis.

12.6.2 **Supports**

Primarily, supports serve to retain pipework and equipment level and at the desired height, and to allow safe removal of equipment for maintenance or replacement.

12.6.2.1 Supports shall be located to contain bending stresses within allowable limits. Care shall be taken in the location of supports to ensure that other stresses also remain within allowable limits.

- 12.6.2.2 Sufficient supports shall be provided to avoid excessive deflections and high stresses caused by the additional weight of fluid contained during hydrostatic testing.
- 12.6.2.3 Where appropriate, heavy components shall be supported to prevent bending or torsional loading of adjacent pipework.
- 12.6.2.4 Supports not intended specifically to anchor pipe shall be designed to minimise interference during pipe expansion.
- 12.6.2.5 Supports shall be designed to cope with any mechanical or noise-excited vibration.
- 12.6.2.6 Supports welded directly to pipe shall be of the full encirclement type. Care shall be taken to minimise local welding stresses, for example by using thick-walled pipe and controlled welding onto the pipe longitudinally.
- 12.6.2.7 Anchor supports shall be located to minimise stresses and should be designed to withstand the loads indicated by stress analysis. The possibility of the reversal of forces shall be considered.
- 12.6.2.8 Buried pipework and headers shall not be considered as anchors unless specifically designed for that purpose.
- 12.6.2.9 Supports shall incorporate electrical insulation to meet the requirements of any CP system.
- 12.6.2.10 Precautions shall be taken to prevent corrosion at the point of contact of the support and the pipework by effectively sealing the interface.
- 12.6.2.11 Where it is considered necessary, pipe supports shall be designed to be removable for maintenance work and for inspection purposes.
- 12.6.2.12 Care shall be taken to adequately support sensing and auxiliary pipework because of its small diameter and inherent vulnerability.
- 12.7 **PIPE AND FITTINGS**
- 12.7.1 Main pipework and fittings, for use above ground, shall be of steel (see Section 5).
- 12.7.2 As far as is practicable, pipework should be designed to allow the removal and replacement of equipment without the need to distort pipework.
- 12.7.3 Pipe shall be selected in accordance with Section 5.
- 12.7.4 Pipe should comply with recognised standards to suit the required duty, such as:
- API 5L (PSL 1 and PSL 2)
 - ASTM A 53
 - ASTM A 106
 - ASTM A 333
 - ASTM A 671
 - ASTM A 672
 - BS EN 10208
 - BS EN 10216
 - BS EN 10217

- BS EN 10255
- ISO 3183-2.

- 12.7.5 The selection of pipe shall be qualified with respect to its yield strength, brittle and ductile fracture toughness and weldability in accordance with Section 5.
- 12.7.6 Any NDT of pipe shall be carried out after all manufacturing processing, heat treatment and stress relieving have been completed.
- 12.7.7 Screwed pipe and fittings shall not be used for pipework of MOP exceeding 16 bar.
- 12.7.8 The minimum wall thickness shall be selected in accordance with Section 5.
- 12.7.9 Fittings shall be of a material compatible with selected pipe and with each other.
- 12.7.10 Fittings shall be of the appropriate strength for the proposed test pressure.
- 12.7.11 The selection of fittings shall be qualified with respect to yield strength, brittle and ductile fracture toughness and weldability.
- 12.7.12 Any NDT of flanges, fittings and branches shall be carried out after all manufacturing processing, heat treatment and stress relieving have been completed. Methods appropriate to specific components, and to particular areas such as seam welds, shall be determined.
- 12.7.13 Branches shall be positioned on pipes so that the edges of branch welds are at least 50 mm away from any other weld.
- 12.7.14 Fabricated branches (type D) shall be used in preference to stub junctions (type A).
- 12.7.15 The inside of butt welds on fabricated tapers shall be aligned. The minimum wall thickness and material grade of the tapered section generally shall be at least equal to the wall thickness of the pipe attached to the larger end. Taper pieces intended to reduce turbulence shall have concentric ends.
- 12.7.16 Bolting and gasket material for flanged joints shall be in accordance with relevant standards.
- 12.7.17 It may be necessary for some components and fittings to be stress-relieved during fabrication and, possibly, after installation. The requirements shall be determined by reference to an acknowledged standard such as PD 5500 (Appendix D).
- 12.7.18 Where fittings are fabricated to other than BS 1640, the fittings shall be of the appropriate strength for the proposed test pressure. They shall be qualified with respect to strength, fracture toughness and weldability in a similar manner to pipe.
- 12.7.19 Mechanical testing shall be carried out after hot forming and final heat treatment. Tensile testing for forged components shall be carried out in accordance with an appropriate standard on specimens taken transverse to the direction of rolling of the original piece. Fittings shall be qualified with regard to fracture toughness by notch ductility testing, for example Charpy testing.

Note: Suitable sampling rates from a given batch of fittings, specimen extraction procedures and acceptable test results are suggested in BS and ASME codes.

12.7.20 The weldability of fittings of a specific type and from a specified source of supply shall be assessed on a full size production sample, preferably a complete butt weld to a pipe pup.

12.7.21 Table 14 should be used when selecting fittings.

Fitting type	Material*	Limitations	Construction in accordance with
Compression fittings	Carbon steel Stainless steel	$\phi \leq 40$ mm	BS 4368
Forged or extruded bends, tees, reducers, caps etc.	Steel		BS 1640 for $\phi > 600$ mm MSS SP 75 for $\phi \geq 600$
Weldolet branches	Steel	$d/D \leq 0.3$	ANSI/ASME B 31.11
Threadolet branches	Steel	$\phi \leq 50$ mm/ 2 in screwed	ANSI/ASME B 31.11
Sweeplet branches	Steel	$d/D \leq 0.6$	BS 1640 or ANSI/ASME B 31.11
Full encirclement branches	Steel		PD 5500 or ANSI/ASME equivalent BS 13445
Cast bends	Steel		
Fabricated tapers	Steel		PD 5500
Forged components (whole or part)	Steel		BS EN 10222-1 to 5
Flanges	Steel - according to relevant flange standards	$\phi \leq 600$ mm $\phi > 600$ mm	ANSI/ASME B 16.5 BS 3293

Note: Steel used to manufacture fittings require at least equivalent wall thickness and physical and chemical properties to those of the pipe.

TABLE 14 - LIMITATIONS ON THE SELECTION AND USE OF FITTINGS

12.7.21 Guidance on requirements for sensing, instrument and auxiliary pipework associated with installations should be sought from IGE/TD/13.

12.7.22 Construction and fabrication shall be carried out in accordance with Section 7. Fabrication requirements shall ensure that the pipeline and its associated installations are of equivalent quality and integrity.

12.8 PROTECTION AGAINST EXTERNAL CORROSION (OTHER THAN CP)

Suitable protection against external corrosion shall be provided unless the material is, in itself, resistant to corrosion, for example stainless steel.

Note: Corrosion of internal surfaces of plant carrying dry Natural Gas will not occur under normal operating conditions.

Any coating shall be specified in accordance with the design requirements of the installation and its environment. Where different coatings are used, joints between the coating systems shall be made by overlapping one coating with another. Where the installation is to be built in an area of contaminated ground or in harsh environmental conditions, consideration shall be given to the use of specialised, high performance, coatings.

12.9 VALVES

12.9.1 The following factors shall be taken into account when deciding upon the type of valve to be used for any particular application:

- the necessity for effective sealing at all operational pressure levels
- any requirements for reducing to a minimum the pressure loss through the valve

- the provision of adequate mechanical strength
- the valve torque characteristic
- special requirements for valves near meters, as noted in IGE/GM/8
- the speed of operation of the valve
- valve duty , including pressure differential and flow conditions
- the need for block and bleed facilities.

12.9.2 All branch connections to main stream pipework, including impulse pipes, shall be valved as close as practicable to the point of attachment.

12.10 **RELIEF VALVES, SLAM-SHUT VALVES AND THERMOWELLS**

12.10.1 **Relief valves, vents and drains**

12.10.1.1 Provision shall be made for venting, purging and draining all sections of pipework and equipment that may have to be isolated during construction or maintenance.

12.10.1.2 All relief valves shall preferably be fitted upstream of consumers' premises. Extreme care shall be taken in choosing the location of relief valves so that the vented gas will not interfere with industrial processes and the chances of ignition are minimum.

12.10.1.3 The capacity of pressure-relief valves and vents shall be designed to limit pressure in the system to the extent required to prevent overpressure of the system to be protected.

12.10.1.4 Relief valves, whether direct-acting or pilot controlled, shall be fully automatic in operation.

12.10.1.5 The construction, testing and performance of relief valves shall be in accordance with the requirements of IGE/TD/13.

12.10.1.6 The vent system shall have adequate support and anchorage to minimise induced stresses in the relief valve and its associated pipework.

12.10.2 **Thermowells**

Where feasible, surface mounted temperature measuring devices shall be used. Where thermowells are required, they shall be:

- designed in accordance with the provisions of an appropriate standard such as BS 2765
- of non-welded construction and preferably forged and manufactured from stainless steel to a specification such as BS EN 10222
- so designed as to minimise stress concentrations at the root of the stem and to prevent resonant vibrations.

Note: These may be caused by a combination of gas velocity, the design features of the individual thermowells and their configuration in multiple unit arrays.

12.10.3 **Slam-shut valves (SSVs)**

Slam-shut valves (SSVs) may be required on some installations such as compressor stations.

12.10.3.1 The design, manufacture and testing of SSVs shall be in accordance with the relevant clauses of Sub-Section 5.6.4.

A SSV may be an independent special purpose unit, a composite unit incorporating a quick closing valve, or a unit comprising a conventional valve and an actuator.

With the latter type, care shall be taken to match the valve and actuator torque characteristics, especially on closing. Each actuator shall include its own adjustable control stops which prevent excessive stresses being imposed by the momentum of the actuator being transmitted to the valve stops and body.

12.10.3.2 Where appropriate, the direction of gas flow shall be clearly marked on the valve body.

12.10.3.3 The selection of a particular type of SSV shall take into account calculations to determine a maximum acceptable safe closing time. The factors involved in these calculations shall include:

- maximum working pressures
- volume of associated downstream pipework
- fail-open characteristics of the regulator(s)
- capacities of the relief valves and vents
- flow rate through the working regulator under fault conditions.

12.10.3.4 Data on dead time, closing time and repeatability of activation of valves shall be obtained from the manufacturer.

12.11 **VIBRATION AND ACOUSTIC FATIGUE**

Account shall be taken of the damaging affects of acoustic fatigue caused by high frequency vibration.

Note: This can affect components installed within the pipework, particularly the elements within silencers, the pipework itself and small bore instrument connections. Specific precautions to secure small-bore pipework against vibration, or even to alter its natural excitation frequency, may be necessary to avoid damage to compression type fittings. Further guidance is given in IGE/TD/13.

12.12 **ELECTRICAL EQUIPMENT**

12.12.1 **General**

12.12.1.1 Fuses shall be of the high-rupturing-capacity type.

12.12.1.2 Any metallic part, including a stairway and its supports, shall be earthed.

12.12.1.3 Any electrical equipment shall be designed, manufactured, installed and maintained in accordance with statutory requirements and appropriate standards.

12.12.1.4 Any cable shall be installed on a cable tray or in a duct.

12.12.2 **Hazardous areas**

12.12.2.1 Areas that may become hazardous as the result of the presence of flammable gas are classified in the UK as Zone 0, 1 and 2 and are defined in IGE/SR/25 and IGE/GM/7.

The installation, testing and maintenance of any equipment within such specified zones shall comply with the requirements of the appropriate parts of BS EN 60079.

Note: Some information on equipment selection is given in BS EN 1127.

12.12.2.2 A zoning diagram, as illustrated in IGE/SR/25, shall be produced and maintained as a permanent record to enable the correct selection and siting of electrical equipment (and other potential sources of ignition) to be undertaken for both initial installation and future modifications.

Note: To avoid proliferation of types of electrical equipment in small installations, it may be desirable to install Zone 1 equipment in both Zone 1 and Zone 2 areas.

12.12.2.3 Due regard shall be paid to the effects of any foreseeable extensions to the installation itself and to other plant in its vicinity.

12.12.3 **Electrical isolation**

12.12.3.1 Electrical isolation shall be as specified in BS EN 60079 and BS 7671.

12.12.3.2 The position and duty of any isolating switch shall be clearly identifiable on site.

12.12.3.3 Any circuit isolator supplying apparatus located in a hazardous area shall disconnect the neutral as well as the phases.

12.12.3.4 Automatic or remotely-controlled equipment shall be provided with immediately-adjacent stay-put-stop buttons or equivalent safeguards, including arrangements for padlocking in order to prevent accidental starting during maintenance or inspection. Where isolation is required for long periods, main isolating switches shall be used and padlocked. Either an isolator shall interrupt all control and monitoring circuits, main phase and neutral connections, or suitable provision shall be made for multiple isolations.

12.13 **LIGHTNING, EARTHING AND LIGHTING**

12.13.1 **Lightning**

Consideration shall be given to installing lightning protection which shall be to a suitable standard.

12.13.2 **Earthing**

12.13.2.1 The whole of the electrical installation must be earthed adequately and effectively and in accordance with appropriate standards.

Note: In the UK, the supply authority has no mandatory obligation to supply the user with an earthing terminal (with the exception of protective multiple earth (PME) systems).

12.13.2.2 The following shall be taken into account when designing earthing arrangements:

- where the supply is taken directly from the local distribution system by means of an underground cable, the electricity supply authority will usually permit connection of the user's earthing conductor to the sheath of that cable
- where the supply is taken directly from the local distribution system by means of an overhead line, it may be necessary for the user to provide an earth
- where the supply is taken from a local transformer, the user's earth connection usually will be made at the same electrode as that to which the transformer secondary neutral is connected.

12.13.2.3 Care shall be taken to avoid interactions between the electrical earthing, instrumentation earthing and CP systems.

- 12.13.2.4 The design and siting of electrical earthing electrodes shall be given specialist attention. Such electrodes shall be manufactured from stainless steel, austenitic steel or other CP-compatible materials.

Note: Copper or any other incompatible electrodes are not suitable as the buried steel pipework may corrode preferentially with respect to the electrode.

Coke or other carbonaceous materials shall not be used as part of the electrode systems.

- 12.13.2.5 Site supplied from PME or combined neutral earth (CNE) systems present certain problems on which specialist advice should be sought.

Note: In particular, this is important where intrinsically safe circuits are employed and the impedance of earth return paths from safety barriers are to be kept below 1.0 ohm.

12.13.3 **Lighting**

- 12.13.3.1 Continuous illumination may be unnecessary in many plant areas, but consideration shall be given to the installation of permanent fixed lighting points, with separate switching at positions where light is frequently required to carry out routine maintenance.

Note: In many cases, the need for flameproof lighting can be avoided by the provision of floodlighting equipment sited outside the hazardous area or mounted at a sufficient height to eliminate the possibility of the flammable mixture approaching the fittings.

- 12.13.3.2 All lighting switches shall be located in safe areas and be readily accessible.

Note: In "classified safe" areas, supplementary lighting for occasional use can be provided by portable equipment.

- 12.13.3.3 In hazardous areas where portable lighting equipment is used, the equipment shall be correctly certified for the position of use.

12.14 **INSTRUMENTATION AND TELEMETRY**

Instrumentation, gas instrumentation pipework and telemetry requirements shall be in accordance with IGE/TD/13.

12.15 **TESTING**

Testing shall be carried out in accordance with Section 8.

12.16 **METERING**

For associated metering, reference shall be made to the following, as appropriate for the pressure and meter type:

- IGE/GM/4
- IGE/GM/5
- IGE/GM/7
- IGE/GM/8.

Note: Reference may also be made to other international metering standards such as BS EN ISO 5167 and AGA 3 for orifice plates.

12.17 **MAINTENANCE**

- 12.17.1 The aims of operation and maintenance are to ensure that the installation:

- operates in a safe and environmentally sound manner

- offers sufficient reliability for the operating conditions within which it is used and will continue to operate until its next maintenance
- is in sound mechanical condition
- operates at the appropriate set points
- is installed correctly.

12.17.2 Operation and maintenance shall be designed to maximise the availability of the associated gas supply. Contractual arrangements for gas supply, with 3rd parties, should be taken into account.

12.17.3 The risks and consequences of failure associated with operating and maintaining an installation shall be considered from design, through installation, commissioning and operation.

The modes of failure will be governed largely by the plant design and the operating method used. Using this knowledge, in addition to a good maintenance history, an effective maintenance strategy can be devised to reduce the risk of failure to an acceptable level.

Consequences to be considered shall include failure to supply gas and impact on the downstream system.

Note: For new plant, or in the absence of any operational or maintenance history, it may be desirable to use manufacturers' recommendations as the initial basis of all maintenance activities. Normally, plant history will be gained, over time, from operational/maintenance data or may be gained from experience of similar equipment/installations.

12.17.4 A maintenance regime, which includes the requisite skills, experience and resources, shall be established or contracted to ensure maintenance is undertaken safely and effectively.

12.17.5 Arrangements shall be made to deal with emergencies both inside and outside normal working hours.

APPENDIX 1 : GLOSSARY, ACRONYMS, ABBREVIATIONS, UNITS AND SYMBOLS

A1.1. GLOSSARY

case length	The axial distance along the pipeline over which the risk is assessed. A length of 1.6 km will encompass most isolated developments and will provide consistency with area classification procedures.
dangerous dose	A dose of 1060 thermal dose units $((\text{kw m}^{-2})^{4/3} \text{ secs})$ which results in: "severe distress to almost everyone; a substantial fraction (of people exposed to it) requiring medical attention; some people (exposed to it) are seriously injured requiring prolonged treatment; any highly-susceptible people (exposed to it) might be killed."
dense traffic	Generally means traffic on a high density traffic route. However, where specific constraints apply which creates traffic congestion, consideration needs to be given to defining lower traffic densities which result in the road being at full capacity as dense.
design pressure	The pressure on which design calculations are based. <i>Note 1: Design pressure is the target MOP</i> <i>Note 2: Design pressure will be greater than or equal to MOP.</i>
event tree	Provides a systematic way of identifying all of the possible outcomes from a hazardous event. In this case, the initial event for a pipeline would be the release itself. The tree is then used to identify the likelihood of leak/rupture, ignition, the possible types of release, etc.
failure cause	The reason for a pipeline reaching a "limit state". Examples are external interference, external corrosion and growth of defects due to fatigue.
failure mechanism	A potential cause of pipeline failure, for example corrosion, external impact, overpressure etc.
failure probability	The likelihood that one or more failure mechanism will occur.
hazard range	A distance from the pipeline beyond which the risk of injury from the worst credible pipeline failure would be of no concern.
high density traffic routes	High density traffic routes include: <ul style="list-style-type: none"> (a) All motorways (b) All roads that carry a volume of traffic totally, in both directions, 2000 vehicles per hour and above, for periods of at least 10 hours per week. The 10 hours may be spread evenly over the week or may be concentrated into set periods. On dual carriageway roads which carry less than this number, consideration needs to be given to future growth. (c) All dual or multi-track rail routes with trains passing any one point, in either direction, at frequencies in excess of one every 15 minutes for a cumulative period of 8 hours in any one day.

initial defect size	The maximum size of defect (or the distribution of actual sizes of defects) which could be left in the pipeline following the commissioning hydrotest.
limit state	The state of the pipeline when it no longer satisfies a particular design requirement, see "ultimate limit state" and "serviceability limit state".
limit state function	Mathematical relationship between the relevant parameters characterising a particular "failure cause" that exists when the pipeline has reached its limit state.
loads	The forces acting on a pipeline or other components.
maximum incidental pressure (MIP)	The maximum pressure which a system is permitted to experience under fault conditions, limited by safety devices.
maximum operating pressure (MOP)	The maximum pressure at which a system can be operated under normal conditions.
multi-storey	Any occupied building with five or more storeys above ground level.
operating pressure (OP)	The pressure at which the gas system operates under normal conditions
peak level OP	The maximum pressure permitted under normal conditions.
pressure deviation	The difference between the measured pressure and the set pressure.
pressure regulating system	A control system, the purpose of which is to hold pressure constant or to vary it in a predetermined manner.
probability density	A function which defines the relationship between the value of a parameter and function the probability of occurrence of that value.
proximity distance	Minimum distance permissible between the pipeline and any normally occupied building or traffic route as derived from Figure 4 and 5.
resistance	The ability of a pipeline or other component to withstand the forces acting on it.
sensitive locations	Locations at which it may be difficult for people to escape or which have concentrations of people who would have difficulty in escaping and/or with an increased sensitivity to thermal radiation. Examples of such developments are hospitals, convalescent homes, nursing homes, old peoples homes, sheltered housing, schools, colleges, buildings with five or more storeys, large community and leisure facilities, large open air gatherings (see IGEM/TD/1 Edition 5 Supplement 2).
serviceability limit state	The state of the pipeline when it no longer meets the full design requirements but is still able to contain the gas it is carrying. This limit state had no direct safety or environmental implications. Examples include yielding, denting and buckling.
set pressure	The command value to a pressure regulating system.

societal risk	The relationship between the frequency and number of people in a given population suffering a specified level of harm from the realisation of specific hazards.
steady oscillation	An oscillation, the amplitude, period and wave form of which remain unchanged.
steady state	The final state which a pipeline system attains when the effects of external disturbances have ceased.
structural reliability model	A mathematical or statistical model of a failure mechanism.
ultimate limit state	The state of the pipeline when it can no longer contain the gas it is carrying. This limit state has safety and environmental implications. Examples are leaks and ruptures.

A1.2 **ACRONYMS AND ABBREVIATIONS**

AC	Alternating current.
ACoP	Approved Code of Practice
ALARP	As low as reasonably practicable.
BPD	Building proximity distance.
BERR	Department for Business, Enterprise and Regulatory Reform
CBA	Cost benefit analysis.
CDM	Construction (Design and Management) Regulations.
CDT	Current drain test
CIPS	Close interval potential survey.
CNE	Combined neutral earth.
CONCAWE	Conservation of Clean Air and Water in Europe.
COPA	Control of Pollution Act.
CP	Cathodic protection.
DC	Direct current.
DCVG	Direct current voltage gradient
DEFRA	Department of Environment, Food and Rural Affairs
DETR	Department of Environment, Transport and the Regions.
DSEAR	Dangerous Substances and Explosive Atmospheres Regulations.
DTLR	Department of Transport, Local Government and Regions
DWTT	Drop Weight Tear Test.
EA	Environment Agency.
EC	European Community
EIA	Environmental Impact Assessment.
EPA	Environmental Protection Act.
EPM	Emergency Procedures Manual.
ES	Environmental Statement.
EU	European Union.
GB	Great Britain
GPS	Global positioning system.
GS(M)R	Gas Safety (Management) Regulations.
GT	Gas transporter.
HAZOP	Hazard and Operability Study.
HSE	Health and Safety Executive.
HSWA	Health and Safety at Work etc. Act
IGEM	Institution of Gas Engineers and Managers.
MAPD	Major Accident Prevention Document.
MIP	Maximum incidental pressure.
MOP	Maximum operating pressure.
NDT	Non-destructive testing.
NRA	National Rivers Authority
NTSB	US National Transportation Safety Board.

O&M	Operation and maintenance
OP	Operating pressure.
PCA	Pipeline Construction Authorisation.
PIMS	Pipeline Integrity Management System.
PME	Protective multiple earth.
PPE	Personal protective equipment.
PPG	Pollution Prevention Guidelines.
PRI	Pressure regulating installation.
PSR	Pipelines Safety Regulations.
PSSR	Pressure Systems Safety Regulations.
QRA	Quantified Risk Assessment.
SCC	Stress corrosion cracking.
SEPA	Scottish Environment Protection Agency.
SMTS	Specified minimum tensile strength.
SMYS	Specified minimum yield strength.
SRA	Structural reliability analysis.
SSV	Slam-shut valve.
STP	Strength test pressure.
UKOPA	United Kingdom Onshore Pipeline Operators Association.

A1.3 UNITS

Am^{-2}	amperes per square metre
cm^2	square centimetres
cpm	chances per million
$^{\circ}\text{C}$	degrees Celsius
hr	hour
in	inch
kW m^{-2}	kilowatts per square metre
km	kilometre
kV	kilovolt
km h^{-1}	kilometres per hour
mins	minutes
m^3	cubic metre
mbar	millibar
mm	millimetre
mm^2	square millimetre
m s^{-1}	metres per second
N	Newton
N mm^{-2}	Newtons per square millimetre
ppm	parts per million
s	second
V	Volt.

A1.4 SYMBOLS

\varnothing	diameter
t_{\min}	minimum wall thickness
N and n	number of cycles
S	constant amplitude stress range
D	outside diameter of pipe
D_F	damage fraction
t	design thickness of pipe
P	design pressure at the relevant design temperature
s	SMYS
f	design factor
>	greater than
<	less than
\leq	less than or equal to
σ_{eg}	Von Mises (equivalent) stress

σ_c	circumferential stress
σ_L	longitudinal stress
σ_k	hoop stress due to internal pressure
σ_a	through wall component of the longitudinal stress
τ	shear stress.
Σ	sum of.

APPENDIX 2 : REFERENCES

A2.1 UK LEGISLATION

This Sub-Appendix lists legislation referred to in this Standard, as well as some legislation not referred to but which may be applicable.

A2.1.1 Acts

- Ancient Monument and Archaeological Areas Act 1979
- Animal Health Act 1981 as amended
- Coastal Protection Act 1949
- Control of Pollution Act 1974
- Deer (Scotland) Act 1996 as amended
- Environment Act 1995
- Environmental Protection Act 1990
- Forestry Act 1991
- Gas Act 1986 and 1995
- Health and Safety at Work etc. Act 1974
- Local Government Act 1999
- Local Government (Scotland) Acts 1973, 1988 and 1994
- New Roads and Street Works Act 1991
- Noise and Statutory Nuisance Act 1993
- Pipelines Act 1962 as amended
- Protection of Badgers Act 1992
- Town and Country Planning Act 1990
- Town and Country Planning Act (Scotland) 1997
- Transport Act 2000
- Water Resources Acts 1963 and 1991
- Wildlife and Countryside Act 1981 as amended
- Wildlife and Countryside Act 1981 (Amendment) Act 1985
- Wild Mammals (Protection) Act 1996.

A2.1.2 Regulations and Orders

- Borehole Sites and Operations Regulations 1995
- Conservation (Natural Habitats etc) Regulations 1994 as amended by the Conservation (Natural Habitats, etc Amendment Regulations 1997)
- Construction (Design and Management) Regulations 1994
- Construction (Health, Safety and Welfare) Regulations 1996
- Control of Substances Hazardous to Health Regulations
- Deregulation (Pipelines) Order 1999
- Electricity at Work Regulations 1989
- Foot and Mouth Disease Order 1983 as amended
- Gas Safety (Management) Regulations 1996 (and associated Guidance L80)
- Health and Safety Information for employees Regulations 1996
- Health and Safety (Safety Signs and Signals) Regulations 1996
- Hedgerows Regulations 1997
- Ionising Radiation Regulations 1999

- Management of Health and Safety at Work Regulations 1999 (and associated Code of Practice L21)
- Manual Handling Operations Regulations 1992
- Noise at Work Regulations 1989 SI 1989
- Personal Protective Equipment at Work Regulations 1992
- Pipelines Safety Regulations 1996 (and associated Guidance L82)
- Pipeline Works (Environmental Impact Assessment) Regulations 2000
- Pressure Systems Safety Regulations 2000 (and associated ACoP L122 and Guidance HS(R)30)
- Provision and Use of Work Equipment Regulations 1993
- Public Gas Transporter Pipeline Works (Environmental Impact Assessment) Regulations 1999
- Reporting of Injuries, Disease and Dangerous Occurrences Regulations (RIDDOR) 1995 (and associated Guidance L73)
- Town and Country Planning (Environmental Impact Assessment) (England and Wales) Regulations 1999
- Town and Country Planning Act (General Permitted Development) Order 1995.

A2.2 **EUROPEAN LEGISLATION**

- EC Directive 97/11/EC on assessing effects of projects on the environment
- EC Directive 79/409/EEC on the conservation of birds
- EC Directive 92/43/EEC on the conservation of natural habitats of wild fauna and flora

A2.3 **HSE ACOPs and GUIDANCE**

- HSE Reducing Risks, Protecting People
HSE Discussion document
DDE11 CISO 5/99
- HSE Tolerability of risk from nuclear power stations
- HSE Risk Criteria for Land Use Planning in the Vicinity of Major Hazard Installations 1998
- HS(G)47 Avoidance of danger from underground services
- HS(G)48 Human factors in industrial safety
- HS(G)65 Successful health and safety management 1997
- HS(G)253 Safe isolation of plant
- HS(GS)6 Avoidance of danger from over head electric lines
- HSE ACMH3 The Control of Major Hazards. HMSO, 1984
- HSE-IND(GI) 163L Five steps to risk assessment.

A2.4

BRITISH STANDARDS (abbreviated titles)

- BS 21 Pipe threads for tubes and fittings
- BS 143 & 1256 Threaded pipe fittings in malleable cast iron and cast copper alloy
- BS 593 Laboratory thermometers
- BS 1041 Temperature measurement
- BS 1523-1 Terms used in automatic controlling and regulating systems
- BS 1560 Circular flanges for pipes, valves and fittings
- BS 1640-1 Steel butt-welding pipe fittings (Imperial)
- BS 1640-3 Steel butt-welding pipe fittings (Metric)
- BS 2633 Class 1 arc welding of ferritic steel pipework
- BS 2765 Temperature detecting elements and pockets
- BS 3293 Carbon steel pipe flanges (over 24 inches nominal size)
- BS 3799 Steel pipe fittings, screwed and socket-welding
- BS 3900 Methods of test for paints
- BS 4368 Metallic tube connectors. Split collect compression fittings.
- BS 5228 Noise and vibration control
- BS 5493 Protective coating of iron and steel structures against corrosion. Current, obsolescent, superseded. BS EN 12944
- BS 5911 Pre-cast concrete pipes, fittings and ancillary products
- BS 6990 Welding on steel pipelines containing process fluids or residuals
- BS 7361 Cathodic protection
- BS 7671 IEE Wiring Regulations
- BS 7910 Assessing the acceptability of flaws in metallic structures
- BS 8004 Foundations
- BS 8110-1,2 Structural use of concrete
- BS EN 437 Test gases
- BS EN 837-1, 2 Pressure gauges
- BS EN 1127 Explosion prevention and protection
- BS EN 1256 Gas welding equipment
- BS EN 1514 Flanges and their joints
- BS EN 1998 Design of structures for earthquake resistance
- BS EN 1555-3 Polyethylene fittings
- BS EN 1594 Pipelines for MOP over 16 bar
- BS EN 1759 Flanges and their joints
- BS EN 10002 Tensile testing of metallic materials
- BS EN 10028 Flat products of steel
- BS EN 10029 Steel plates for pressure purposes
- BS EN 10045 Charpy testing
- BS EN 10208-2 Steels for pressure purposes, Class B

- BS EN 10216 Seamless tubes
- BS EN 10217 Welded steel tubes
- BS EN 10222 Steel forgings for pressure purposes
- BS EN 10255 Non-alloy steel tubes.
- BS EN 10274 Metallic materials. Drop weight tear test
- BS EN ISO 12944 Corrosion protection of steel structures by protection paint systems
- BS EN 13445 Unfired pressure vessels
- BS EN 23270 Temperature and humidities for conditioning and testing paints etc.
- BS EN 60079 Electrical apparatus for explosive gas atmospheres
- BS EN ISO 2813 Paints and varnishes
- BS EN ISO 5167 Measurement of fluid flow
- BS EN ISO 9001 Quality Management Systems
- PD 5500 Unfired fusion welded pressure vessels.

A2.5 **EUROPEAN STANDARDS (abbreviated titles)**

- EN 1998-4 Design of structures for earthquake resistance
- EN 10045-1 Charpy impact test – Test method (V- and U-notches)
- CEN/TS 15173 Gas supply systems. Frame of reference for PIMs
- CEN/TS 15174 Gas supply systems. Guidelines for safety management systems for Natural Gas transmission pipelines.

A2.6 **INTERNATIONAL STANDARDS (abbreviated titles)**

- ISO 3419
- ISO 3183 Steel pipe for pipelines transportation systems
- ISO 13623 Pipeline transportation systems
- ISO 14313 Pipeline transportation systems. Valves
- ISO/13847 Pipeline transportation systems. Welding
- ISO 15590 Pipeline transportation systems.
- ISO 7005 Metallic flanges.

A2.7 **OTHER STANDARDS (abbreviated titles)**

- AGA 3 Orifice Metering of Natural Gas and other related hydrocarbon fluids
- API 6D Pipeline valves (gate, plug, ball and check valves)
- API 5L Linepipe
- API 5L3 Recommended Practice for Conducting Drop-Weight Tear Tests on Line Pipe
- ANSI/ASME B16.5 Flanges and flange fittings
- ANSI/ASME B16.9 Factory made wrought steel butt/welding fittings
- ANSI/ASME B31.3 Process piping
- ANSI/ASME B16.28 Wrought steel butt/welding elbows and returns
- ANSI/ASME B16.47 Large diameter steel flanges
- ANSI/ASME B31.8 Managing system integrity of pipelines

- ANSI/ASME B31.11 Slurry transportation piping systems
- ASTM A53 Standard Specification for Pipe, Steel, Black and Hot-Dipped, Zinc-Coated, Welded and Seamless
- ASTM A105 Carbon steel forgings for piping applications
- ASTM A106 Seamless carbon steel pipe
- ASTM A234 Piping fittings of wrought carbon steel and alloy steel. High and moderate temperature
- ASTM A312 Austenitic stainless steel pipes
- ASTM A333 Standard Specification for Seamless and Welded Steel Pipe for Low-Temperature Service
- ASTM A420 Piping fittings of wrought carbon steel and alloy steel
- ASTM A671 Standard Specification for Electric-Fusion-Welded Steel Pipe for Atmospheric and Lower Temperatures
- ASTM A672 Standard Specification for Electric-Fusion-Welded Steel Pipe for High-Pressure Service at Moderate Temperatures
- ASTM A860 Wrought high strength, low alloy steel butt welding fittings
- ASTM E1049-85 Standard practices for cycle counting in fatigue analysis
- MSS SP-6 Standard finishes for contact faces of pipe flanges
- MSS SP-44 Steel pipeline flanges
- MSS SP-48 Steel Butt Welding Fittings (26" and larger).
- MSS SP-59 Steel Butt Welding Short Radius Elbows and Returns.
- MSS SP-63 High Strength Wrought Welding Fittings.
- MSS SP-75 High test wrought butt welding fittings.

A2.8

ADVANTICA LTD

Technical specifications (abbreviated titles available from IGEM)

Note: Advantica Ltd standards are not routinely reviewed and updated and, hence, caution is required when referencing them. However, they are relatively modern standards, and their scopes and specifications remain relevant at the time of publication of IGEM/TD/1 Edition 5.

- B4/E Carbon and carbon manganese steel bends 50 mm to 400 mm inclusive nominal size, pressures greater than 7 bar
- B7/E Carbon and carbon manganese steel bends equal to or greater than 450 mm nominal size for operating pressures greater than 7 bar
- B11/E Carbon and carbon manganese steel bends 200 mm nominal size and above produced from pipe by induction bending, at pressures above 7 bar
- E17/E Part 1 Insulation joints – Joints equal to or greater than 80 mm nominal size, pressures greater than 7 bar for class ratings 150, 300 and 600
- E17/E Part 3 Insulation joints – Joints less than 80 mm nominal size, pressures greater than 7 bar for class rating 150, 300 and 600
- F1/E Carbon and carbon manganese steel forgings and forged components, pressures greater than 7 bar

- F3/E Carbon and carbon manganese steel reducers 50 mm to 1050 mm inclusive nominal size, pressures greater than 7 bar
- F8/E Carbon and carbon manganese steel butt welding end caps
- L1/E Seamless line pipe 40 mm to 100 mm inclusive nominal size, pressures greater than 7 bar
- LX1/E Submerged-arc welded pipe 400 mm to 1400 mm inclusive nominal size, pressures greater than 7 bar
- LX4/E Seamless pipe 150 mm to 450 mm inclusive nominal size, pressures greater than 7 bar
- LX5/E Electric-welded pipe 150 mm to 450 mm inclusive nominal size, pressures greater than 7 bar
- T1/E Carbon and carbon manganese steel tees equal to or greater than 450 mm nominal size, pressures greater than 7 bar
- T2/E Carbon and carbon manganese steel tees 50 mm to 450 mm inclusive nominal size, pressures greater than 7 bar
- V6/E Part 1 Steel valves for use with natural gas, pressures above 7 bar, 100 mm nominal size and above
- V6/E Part 2 Steel valves for use with natural gas, pressures above 7 bar, 80 mm nominal size and below.

Technical procedure

- WP1/E Procedure for weldability testing of pipe fittings for service at pressures above 7 bar.

Data sheet

- DAT6/E Carbon and carbon manganese steel pipe. pressures greater than 7 bar.

A2.9

MISCELLANEOUS

- Oil Industry Advisory Committee – Guidance on permit to work systems in the petroleum industry. HSE Books 1997 ISBN 0 7176 1281 3
- Oil Industry Advisory Committee – Guidance on the safe isolation of plant and equipment. HSE Books 1997 ISBN 0 7176 0871 9
- ASME B31G – 1991, Manual for determining the remaining strength of corroded pipelines
- EEMUA Pub. 185:1996, Guide for hot tapping on piping and other equipment
- EEMUA Pub 153:1995, Chemical plant and petroleum refinery piping
- EA and SEPA Pollution Prevention Guidelines.

A2.10

IGEM

- IGE/TD/3 Steel and PE pipelines for gas distribution
Edition 4
- IGE/TD/4 PE and steel gas services and service pipework
Edition 4
- IGE/TD/12 Pipework stress analysis for gas industry plant
Edition 2
- IGE/TD/13 Pressure regulating installations for transmission and distribution systems

- IGE/GL/5
Edition 2 Managing new works, modifications and repairs
- IGE/SR/18
Edition 2 Safe working practices to ensure the integrity of gas pipelines and associated installations
- IGE/SR/20
Edition 2 Dealing with reported gas escapes
- IGE/SR/22 Purging operations for fuel gases in transmission, distribution and storage
- IGE/SR/23 Venting of Natural Gas
- IGE/SR/24 Risk assessment techniques
- IGE/SR/25 Hazardous area classification of Natural Gas installations
- IGE/GM/4
Edition 2 Flowmetering practices. Inlet pressure exceeding 38 bar and not exceeding 100 bar
- IGE/GM/5
Edition 2 Selection, installation and use of electronic gas meter volume conversion systems
- IGE/GM/6 Specification for low pressure diaphragm and rotary displacement meter installations with badged meter capacities exceeding 6 m³/h (212 ft³/h) but not exceeding 1076 m³/h (38000 ft³/h)
- IGE/GM/7
Edition 2 Electrical connections and hazardous area classification for gas metering equipment
- IGE/GM/8 Non-domestic meter installations. Flow rate exceeding 6 m³ h⁻¹ and inlet pressure not exceeding 38 bar.

APPENDIX 3 : RISK ASSESSMENT TECHNIQUES

A3.1 INTRODUCTION

A3.1.1 This appendix provides guidance on the techniques and criteria used for the assessment of risk in connection with the evaluation of pipeline safety.

The guidance outlines how to assess both the frequency of pipeline failure during service and the harm done to the surrounding population as a result of any failure. Consideration is given to both individual and societal risk together with other factors such as cost benefit analysis and the need, in the UK, to satisfy the principle of ALARP.

A3.1.2 A range of methodologies had been developed to assess the frequency and consequences of gas pipeline failure. Largely, these are company-based and, consequently, their level of sophistication reflects the needs of the company and the information available to the company. Similarly, various methods have been developed to present risk information and these are reflected in the range of acceptance criteria developed.

A3.1.3 The guidance aims to ensure that, whichever methodology and criteria are adopted, the outcome of any assessment will achieve a consistent level of safety. However, the validity of any procedure and methodology adopted needs to be capable of being demonstrated to the relevant statutory body for which a quantified risk assessment (QRA) normally will be required.

A3.1.4 Some assessments are carried out in order to assist management of safety and the discharging of general legal duties. However, most assessments are carried out to satisfy specific requirements of health and safety legislation and there may be a need for the results to be reviewed by the relevant statutory body. In the latter case, a QRA normally will be required. For this reason, risk criteria data extracted from current HSE publications are incorporated into this appendix for guidance.

A3.2 ASSESSMENT FRAMEWORK

A full risk assessment involves estimation of the frequency and consequences of a range of hazard scenarios and of the individual and societal risk associated with them. Although several different methodologies may be available for each stage of the assessment, each assessment has the following basic steps:

- collect data and define cases to be assessed
- identify all credible failures
- evaluation failure frequencies
- evaluate consequences of failure
- evaluate individual and societal risk
- assess the acceptability/tolerability of the risks
- implement any new mitigation measures required as a result of the assessment
- record and review results.

While these steps are listed in order, there may be significant overlap in their execution. Each of them is described in detail below.

A3.2.1 **Collect data and define case to be assessed**

A3.2.1.1 The first stage of any assessment involves collection of all of the necessary data. Consider the pipeline, the surrounding infrastructure and, in some cases, the local meteorology.

A3.2.1.2 Include in the pipeline data, details of:

- geometry
- operating conditions
- gas properties
- pipeline system behaviour
- time to achieve shutdown
- material properties
- control measures
- any mitigation measures against third party interference, for example slabbing, depth of cover, marker tape, etc.

Also, consider the damage and maintenance history of the pipeline for in-service assessments or, if possible, the histories of similar pipelines for new design.

A3.2.1.3 Include in the infrastructure data, details of:

- location
- occupancy
- pattern of use of all occupied buildings and surroundings within the hazard range of the worst credible failure (see A3.2.2). Data may be needed for consideration of escape from buildings and shelter provided by them. In the UK, sensitive locations (see Appendix 1) need to be identified since these may be subject to more onerous assumptions or criteria.

A3.2.1.4 Collect details of any major road, rail or other traffic flows for the assessment of crossings and in other circumstances where traffic is a necessary consideration.

A3.2.1.5 When needed, include in the meteorological data details of wind strength, direction and atmospheric stability.

A3.2.1.6 Define the extent of the infrastructure and length of pipe to be assessed using the above data.

A3.2.2 **Determine credible failures**

A3.2.2.1 Consider all possible causes and potential modes of failure throughout the life of the pipeline, including but not limited to:

- external damage
- internal and external corrosion
- seam weld defects
- circumferential butt/girth weld defects
- SCC
- fatigue
- ground movement
- material problems
- extreme natural causes – earthquake, flood and lightning
- valve or fitting defect
- operational error

- design error
- construction defect
- combinations of the above.

A3.2.3 **Evaluate failure frequencies**

A3.2.3.1 Address each of these causes in terms of their likelihood of occurrence. Include in the assessment any cause of failure considered credible. Assess the various failure rates after which the contribution to risk will become apparent. Frequencies of occurrence may be obtained from company-specific databases, from published data sources such as UKOPA, EGIG, NTSB or CONCAWE or from models based on damage data and failure behaviour. Whichever source is chosen, take care to ensure that the data used is relevant to the pipeline being assessed and does not lead to an underestimation of the failure frequency.

Aim to obtain cautious best estimates of the frequency (the greater the uncertainty, the greater the caution which will be required). It may be necessary to adapt the data to allow for higher likelihoods of certain types of failure in some situations. Allowance may be made for mitigation measures (A3.2.7).

A3.2.3.2 Consider all modes of failure including:

- full bore rupture
- major leaks
- minor leaks
- pin hole leaks.

A3.2.4 **Evaluate consequences of failure**

Consider the nature of the gas release. For example, will the release lead to a vertical plume, a free jet (at what angle) or an impacted jet, and will the gas ignite? The aim is to define an event tree with an overall frequency of occurrence for each failure mode and type of gas release.

A3.2.5 **Estimate individual and societal risk**

This is the most complex stage of the procedure. Consider each credible failure mode and type of gas release identified and the sum estimated risk in the appropriate manner to give overall figures. Take account of the distributed nature of the hazard. For any particular location, this means assessing the effects of failure at a number of positions along the length of pipeline within which failures could affect the infrastructure being considered (interaction length). Sum the risk at each position to give an overall distribution. A typical procedure (see Figure 16) is described by the following list of actions:

1. Choose failure mode and type of release
2. Estimate rate of gas release
3. Estimate thermal radiation distribution resulting from gas released and ignited
4. Choose a failure position within the length of pipeline being considered
5. Estimate the effects of radiation on buildings and people and sum risk (see Figure 16)
6. Repeat steps 4-5 for all failure positions considered.

In the UK, the criteria adopted has to satisfy ALARP and its application will need to take account of:

- simple aversion
- company values
- societal concerns.

A common method of presenting societal risk is by means of an F-N diagram. A schematic example is given in Figure 19. This is a graph of the frequency F (usually per year) of events causing N or more fatalities. Criteria are often set by dividing the domain of the graph into two or more regions. These divisions take the form of a line separating an unacceptable area (high risk) from the area where risks may be tolerated and/or a line defining an envelope within which the risks are sufficiently low as to be considered “negligible” or at least “acceptable”. The societal risks calculated for the proposed pipeline are superimposed upon the risk criteria diagram to demonstrate compliance, or to identify the events for which the frequency is to be reduced.

It is essential when using such diagrams that both the criteria and the assessment data are derived using the same methodology and procedure and conform to the same case length.

Figure 19 provides a sample of an actual FN criterion based upon extensive application of previous editions of these Recommendations, to pipeline systems, for a case length of 1.6 km. The enclosed area defines the envelope within which the risks are sufficiently low as to be considered “negligible” or at least “acceptable”. ALARP consideration would, normally, be given to risks which are close to the envelope or outside the envelope.

Where no risk criteria have been defined, compare the predicted risks with risks for pipelines which conform to the design requirements of these Recommendations and are considered to be of acceptable design. However, the methodology and procedure used to assess risk for the pipeline being assessed has to be the same as the methodology and procedure used to assess the pipelines to which it is being compared.

A3.2.6.3 *Cost benefit analysis (CBA)*

When the individual risk is assessed to be in the tolerable region and/or the societal risk is outside the acceptable region, carry out a Cost Benefit Analysis (CBA) to evaluate whether the risk is ALARP (see example in A3.2.8). CBA needs to consider the range of mitigation measures available, their costs, and any savings in costs made by the operator as a result of introducing the mitigation measures and a cost for death or injuries.

A3.2.7 **Implementing new mitigation measures**

Implement any risk mitigation measures which are identified as being necessary, as a result of an assessment of proposed changes to pipeline design or operating conditions, before or when the changes to design or operating conditions are made.

Implement any risk mitigation measures identified as being necessary as a result of assessment of changes to the surrounding infrastructure within a reasonable time scale.

In some cases, the risk mitigation measures may have been agreed with, or introduced at the request of, the statutory body.

A3.2.8 Record and review results

Produce a report detailing each risk assessment to include all relevant details of the pipeline and surroundings. Retain it for the life of each pipeline. Incorporate a clear plan of all buildings and other relevant infrastructure showing locations of these in relation to the pipeline.

Incorporate reference to all data sources and software used in the assessment and record all failure causes, modes and types of release assessed together with any assumptions made. Results of the assessment need to be stated clearly together with any conclusions and recommendations.

Reaffirm the results of any assessment at regular intervals. Normally, this is carried out as part of the affirmation of MOP (see clause 11.4.2).

A3.2.9 Risk assessment of sleeving

Perform a risk assessment of any sleeve to identify and account for each mechanism which could cause failure of the carrier pipe within the sleeve and identify the consequences of failure.

Failure mechanisms to identify include:

- construction defects
- corrosion
- external interference
- ground movement.

For each mechanism, relevant mitigating factors such as surveillance, CP, maintenance, and condition monitoring should be taken into account, when evaluating the probability of failure.

A3.2.10 Sample individual risk calculation

All persons within the hazard range of a pipeline will be subjected to some level of individual risk.

Suppose that a particular pipeline is predicted to rupture at a frequency of f per km per year and there is a probability of p_i that the gas released will ignite. If a person at a distance y from a rupture in the pipeline has a probability of p_{cy} of becoming a casualty, and this probability can be assumed to be correct for a length of the pipeline dx , their individual risk per year from rupture in this particular length of pipe will be:

$$\delta x f p_i p_{cx}$$

The overall individual risk, from this failure mode, for someone at this distance from the pipe, is obtained by summing the results of this equation over the length of pipe in which failures will interact with the person (interaction length). The summation takes account of the variation in casualty probability from a maximum value when the failure is at the closest point to the person to zero when the failure is at the interaction limit. It may also need to take account of any changes in failure frequency along the pipeline.

$$\text{Individual Risk} = \delta x p_i [f p_{cx}]_1 + (f p_{cx})_2 + \dots (f p_{cx})_I$$

The overall individual risk for all failure modes and types of release will be a summation of the risk resulting from each. By repeating the calculation for a range of distances from the pipeline, it becomes possible to construct a risk transect for the pipeline (see Figure 20).

A3.2.11 **Sample cost per life saved calculation**

The usual aim of a cost per life saved calculation is to provide information to assist in a judgement on whether possible measures to reduce risk should be taken, or whether the cost of such measures would be grossly disproportionate to the reduction in risk achieved.

Suppose that rupture of a particular section of pipeline is predicted to result in N fatalities at a frequency of f_i per year. A new control measure costing C is proposed and is expected to reduce the frequency of this number of casualties to f_2 per year. If the remaining lifetime of the proposed measure is expected to be L years, the inferred cost per life saved will be:

$$C (\text{LN } (f_i - f_w))^{-1}$$

Note: C could be a one-off cost for the installation of a protective measure such as slabbing or it could be a summation of the cost over the remaining life of the pipeline of an operational measure such as increased surveillance.

Example

Rupture of this particular section of pipeline is predicted to result in 20 fatalities at a frequency of 3×10^{-6} per year and 250 m of the pipeline is slabbed at a cost of £200 per metre resulting in a reduction of the frequency to 1×10^{-7} . If the remaining life of the pipeline is 40 years and the slabs are expected to remain in place for this time, the inferred cost per life saved is:

$$10^7(200 \times 250)/[40 \times 20(30 - 1)] = \text{£}21.55\text{M}$$

Because of the distributed nature of the hazard associated with pipelines, it is usual for a pipeline risk assessment to result in a range of casualties at a range of frequencies. Therefore, in general, it is necessary to sum the effect of the control measure over the whole range to obtain an overall figure. In this case, the inferred cost per life saved is:

$$C (\sum(\text{LN } (f_1 - f_2)_N))^{-1}.$$

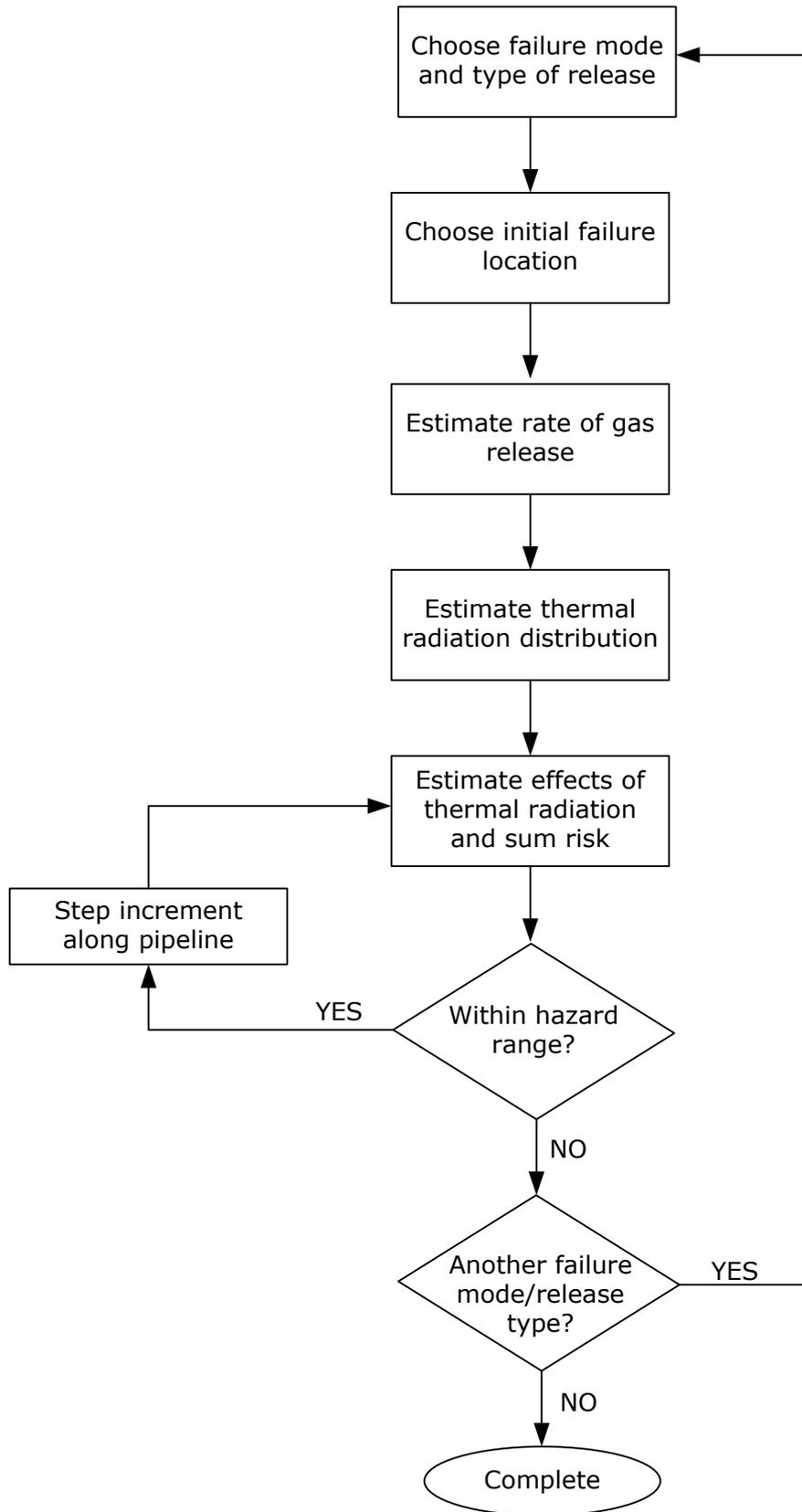


FIGURE 16 - ESTIMATION OF INDIVIDUAL AND SOCIETAL RISK

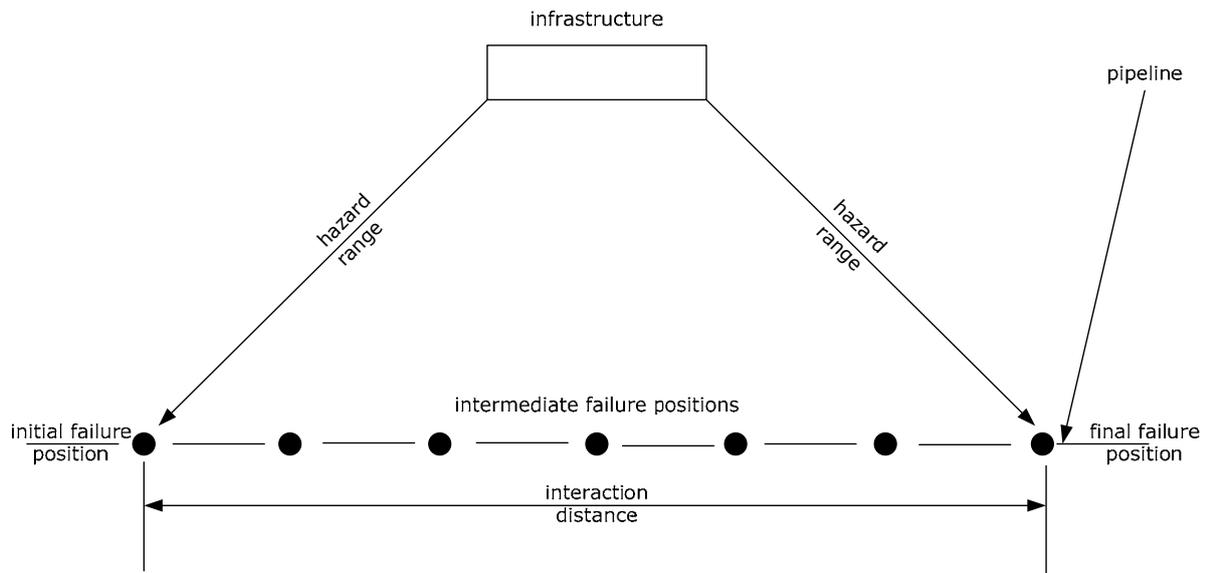


FIGURE 17 - SOCIETAL RISK

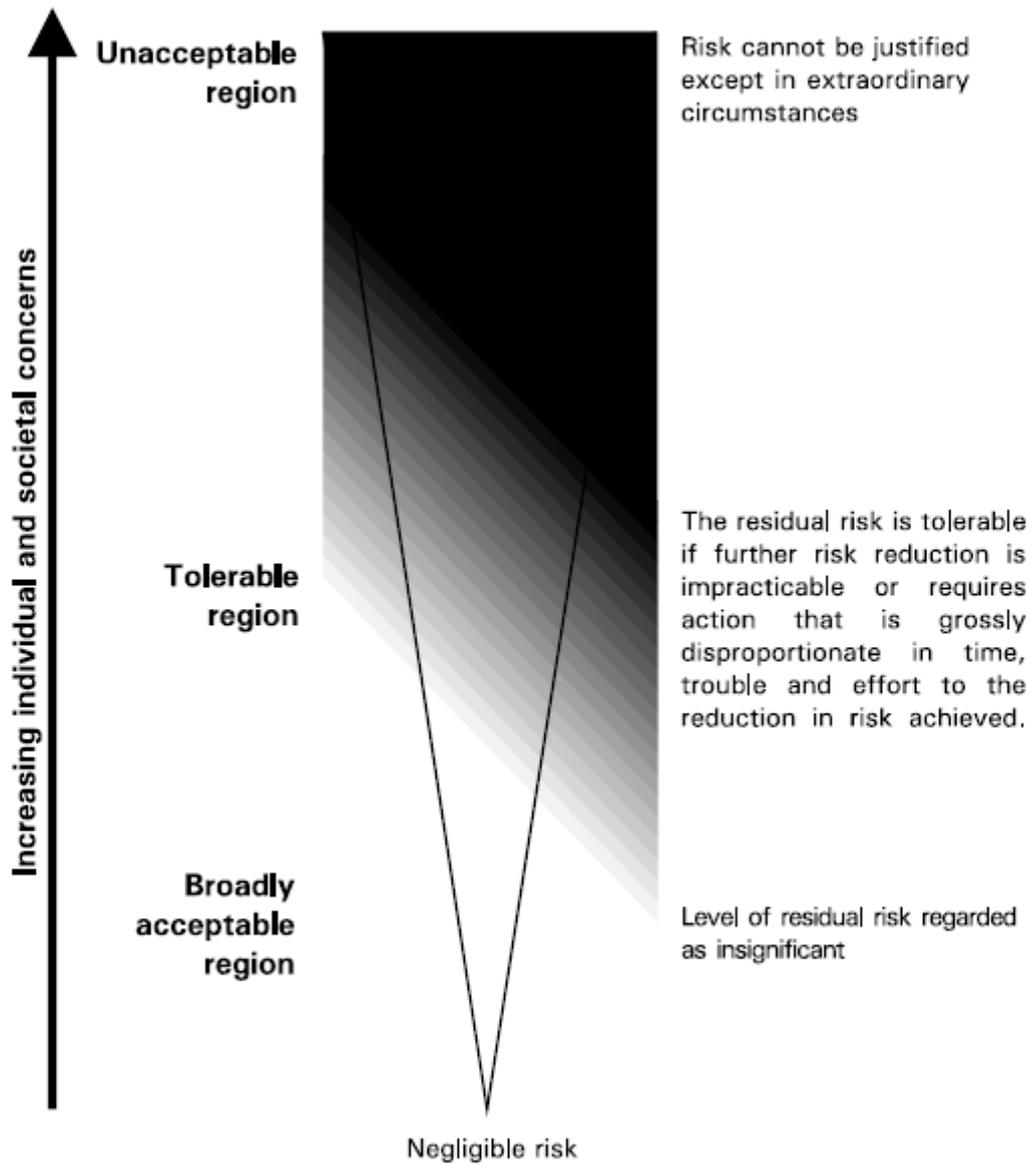


FIGURE 18 – TOLERABILITY OF RISK

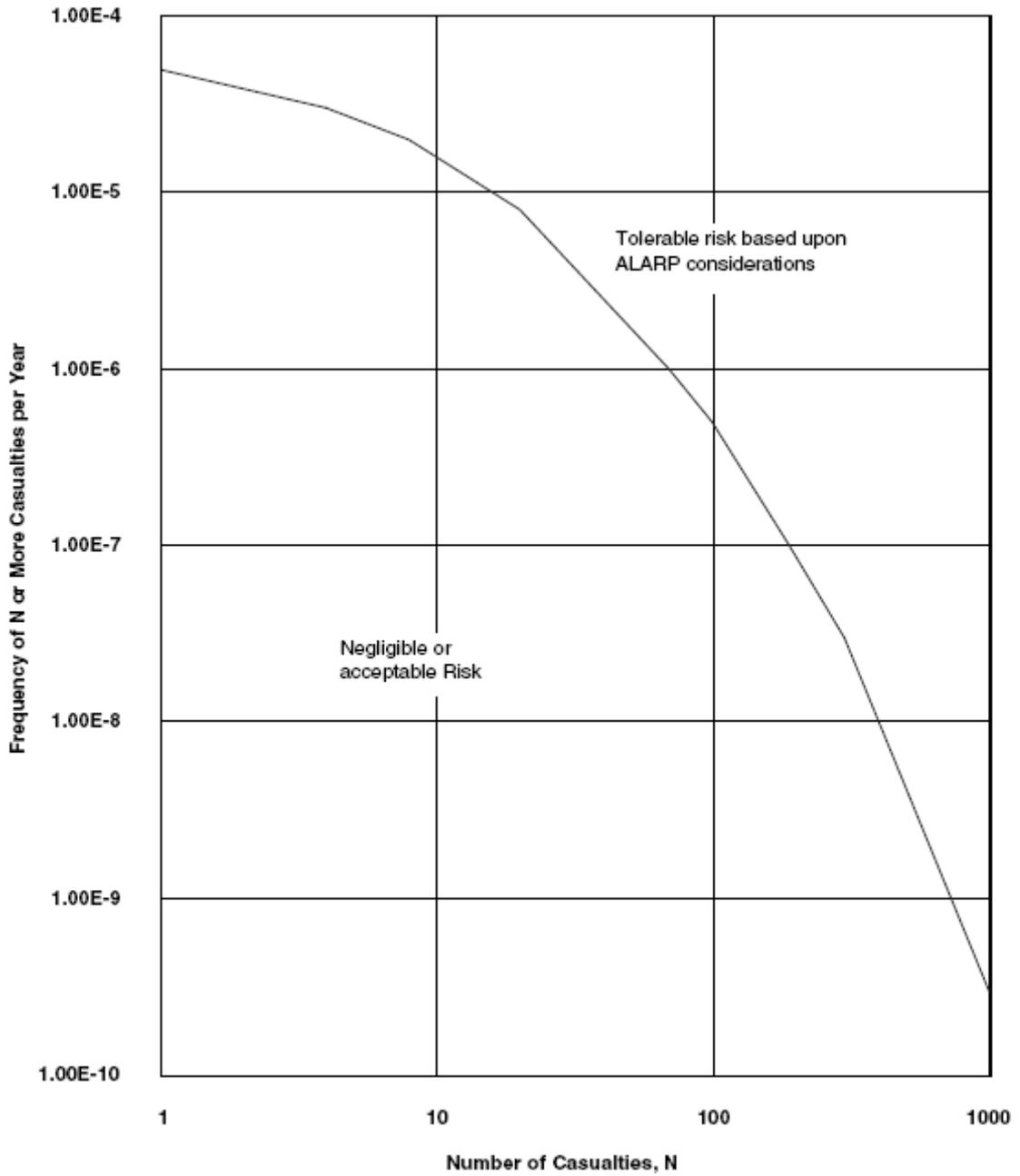


FIGURE 19 - SAMPLE FN CRITERION (BASED ON EXTENSIVE APPLICATION OF PREVIOUS EDITIONS OF IGEN/TD/1)

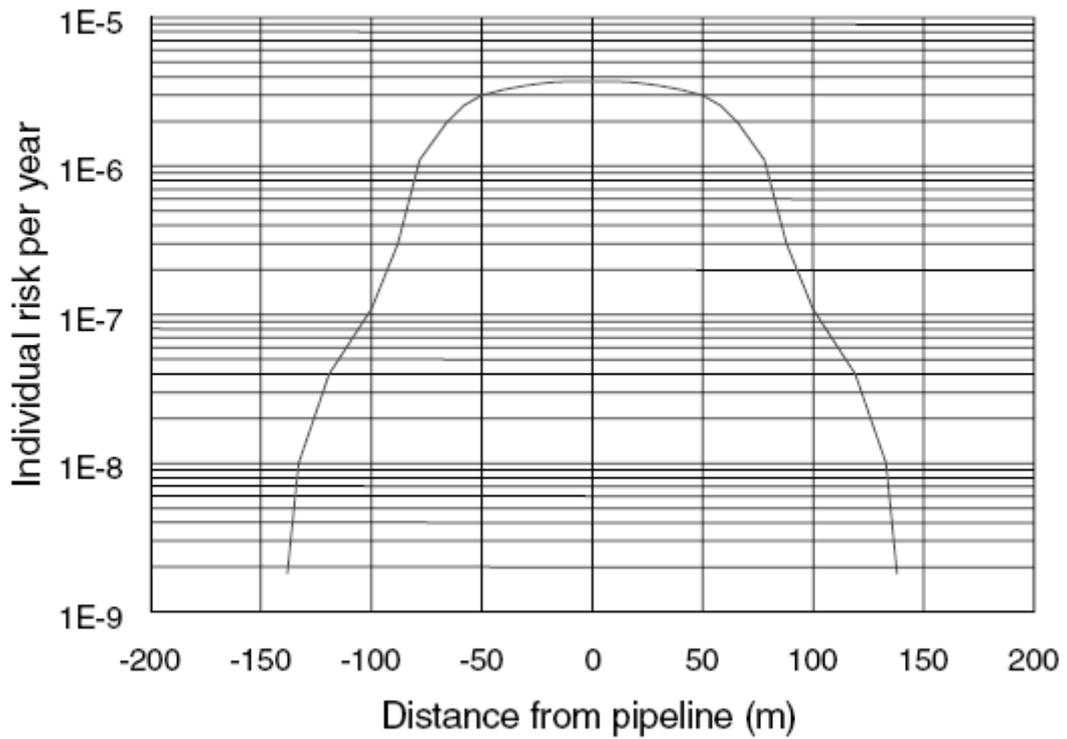
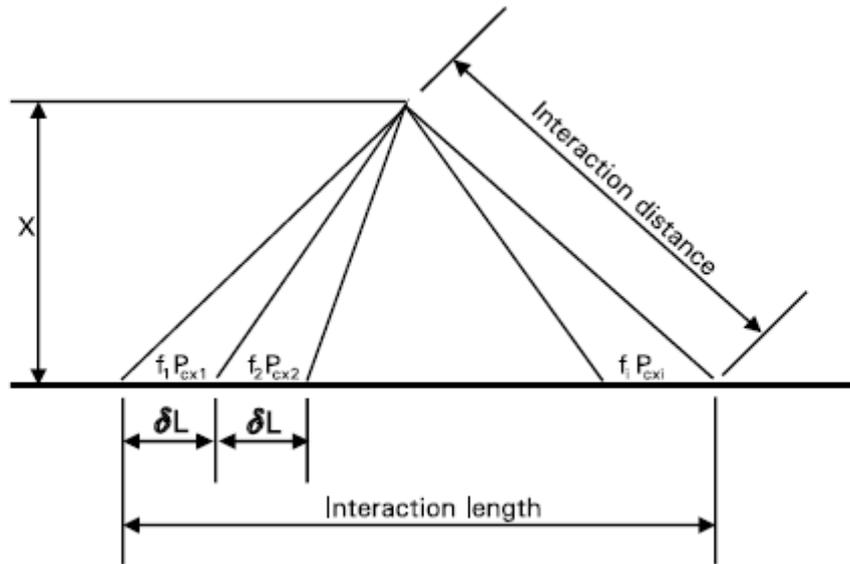


FIGURE 20 - INDIVIDUAL RISK TRANSECT

APPENDIX 4 : STRUCTURAL RELIABILITY ASSESSMENTS (SRAs)

A4.1 GENERAL

This appendix explains how to assess the possibility and frequency of pipeline failure during service using a Structural Reliability Analysis (SRA) approach. The consequences, for example for the surrounding population, as a result of failure, needs to be assessed in terms of individual risk, societal risk and cost benefit analysis. In the UK, this involves satisfying the principle of ALARP. Guidance on risk analysis is provided in Appendix 3.

The SRA approach in this appendix is applicable where it is the intention to operate a pipeline at a design factor exceeding 0.72, but not exceeding 0.80. This design factor is, subsequently, referred to as the "Higher Design Factor".

A4.2 STRUCTURAL RELIABILITY STUDIES

A4.2.1 Study process

A4.2.1.1 The assessment will need to demonstrate that the increase in failure probability of the pipeline as a result of operating at the Higher Design Factor, compared with 0.72, is acceptable. Include the following elements:

- identification of all credible failure mechanism, based on consideration of all the loads the pipeline is likely to see and the ability of the pipeline to resist those loads
- assessment of the proportionate increase in failure probability when operating at the Higher Design Factor rather than 0.72, for each failure mechanism
- assessment of whether the absolute value of failure probability from a particular failure mechanism at the Higher Design Factor is a significant contributor to the overall pipeline failure probability. This applies for each failure mechanism for which the proportionate increased in failure probability is significant.

A4.2.1.2 Significant proportional increases in failure probability, identified for a specific mechanism, are acceptable only if the relevant mechanisms do not contribute significantly to the overall failure probability at the Higher Design Factor. Hence, the overall failure probability, compared with that for a 0.72 design factor, would be significant.

A4.2.1.3 Interpret a "significant" increase in failure probability with due consideration being given to the absolute value of failure probability and the risk associated with any such failure.

A4.2.2 Failure mechanisms

A4.2.2.1 Consider any credible failure mechanism for a particular pipeline. Include the following loads and modifications to the resistance of the pipeline or justify exclusion:

- loads
 - internal pressure
 - axial loads, for example, thermal or due to soil interactions
 - geometric stress concentrations at seam welds
 - stress concentrations at fittings
- resistance
 - distribution of steel properties, diameter, wall thickness
 - defects in the pipe due to:
 - external impact

- corrosion
- construction defects
- fatigue
- stress corrosion cracking.

A4.2.2.2 Consider identifying any other loads or resistance affecting failure mechanisms, which may be relevant to the specific pipeline under consideration.

A4.2.3 **Failure models**

Validate the failure models used in the assessments described in A4.2.2 against experience in that part of their range for which evidence is available.

In addition, ensure the predictions of models are in keeping with best understanding of the physical processes involved in display stability, i.e. give answers which do not change disproportionately to a small change in input parameters over the entire range of interest. Ensure that changes in the input data within the actual error bounds do not result in significant changes to the predictions made by models.

A4.2.4 **Data for Structural Reliability Analysis**

A4.2.4.1 Use one of the following two forms of input data for SRA:

- absolute values (either specified worst cases or actual worst cases where sufficient data is available to establish the actual value with high confidence) or
- distributions of measured values.

A4.2.4.2 Where distributions of measured values are used, ensure the assessment performed allows for any uncertainty in the modelling of those distributions.

A4.3 **WALL THICKNESS, MATERIALS STRENGTH AND GRADES OF LINEPIPE**

Structural reliability based methods require as inputs either:

- minimum values of wall thickness and material strength and grades of linepipe or
- probability density functions describing the actual variation in wall thickness and material strength and grades based on measured data, for example from mill certificates.

Note: The use of probability density functions will lead to increased accuracy in the prediction of failure probabilities. However, the benefits achieved through an increase in accuracy may be swamped by the effect of the probability density functions describing variation in possible damage to the pipeline, since the defect distribution is likely to have far wider confidence limits than those for wall thickness and strength will be limited.

A4.4 **FATIGUE**

A4.4.1 **General**

A4.4.1.1 Calculate the probability of failure due to fatigue by a fracture mechanics analysis using the general method of BS 7910. Take particular care to ensure that input data for this calculation is fully justified and the assumptions documented.

A4.4.1.2 Consider fatigue for fittings and other areas with non-standard stresses as well as for the basic pipeline geometry.

A4.4.2 **Initial defect size**

Assume for the fatigue analysis performed, either:

- initial defect sizes based on defect length/depth combinations which would just have survived the hydrostatic test, taking into account appropriate material properties and manufacturing processes, or
- a distribution of initial defect sizes based on actual size measurements.

A4.4.3 **Stress cycles**

A4.4.3.1 Base the analysis of the cyclic loading on either:

- conservative assessments of the stress range which the pipeline would experience in a worst-case day, or
- actual measured variations in pipeline stress, converted to equivalent stress ranges using an established cycle-counting routine, for example the rainflow method or the reservoir method.

A4.4.3.2 Apply the assessed cyclic loading for every day of the pipeline's service from commissioning.

A4.4.3.3 For uprating, establish the effect on the future cyclic loading of the pipeline and this modified loading applied for the design life of the pipeline following uprating.

A4.5 **FIELD BENDING**

Include in the assessments described in A4.2 consideration of any stress concentration effects at field bends.

A4.6 **TESTING OF PIPELINES**

When assessing the acceptability of operating at Higher Design Factor, using structural reliability based techniques (see A4.2), consider the hydrostatic test level and its relationship to MOP.

Note: The primary function of the hydrostatic test is to reveal construction defects that could lead to failure of the pipeline during the lifetime of the pipeline. Without the hydrostatic test, such failures could occur during the first gaseous pressure raising (gross construction defects) or at some time in the future due to pressure cycling and associated fatigue crack growth.

The assurance given by the linepipe specification and effective quality assurance procedures regarding the material grade and wall thickness is sufficient to ensure that there are no defects which would affect the integrity of the pipeline.

The SRA (as described in A4.2) will have taken account of the effect of the hydrostatic test on the probability of failure due to damage associated with in-service processes such as corrosion and external impact. In situations where the probability of failure is dominated by these types of damage, the optimum mitigation method is to carry out high resolution internal inspection.

A4.7 **OVERPRESSURE**

In the assessments described in A4.2, assume that the pressure in the pipeline may rise to the overpressure limit defined in Sub-Section 12.7 for up to 20 hours in any year.

A4.8 **DEPTH OF COVER**

In the assessment of external impact failure probability given in A4.2, take account of either the minimum depth of cover (which for new-build pipelines may be equal to or greater than the 1.1 m identified in clause 8.15.1) or the

distribution of actual depths of cover along the pipeline, and the predicted effect of this on the probability of impact damage.

APPENDIX 5 : PRESSURE TESTING PROCEDURES

A5.1 TESTING PROCEDURE – GENERAL

A5.1.1 Ensure all test equipment is designed for an operating pressure of not less than the specified test pressure.

A5.1.2 Hydrostatically strength test and pneumatically leak test installations, before putting into service.

Note: Sections of the installation may require hydrostatic testing at different pressure levels, according to their design pressures.

A5.1.3 If any components or sub-assemblies are to be omitted from a hydrostatic test, test them separately to an equivalent standard.

Note: When the components or sub-assemblies are subsequently installed to the main installation, it is not necessary to repeat the hydrostatic test for the whole installation provided that:

(a) All welded tie-ins are subjected to full NDT inspection, to a standard at least equivalent to that applied to the main installation.

(b) All tie-in connections are carefully inspected for leaks during the pneumatic leak test (installation tests only).

A5.1.4 Backfill below-ground welded pipework and fittings prior to hydrostatic testing to minimise the risk of subsequent post-test damage.

Expose all screwed, bolted or other connections prone to leakage, such as valve spindles and the like, for inspection during the test procedure.

A5.1.5 Blow through small fabrications and check to ensure freedom from blockage and that all foreign matter has been removed.

A5.1.6 Remove any instrumentation or other equipment, which may be damaged during the test procedure and plug the pipework as necessary.

A5.1.7 Measure the volume of water, injected during pressurisation, either by direct measurement or inference from the count of the strokes of a calibrated pump.

A5.2 TESTING PROCEDURE – PIPELINES DESIGNED TO OPERATE AT A DESIGN FACTOR EXCEEDING 0.3

A5.2.1 Raise the pressure in the test section at a controlled rate.

A5.2.2 Record the rise in pressure measured by the dead weight tester and the volume of water injected.

Use a calibrated tank to make spot checks of the volume injected during pressurisation.

A5.2.3 Commence a pressure and temperature record, by chart or digital recorder, and continue for the duration of the test.

A5.2.4 During preliminary pressurisation, adjust the rate of pressure increase to give a maximum pressure rise of 1 bar/minute.

A5.2.5 Carry out a graphical air inclusion plot of pressure against volume (P/V plot) from static head pressure to determine the residual air content of the test section. To ensure accuracy, make the plot to 50% of the design pressure.

Determine the volume of air by extrapolation of the linear portion of the graph.

A5.2.6 Raise the pressure in the test section to such a level as to give a corresponding design factor of 0.65.

A5.2.7 Investigate the cause of any significant pressure losses. In the absence of any significant pressure loss, commence a separate graphical P/V plot. This P/V plot represents a stress/strain graph of the test section steel.

A5.2.8 At the commencement of the second P/V plot, determine the volume of water required to raise the pressure by bar. During subsequent pressurisation, check this value frequently to observe any deviation.

A5.2.9 Continue pressurisation until the lesser of the following is reached (this pressure is known as the Limiting Pressure):

- the required maximum test pressure in the test section, as stated in the procedure certificate or,
- the pressure at which twice the volume of water determined at the start of the P/V plot is required to give 1 bar increase in pressure. This effect is, usually, referred to as "double stroking" or "half sloping".

A5.2.10 If, for any reason during pressurisation, the safety of the test is in doubt, suspend the test pending an investigation.

Where half slope occurs before the required maximum test pressure, stop the test for investigation, to include a detailed check of the test procedure and a calibration check of measuring equipment, followed by a check on the pipe mechanical properties.

A5.2.11 When the limiting pressure is reached, stop the pressurising pump and isolate the test section, record the temperature of the test section and cease the P/V plot.

A5.2.12 At the completion of the P/V plot, compare the actual curve with the theoretical elastic line on the P/V plot. If the slopes differ by more than 10%, investigate to determine the cause.

A5.2.13 The test section pipework will continue to yield. Plot the resulting drop in pressure together with the temperature at 10 minute intervals over a 2 hour period, known as the "decay period", on the same x-y axis.

A5.2.14 At the end of the 2 hour decay period, make an assessment as to whether the test section is leak free and if the test procedure may continue.

A5.2.15 If a pressure drop is still observed in subsequent 10 minute intervals, continue the decay period record to help establish the condition of the pipeline.

A5.2.16 If a leak is suspected, reduce the pressure to not more than the design pressure of the test section prior to encroaching within the safety distance, for the purpose of visual examination.

A5.2.17 Continue the test for 24 hours from attaining the limiting pressure. If, for any reason, the test pressure has to be reduced other than for bleed-off of excess pressure, extend the duration of the test by an equivalent period.

A5.2.18 If the test is to continue, re-start the pressurising pump and repressurise the test section to the limiting pressure. Measure and record the quantity of water required to restore the limiting pressure.

- A5.2.19 During the subsequent 22 hours continue to record, the pressure and temperature at half hourly intervals.
- If the pressure drops 1 bar below the limiting pressure, restart the pressurising pump and restored the limiting test pressure.
- Measure and record the quantity of water required on each occasion to restore the pressure to the limiting test pressure and identify on the graphical plot. However, during the last 6 hours of this 22-hour period, no further re-pressurisation will be permitted.
- A5.2.20 If, due to changes in temperature, the pressure rises and exceeds the limiting pressure by 0.4 bar, bleed off the excess pressure and remove, measure and record the quantity of water removed from the test section.
- A5.2.21 During the last 3 hours of the test period, make graphical plots of pressure and temperature, at maximum half-hourly intervals, on the same x-y axis.
- A5.2.22 Decide, from the plot over the last 3 hours, if the test is satisfactory, make pressure corrections, due to variations in temperature (see A5.7).
- A5.2.23 The test may be considered satisfactory if the pressure loss over the last 3 hours of the test period is not greater than 0.2 bar in total.
- A5.2.24 Calculate and record the pressure at the maximum and minimum elevations of the test section from the limiting test pressure.
- A5.2.25 Calculate the design factor at the minimum elevation should be calculated based on the limiting pressure.
- A5.3 **TESTING PROCEDURE – PIPELINES DESIGNED TO OPERATE AT A DESIGN FACTOR NOT EXCEEDING 0.3**
- A5.3.1 Raise the pressure in the test section at a controlled rate.
- A5.3.2 Record the rise in pressure measured by the dead weight tester and the volume of water injected.
- Use a calibrated tank to make spot checks of the volume injected during pressurisation.
- A5.3.3 Commence a pressure and temperature record, by chart or digital recorder, and continue for the duration of the test.
- A5.3.4 During preliminary pressurisation, adjust the rate of pressure increase to give a maximum pressure rise of 1 bar/minute
- A5.3.5 Carry out a graphical air inclusion plot of pressure against volume (P/V plot), from static head pressure, to determine the residual air content of the test section. Make the plot to 50% of the design pressure.
- Determine the volume of air by extrapolation of the linear portion of the graph.
- A5.3.6 Where the P/V plot has not become linear at 50% of the design pressure, it may be continued up to a maximum value of 35 bar or 100% of the design pressure, whichever is the lesser.
- A5.3.7 On completion of the air inclusion plot, commence a separate P/V plot and continue until the test pressure is reached. Stop the pressurising pump and take a preliminary reading from the dead weight tester.

- A5.3.8 If the test pressure cannot be attained, or if half slope on the P/V plot is reached (see A5.2.9), terminate the test and record as a test failure.
- A5.3.9 At the completion of the P/V plot, compare the actual curve with the theoretical elastic line on the P/V plot. If the slopes differ by more than 10%, carry out an investigation to determine the cause.
- A5.3.10 On achieving the test pressure, allow an adequate period for the pressure to stabilise. The duration of the stabilisation period will vary according to physical and ambient factors.
- A5.3.11 At the end of the stabilisation period, restore the test pressure where necessary, and isolate the pressurising pump. Record the volume of water injected or expelled to restore the test pressure.
- A5.3.12 Commence the test period at the restoration of the test pressure and continue for 4 hours.
- A5.3.13 During the 4-hour test period, make graphical plots of pressure and temperature, at maximum half-hourly intervals, on the same x-y axes.
- A5.3.14 If, during the 4-hour test period, the pressure rise and exceeds the test pressure by 0.4 bar, bleed off the excess pressure and expel, measure and record the quantity of water.
- A5.3.15 If, due to temperature variations, the pressure falls 1 bar below the test pressure during the first 3 hours of the test period, restore the test pressure. However, do not allow re-pressurisation during the last hour of the 4 hour test period.
- Measure and record the quantity of water required on each occasion to restore the pressure to the limiting test pressure and identify on the graphical plot.
- A5.3.16 Decide, from the test period pressure and temperature graphs, if the test is acceptable. Make pressure corrections due to variations in temperature (see clause A5.7).
- A5.3.17 The test result is acceptable if there are no significant pressure changes, other than those due to variations in temperature.
- A5.3.18 In the event of an unacceptable pressure loss, reduce the pressure to a value not greater than the design pressure, before any visual examination is carried out.
- A5.3.19 Calculate the design factor at the maximum elevation.

A5.4 **TESTING PROCEDURE INSTALLATIONS**

A5.4.1 **Testing of small fabrications**

- A5.4.1.1 This procedure is intended for small fabrications which readily may be inspected visually and whose volume makes longer term test durations impractical due to the impact of ambient temperature variations.
- A5.4.1.2 A plot of pressure against volume (P/V plot) is not required for this test.
- A5.4.1.3 Raise the test section pressure in a controlled manner to the test pressure and stop the pump.
- A5.4.1.4 Allow the pressure in the test section to stabilise.

The stabilisation period will vary considerably with site conditions, but it is not to be less than 30 minutes.

A5.4.1.5 Once stabilisation has occurred, restore the test pressure if necessary, isolate the pressurising pump, and record the temperature and pressure.

A5.4.1.6 Maintain the test pressure for the test period (not less than 30 minutes).

A5.4.1.7 Investigate any loss in pressure, other than due to variations in temperature, and extend the test period accordingly.

Make pressure corrections due to variations in temperature (see A5.7).

A5.4.1.8 The test result is acceptable if there are no significant pressure changes, other than those due to variations in temperature.

A5.4.1.9 Reduce the test pressure to the design pressure, before any close visual examination takes place.

A5.4.1.10 On completion of testing, release the test pressure in a safe controlled manner.

A5.4.1.11 Produce a test certificate which, together with appropriate drawings detailing the test physical limits and the instrument calibration certificates, will provide the documentation for the test.

A5.4.2 **Testing of installations other than small fabrications**

A5.4.2.1 A plot of pressure against volume (P/V plot) is required for this test.

A5.4.2.2 Record the P/V plot from the rise in pressure measured by the dead weight tester and inject the volume of water.

Use a calibrated tank to make spot checks of the volume injected during pressurisation.

A5.4.2.3 Continuously record ambient temperature and water temperature throughout the test.

A5.4.2.4 Raise the pressure in the test section at a controlled rate.

A5.4.2.5 Commence a pressure and temperature record, by chart or digital recorder, and continue for the duration of the test.

A5.4.2.6 During preliminary pressurisation, adjust the rate of pressure increase to give a maximum pressure rise of 1 bar/minute.

A5.4.2.7 Carry out a graphical air inclusion P/V plot from static head pressure, to determine the residual air content of the test section.

To ensure accuracy, make the plot to 50% of the design pressure before the estimation of residual air volume is made.

Determine the volume of air by extrapolation of the linear portion of the graph (see Sub-Section 8.6).

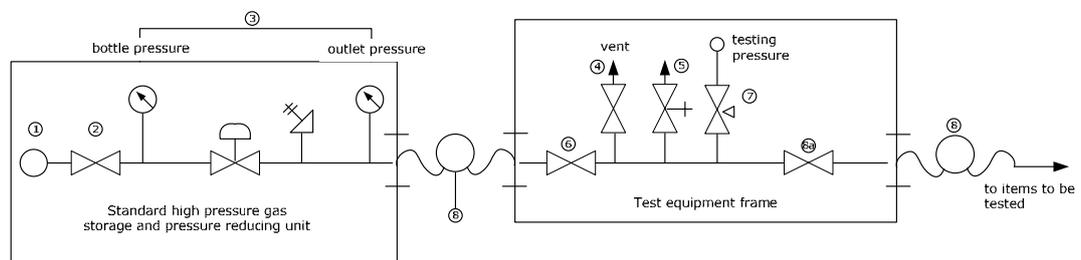
A5.4.2.8 Where the P/V plot has not become linear at 50% of the design pressure, it may be continued up to a maximum value of 35 bar or 100% of the design pressure, whichever is lesser.

A5.4.2.9 On completion of the air inclusion P/V plot, commence a separate P/V plot and continue until the test pressure is reached.

- A5.4.2.10 Compare the actual curve of the P/V plot with the theoretical elastic line.
- Any reduction in the slope of the P/V plot could indicate a leak or yield of a component when stop the pressurising pump and investigate.
- A5.4.2.11 When the test pressure is reached, stop and isolate the pressurising pump and cease the P/V plot.
- A5.4.2.12 Allow an adequate period for the pressure to stabilise, i.e after equalisation of the pipe and water temperature.
- A5.4.2.13 At the end of the stabilisation period, restore the test pressure, where necessary and isolate the pressurising pump.
- Record the volume of water injected or expelled to restore the test pressure.
- A5.4.2.14 Commence the test period at the restoration of the test pressure and continue for a period of not less than 2 hours.
- A5.4.2.15 Take regular readings, maximum 15 minutes interval, of pressure and temperature during the test period and graphically plot against time on the same x-y axes.
- A5.4.2.16 At no time during the test period allow the pressure to rise by more than 5% above the test pressure.
- Bleed off excess pressure and measure and record the quantity of water released for reference when the assessment of the pressure/time plot is made.
- A5.4.2.17 If, during the test period, the pressure falls by more than 10%, due to temperature effects, restore the pressure to the test pressure and maintain the test pressure for a minimum period of 30 minutes.
- A5.4.2.18 Where necessary, make pressure corrections due to variations in temperature (see A5.7).
- A5.4.2.19 The test result is acceptable if there are no significant pressure changes, other than those due to variations in temperature.
- A5.4.2.20 On completion of testing, release the test pressure in a safe controlled manner.
- A5.4.2.21 Produce a test certificate which, together with appropriate drawings detailing the test physical limits and the instrument calibration certificates, will provide the documentation for the test.
- A5.4.3 **Pneumatic leak test**
- A5.4.3.1 As a test medium use clean dry air or nitrogen.
- A5.4.3.2 Apply the test to the assembled installation and include all equipment and associated small bore pipework which may have been removed for the hydrostatic pressure test.
- For installations that include meters, refer to IGE/GM/8.
- A5.4.3.3 Ensure that all valves are in the open position.
- A5.4.3.4 Gradually increase the test pressure to 7 bar.

- A5.4.3.5 Carry out soap solution tests on all connections made after the hydrostatic test to ensure there are no leakages.
- A5.4.3.6 Permit only limited tightening of fittings or the making good of minor leakages while the system is under pressure. Carry out any major remedial work only after the test pressure has been completely released.
- After any leakages have been made good, restore the test pressure and recheck the system for leakage.
- A5.4.3.7 On completion, issue a certificate stating that the installation has been leak tested in accordance with this procedure.
- A5.4.3.8 This test may be combined with the nitrogen purge prior to commissioning.
- A5.5 **TESTING PROCEDURE – SMALL BORE PIPEWORK**
- A5.5.1 Small-bore pipework, for the purpose of this procedure, is an above-ground pipework system of up to and including 25 mm diameter. This will, generally, be restricted to impulse or instrumentation pipework.
- The purpose of the test is to prove strength as well as leak tightness.
- A5.5.2 Test small-bore pipework, wherever possible, in the final installed configuration, to maximise the testing of as many complete joints as possible.
- A5.5.3 Wherever practical, subject small-bore pipework to hydrostatic testing.
- A5.5.4 Where, because of application or configuration, the use of hydrostatic testing of small-bore pipework is impractical, then carry out pneumatic testing.
- A5.5.5 Place a person in full charge of all testing and to be on site during all testing operations.
- A5.5.6 Connect the pipework to be tested to the test medium using suitable control valves, relief valves and a calibrated standard test gauge, so arranged that the maximum test pressure cannot be exceeded.
- See Figure 21 and its notes for a typical procedure and test rig arrangement.
- A5.5.7 Make all pressure measurements by means of a standard test gauge (see Sub-Section 8.6).
- A5.5.8 Immediately prior to use, calibrate the standard test gauge against a dead weight tester and certify for accuracy. Retain the calibration certificate with the final test documentation.
- Make the original manufacturer's test certificate available at the time of the calibration check, in order that any pertinent information can be transferred to the calibration certificate.
- A5.5.9 Use a test medium of dry oil-free air or nitrogen.
- A5.5.10 Securely anchor all hoses using a method to reduce the risk of injury to personnel in the event of failure.
- A5.5.11 Carry out an initial proving test, using a soapy water solution at a pressure not exceeding 2 bar to check the integrity of all joints.

- A5.5.12 Following the successful completion of the proving test, increase the test pressure in stages of not more than 10% of the final test pressure to allow pressure conditions stabilise.
- A5.5.13 After reaching the final test pressure, isolate the test pipework from the pressure source and allow the pressure to stabilise.
- A5.5.14 Once the pressure has stabilised, monitor for a period of 10 minutes, during which time there should be no pressure loss.
- A5.5.15 After the 10 minute test period, gradually reduce the test pressure to the design pressure and carry out a further soap solution leak test. There should be no leakage.
- A5.5.16 Release the test pressure in a controlled manner, by the use of a suitable pressure let down valve, vented to a safe location.
- A5.5.17 If pressure loss or leakage is detected, deem the test a failure and repeat the test procedure once remedial work has been completed.
- A5.5.18 Where a partial test failure occurs, do not permit personnel to approach the test section until the pressure has been reduced to not more than 2 bar or to a safe level.
- A5.5.19 Where practical, carry out a further proving test once the pipework has been reinstalled in its final position. This may be tested with gas during initial pressurisation.
- A5.5.20 Complete a test certificate which, together with the relevant drawings and test gauge calibration certificate, comprise the permanent test record.



1. Assemble and test the high-pressure storage cylinder and regulator unit in accordance with the manufacturer's instructions.
2. Carry out a visual inspection for damage of all parts of the test rig.
3. Calibrate the test gauge (Item 7), using a dead weight test and fit the gauge to the test rig.
4. Close the shut off valve at the outlet to the test frame (Item 6a).
5. Lower the setting of the test frame relief valve (Item 4) until it is proved to be working. The setting should then be raised in small stages until the test pressure plus 10% is reached.
6. Open the shut off valve (Item 6a) at the outlet to the test frame, to pressurise the pipework system.
7. Close the shut off valve (Item 6) at the inlet to the test frame when the test pressure is reached, in order to isolate the system under test.
8. Upon completion of the test, the pressure should be relieved using the vent (Item 5).

FIGURE 21 - PNEUMATIC TESTING OF SMALL BORE PIPEWORK – TYPICAL TEST RIG ARRANGEMENT

Wall thickness: 5.54 mm			R	U
Temp range			bar	bar
°C				
0	to	1	-1.46	-1.64
1	to	2	-1.15	-1.34
2	to	3	-0.85	-1.04
3	to	4	-0.56	-0.75
4	to	5	-0.27	-0.46
5	to	6	0.02	-0.17
6	to	7	0.30	-0.11
7	to	8	0.58	0.38
8	to	9	0.86	0.66
9	to	10	1.13	0.93
10	to	11	1.39	1.19
11	to	12	1.66	1.45
12	to	13	1.92	1.71
13	to	14	2.17	1.97
14	to	15	2.43	2.22
15	to	16	2.68	2.47
16	to	17	2.93	2.71
17	to	18	3.17	2.96
18	to	19	3.41	3.20
19	to	20	3.65	3.43
20	to	21	3.89	3.67
21	to	22	4.13	3.90
22	to	23	4.36	4.14
23	to	24	4.59	4.37
24	to	25	4.83	4.60
25	to	26	5.05	4.82
26	to	27	5.28	5.05
27	to	28	5.51	5.27
28	to	29	5.74	5.50
29	to	30	5.96	5.72

TABLE 15 - TEMPERATURE/PRESSURE CORRECTIONS OD = 60.3 mm

Wall thickness: 5.49 mm		
Temp range °C	R bar	U bar
0 to 1	-1.40	-1.57
1 to 2	-1.11	-1.28
2 to 3	-0.82	-1.00
3 to 4	-0.53	-0.71
4 to 5	-0.26	-0.44
5 to 6	0.02	-0.17
6 to 7	0.29	-0.10
7 to 8	0.56	0.37
8 to 9	0.82	0.63
9 to 10	1.08	0.88
10 to 11	1.33	1.14
11 to 12	1.58	1.39
12 to 13	1.83	1.63
13 to 14	2.08	1.88
14 to 15	2.32	2.12
15 to 16	2.56	2.35
16 to 17	2.80	2.59
17 to 18	3.03	2.82
18 to 19	3.26	3.05
19 to 20	3.49	3.27
20 to 21	3.71	3.50
21 to 22	3.94	3.72
22 to 23	4.16	3.94
23 to 24	4.38	4.16
24 to 25	4.60	4.37
25 to 26	5.82	4.59
26 to 27	5.04	4.80
27 to 28	5.25	5.02
28 to 29	5.47	5.23
29 to 30	5.68	5.44

TABLE 16 - TEMPERATURE/PRESSURE CORRECTIONS OD = 88.9 mm

Temp range °C	Wall thickness					
	4.78 mm		6.01 mm		11.91 mm	
	R bar	U bar	R bar	U bar	R bar	U bar
0 to 1	-1.32	-1.48	-1.37	-1.54	-1.48	-1.66
1 to 2	-1.04	-1.21	-1.08	-1.25	-1.17	-1.35
2 to 3	-0.77	-0.94	-0.80	-0.97	-0.86	-1.05
3 to 4	-0.50	-0.67	-0.52	-0.70	-0.56	-0.76
4 to 5	-0.24	-0.41	-0.25	-0.43	-0.27	-0.46
5 to 6	0.02	-0.16	0.02	-0.16	0.02	-0.17
6 to 7	0.27	-0.10	0.28	-0.10	0.31	-0.11
7 to 8	0.52	0.34	0.54	0.36	0.59	0.39
8 to 9	0.77	0.59	0.80	0.61	0.87	0.66
9 to 10	1.01	0.83	1.05	0.86	1.14	0.94
10 to 11	1.25	1.07	1.30	1.11	1.41	1.21
11 to 12	1.49	1.30	1.55	1.35	1.68	1.47
12 to 13	1.72	1.53	1.79	1.59	1.94	1.73
13 to 14	1.95	1.76	2.03	1.83	2.20	1.99
14 to 15	2.18	1.98	2.27	2.06	2.46	2.24
15 to 16	2.40	2.20	2.50	2.30	2.71	2.50
16 to 17	2.62	2.42	2.73	2.52	2.96	2.74
17 to 18	2.84	2.64	2.96	2.75	3.21	2.99
18 to 19	3.06	2.85	3.18	2.97	3.45	3.23
19 to 20	3.27	3.06	3.41	3.19	3.70	3.48
20 to 21	3.48	3.27	3.63	3.41	3.94	3.71
21 to 22	3.69	3.48	3.85	3.63	4.18	3.95
22 to 23	3.90	3.68	4.06	3.84	4.41	4.19
23 to 24	4.11	3.89	4.28	4.05	4.65	4.42
24 to 25	4.31	4.09	4.49	4.26	4.88	4.65
25 to 26	4.51	4.29	4.70	4.47	5.12	4.88
26 to 27	4.71	4.49	4.91	4.68	5.35	5.11
27 to 28	4.91	4.68	5.12	4.89	5.58	5.34
28 to 29	5.11	4.88	5.33	5.10	5.81	5.57
29 to 30	5.31	5.08	5.54	5.30	6.04	5.80

TABLE 17 - TEMPERATURE/PRESSURE CORRECTIONS OD = 114.3 mm

Temp range °C	Wall thickness					
	5.56 mm		7.11 mm		11.91 mm	
	R bar	U bar	R bar	U bar	R bar	U bar
0 to 1	-1.26	-1.41	-1.32	-1.48	-1.42	-1.60
1 to 2	-1.00	-1.15	-1.04	-1.21	-1.12	-1.30
2 to 3	-0.74	-0.89	-0.77	-0.94	-0.83	-1.01
3 to 4	-0.48	-0.64	-0.50	-0.67	-0.54	-0.73
4 to 5	-0.23	-0.39	-0.24	-0.41	-0.26	-0.45
5 to 6	0.02	-0.15	0.02	-0.16	0.02	-0.17
6 to 7	0.26	-0.09	0.27	-0.10	0.29	-0.10
7 to 8	0.50	0.33	0.52	0.35	0.57	0.37
8 to 9	0.73	0.56	0.77	0.59	0.83	0.64
9 to 10	0.97	0.79	1.02	0.83	1.10	0.90
10 to 11	1.20	1.02	1.26	1.07	1.36	1.16
11 to 12	1.42	1.24	1.49	1.30	1.61	1.41
12 to 13	1.64	1.46	1.73	1.53	1.87	1.66
13 to 14	1.86	1.67	1.96	1.76	2.11	1.91
14 to 15	2.08	1.89	2.18	1.99	2.36	2.15
15 to 16	2.29	2.10	2.41	2.21	2.60	2.40
16 to 17	2.50	2.30	2.63	2.43	2.84	2.63
17 to 18	2.71	2.51	2.85	2.64	3.08	2.87
18 to 19	2.91	2.71	3.06	2.86	3.32	3.10
19 to 20	3.11	3.91	3.28	3.07	3.55	3.33
20 to 21	3.31	3.11	3.49	3.28	3.78	3.56
21 to 22	3.51	3.30	3.70	3.49	4.01	3.79
22 to 23	3.71	3.50	3.91	3.69	4.24	4.01
23 to 24	3.90	3.69	4.11	3.89	4.46	4.24
24 to 25	4.10	3.88	4.32	4.10	4.69	4.46
25 to 26	4.29	4.07	4.52	4.30	4.91	4.68
26 to 27	4.48	4.25	4.72	4.50	5.13	4.90
27 to 28	4.67	4.44	4.92	4.69	5.35	5.11
28 to 29	4.86	4.63	5.12	4.89	5.57	5.33
29 to 30	5.04	4.81	5.32	5.09	5.79	5.55

TABLE 18 - TEMPERATURE/PRESSURE CORRECTIONS OD = 168.3 mm

Temp range °C	Wall thickness					
	6.35 mm		8.18 mm		12.70 mm	
	R bar	U bar	R bar	U bar	R bar	U bar
0 to 1	-1.22	-1.37	-1.29	-1.45	-1.39	-1.56
1 to 2	-0.97	-1.11	-1.02	-1.18	-1.10	-1.27
2 to 3	-0.71	-0.87	-0.75	-0.92	-0.81	-0.99
3 to 4	-0.47	-0.62	-0.49	-0.66	-0.53	-0.71
4 to 5	-0.22	-0.38	-0.24	-0.40	-0.25	-0.43
5 to 6	0.02	-0.14	0.02	-0.15	0.02	-0.16
6 to 7	0.25	-0.09	0.27	-0.09	0.29	-0.10
7 to 8	0.48	0.32	0.51	0.34	0.55	0.36
8 to 9	0.71	0.54	0.75	0.58	0.81	0.62
9 to 10	0.94	0.77	0.99	0.81	1.07	0.88
10 to 11	1.16	0.98	1.23	1.04	1.32	1.13
11 to 12	1.38	1.20	1.46	1.27	1.57	1.37
12 to 13	1.59	1.41	1.69	1.50	1.82	1.62
13 to 14	1.80	1.62	1.91	1.72	2.06	1.86
14 to 15	2.01	1.83	2.13	1.94	2.30	2.10
15 to 16	2.22	2.03	2.35	2.15	2.54	2.33
16 to 17	2.42	2.23	2.57	2.37	2.77	2.56
17 to 18	2.62	2.43	2.78	2.58	3.00	2.79
18 to 19	2.82	2.62	2.99	2.79	3.23	3.02
19 to 20	3.02	2.82	3.20	2.99	3.46	3.24
20 to 21	3.21	3.01	3.41	3.19	3.68	3.46
21 to 22	3.40	3.19	3.61	3.40	3.90	3.68
22 to 23	3.59	3.38	3.81	3.60	4.12	3.90
23 to 24	3.78	3.57	4.01	3.79	4.34	4.12
24 to 25	3.97	3.75	4.21	3.99	4.56	4.33
25 to 26	4.15	3.93	4.41	4.19	4.77	4.55
26 to 27	4.33	4.11	4.61	4.38	4.99	4.76
27 to 28	4.52	4.29	4.80	4.57	5.20	4.97
28 to 29	4.70	4.47	4.99	4.76	5.41	5.18
29 to 30	4.88	4.65	5.19	4.95	5.63	5.39

TABLE 19 - TEMPERATURE/PRESSURE CORRECTIONS OD = 219.1 mm

Temp range °C	Wall thickness					
	6.35 mm		8.74 mm		12.70 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar
0 to 1	-1.15	-1.29	-1.25	-1.40	-1.34	-1.51
1 to 2	-0.91	-1.05	-0.99	-1.14	-1.06	-1.23
2 to 3	-0.67	-0.82	-0.73	-0.89	-0.78	-0.95
3 to 4	-0.44	-0.58	-0.48	-0.64	-0.51	-0.68
4 to 5	-0.21	-0.36	-0.23	-0.39	-0.24	-0.42
5 to 6	0.02	-0.14	0.02	-0.15	0.02	-0.16
6 to 7	0.24	-0.08	0.26	-0.09	0.28	-0.10
7 to 8	0.46	0.30	0.50	0.33	0.53	0.35
8 to 9	0.67	0.51	0.73	0.56	0.79	0.60
9 to 10	0.88	0.72	0.96	0.78	1.03	0.85
10 to 11	1.09	0.93	1.19	1.01	1.28	1.09
11 to 12	1.30	1.13	1.41	1.23	1.52	1.33
12 to 13	1.50	1.33	1.63	1.45	1.76	1.56
13 to 14	1.70	1.52	1.85	1.66	1.99	1.79
14 to 15	1.90	1.72	2.06	1.87	2.22	2.02
15 to 16	2.09	1.91	2.27	2.08	2.45	2.25
16 to 17	2.28	2.09	2.48	2.29	2.68	2.46
17 to 18	2.47	2.28	2.69	2.49	2.90	2.69
18 to 19	2.65	2.46	2.89	2.	3.12	2.91
19 to 20	2.84	2.64	3.09	2.89	3.34	3.13
20 to 21	3.02	2.82	3.29	3.0	3.55	3.34
21 to 22	3.20	3.00	3.49	3.28	3.77	3.55
22 to 23	3.38	3.17	3.68	3.47	3.98	3.76
23 to 24	3.55	3.35	3.87	3.66	4.19	3.97
24 to 25	3.73	3.52	4.07	3.85	4.40	4.17
25 to 26	3.90	3.69	4.26	4.04	4.60	4.38
26 to 27	4.07	3.86	4.45	4.22	4.81	4.58
27 to 28	4.24	4.02	4.63	4.41	5.02	4.78
28 to 29	4.41	4.19	4.82	4.59	5.22	4.98
29 to 30	4.58	4.36	5.01	4.77	5.42	5.18

TABLE 20 - TEMPERATURE/PRESSURE CORRECTIONS OD = 273.0 mm

Temp range °C	Wall thickness					
	6.35 mm		7.14 mm		7.92 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar
0 to 1	-1.10	-1.22	-1.14	-1.27	-1.17	-1.31
1 to 2	-0.87	-1.00	-0.90	-1.03	-0.93	-1.07
2 to 3	-0.64	-0.77	-0.66	-0.80	-0.68	-0.83
3 to 4	-0.42	-0.55	-0.43	-0.58	-0.45	-0.59
4 to 5	-0.20	-0.34	-0.21	-0.35	-0.21	-0.36
5 to 6	0.02	-0.13	0.02	-0.13	0.02	-0.14
6 to 7	0.23	-0.08	0.23	-0.08	0.24	-0.09
7 to 8	0.43	0.28	0.45	0.29	0.46	0.30
8 to 9	0.64	0.49	0.66	0.50	0.68	0.52
9 to 10	0.84	0.68	0.87	0.71	0.90	0.73
10 to 11	1.04	0.88	1.08	0.91	1.11	0.94
11 to 12	1.23	1.07	1.28	1.11	1.32	1.14
12 to 13	1.42	1.26	1.48	1.31	1.52	1.35
13 to 14	1.61	1.44	1.67	1.50	1.72	1.55
14 to 15	1.80	1.62	1.87	1.69	1.92	1.74
15 to 16	1.98	1.80	2.06	1.88	2.12	1.94
16 to 17	2.16	1.98	2.24	2.06	2.31	2.13
17 to 18	2.34	2.16	2.43	2.24	2.50	2.31
18 to 19	2.52	2.33	2.61	2.42	2.69	2.50
19 to 20	2.69	2.50	2.79	2.60	2.88	2.68
20 to 21	2.86	2.67	2.97	2.78	3.07	2.87
21 to 22	3.03	2.84	3.15	2.95	3.25	3.05
22 to 23	3.20	3.00	3.32	3.12	3.43	3.22
23 to 24	3.36	3.16	3.50	3.29	3.61	3.40
24 to 25	3.53	3.32	3.67	3.46	3.78	3.57
25 to 26	3.69	3.48	3.84	3.63	3.96	3.75
26 to 27	3.85	3.64	4.00	3.79	4.13	3.92
27 to 28	4.01	3.80	4.17	3.96	4.31	4.09
28 to 29	4.17	3.96	4.34	4.12	4.48	4.26
29 to 30	4.33	4.11	4.50	4.28	4.65	4.43

TABLE 21 - TEMPERATURE/PRESSURE CORRECTIONS OD = 323.8 mm

Wall thickness						
Temp range °C			9.52 mm		12.70 mm	
			R bar	U Bar	R bar	U bar
0	to	1	-1.23	-1.37	-1.30	-1.46
1	to	2	-0.97	-1.12	-1.03	-1.19
2	to	3	-0.72	-0.87	-0.76	-0.92
3	to	4	-0.47	-0.62	-0.50	-0.66
4	to	5	-0.22	-0.38	-0.24	-0.41
5	to	6	0.02	-0.14	0.02	-0.15
6	to	7	0.25	-0.09	0.27	-0.10
7	to	8	0.49	0.32	0.52	0.34
8	to	9	0.72	0.55	0.76	0.58
9	to	10	0.94	0.77	1.00	0.82
10	to	11	1.16	0.99	1.24	1.05
11	to	12	1.38	1.20	1.47	1.28
12	to	13	1.60	1.42	1.70	1.51
13	to	14	1.81	1.63	1.93	1.74
14	to	15	2.02	1.83	2.15	1.96
15	to	16	2.23	2.04	2.37	2.18
16	to	17	2.43	2.24	2.59	2.39
17	to	18	2.63	2.44	2.81	2.60
18	to	19	2.83	2.63	3.02	2.81
19	to	20	3.03	2.83	3.23	3.02
20	to	21	3.22	3.02	3.44	3.23
21	to	22	3.41	3.21	3.65	3.43
22	to	23	3.60	3.39	3.85	3.63
23	to	24	3.79	3.58	4.05	3.83
24	to	25	3.98	3.76	4.26	4.03
25	to	26	4.17	3.95	4.45	4.23
26	to	27	4.35	4.13	4.65	4.43
27	to	28	4.53	4.31	4.85	4.62
28	to	29	4.72	4.49	5.05	4.81
29	to	30	4.90	4.67	5.24	5.01

TABLE 21 cont'd - TEMPERATURE/PRESSURE CORRECTIONS OD = 323.8 mm

Wall thickness: 7.92 mm		
Temp range °C	R bar	U bar
0 to 1	-1.14	-1.57
1 to 2	-0.90	-1.28
2 to 3	-0.67	-1.00
3 to 4	-0.43	-0.71
4 to 5	-0.21	-0.44
5 to 6	0.02	-0.17
6 to 7	0.24	-0.10
7 to 8	0.45	0.37
8 to 9	0.66	0.63
9 to 10	0.87	0.88
10 to 11	1.08	1.14
11 to 12	1.28	1.39
12 to 13	1.48	1.63
13 to 14	1.68	1.88
14 to 15	1.87	2.12
15 to 16	2.06	2.35
16 to 17	2.25	2.59
17 to 18	2.44	2.82
18 to 19	2.62	3.05
19 to 20	2.80	3.27
20 to 21	2.98	3.50
21 to 22	3.16	3.72
22 to 23	3.33	3.94
23 to 24	3.51	4.16
24 to 25	3.68	4.37
25 to 26	3.85	4.59
26 to 27	4.02	4.80
27 to 28	4.19	5.02
28 to 29	4.25	5.23
29 to 30	4.52	5.44

TABLE 22 - TEMPERATURE/PRESSURE CORRECTIONS OD = 355.6 mm

Temp range °C	Wall thickness							
	7.92 mm		8.74 mm		10.31 mm		14.27 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar	U bar	
0 to 1	-1.10	-1.22	-1.13	-1.26	-1.18	-1.32	-1.28	-1.43
1 to 2	-0.87	-0.99	-0.89	-1.03	-0.93	-1.08	-1.01	-1.16
2 to 3	-0.64	-0.77	-0.66	-0.80	-0.69	-0.84	-0.75	-0.90
3 to 4	-0.42	-0.55	-0.43	-0.57	-0.45	-0.60	-0.49	-0.65
4 to 5	-0.20	-0.34	-0.21	-0.35	-0.22	-0.37	-0.23	-0.40
5 to 6	0.02	-0.13	0.02	-0.13	0.02	-0.14	0.02	-0.15
6 to 7	0.23	-0.08	0.23	-0.08	0.24	-0.09	0.26	-0.09
7 to 8	0.43	0.28	0.45	0.29	0.47	0.31	0.51	0.33
8 to 9	0.64	0.48	0.66	0.50	0.69	0.52	0.74	0.57
9 to 10	0.84	0.68	0.86	0.70	0.91	0.74	0.98	0.80
10 to 11	1.03	0.88	1.07	0.90	1.12	0.95	1.21	1.03
11 to 12	1.23	1.07	1.27	1.10	1.33	1.16	1.44	1.25
12 to 13	1.42	1.25	1.47	1.30	1.54	1.36	1.66	1.48
13 to 14	1.61	1.44	1.66	1.49	1.74	1.56	1.89	1.70
14 to 15	1.79	1.62	1.85	1.67	1.94	1.76	2.10	1.91
15 to 16	1.98	1.80	2.04	1.86	2.14	1.96	2.32	2.12
16 to 17	2.16	1.98	2.23	2.04	2.34	2.15	2.53	2.33
17 to 18	2.33	2.15	2.41	2.22	2.53	2.34	2.74	2.54
18 to 19	2.51	2.32	2.59	2.40	2.72	2.53	2.95	2.75
19 to 20	2.68	2.49	2.77	2.58	2.91	2.71	3.16	2.95
20 to 21	2.85	2.66	2.95	2.75	3.10	2.90	3.36	3.15
21 to 22	3.02	2.83	3.12	2.92	3.28	3.08	3.56	3.35
22 to 23	3.19	2.99	3.30	3.10	3.46	3.26	3.76	3.55
23 to 24	3.36	3.16	3.47	3.26	3.65	3.44	3.96	3.74
24 to 25	3.52	3.32	3.64	3.43	3.82	3.61	4.15	3.94
25 to 26	3.68	3.48	3.81	3.60	4.00	3.79	4.35	4.13
26 to 27	3.84	3.63	3.97	3.76	4.18	3.96	4.54	4.32
27 to 28	4.00	3.79	4.14	3.92	4.35	4.13	4.74	4.51
28 to 29	4.16	3.95	4.30	4.08	4.53	4.30	4.93	4.70
29 to 30	4.32	4.10	4.47	4.25	4.70	4.47	5.12	4.88

TABLE 23 - TEMPERATURE/PRESSURE CORRECTIONS OD = 406.4 mm

Temp range °C	Wall thickness					
	7.92 mm		9.52 mm		10.31 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar
0 to 1	-1.05	-1.17	-1.12	-1.25	-1.14	-1.28
1 to 2	-0.83	-1.96	-0.88	-1.02	-0.90	-1.04
2 to 3	-0.62	-0.74	-0.65	-0.79	-0.67	-0.81
3 to 4	-0.40	-0.53	-0.43	-0.57	-0.44	-0.58
4 to 5	-0.19	-0.33	-0.20	-0.35	-0.21	-0.35
5 to 6	0.01	-0.12	0.02	-0.13	0.02	-0.13
6 to 7	0.22	-0.08	0.23	-0.08	0.24	-0.08
7 to 8	0.42	0.27	0.44	0.29	0.45	0.30
8 to 9	0.61	0.46	0.65	0.49	0.67	0.51
9 to 10	0.80	0.65	0.86	0.70	0.88	0.71
10 to 11	0.99	0.84	1.06	0.89	1.08	0.92
11 to 12	1.18	1.02	1.26	1.09	1.29	1.12
12 to 13	1.36	1.20	1.45	1.28	1.49	1.31
13 to 14	1.54	1.38	1.64	1.47	1.68	1.51
14 to 15	1.72	1.55	1.83	1.66	1.88	1.70
15 to 16	1.90	1.73	2.02	1.84	2.07	1.89
16 to 17	2.07	1.90	2.20	2.02	2.26	2.07
17 to 18	2.24	2.06	2.39	2.20	2.45	2.26
18 to 19	2.41	2.23	2.57	2.38	2.63	2.44
19 to 20	2.57	2.39	2.74	2.55	2.81	2.62
20 to 21	2.74	2.55	2.92	2.72	2.99	2.80
21 to 22	2.90	2.71	3.09	2.89	3.17	2.97
22 to 23	3.06	2.87	3.26	3.06	3.35	3.14
23 to 24	3.22	3.02	3.43	3.23	3.52	3.31
24 to 25	3.38	3.18	3.60	3.39	3.69	3.48
25 to 26	3.53	3.33	3.77	3.56	3.86	3.65
26 to 27	3.68	3.48	3.93	3.72	4.03	3.82
27 to 28	3.84	3.63	4.10	3.88	4.20	3.98
28 to 29	3.99	3.78	4.26	4.04	4.37	4.15
29 to 30	4.14	3.93	4.42	4.20	4.54	4.31

TABLE 24 - TEMPERATURE/PRESSURE CORRECTIONS OD = 457.2 mm

Temp range °C	Wall thickness			
	11.91 mm		15.88 mm	
	R bar	U Bar	R bar	U bar
0 to 1	-1.19	-1.33	-1.27	-1.43
1 to 2	-0.94	-1.08	-1.01	-1.16
2 to 3	-0.70	-0.84	-0.74	-0.90
3 to 4	-0.45	-0.60	-0.49	-0.65
4 to 5	-0.22	-0.37	-0.23	-0.40
5 to 6	0.02	-0.14	0.02	-0.15
6 to 7	0.25	-0.09	0.26	-0.09
7 to 8	0.47	0.31	0.51	0.33
8 to 9	0.69	0.53	0.74	0.57
9 to 10	0.91	0.74	0.98	0.80
10 to 11	1.13	0.96	1.21	1.03
11 to 12	1.34	1.17	1.44	1.25
12 to 13	1.55	1.37	1.66	1.47
13 to 14	1.75	1.57	1.88	1.69
14 to 15	1.96	1.77	2.10	1.91
15 to 16	2.16	1.97	2.31	2.12
16 to 17	2.35	2.17	2.53	2.33
17 to 18	2.55	2.36	2.74	2.54
18 to 19	2.74	2.55	2.94	2.74
19 to 20	2.93	2.73	3.15	2.94
20 to 21	3.12	2.92	3.35	3.14
21 to 22	3.31	3.10	3.55	3.34
22 to 23	3.49	3.28	3.75	3.54
23 to 24	3.67	3.46	3.95	3.73
24 to 25	3.85	3.64	4.14	3.93
25 to 26	4.03	3.82	4.34	4.12
26 to 27	4.21	3.99	4.53	4.31
27 to 28	4.39	4.17	4.72	4.50
28 to 29	4.56	4.34	4.91	4.68
29 to 30	4.74	4.51	5.10	4.87

TABLE 24 cont'd - TEMPERATURE/PRESSURE CORRECTIONS OD = 457.2 mm

Wall thickness						
Temp range °C			9.52 mm		17.48 mm	
			R bar	U Bar	R bar	U bar
0	to	1	-1.08	-1.21	-1.27	-1.42
1	to	2	-0.85	-0.98	-1.00	-1.16
2	to	3	-0.63	-0.76	-0.74	-0.90
3	to	4	-0.41	-0.5	-0.48	-0.65
4	to	5	-0.20	-0.33	-0.23	-0.40
5	to	6	0.01	-0.13	0.02	-0.15
6	to	7	0.22	-0.08	0.26	-0.09
7	to	8	0.43	0.28	0.50	0.33
8	to	9	0.63	0.48	0.74	0.57
9	to	10	0.83	0.67	0.98	0.80
10	to	11	1.02	0.86	1.21	1.02
11	to	12	1.21	1.05	1.43	1.25
12	to	13	1.40	1.24	1.66	1.47
13	to	14	1.59	1.42	1.88	1.69
14	to	15	1.77	1.60	2.09	1.90
15	to	16	1.95	1.78	2.31	2.11
16	to	17	2.13	1.95	2.52	2.32
17	to	18	2.30	2.12	2.73	2.53
18	to	19	2.48	2.29	2.94	2.74
19	to	20	2.65	2.46	3.14	2.94
20	to	21	2.82	2.63	3.35	3.14
21	to	22	2.98	2.79	3.55	3.33
22	to	23	3.15	2.95	3.74	3.53
23	to	24	3.31	3.11	3.94	3.72
24	to	25	3.47	3.27	4.14	3.92
25	to	26	3.63	3.43	4.33	4.11
26	to	27	3.79	3.58	4.52	4.30
27	to	28	3.95	3.74	4.71	4.49
28	to	29	4.11	3.89	4.90	4.69
29	to	30	4.26	4.04	5.09	4.86

TABLE 25 - TEMPERATURE/PRESSURE CORRECTIONS OD = 508.0 mm

Temp range °C	Wall thickness							
	9.52 mm		11.91 mm		12.70 mm		14.27 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar	U bar	
0 to 1	-1.02	-1.13	-1.10	-1.22	-1.12	-1.25	-1.16	-1.29
1 to 2	-0.80	-0.92	-0.87	-1.00	-0.88	-1.02	-0.91	-1.05
2 to 3	-0.59	-0.71	-0.64	-0.77	-0.65	-0.79	-0.68	-0.82
3 to 4	-0.39	-0.51	-0.42	-0.55	-0.43	-0.57	-0.44	-0.59
4 to 5	-0.18	-0.31	-0.20	-0.34	-0.20	-0.35	-0.21	-0.36
5 to 6	0.01	-0.12	0.02	-0.13	0.02	-0.13	0.02	-0.14
6 to 7	0.21	-0.07	0.23	-0.08	0.23	-0.08	0.24	-0.08
7 to 8	0.40	0.26	0.43	0.28	0.44	0.29	0.46	0.30
8 to 9	0.59	0.45	0.64	0.48	0.65	0.49	0.67	0.51
9 to 10	0.77	0.63	0.84	0.68	0.86	0.70	0.89	0.72
10 to 11	0.96	0.81	1.04	0.88	1.06	0.89	1.09	0.93
11 to 12	1.14	0.98	1.23	1.07	1.26	1.09	1.30	1.13
12 to 13	1.31	1.16	1.42	1.26	1.45	1.28	1.50	1.33
13 to 14	1.49	1.33	1.61	1.44	1.64	1.47	1.70	1.53
14 to 15	1.66	1.49	1.80	1.62	1.83	1.66	1.90	1.72
15 to 16	1.83	1.66	1.98	1.80	2.02	1.84	2.09	1.91
16 to 17	1.99	1.82	2.16	1.98	2.20	2.02	2.28	2.10
17 to 18	2.16	1.98	2.34	2.15	2.39	2.20	2.47	2.28
18 to 19	2.32	2.14	2.51	2.33	2.57	2.38	2.66	2.47
19 to 20	2.48	2.30	2.69	2.50	2.74	2.55	2.84	2.65
20 to 21	2.63	2.45	2.86	2.67	2.92	2.72	3.03	3.83
21 to 22	2.79	2.60	3.03	2.83	3.09	2.89	3.21	3.00
22 to 23	2.94	2.75	3.19	3.00	3.26	3.06	3.38	3.18
23 to 24	3.09	2.90	3.36	3.16	3.43	3.23	3.56	3.35
24 to 25	3.24	3.05	3.52	3.32	3.60	3.39	3.73	3.53
25 to 26	3.39	3.20	3.69	3.48	3.77	3.56	3.91	3.70
26 to 27	3.54	3.34	3.85	3.64	3.93	3.72	4.08	3.86
27 to 28	3.69	3.48	4.01	3.79	4.10	3.88	4.25	4.03
28 to 29	3.83	3.63	4.17	3.85	4.26	4.04	4.42	4.20
29 to 30	3.98	3.77	4.32	4.11	4.42	4.20	5.59	4.36

TABLE 26 - TEMPERATURE/PRESSURE CORRECTIONS OD = 609.6 mm

Temp range °C	Wall thickness					
	15.88 mm		17.48 mm		25.40 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar
0 to 1	-1.19	-1.33	-1.22	-1.36	-1.32	-1.48
1 to 2	-0.94	-1.08	-0.96	-1.11	-1.04	-1.20
2 to 3	-0.70	-0.84	-0.71	-0.86	-0.77	-0.94
3 to 4	-0.45	-0.60	-0.47	-0.62	-0.50	-0.67
4 to 5	-0.22	-0.37	-0.22	-0.38	-0.24	-0.41
5 to 6	0.02	-0.14	0.02	-0.14	0.02	-0.16
6 to 7	0.25	-0.09	0.25	-0.09	0.27	-0.10
7 to 8	0.47	0.31	0.48	0.32	0.52	0.34
8 to 9	0.69	0.53	0.71	0.54	0.77	0.59
9 to 10	0.91	0.74	0.94	0.76	1.01	0.83
10 to 11	1.13	0.96	1.16	0.98	1.25	1.07
11 to 12	1.34	1.17	1.37	1.20	1.49	1.30
12 to 13	1.55	1.37	1.59	1.41	1.72	1.53
13 to 14	1.75	1.57	1.80	1.62	1.95	1.76
14 to 15	1.96	1.77	2.01	1.82	2.18	1.98
15 to 16	2.16	1.97	2.21	2.02	2.40	2.20
16 to 17	2.35	2.17	2.41	2.22	2.62	2.42
17 to 18	2.55	2.36	2.62	2.42	2.84	2.64
18 to 19	2.74	2.55	2.81	2.61	3.06	2.85
19 to 20	2.93	2.73	3.01	2.81	3.27	3.06
20 to 21	3.12	2.92	3.20	3.00	3.48	3.27
21 to 22	3.31	3.10	3.39	3.19	3.69	3.48
22 to 23	3.49	3.28	3.58	3.37	3.90	3.68
23 to 24	3.67	3.46	3.77	3.56	4.10	3.88
24 to 25	3.85	3.64	3.96	3.74	4.31	4.08
25 to 26	4.03	3.82	4.14	3.92	4.51	4.28
26 to 27	4.21	3.99	4.32	4.10	4.71	4.48
27 to 28	4.39	4.17	4.50	4.28	4.91	4.68
28 to 29	4.56	4.34	4.69	4.46	5.11	4.88
29 to 30	4.74	4.51	4.87	4.64	5.31	5.07

TABLE 26 cont'd - TEMPERATURE/PRESSURE CORRECTIONS OD = 609.6 mm

Temp range °C	Wall thickness							
	11.91 mm		15.88 mm		19.05 mm		22.22 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar	U bar	
0 to 1	-1.02	-1.13	-1.12	-1.25	-1.18	-1.32	-1.22	-1.37
1 to 2	-0.80	-0.92	-0.88	-1.02	-0.93	-1.07	-0.97	-1.12
2 to 3	-0.59	-0.71	-0.65	-0.79	-0.69	-0.83	-0.72	-0.87
3 to 4	-0.39	-0.51	-0.43	-0.57	-0.45	-0.60	-0.47	-0.62
4 to 5	-0.18	-0.31	-0.20	-0.35	-0.21	-0.37	-0.22	-0.38
5 to 6	0.01	-0.12	0.02	-0.13	0.02	-0.14	0.02	-0.14
6 to 7	0.21	-0.07	0.23	-0.08	0.24	-0.09	0.25	-0.09
7 to 8	0.40	0.26	0.44	0.29	0.47	0.31	0.49	0.32
8 to 9	0.59	0.45	0.65	0.49	0.69	0.52	0.71	0.54
9 to 10	0.78	0.63	0.86	0.70	0.90	0.74	0.94	0.77
10 to 11	0.96	0.81	1.06	0.89	1.12	0.95	1.16	0.99
11 to 12	1.14	0.98	1.26	1.09	1.32	1.15	1.38	1.20
12 to 13	1.31	1.16	1.45	1.28	1.53	1.36	1.59	1.41
13 to 14	1.49	1.33	1.64	1.47	1.73	1.56	1.81	1.62
14 to 15	1.66	1.50	1.83	1.66	1.94	1.75	2.02	1.83
15 to 16	1.83	1.66	2.02	1.84	2.13	1.95	2.22	2.03
16 to 17	1.99	1.82	2.20	2.02	2.33	2.14	2.43	2.23
17 to 18	2.16	1.98	2.39	2.20	2.52	2.33	2.63	2.43
18 to 19	2.32	2.14	2.57	2.38	2.71	2.52	2.82	2.63
19 to 20	2.48	2.30	2.74	2.55	2.90	2.70	3.02	2.82
20 to 21	2.63	2.45	2.92	2.72	3.08	2.88	3.22	3.01
21 to 22	2.79	2.60	3.09	2.89	3.27	3.07	3.41	3.20
22 to 23	2.94	2.75	3.26	3.06	3.45	3.24	3.60	3.39
23 to 24	3.09	2.90	3.43	3.23	3.63	3.42	3.79	3.57
24 to 25	3.25	3.05	3.60	3.39	3.81	3.60	3.97	3.76
25 to 26	3.39	3.20	3.77	3.56	3.99	3.77	4.16	3.94
26 to 27	3.54	3.34	3.93	3.72	4.16	3.94	4.34	4.12
27 to 28	3.69	3.48	4.10	3.88	4.34	4.11	4.52	4.30
28 to 29	3.83	3.63	4.26	3.04	4.51	4.29	4.71	4.48
29 to 30	3.98	3.77	4.42	4.20	4.68	4.46	4.89	4.66

TABLE 27 - TEMPERATURE/PRESSURE CORRECTIONS OD = 762.0 mm

Temp range °C		Wall thickness							
		12.70 mm		15.88 mm		19.05 mm		25.40 mm	
		R bar	U Bar	R bar	U bar	R bar	U bar	U bar	
0 to 1		-0.97	-1.08	-1.05	-1.17	-1.12	-1.25	-1.21	-1.35
1 to 2		-0.77	-0.88	-0.83	-0.96	-0.88	-1.02	-0.96	-1.10
2 to 3		-0.57	-0.68	-0.62	-0.74	-0.65	-0.79	-0.71	-0.86
3 to 4		-0.37	-0.49	-0.40	-0.53	-0.43	-0.57	-0.46	-0.61
4 to 5		-0.18	-0.30	-0.19	-0.33	-0.20	-0.35	-0.22	-0.38
5 to 6		0.01	-0.11	0.01	-0.12	0.02	-0.13	0.02	-0.14
6 to 7		0.20	-0.07	0.22	-0.08	0.23	-0.08	0.25	-0.09
7 to 8		0.38	0.25	0.42	0.27	0.44	0.29	0.48	0.31
8 to 9		0.56	0.43	0.61	0.47	0.65	0.49	0.71	0.54
9 to 10		0.74	0.60	0.81	0.65	0.86	0.70	0.93	0.76
10 to 11		0.91	0.77	1.00	0.84	1.06	0.89	1.15	0.97
11 to 12		1.09	0.94	1.18	1.02	1.26	1.09	1.36	1.19
12 to 13		1.25	1.10	1.37	1.20	1.45	1.28	1.57	1.40
13 to 14		1.42	1.27	1.55	1.38	1.64	1.47	1.78	1.60
14 to 15		1.58	1.43	1.72	1.56	1.83	1.66	1.99	1.81
15 to 16		1.74	1.58	1.90	1.73	2.02	1.84	2.19	2.01
16 to 17		1.90	1.74	2.07	1.90	2.20	2.02	2.40	2.20
17 to 18		2.06	1.89	2.24	2.07	2.39	2.20	2.59	2.40
18 to 19		2.21	2.04	2.41	2.23	2.57	2.38	2.79	2.59
19 to 20		2.36	2.29	2.58	2.39	2.74	2.55	2.98	2.78
20 to 21		2.51	2.34	2.74	2.55	2.92	2.72	3.17	2.97
21 to 22		2.66	2.48	2.90	2.71	3.09	2.89	3.36	3.16
22 to 23		2.81	2.62	3.06	2.87	3.26	3.06	3.55	3.34
23 to 24		2.95	2.76	3.22	3.03	3.43	3.23	3.74	3.53
24 to 25		3.09	2.90	3.38	3.18	3.60	3.39	3.92	3.71
25 to 26		3.23	3.04	3.53	3.33	3.77	3.56	4.10	3.89
26 to 27		3.37	3.18	3.69	3.48	3.93	3.72	4.29	4.07
27 to 28		3.51	3.31	3.84	3.63	4.10	3.88	4.47	4.24
28 to 29		3.65	3.45	3.99	3.78	4.26	4.04	4.65	4.42
29 to 30		3.98	3.58	4.14	3.93	4.42	4.20	4.82	4.59

TABLE 28 - TEMPERATURE/PRESSURE CORRECTIONS OD = 914.4 mm

Temp range °C	Wall thickness							
	14.27 mm		17.48 mm		19.05 mm		28.71 mm	
	R bar	U Bar	R bar	U bar	R bar	U bar	U Bar	
0 to 1	-0.96	-1.06	-1.03	-1.15	-1.06	-1.19	-1.20	-1.34
1 to 2	-0.76	-0.87	-0.82	-0.94	-0.84	-0.97	-0.95	-1.09
2 to 3	-0.56	-0.67	-0.60	-0.73	-0.62	-0.75	-0.70	-0.85
3 to 4	-0.36	-0.48	-0.39	-0.52	-0.41	-0.54	-0.46	-0.61
4 to 5	-0.17	-0.29	-0.19	-0.32	-0.19	-0.33	-0.22	-0.37
5 to 6	0.01	-0.11	0.01	-0.12	0.01	-0.12	0.02	-0.14
6 to 7	0.20	-0.07	0.21	-0.07	0.22	-0.08	0.25	-0.09
7 to 8	0.38	0.25	0.41	0.27	0.42	0.28	0.48	0.31
8 to 9	0.55	0.42	0.60	0.46	0.62	0.47	0.70	0.53
9 to 10	0.73	0.59	0.79	0.64	0.81	0.66	0.92	0.75
10 to 11	0.90	0.76	0.97	0.82	1.00	0.85	1.14	0.96
11 to 12	1.07	0.92	1.16	1.00	1.19	1.03	1.35	1.18
12 to 13	1.23	1.09	1.34	1.18	1.38	1.22	1.56	1.38
13 to 14	1.40	1.25	1.51	1.35	1.56	1.40	1.77	1.59
14 to 15	1.56	1.40	1.69	1.52	1.74	1.57	1.97	1.79
15 to 16	1.72	1.56	1.86	1.69	1.94	1.75	2.18	1.99
16 to 17	1.87	1.71	2.03	1.86	2.09	1.92	2.38	2.19
17 to 18	2.02	1.86	2.20	2.02	2.27	2.09	2.57	2.38
18 to 19	2.18	2.01	2.36	2.18	2.44	2.25	2.77	2.57
19 to 20	2.32	2.15	2.52	2.34	2.60	2.42	2.96	2.76
20 to 21	2.47	2.30	2.68	2.50	2.77	2.58	3.15	2.95
21 to 22	2.62	2.44	2.84	2.65	2.93	2.74	3.34	3.13
22 to 23	2.76	2.58	3.00	2.81	3.09	2.90	3.52	3.31
23 to 24	2.90	2.72	3.15	2.96	3.25	3.06	3.71	3.50
24 to 25	3.04	2.86	3.31	3.11	3.41	3.21	3.89	3.67
25 to 26	3.18	2.99	3.46	3.26	3.57	3.37	4.07	3.85
26 to 27	3.32	3.13	3.61	3.40	3.73	3.52	4.25	4.03
27 to 28	3.46	3.26	3.76	3.55	3.88	3.57	4.43	4.21
28 to 29	3.59	3.39	3.91	3.70	4.03	3.82	4.61	4.38
29 to 30	3.73	3.52	4.05	3.84	4.19	3.97	4.78	4.55

TABLE 29 - TEMPERATURE/PRESSURE CORRECTIONS OD = 1066.8 mm

Temperature range °C	Wall thickness							
	15.88 mm		17.48 mm		25.4 mm		38.1 mm	
	R bar	U bar	R bar	U bar	R bar	U bar	R bar	U bar
0 to 1	-0.97	-1.09	-1.01	-1.14	-1.14	-1.28	-1.25	-1.43
1 to 2	-0.77	-0.89	-0.80	-0.93	-0.90	-1.05	-0.99	-1.17
2 to 3	-0.57	-0.70	-0.59	-0.72	-0.66	-0.82	-0.73	-0.91
3 to 4	-0.37	-0.50	-0.38	-0.52	-0.43	-0.59	-0.48	-0.66
4 to 5	-0.18	-0.31	-0.18	-0.32	-0.21	-0.37	-0.23	-0.41
5 to 6	0.01	-0.13	0.01	-0.13	0.02	-0.15	0.02	-0.16
6 to 7	0.20	0.06	0.21	0.06	0.23	0.07	0.26	0.08
7 to 8	0.38	0.24	0.40	0.25	0.45	0.28	0.50	0.31
8 to 9	0.56	0.41	0.58	0.43	0.66	0.49	0.73	0.55
9 to 10	0.74	0.59	0.77	0.61	0.87	0.69	0.96	0.78
10 to 11	0.91	0.76	0.95	0.79	1.07	0.89	1.19	1.00
11 to 12	1.09	0.93	1.13	0.96	1.27	1.09	1.41	1.22
12 to 13	1.25	1.09	1.30	1.13	1.47	1.29	1.63	1.44
13 to 14	1.42	1.25	1.47	1.30	1.67	1.48	1.85	1.66
14 to 15	1.58	1.41	1.64	1.47	1.86	1.67	2.06	1.87
15 to 16	1.74	1.57	1.81	1.63	2.05	1.85	2.27	2.08
16 to 17	1.90	1.72	1.97	1.79	2.24	2.04	2.48	2.29
17 to 18	2.06	1.88	2.13	1.95	2.42	2.22	2.68	2.49
18 to 19	2.21	2.03	2.29	2.11	2.60	2.40	2.89	2.69
19 to 20	2.36	2.17	2.45	2.26	2.78	2.57	3.09	2.89
20 to 21	2.51	2.32	2.60	2.41	2.96	2.75	3.28	3.09
21 to 22	2.66	2.46	2.76	2.56	3.13	2.92	3.48	3.29
22 to 23	2.80	2.61	2.91	2.71	3.30	3.09	3.67	3.48
23 to 24	2.94	2.75	3.06	2.86	3.48	3.26	3.86	3.67
24 to 25	3.09	2.89	3.21	3.00	3.65	3.43	4.05	3.86
25 to 26	3.23	3.02	3.35	3.14	3.81	3.59	4.24	4.05
26 to 27	3.37	3.16	3.50	3.29	3.98	3.75	4.43	4.23
27 to 28	3.50	3.29	3.64	3.43	4.15	3.92	4.62	4.42
28 to 29	3.64	3.43	3.78	3.57	4.31	4.08	4.80	4.60
29 to 30	3.78	3.56	3.93	3.71	4.47	4.24	4.98	4.78

TABLE 30 - TEMPERATURE/PRESSURE CORRECTIONS OD = 1219.2 mm

A5.6 DERIVATION OF TABLES

For unrestrained pipework i.e. free to move:

$$dP = \frac{10(A - 3B)}{\frac{Dm}{E \cdot tn} \cdot (1 - \nu^2) + \frac{1}{C}}$$

For restrained pipework i.e. buried or anchored:

$$dP = \frac{10(A - 2B)}{\frac{Dm}{4E \cdot tn} \cdot (5 - 4\nu) + \frac{1}{C}}$$

dP = change in internal pressure of water from T°C to (T+1)°C, (bar).

A = coefficient of volumetric expansion of water at T°C.

$$\frac{-64.268 + 17.0105T - 0.20369T^2 + 0.0016048T^3}{10^6}$$

B = coefficient of expansion of linear expansion of carbon steel taken at T°C (0.000011).

Dm = pipe mean diameter (mm), i.e. in the centre of pipe wall.

tn = nominal pipe wall thickness, (mm).

E = Young's modulus N mm² (21 × 10⁴ N mm² for carbon steel).

C = bulk modulus of water N mm². This is variable in the tables with temperature between 2,184 N mm² at 0°C to 1,962 N mm² at 30°C and a constant pressure of 70 bar.

ν = Poisson's ratio taken as 0.3 for steel.

See A5.7 for typical graphical representation of the temperature/pressure relationship.

A5.7 USE OF TABLES

Example 1 – Pipelines

Assume a test section for a pipeline as follows:

Length 5000 m, outside diameter 457.20 mm, wall thickness 9.52 mm.

The whole of the test section is buried, i.e. restrained, with the exception of the test points at either end which are exposed, i.e. unrestrained. The exposed sections are 100 m and 50 m long respectively.

The pipe/water temperature for the exposed sections falls from 20°C at the start of the test period to 16°C at the end of the test.

The pipe/water temperature for the buried section remains unchanged.

$$\begin{aligned} \text{\% pipe exposed (unstrained)} &= \frac{(100 + 50)100}{5000} \\ &= 3.0\% \end{aligned}$$

From appropriate table:

°C	DECREASE IN PRESSURE (bar)
20 19	2.55
19 18	2.38
18 17	2.20
17 16	2.02

So, the total reduction in pressure for a fall from 20°C to 16°C will be the sum of the above pressures:

$$2.55 + 2.38 + 2.20 + 2.02 = 9.15 \text{ bar decrease.}$$

If the temperature had risen from 16°C to 20°C, there would be an increase in pressure of 9.15 bar.

Thence the reduction in pressure of the unrestrained test section would be 3% of 9.15 bar, i.e. 0.275 bar.

Example 2 – Installations

Assume an installation with a mix of pipe sizes as follows. The percentages shown are the percentage pipework of the total installation, by volume.

DIAMETER (mm)	WALL THICKNESS (mm)	TYPE
323.8	9.52	above ground, unrestrained 40%
219.1	8.18	above ground, unrestrained 20%
168.3	7.11	above ground, unrestrained 10%
323.8	9.52	buried, restrained 30%

Temperature measurement showed that the unrestrained above ground pipework rose in temperature from 15°C to 18°C and the restrained below ground pipework rose in temperature from 16°C to 16.5°C.

Using appropriate table, as demonstrated in Example 1:

DIAMETER (mm)	PRESSURE CHANGE (bar)	%	TYPE
323.8	9.52	40	2.688 bar
219.1	8.18	20	1.420 bar
168.3	7.11	10	0.728 bar
323.8	9.51	30	0.365 bar
Total			5.201 bar

Thus, the total pressure increase for the installation would be 5.201 bar.

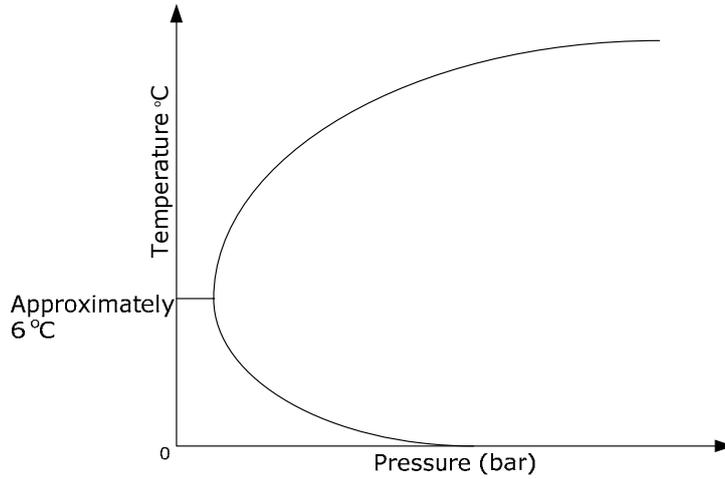


FIGURE 22 - TYPICAL TEMPERATURE/PRESSURE CORRELATION FOR PURE WATER IN STEEL PIPE

A5.8 ACCEPTANCE CRITERIA

For the temperature range of 6°C to 30°C, the pressure will rise with rise in temperature.

For the temperature range of 0°C to 6°C the opposite reaction will occur, i.e. a rise in temperature will produce a fall in pressure and vice-versa.

APPENDIX 6 : TESTING - WATER FILLING AND EMPTYING PROCEDURES

A6.1 GENERAL

Prior to the commencement of filling, check to ensure that:

- the proposed test section is free from debris or other extraneous matter. Where necessary, this may be accomplished by preparatory pigging
- adequate vent and drain points exist and steps have been taken to ensure that all pipework, including bridles and the like, can be fully vented, filled with test water and emptied on completion
- all valves are in the open position.

Note: Annuli of ball valves are capable of being pressurized where necessary, by means of temporary connections from the annulus vent to the test section pipework or by closing the valve by approximately 50%. In all cases, the manufacturers' instructions for testing need to be observed.

- all below-ground pipework has been backfilled, so far as is practical
- all below-ground connections prone to leakage such as flanged joints, drains, valve spindles and the like, have been left fully exposed for inspection during the test
- small bore pipework has been disconnected and suitable plugs or blind flanges installed, whenever it is not practical to include such pipework within the main hydrostatic test
- a good system of communication exists between the filling and venting stations to provide adequate control of filling and venting operations
- the pumping system used for filling is such as to reduce entrained air to a minimum and includes a break tank
- wherever practical, the filling point connection is connected to the lowest point in the test section
- the filling pump is capable of overcoming hydrostatic head due to changes in elevation and of maintaining a continuous and even flow of water
- due regard has been paid to freezing conditions and the need to protect vulnerable pipework.

Postpone filling and testing operations during periods when the air temperature is 2°C and falling, unless adequate precautions have been taken. Consider the use of insulation materials and antifreeze solutions.

Small-bore instrument pipework, including that monitoring the testing operations, is particularly vulnerable.

It may be necessary to empty sections deemed to be vulnerable.

- a safe, controlled means of releasing the test pressure is available, to take account of thermal expansion during the test and on completion of the test
- provision has been made for the removal of all test water on completion of testing
- where pigs are used for filling or emptying, consideration is given to the use of pig locators/tracking devices.

A6.2 FILLING

A6.2.1 Wherever practical, carry out filling of the pipeline test sections by pigging, to minimize the volume of air remaining in the test section.

- A6.2.2 Use two hi-seal pigs separated by a slug of water of adequate length to ensure entrained air behind the second pig is reduced to a minimum.
- A6.2.3 Check pig rubbers for adverse wear and change where necessary, prior to the commencement of any filling operations.
- A6.2.4 Consider the use of face-or backpressure on the lead filling pig to prevent breakaway from the line fill.
- It is recommended that this face pressure is not less than 2 bar and the pig speed is, generally, between 2 km h⁻¹.
- A6.2.5 Maintain a pig register for the purpose of logging pigs in and out of the test sections and recording their condition immediately after each use.
- A6.2.6 Where, as in installation tests, it is impractical to use pigs for filling, consider the gradient or slope of the pipework and the possible use of multiple fill points.
- A6.2.7 On completion of filling operations, allow time for the water temperature to stabilize prior to the commencement of pressurization. The time needed is dependent upon the temperature differential between the water source and ground.
- A6.2.8 Once stabilisation has occurred, determine the air content of the test section (see Sub-Sections 8.6 and Appendix 5 as appropriate), utilising a P/V plot. If the air content is found to exceed the limits set in Sub-Section 8.6, take remedial measures which may include refilling or additional venting.

A6.3 **EMPTYING**

- A6.3.1 After satisfactory completion of the hydrostatic test, reduce the test pressure to a safe level, by means of a pressure letdown valve. Consider the rate of reduction and agree in advance. Take into account the condition of the test water, the means of disposal and any potential impact on third parties.
- A6.3.2 Do not retain the full test pressure for transfer to another test section.
- A6.3.3 For associated installations, remove all water from the test section. Pay particular attention to low points, bypasses and such items as valve bodies, where siphoning or other techniques may be required to remove completely all the water.
- A6.3.4 Where pigs were used for filling, emptying may be achieved by the same means, using compressed air as a propellant.
- Under this circumstance, do not attempt to empty the test section by allowing the water to drain away under the effects of gravity alone.
- A6.3.5 Either transfer discharge water to an adjacent test section or dispose of it to an agreed location.
- A6.3.6 Transfer of water to an adjacent test sections should not be carried out using flexible hoses. Purpose built steel fabrications utilising mechanical joints must be used to reduce the risk of injury to personnel in the event of failure.

Note: Flexible hoses are more prone to whip in the event of failure, increasing the risk of serious injury.

APPENDIX 7 : IN-LINE PIGGING OPERATIONS

A7.1 SAFETY

A7.1.1 Adequate supervision, as well as clearly defined codes of practice, standards and maintenance schedules are necessary, if protection is to be afforded to all personnel, members of the public, property and plant.

A7.1.2 Install all equipment required for the operation in accordance with relevant codes of practice, corresponding to current pipeline construction standards and test before attachment.

A7.1.3 Hazardous areas

- Consider the hazardous areas designated around the pig traps and the temporary venting sites
- the requirements for the hazardous areas, during the pigging, may be different from those for normal working conditions on the site. Site any source of ignition as far away as possible and in no case less than 15 m away from any point of possible leakage of gas or flammable liquids. Consider the prevailing wind conditions
- treat temporary lighting as a source of potential ignition.

A7.1.4 Venting arrangements

- Consider the implication of venting and gas dispersion to atmosphere. Situate vents in a safe location and, on the day of the operation determine that conditions are safe for venting large quantities of gas. Additional guidance is provided in IGE/SR/23
- for temporary vent systems, the actual vent flow rate chosen depends upon a number of factors including:
 - location
 - available size for the controlled vent area
 - permissible noise levels
 - time available
 - weather conditions.
- arrange vent stacks to discharge vertically upwards with the top of any vent stack at least 3 m above the ground and any adjacent platform. Ensure the stack exit velocity is sufficient to ensure rapid gas dispersion, with due regard to environmental constraints
- for vents stacks used to vent from pressures above 15 bar, incorporate 2 vent valves. Use the downstream valve to control the vent so that, if it freezes, the upstream valve can be used to close off the vent
- considering thermal radiation, in the event of venting gases igniting, locate the vent stack in a controlled vent area, subject to operational procedures. Provide for emergency shut down by, for example, fitting remotely operable valves in series with the venting control valves.

A7.1.5 Noise abatement

A certain amount of noise is inherent in a pigging operation, particularly with the gas venting and the use of mechanical plant. Employ the best practicable means to minimize noise emission to levels acceptable to site personnel and third parties. Such means include:

- siting and screening of plant
- use of acoustically-attenuated power tools, compressors and generators

- avoidance of operations outside normal working hours.

A7.1.6 **Electrical equipment**

Install suitable explosion-protected electrical apparatus used on site where gas may be present.

Note: The requirements for the hazardous areas during pigging may be different from those for normal working conditions on site.

A7.2 **PLANNING AND PRELIMINARY WORKS**

A7.2.1 Prepare a detailed programme of operations and agree it with all affected parties. Define individual and functional responsibilities as well as safety procedures.

A7.2.2 In the preparation of the programme, consider the following:

- the mechanism to be used to control the pig speed
- the mechanism to be used to track the pig and measure the speed
- the need to isolate offtakes and/or branches along the length of the pipeline
- consultation with the appropriate gas control organizations
- the pigging sequence needed to complete the on-line inspection
- any special requirements of any of the pigs for example speed range
- the need to specify the valve operating sequence. Prepare a suitable procedure
- the need to establish emergency, safety and operational procedures, to be followed in the event of the failure, sticking or stalling of the pig, a pipeline failure or a gas supply failure
- the impact of the pigging operation on other site work and activities
- the establishment of good communication links
- the need to check the condition of pig trap seals and replace if necessary
- the availability of supplies of nitrogen, to purge the pig traps before the insertion and removal of the pigs
- the implications of venting gas to atmosphere and the need to give notice to the Police, Fire and aviation authorities, nearby inhabitants and other interested parties
- the likely weather conditions and the proximity of any sources of ignition and hazardous areas
- the possibility of liquid being present and the requirement to install tankage, drip trays and pipework at the reception site
- the regulations applying to the safe handling, storage and disposal of flammable liquids
- the methods to be used and the requirements for the disposal of any deposits or liquids recovered, including safe removal of the tankage. Take account of the possibility of extracting pyrophoric material
- the need to brief all staff on their involvement immediately prior to the commencement of the operation and to undertake a final check of all equipment and the position of all valves
- the need for welfare facilities on site for the duration of the pigging operation.

Do not consider the above list to be exhaustive. They can be adapted to prevailing circumstances. Some of the items are covered in greater detail in the rest of this Appendix.

A7.2.3 **Pigging procedure**

Treat all pigging operations as non-routine operations. Prepare a detailed written procedure detailing the valve operating sequence and all the steps required to complete the pigging operation and having regard to and indicating clearly, preparations and actions necessary to ensure:

- that the line is free of any liquid or, if liquid is thought to be present, it should include items for the collection and disposal of any liquid
- that gas flow will be maintained throughout the operation
- that it is understood what actions are to be taken in the event of an unscheduled circumstance, such as the pig sticking.

A7.2.4 **Speed control**

Make arrangements for controlling the speed of the pig. This can be achieved by:

- controlling the gas flow in the pipeline network
- throttling the gas flow at the launch or receive site via a plug valve that can easily be replaced if damaged. Do not use a ball valve for throttling
- using a pig with an on board speed control mechanism.

A7.2.5 **Offtakes**

A7.2.5.1 Wherever possible, isolate offtakes which have a diameter greater than 50% of the mainline diameter and which do not or may not, have guide bars fitted to the offtake tee, during the pig's passage to prevent the pig jamming in the throat of the tee.

A7.2.5.2 For offtakes with more than one inlet connection on the piggable pipeline close all but one inlet to avoid a duplicate gas path that would cause the pig to stop.

A7.2.5.3 Monitor offtake filters during the pigging operation in case they are blocked by debris disturbed by the pig.

A7.2.6 **Pig tracking**

Use specialist pig tracking instrumentation to record and monitor the pig's progress. If this is not possible, establish listening posts along the length of the pipeline, to provide information on the pig's progress. It may be necessary to excavate to expose the pipeline at some locations to provide an adequate coverage of listening posts.

A7.2.7 **Pig characteristics**

A7.2.7.1 Consider additional factors relating to the pig performance, for example acceptable velocity, range and differential pressures, during the pigging operation.

A7.2.7.2 Determine the limits which can be tolerated in the event of an unscheduled occurrence, such as a pig sticking.

A7.2.8 **Non pigging site activities**

A7.2.8.1 Fence the site to prevent unauthorised access and to give protection from other activities taking place in the vicinity. Where necessary, suspend these activities during critical periods of the pigging operation.

- A7.2.8.2 When tanks to receive liquid are to be installed ensure they are:
- of a standard suitable for the storage of a volatile liquid
 - tested hydrostatically to 0.7 bar after fabrication and revalidated annually
 - a sufficient capacity to contain all the liquid which may be present in the pipeline
 - provided with facilities for sealing the tanks, with provision left for breathing to atmosphere through a flame trap, which is to be open during the pigging operation
 - fitted with large diameter vents, without flame traps and of suitable height to be used during the operation, to prevent build up of pressure in the tank. Do not fit valves to these large diameter vents
 - constructed and supported such that interconnecting pipework will withstand full pipeline pressure and be complete with a liquid flow control valve and a form of slam-shut device to prevent the tank being over-pressurised
 - fitted with a suitable pressure gauge
 - installed in a safe place, at least 15 m from the pig receive trap and any source of ignition and be on good hard standing, accessible to road transport. The provision of bunds may be necessary if the tanks are not fitted with integral bunds
 - arranged such that all flanged joints are electrically bonded and the pipework connected to earth with a resistance not exceeding 20 ohms.

A typical pipework layout incorporating appropriate safety devices is shown in Figure 23.

A7.3 **PIGGING SEQUENCE**

Before an on-line inspection tool can be used, prove that its passage will not be impeded in any way. A typical sequence of operations for proving the pipeline requires steps 1 to 5 as detailed below, although there may be variations in the detail in particular circumstances.

For repeat inspections, discretion may be used to modify or omit some of these steps. In exceptional circumstances, where large accumulations of debris are suspected, specialist advice will be needed concerning preferred cleaning procedures, before any pigs are passed through the pipeline.

A7.3.1 **Pigging sequence : Step 1 : Check for severe bore reductions**

A7.3.1.1 The first pig which is passed through the pipeline needs to be capable of passing severe bore reductions, of typically 25%. The pig is used to prove that the gauging or geometry pig will pass through the pipeline.

A7.3.1.2 Pigs need to have a small diameter body fitted with conical cups, having "blow over" characteristics appropriate to flow demands at the time of pigging, or be equipped with a bypass arrangement which will come into effect if the pig becomes stuck. The pigs need to be constructed of such materials and be to a design that does not result in damage during the passage through the pipeline.

A7.3.2 **Pigging sequence : Step 2 : Record changes in pipeline cross section (detect dents)**

Pass a pig which can measure and/or record the location of gross changes in the cross-sectional dimensions of the pipeline from the launcher to the receiver. This is to prove that the pipeline bore will accommodate the pigs intended to be passed through the pipeline. Use the interpretation of this record to help determine whether to proceed with the sequence or to stop and investigate

anomalies. The record may also be used to assess the degree of cleaning required.

A7.3.3 **Pigging sequence : Step 3 : Check for bends less than 3D**

Subject to the bend-passing ability of the inspection pig and/or cleaning pigs to be used, it may be necessary to use a suitable gauge pig, to confirm the absence of bends of equivalent radius of less than 3 times the diameter of the pipe.

A7.3.4 **Pigging sequence : Step : Clean the pipeline (this may involve several pig runs)**

Remove pipeline debris from the pipeline using a "cleaning pig". Magnets may be fitted to the cleaning pig in order to remove ferrous material. Repeat the operation until the pipeline is judged to be clean.

A7.3.5 **Pigging sequence : Step 5 : Profile the pipeline to ensure the inspection pig can pass through**

Pass a "profile pig", which has been designed to check that the configuration of the pipeline is compatible with the inspection pig, through the pipeline. Depending on the type of cleaning pig, it may be necessary to pass the profile pig through the pipeline prior to the use of the cleaning pig.

A7.3.6 **Pigging sequence : Step 6 : The on-line inspection**

Do not allow the time interval between the completion of the pigging operations steps 1 to 5 and the on-line inspection pigging operation to be excessive. Ensure it is appropriate to local circumstances and as short as possible, to reduce the possibility of changes occurring as a result of ground movement or interference.

A7.4 **RUNNING THE PIG**

A7.4.1 Prior to commencing a pig run, confirm that:

- all preparatory work has been completed at all sites
- all valves are in the correct open or closed positions
- tankage, if installed, has been purged with nitrogen. In the event of delay between purging and arrival of liquids, allow the nitrogen purge to continue to prevent diffusion of atmospheric air into the tanks
- all personnel are at their appointed posts
- communications are established and secure
- notifications required by third parties have been complied with
- the effect of actual weather conditions and the proximity of any sources of ignition and hazardous areas to the operational areas have been considered
- a final consent is obtained to proceed from the gas control centre.

A7.4.2 **Launch**

A7.4.2.1 Carry out a final check as to size and serviceability of the pig, prior to loading into the pig trap.

A7.4.2.2 Connect electrically the launching equipment and pig to the pig trap before opening the pig trap door to dissipate any build up of static charge.

A7.4.2.3 During pressurization of the pig trap, take care to equalize pressure across the pig and the downstream pig trap isolation valve, to avoid damage to the pig trap valve in the event of the pig moving forward and to prevent the pig moving backwards into the pig trap oversize when the pig trap valve is opened.

A7.4.3 **Pig running**

Monitor the progress of the pig using the tracking equipment or by reports from the listening posts. Control the pressures upstream and downstream, to achieve a consistent pig speed. Maintain an appropriate downstream pressure to avoid velocity excursions and to avoid sustained excessive velocities.

A7.4.4 **Reception**

A7.4.4.1 Connect electrically the receiving equipment to the pig trap before opening the pig trap door to dissipate any build up of static charge.

A7.4.4.2 As the pig approaches the receive trap, carefully monitor its progress.

A7.4.4.3 If the receive tee has guide bars, stop the pig at the tee and then receive it in a controlled and safe manner.

A7.4.4.4 If the receive tee does not have guide bars, control the pig velocity to ensure that the pig can be received in a safe manner.

A7.4.4.5 Where liquid is present or suspected, route the venting gas to the reception tanks at a stage early enough to ensure that liquid is not carried forward into the offtake or next section of the pipeline or discharged to atmosphere. A suitably positioned listening post can be used to indicate the pig approach.

A7.4.4.6 Fill reception tanks successively, leaving sufficient ullage in each tank to ensure no overflow, for example 90% full. Vent the pig trap, ensuring that no pressure is trapped between the pig and the pig trap isolation valve, purged to nitrogen and remove the pig. Where liquid is present, take care to avoid spillage.

A7.4.5 **Completion**

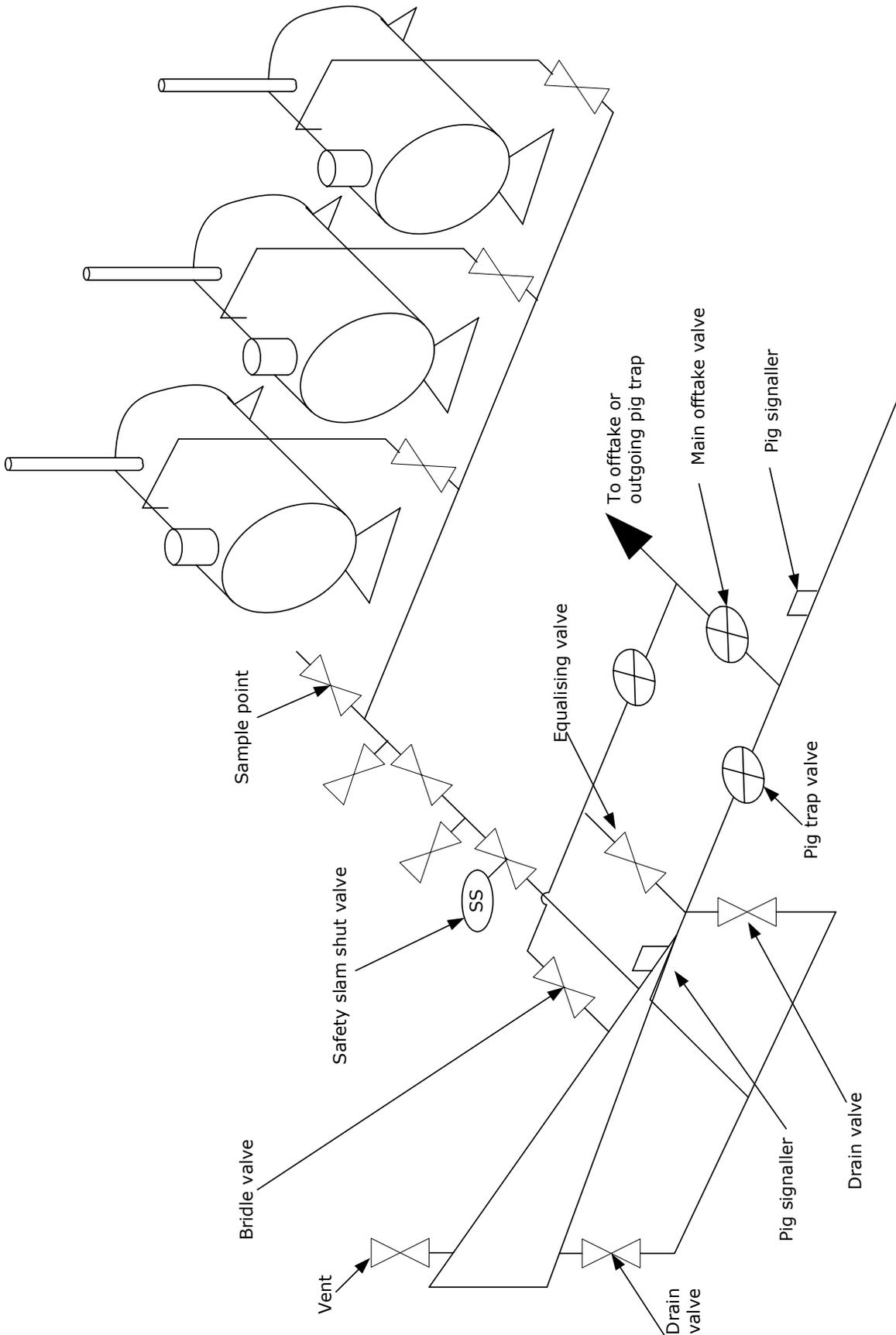
Immediately on completion, take the following actions in accordance with the written procedure:

- notify the gas control centre
- readjust the system pressures and restore valves to the required operational position
- if liquid has been present, regrease all valves
- if offtakes exist on the system, check all filers
- maintain the pig trap doors, for example clean sealing faces and regrease and replace seals as necessary
- purge all temporary connections to nitrogen before removing and blanking off
- blank off all tank vents except one, which is fitted with a flame trap. Do not fit a valve with the flame trap
- determine the mass of deposits and/or liquids and take samples for analysis
- remove the deposits and/or liquids from the site as soon as possible and dispose of in accordance with appropriate regulations.

A7.5

RECORDS

Prepare a report of the inspection operation, incorporating all the results and experiences. Retain this report as part of the pipeline records.



Note 1: Some difference in layout may occur if the pig trap is not "universal" as shown.

Note 2: Two drain valves are fitted on the pig trap to cater for the possibility of one aperture being sealed off by pig cups

FIGURE 23 - TYPICAL ARRANGEMENT OF PIPEWORK AT A PIG RECEPTION

APPENDIX 8 : WATER COURSE CROSSING SURVEY TECHNIQUES

A8.1 SELECTION OF SURVEY TECHNIQUES

A8.1.1 Table 31 provides a guide to methods of inspecting water course crossings according to the water depth.

A8.1.1.1 Minor, very shallow water course crossings may be surveyed by wading. Take special care in fast flowing waterways or where water temperatures are low.

A8.1.1.2 Hydrographic surveys can provide sufficient data to quantify any change in status, for example position, exposure, burial and cathodic protection levels of the pipeline. However, they may not be able to highlight damage, unless of significant proportions. Shallow water imposes limitations on the performance of acoustic equipment and operations may be restricted at times of high water current.

A8.1.1.3 Remote operated vehicle operations vary depending on the vehicle size but, in the simplest form, can operate in similar conditions to a hydrographic survey. The larger and more complex the remote operated vehicle, the larger the required support vessel and crew. Work will be restricted by high water current, lack of visibility and by access limitations due to the support vessels draught.

The advantage of remote operated vehicle surveys is that both acoustic and visual data can be obtained, but they can take longer to complete than hydrographic surveys.

A8.1.1.4 In shallow water, diving operations, using graduated poles, is the basic method of determining the location of a pipeline. In deeper water, where the pipeline is exposed, the versatility of a diver is unequalled, because of their ability to feel and see the pipeline.

Carry out all diving operations in accordance with appropriate diving regulations. Due to the specialist nature of this type of work, obtain the advice of personnel experienced in diving before operations and undertaken.

A8.1.1.5 The monitoring of the external condition of a pipeline crossing, by internal inspection equipment, is not limited by the nature of the water course, only by the ability of the pipeline to be pigged (see clause 11.8.3). Give careful consideration to duplicate or twin crossing, where the standby line may not be piggable.

WATER DEPTH (m)	WADING	HYDROGRAPHIC	REMOTE OPERATED VEHICLE	DIVER	INTERNAL INSPECTION
< 1	Possible	Not practical	Not practical	Not practical	Applicable
1 to 5	Not applicable	Possible ¹	Not practical	Applicable	Applicable
5 to 15	Not applicable	Applicable	Possible ²	Applicable	Applicable
15 to 50	Not applicable	Applicable	Applicable	Applicable ³	Applicable
> 50	Not applicable	Applicable	Applicable	Applicable ⁴	Applicable
<p><i>Notes:</i></p> <p>1 – Resolution of records deteriorates as water depth decreases</p> <p>2 – Operations can be limited by the size of the remote operated vehicle and the draft of the support vessel</p> <p>3 – Remotely operated vehicle inspection is safer than diver inspection, especially at the greater depths (when saturation diving may be required)</p> <p>4 – Saturation diving only</p>					

TABLE 31 - UNDERWATER SURVEY METHODS**A8.2****UNDERWATER PIPELINE INSPECTION TECHNIQUES****A8.2.1**

Inspection of major water course or estuary crossings can be undertaken by one or more methods, depending on the amount of information required and the local conditions.

The following is a brief description of the options currently available.

A8.2.1.1*Hydrographic survey*

A hydrographic or acoustic survey involves the gathering of data, from the transmission and reception of acoustic signals. The survey is undertaken from a shallow draft vessel, suitably equipped for the operation, with position control maintained by an appropriate navigation system.

The type of survey equipment used can be categorised as follows:

- (a) Echo sounder – this equipment continuously records the depth of water beneath the survey vessel. The data is used to produce a plot of sea bed topography and may also indicate trenches, spoil heaps or areas of pipeline exposure. By comparing with previous survey data, major changes in sea bed material can be monitored.
- (b) Sub-bottom profiler – this system operates in a similar manner to an echo sounder, but at lower frequencies. At these lower frequencies, the beam penetrates the sea bed and some energy is reflected at density change interfaces. Concrete coated pipelines are excellent reflectors and produce a characteristic pattern on the records, which enables the depth of burial to be determined.
- (c) Side scan sonar – this equipment emits a pulse of acoustic energy across the sea bed the reflected signals being recorded. The strength of the reflected signal is a characteristic of the sea bed material and topography and is used to produce a representational high-resolution plot from which the position and lengths of exposed pipeline can be ascertained. In addition, should the pipeline be suspended above the sea bed, then the height of free span can be calculated from the records.
- (d) Trailing wire cathodic protection system – although not an acoustic device, this system is usually operated in conjunction with the above. Depending on the length of crossing, the amount of shipping and the

water current, an insulated wire, connected to the pipeline ashore can be trailed over the crossing. By reference to a half cell suspended from the vessel, gross deficiencies in the cathodic protection levels can be highlighted.

A8.2.1.2 *Remote operated vehicle survey*

Where there is sufficient water depth and suitable environmental conditions, a remote operated vehicle can be used to visually and acoustically inspect the pipeline and the adjacent ground. A remote operated vehicle is a tethered submersible which is operated from a surface vessel and varies in size according to its required tasks.

A remote operated vehicle equipped only with a video camera can be used, but, for detailed inspection, it would carry a suite of cameras, together with pipe tracking sensors described in A8.2.1.1 can also be carried, using the remote operated vehicle as a stable work platform.

A8.2.1.3 *Diver inspection*

Divers, using surface demand air or mixed gas saturation diving techniques, can inspect all exposed areas of a pipeline and, where necessary, depending on environmental conditions, record, on video the state of the pipeline, for further viewing. NDT inspection can also be undertaken on any damaged sections of pipeline.

If the pipeline is buried, a graduated probe magnetometer can be used to determine the approximate depth of burial or to confirm that the pipeline is at least buried to the minimum depth required. CP levels can be obtained using a half cell and meter or, for bare steel, bathycorrometer.

A8.2.1.4 *Internal inspection*

Refer to clause 11.6.3.5 for details of the application of internal inspection equipment and for external condition monitoring of water course crossings. Inspection vehicles are available for the detection of metal loss, loss of weight coating and sizing free spans.

A8.3 **SURVEY PROCEDURES**

A8.3.1 Prepare a detailed programme of operations and agree it with affected parties. Define individual and functional responsibilities as well as safety procedures.

A8.3.2 Prior to commencing any operations, confirm that:

- equipment is fit for purpose and that all calibration and/or test certificates are current
- the survey works are covered by a permit to work system
- all necessary licenses and approvals from any interested parties/authorities have been obtained. In particular, ensure all agreements with affected landowners are available.

A8.3.3 In order that survey data can be prepared, use a standard reference datum.

Note: The most common reference datums in the UK are OSGB (1936). Datum for the horizontal plane and Ordnance Datum (Newlyn) for the vertical plane.

A8.3.4 During the site works, prepare a report detailing the work carried out during the previous 23 hours, including any significant findings, rate of progress and proposed work for the next period.

SURVEY REPORTS

Include in the survey report:

- Background
 - the title of the owner and controlling authority
 - frequency and extent of dredging operations
 - tidal effects
 - extracts from hydrographic survey data
 - location of sand and mud banks, including details of drift
 - anchoring of navigational aids and vessel anchoring points
 - bank erosion
 - harbour and civil works.
- Details and results of the survey
 - workscope
 - methodology and practices used
 - details of equipment and personnel
 - survey results
 - charts and drawings
 - conclusions.

Communication

Price Code:

ISBN 0-7177

ISSN

This copyright publication forms part of a series of Standards published by the Institution of Gas Engineers and Managers, Charnwood Wing, Ashby Road, Loughborough, Leicestershire, LE11 3GH.

The latest titles that are currently available in this series are the following:

<i>Item No.</i>	<i>Title</i>	<i>Date of Current Edition</i>	<i>Comm No</i>
IGEM/TD/1 Edition 5	Steel pipelines for high pressure gas transmission		
IGE/TD/1 Edition 4 Supplement 1	Handling, transport and storage of steel pipe, bends and fittings	2001	1671
IGE/TD/3 Edition 4	Steel and PE pipelines for gas distribution	2003	1677
IGE/TD/3 Edition 4 Supplement 1	Handling, transport and storage of PE pipes and fittings	2003	1682
IGE/TD/4 Edition 4	PE and steel gas services and service pipework	2007	1725
IGE/TD/12 Edition 2	Pipework stress analysis for gas industry plant	2003	1681
IGE/TD/13	Pressure regulating installations For transmission and distribution	2001	1672
IGE/TD/101	Adoption of pipe systems by a GT – Management of UIP activities	2002	1674