



## PD 8010 - Part 4: *Risk-Based Integrity management for steel pipelines on land and subsea pipelines* – DPC Overview

UKOPA/12/0016

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# Contents

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## Annexes:-

- Typical policy requirements
- The chemical injection system (CIS)
- Risk analysis
- Inspection, monitoring and maintenance plans
- In-service inspection
- Information management

# Key Principles of Integrity Management

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- Policy & authorisation
- Organization & resources,
- Roles & responsibilities
- Process and performance indicators
- Review, audit, update
- Reporting (to senior management, regulator)
- Management of interfaces (technical groups, project/operations, 3<sup>rd</sup> parties)
- Clear definition of failure
- Incident investigations (& learning)
- Life cycle management

# Management Process

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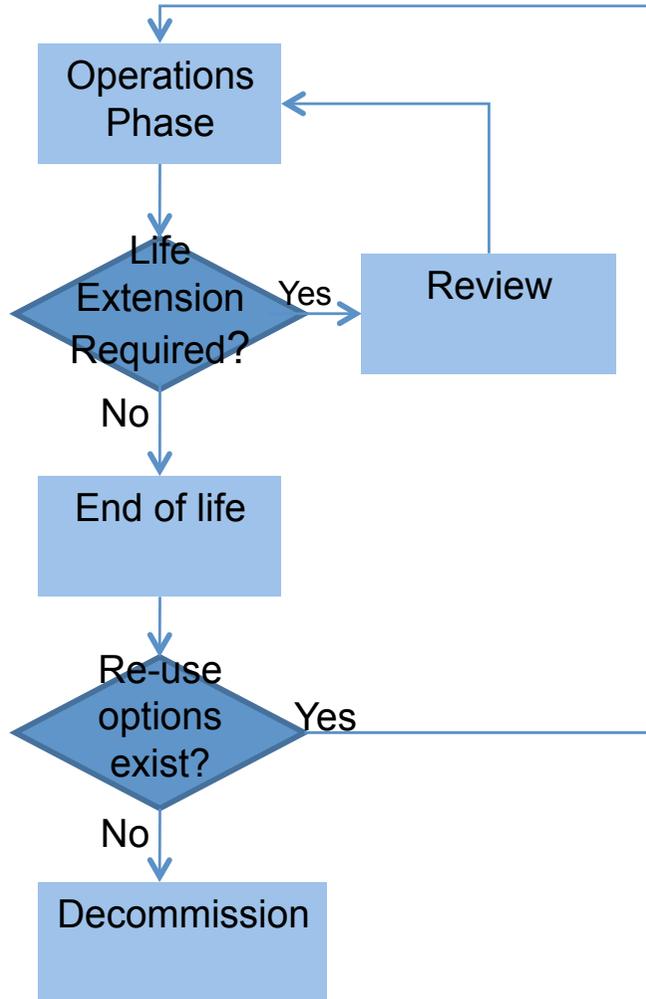
- Operational procedures
- Spares philosophy
- Preparedness
- Review and audit
- Management of change
- Emergency response
- Incident investigation and learning
- Competence Assurance

# Outline of the Integrity Management Process

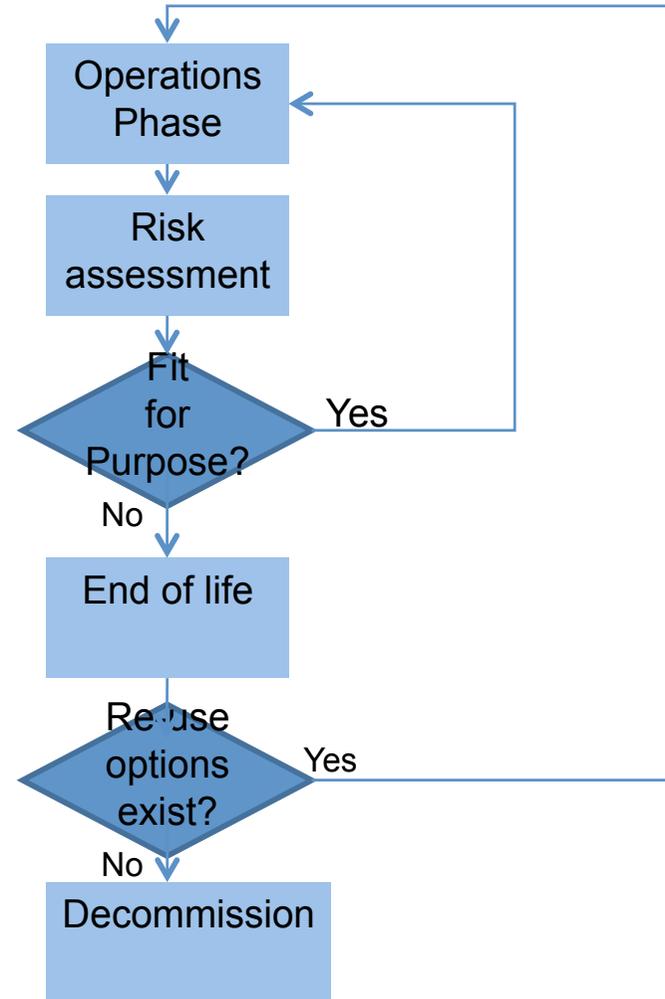
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- Contribute to the design of the pipeline system
- Define the pipeline system
- Subdivide the pipeline system into segments
- Define the threats to the pipeline system
- Gather likelihood data
- Carry out a risk assessment
- Plan for mitigation
- Carry out process and condition monitoring
- Carry out inspection
- Manage information

# End of Operating Life



Traditional design life extension



Risk based design life extension

# Check List Example – Incident Investigation

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- *facilities – not inspected according to current plan;*
- *facilities – not addressed, or incorrectly addressed, in risk assessment;*
- *equipment, materials, tools – defective, inadequate or wrong type for function or task;*
- *facilities or equipment – lack of maintenance, inspection or housekeeping;*
- *correct safety protection or equipment not provided;*
- *failure to use safety protection or equipment provided;*
- *HAZOP – not carried out, or actions not completed ahead of task;*
- *inadequate procedure;*
- *lack of training;*
- *use of unqualified or non-competent personnel;*
- *lack of suitable supervision;*
- *poor communications;*
- *poor interface management.*

# Integrity Management Activities

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- Contribute to the design of the pipeline system
- Define the pipeline system
- Subdivide the pipeline system into segments
- Define the threats to the pipeline system
- Gather likelihood data
- Carry out a risk assessment
- Plan for mitigation
- Carry out process and condition monitoring
- Carry out inspection
- Manage information

# Documentation

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- Risk mitigation document
- Design, fabrication and installation document
- Operations documents
  - Pipeline operations and control philosophy.
  - Pipeline maintenance philosophy.
  - Pipeline integrity management systems.
- Integrity management manuals.
- Operations procedures.

# Roles & Responsibilities

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- asset owner;
- responsible person;
- technical authorities;
- operator.

# Performance Indicators

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A system should be put in place ... including leading and lagging indicators:-

- Leading indicators are used to confirm that integrity tasks are undertaken - to show that the mitigations in place are active.
- Lagging indicators measure the degree to which the system has not worked as intended - identifying failures

The indicators should be selected by those involved in the process (i.e. not externally imposed), and should be SMART

**Specific, Measurable, Achievable, Reliable, Time-based**

## Example – leading indicators

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- percentage of aerial surveys achieved against the annual plan;
- percentage of intelligent pig runs achieved against the annual plan;
- chemical injection system availability against design requirement;
- percentage of anomalies not closed out by the due date.

## Example – lagging indicators

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- number of third party infringements;
- number of intelligent pig runs that reveal corrosion rates in excess of the design assumption (or that rate modified in the light of subsequent trending);
- number of valves failing to meet performance standard;
- number of leaks of hydrocarbons to the environment from the pipeline system.

# Design for Integrity

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- Procurement quality assurance
- Installation, testing and commissioning
- Piggable systems
- Reliability, maintainability and data accessibility

# Risk Management

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## Risk Assessment:-

- Segmentation
- Identification of threats
- Estimation of likelihood
- Identification of failure mode
- Estimation of failure impact
- Evaluation of risk

# Example Risk Matrix

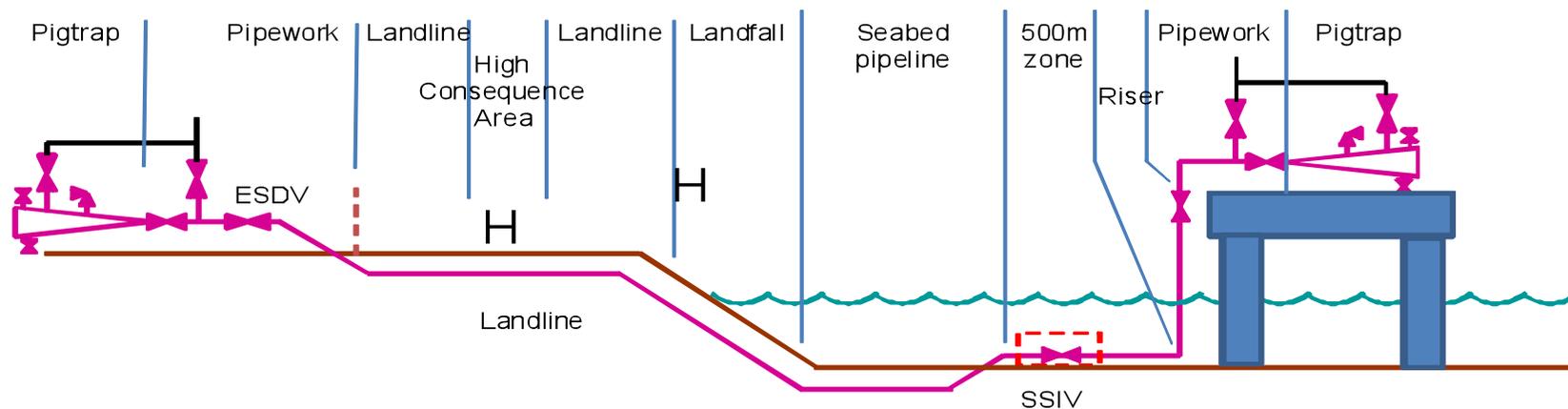
			Risk				
Probability	<b>E</b>	Almost certain	<b>M</b>	<b>H</b>	<b>H</b>	<b>X</b>	<b>X</b>
	<b>H</b>	Likely	<b>L</b>	<b>M</b>	<b>H</b>	<b>H</b>	<b>X</b>
	<b>M</b>	Possible	<b>L</b>	<b>M</b>	<b>M</b>	<b>H</b>	<b>H</b>
	<b>L</b>	Unlikely	<b>N</b>	<b>L</b>	<b>M</b>	<b>M</b>	<b>H</b>
	<b>N</b>	Improbable	<b>N</b>	<b>N</b>	<b>L</b>	<b>L</b>	<b>M</b>
Consequence category	Safety	First aid	Lost time injuries	Few major injuries	Few fatalities	Many fatalities	
	Environment	Low-level	Moderate	Large	Major	Disaster	
	Cost (millions)	<0.01	0.01 – 0.25	0.25 - 1	1 - 10	>10	
<b>Consequence</b>			<b>N</b>	<b>L</b>	<b>M</b>	<b>H</b>	<b>E</b>

# Risk Level vs Inspection Interval

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Risk Level	Inspection Interval
X	(unacceptable level of risk)
H	1 year (i.e. annual)
M	2 years (i.e. biennial)
L	5 years
N	10 years

# Segmentation of Pipeline System



## Plus

- o CP Systems including anodes, transformer rectifiers, ground beds
- o Corrosion and hydrate inhibitions systems
- o SCADA system including sensors, telemetry, processors, displays
- o Control systems including buttons, telemetry, cables, actuators
- o Over-pressure protection systems
- o Leak detection systems including inputs, processors and outputs
- o ESD system including inputs, processors, outputs

# Threats & Mitigations

Category	Threat	Mitigation – design	Mitigation - Operation
Internal Corrosion	CO <sub>2</sub> corrosion O <sub>2</sub> corrosion H <sub>2</sub> S corrosion MIC Erosion	Material selection e.g. CRA Corrosion allowance	Corrosion inhibition Inlet spec. control
External Corrosion	Galvanic corrosion Crevice corrosion Soil corrosion AC corrosion DC stray current corrosion Atmospheric corrosion CUI MIC	Coating CP	

# Threats & Mitigations

Category	Threat	Mitigation – design	Mitigation - Operation
Environmentally Assisted Cracking	HIC SCC etc.	Material selection	
Mechanical Damage	Third party impact e.g. excavator, trawl gear, anchor, vehicle impact Dropped objects Sabotage Illegal hot taps	Burial	Surveillance ROW marking Public awareness e.g. one-call Impact protection e.g. concrete coating/ rockdump/concrete slabs
Natural Hazards	Earthquake Landslide River crossing scour	Routing Backfill selection	River bank civil works
Operational Issues	Blockage/freezing Incorrect operation		Operator competence assessment/training

# Threats & Mitigations

Category	Threat	Mitigation – design	Mitigation - Operation
Operational Issues	Blockage/freezing Incorrect operation		Operator competence assessment/training
Design & Materials	Pipe body defects Seam weld defects	Mill QA/QC	Pre-commissioning hydrotest
Construction	Girth weld defects	Construction QA/QC	Pre-commissioning hydrotest
Equipment Failure	Valve Flange Pig launcher/receiver		
Fatigue	Pressure cycling Thermal cycling		

# Final Sections

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- Process & Condition Monitoring
- In Service Inspection
  - Pipeline Surveillance
  - Interpretation of Results
- Information Management
- Maintainability, spares & preparedness
  - Maintainability
  - Spares philosophy
  - Preparedness
- Audit & Review

# Features and Assessment Methodologies

Feature	Applicable code or guideline
Anode loss or depletion	DNV-RP-F103 ISO 15589-1 &2 Norsok standard M-503
Coating damage/loss	DNV-RP-F102
Corrosion/metal loss	API 579-1/ASME FFS-1 ASME B31G DNV-RP-F101 PDAM
Crack	API 579-1/ASME FFS-1 BS 7910 DNV-OS-F101 & RP-F113 PDAM
Dent	API 579-1/ASME FFS-1 BS 7608 DNV-OS-F101, RP-C203, F111, F113 PDAM

# Features and Assessment Methodologies

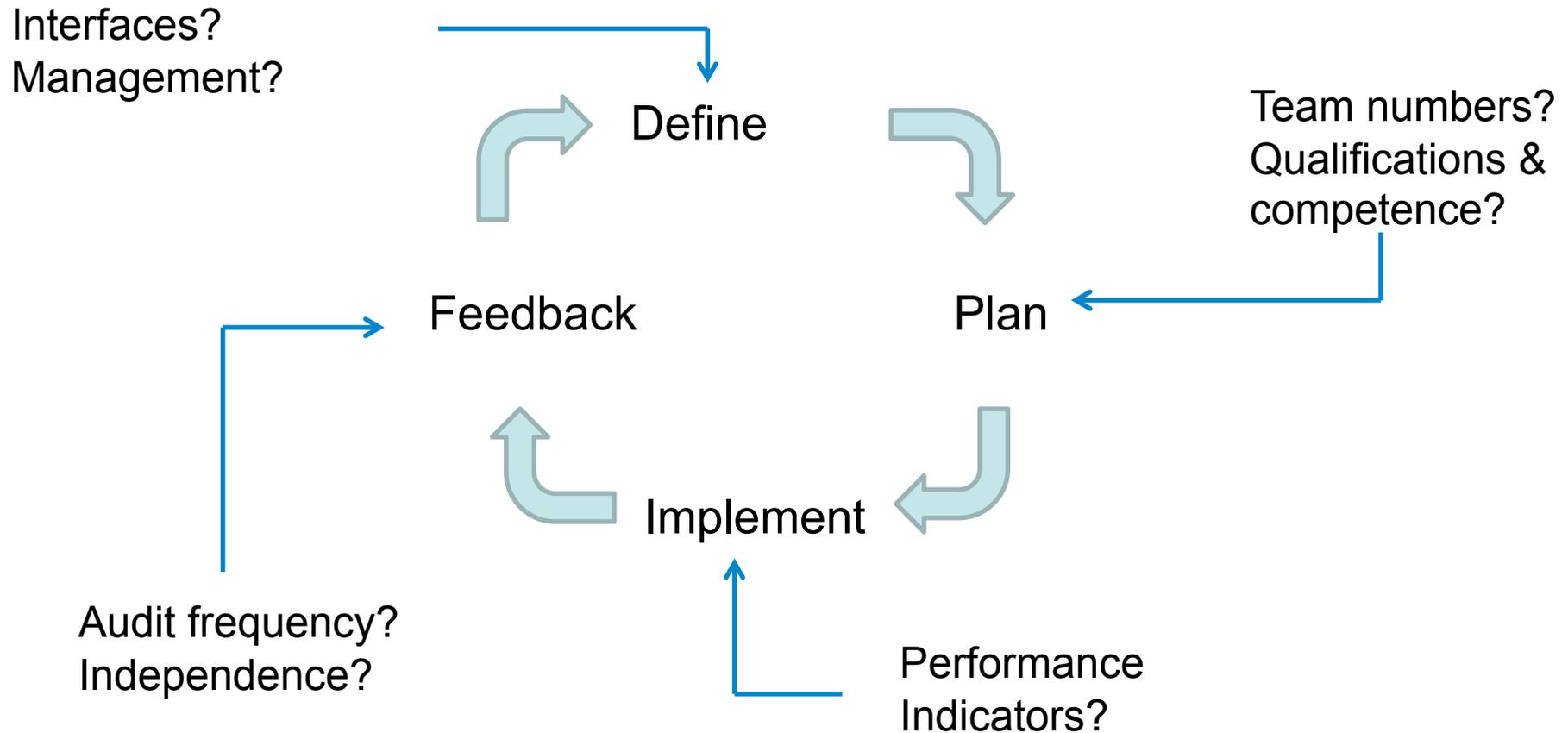


Feature	Applicable code or guideline
Exposure	DNV-RP-F107, F109, F110
Free span	DNV-RP-F105
Global buckle	DNV-RP-F110 Germanischer Lloyd Rules for Classification and Construction – III Offshore Technology – Part 4 – Subsea Pipelines and Risers
Gouge	API 579-1/ASME FFS-1 PDAM
Local buckle	DNV-OS-F101 PD 8010-2

# Example – Data Stream Allocation

<b>Data Type</b>	<b>Operators</b>	<b>Integrity Engineers</b>	<b>Reliability Engineers</b>	<b>Subsea Engineers</b>
Temp, Pressure, Flow rate, etc	Assessment of well performance Confirm safe to continue operating	Input to calculations of corrosivity and chemical injection rate Confirm operation within SOL	Sensor performance data (MTBF, etc)	Sensors OK <i>/or/</i> maintenance task to plan
Isolation valve operated	Task complete	Requirement to calculate new corrosivity in each leg	Valve condition monitoring data (footprint)	Valve status
Dewpoint, gas sampling (CO <sub>2</sub> , H <sub>2</sub> S, etc)	Confirm safe to continue operating	Assessment of corrosivity	Sensor performance data (MTBF, etc)	–
Chemical injection performance	Requirements achieved	Achieving protection (anticipate corrosivity)	Achieving availability (system condition monitoring)	Pumps, IRCDs, umbilical cores OK <i>/or/</i> maintenance task to plan
Corrosion / erosion probe output	--	Confirm corrosion under control, or calculate remaining life	Achieving availability (system condition monitoring)	Probes OK <i>/or/</i> maintenance task to plan
Subsea Control Module performance	Confirm ability to control <i>/or/</i> shut-down required	--	SCM component performance data (MTBF, etc)	SCM OK <i>/or/</i> intervention required

# Audit & Review



# Comments & Feedback to BSI Please